

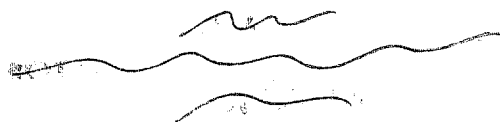


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Studies of the Turbulent Boundary Layer on a
Waisted Body of Revolution in Subsonic and
Supersonic Flow

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Studies of the Turbulent Boundary Layer on a Waisted Body of Revolution in Subsonic and Supersonic Flow

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Summary.

The object of the study was to determine the influence of Mach number, pressure gradients and stream-line convergence and divergence on the development of turbulent boundary layers. Measurements were made of pressure distribution, local skin friction and boundary-layer profiles along the body, at Mach numbers between 0.6 and 2.8 and Reynolds numbers, based on the length of the body, between 5×10^6 and 2×10^7 . The results of comparative calculations based on simultaneous integration of the momentum and kinetic energy equations are generally in fair agreement with the experiments except at the two higher Mach numbers (2.4 and 2.8). The study was a result of collaboration between the Aerodynamische Versuchsanstalt, Göttingen and the Royal Aircraft Establishment, Bedford.

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Detachable Abstract Cards

1. Introduction.

For a slender wing supersonic transport aircraft skin friction may contribute about a third of the total drag. Engines are likely to be installed on the wings and their intake design and performance will be strongly influenced by the local boundary-layer conditions on the wing surface. A detailed knowledge of the boundary-layer development over the wings is thus essential.

Following the ideas of Spence¹, methods of calculation for turbulent boundary layers at supersonic speeds on slender wings were developed by Cooke². One of the assumptions in this work was that the relationships between skin friction and Reynolds number based on local boundary-layer momentum thickness could be taken to be the same as on a flat plate, and in fact a power law was used. Calculations of this nature were found inadequate in predicting skin-friction coefficients measured on a cambered delta wing³. The inference taken from Ref. 3 was that the skin-friction law used was of a too simple form. The measurements showed that though the total skin-friction drag was fairly close to that of a flat plate, local values as low as half that on a flat plate at the same length Reynolds number were found. These low values occurred in regions where there was convergence of the flow combined with a mild adverse pressure gradient. In Ref. 3, skin friction only was measured and knowledge of the local boundary-layer profiles was clearly required to make any progress in understanding the flow. To avoid the experimental difficulties of boundary-layer exploration on the wing, which would arise from the crossflows, the present study was undertaken.

The main aim of the study was to produce an axisymmetric converging flow with an adverse pressure gradient. At the same time, it was appreciated that general information on the behaviour of turbulent boundary layers in compressible flows with pressure gradients could be of great value in developing and checking methods of calculation, which, in the present state of knowledge, must generally be based upon empirical correlations.

The study was a joint effort of the Aerodynamische Versuchsanstalt Göttingen and the Royal Aircraft Establishment Bedford. The measurements were made in the RAE 8ft × 8ft wind tunnel. A brief description of the work is contained in Ref. 4 and a more complete account in German in Ref. 5.

2. Model Design.

The obvious simple example of a supersonic flow with an adverse pressure gradient and converging streamlines is the aft end of a parabolic body of revolution. However, the convergence for a parabolic body increases as the tail is approached, and a more nearly constant value of the convergence parameters was felt to be desirable. (It was, in fact, visualised initially that a series of bodies with various values of convergence and divergence might be studied.) The starting point for the model design was thus a body approximating to a parabolic body over the forepart but with concavity introduced over the aft end. By adding a flare to the body it was hoped to obtain a diverging flow, whilst retaining for some part the adverse pressure gradient.

On the delta wing model of Ref. 3 the convergence of the external flow measured was about 0.04 radian per inch, and values of divergence up to 0.08 radian per inch were found. Since the intended model was to be of the same length (60 in.) as the delta wing and to be tested at the same conditions, it was reasonable to use the same dimensional values of convergence and divergence. This was taken to be 0.05 radian per inch, i.e.

$$\frac{1}{R} \frac{dR}{dX} = \pm 0.05 \quad (2.1)$$

when R and X the body radius and distance from the nose are measured in inches. Equation (2.1) implies an exponential variation of radius with distance but it was found that a cubic equation would give a sensibly constant value of $\frac{1}{R} \frac{dR}{dX}$ over the regions of interest.

The final shape of the model is shown in Fig. 1. Its shape is specified in five sections with continuity of ordinate, slope and curvature at the junctions of the sections except at the end of the conical part of the nose where the curvature is discontinuous. The conical nose has an included angle of 40 degrees, being the largest angle to give an attached shock wave at the lowest supersonic speed of the test ($M_\infty = 1.4$). This is followed by a shape defined by a quartic curve which joins the cubic giving approximately constant convergence. A mirror image of this cubic provides the final flare and a quartic fairing curve joins the converging and diverging regions.

The non-dimensional divergence parameter $\frac{\eta'}{\eta}$ where $\eta = \frac{R}{l}$ and the prime denotes differentiation with respect to $x = \frac{X}{l}$, is shown in Fig. 2, together with the non-dimensional longitudinal curvature. The pressure distribution is shown in Fig. 3, and by comparison with Fig. 2, it can be seen that combinations of streamline convergence or divergence, and sign of pressure gradient as in the following table are obtained.

Supersonic speeds

x	0-0.142	0.142-0.3	0.3-0.4	0.4-0.7	0.7-1.0
Streamlines	divergent	divergent	convergent	convergent	divergent
Pressure gradient	zero	favourable	favourable	adverse	slightly adverse

Subsonic speeds

x	0-0.3	0.3-0.7	0.7-1.0
Streamlines	divergent	convergent	divergent
Pressure gradient	favourable	adverse	favourable

All four possible combinations, the last only marginally, are obtained at supersonic speeds but only two at subsonic speed.

Fig. 4 compares the calculated pressure distribution at $M_\infty = 1.4$, using linear theory⁶, with the measured pressures. Despite the absence of any boundary-layer displacement correction in the calculations the comparison is good.

3. Experimental Details.

3.1. Model Construction.

The model was constructed of fiberglass skin and bulkheads assembled over a steel core, and filled with foamed resin. The skin and bulkheads were 0.25 inch thick. Pressure tubes were built into the skin and emerged at the model base. 29 tubes were provided along each of two generators 30 degrees apart ($\varphi = 0$ and $\varphi = 30^\circ$) and extra holes at 90 degree intervals were added at $X = 6, 24, 42, 59$ inches. The pressure holes were 0.03 inch diameter. The hole at $X = 9$ inches $\varphi = 0$ became blocked early in the experiment and could not be cleared.

3.2. Skin-Friction Measurement.

Skin friction was measured by the razor blade technique described in Ref. 7. The portions of razor blade (about 0.2 inch square) were mounted over the row of holes at $\varphi = 30$ degrees, and the pressure difference taken from the static pressure measured on the row of holes at $\varphi = 0$ degrees. The height of the razor blades was approximately 0.005 inch. That the presence of the razor blades did not influence the results was checked by repeating measurements with alternate blades removed. The calibration used differed from that given in Ref. 7 being based upon measurements taken during the tests of Ref. 8 in which surface shear was measured directly.

3.3. Velocity Profiles.

Boundary-layer profiles were measured using the standard tunnel flow survey equipment. This is illustrated in Figs. 5a and b. Four remotely controlled motions are available with this equipment, a primary rotation coaxial with the model support sting, a secondary rotation about a parallel offset axis at the end of the primary arm, a tertiary rotation about an axis at the end of the secondary arm and a longitudinal motion along this axis. In addition the secondary arm can be adjusted manually through ± 10 degrees about two axes to change the direction of the longitudinal motion. The movement used for profile measurements was the tertiary rotation with an arm of length 3 inches. The probe thus traversed along circular arcs but the distance used in defining the profiles was the radial distance from the body. The survey probe used had five pitot tubes of 0.0195 inch outside diameter and 0.0103 inch inside diameter spaced 0.1 inch apart. The use of multiple tubes enabled a check to be made on any interference and backlash effects by repeating readings at a given point with different tubes, and also of course diminished the time necessary for a traverse. The angular setting was measured in steps of 0.05 degree, i.e. the error was less than or equal to 0.025 degree so that the positional accuracy was 0.0013 inch. The small backlash present in the gear train would give an error in excess of this. The backlash was however largely eliminated by using the surface of the model as datum, and little change in aerodynamic load on the probes would occur during the course of a traverse. Contact was determined electrically by using silver paint on the model surface and a sensitive relay circuit.

The fore and aft travel of the probe is limited to 24 inches so that different extension pieces were required for the forward and rearward parts of the body. Because of the shape of the body it was not possible to align the probes with the local direction of a generator of the body. The misalignment generally was about 5 degrees except for traverses in the waist of the body ($x = 0.7$) when it was 11 degrees.

The pressures from the probes were measured using a strain gauge pressure transducer mounted in a pressure switch at the base of the secondary arm. The pressure switch had 24 ways with the connections arranged in four sequences of six each giving five pressures, from the five pitot tubes, plus either a calibration pressure or a zero. Velocities were evaluated from the measured pressures assuming the static pressure

to be constant across the boundary-layer thickness*. At subsonic speeds the measured pressure at the wall was used. At supersonic speeds the static pressure was determined from the Mach number evaluated from the pitot reading at the assumed edge of the boundary layer using normal shock relations. A calculated total-pressure loss through the nose shock of the body was taken into account. For the temperature distribution the parabolic formula,

$$\frac{T}{T_\delta} = 1 + r \frac{\gamma - 1}{2} M_\delta^2 \left[1 - \left(\frac{u}{u_\delta} \right)^2 \right] \quad (3.1)$$

was used, and both $r = 1$ (constant total temperature) and $r = 0.89$ were taken. For the profiles measured by Nothwang⁹ the use of equation (3.1) with $r = 0.89$ has been found to give values of momentum thickness which are too high by about 9 per cent at $M = 3$ compared with using his measured temperature distribution. Taking $r = 1$ gives momentum thickness correctly to within about 1 per cent. For the present results Tables 3a and b show a difference at $M_\infty = 2.8$ of 6 to 7 per cent for the two assumptions. Similar results are found in Ref. 8. It is interesting to note that the results of Ref. 8 show that the important parameter H_{12}^i has more nearly the correct value by taking $r = 0.89$; the error at $M = 2.8$ is about -0.3 per cent compared with -1.1 per cent for $r = 1$.

The various integral properties of the boundary layer, as defined in the list of symbols, were calculated taking into account the radius of the body. This of course is necessary in order that the quantities in the momentum integral equation do satisfy the equation. The application of the factor $1 + \frac{y}{R}$ in the integrands of quantities such as δ_1^i (see Section 5) may be questioned, since in some respects these quantities may be regarded merely as descriptive geometric parameters of the boundary-layer profiles. However, the correlation given in Ref. 8 for compressible boundary-layer profiles on the basis of similarity of 'incompressible' profiles implies some physical significance of the various δ^i . Accordingly the factor $1 + \frac{y}{R}$ in the integrals has been applied consistently throughout. In fact the influence of the factor on the shape parameters used is small.

3.4. Transition Trip.

For all experiments a transition trip was attached 1.5 inches from the nose of the body. The trip was of Ballotini of size 0.005 inch. The size proved to be inadequate at Mach numbers above 1.4. Using the criterion of Ref. 10 (established after the initial experiments) a trip of size, 0.013 inch would be required to bring transition forward to the roughness band at $M_\infty = 2.8$ and a unit Reynolds number of 1 million per foot.

3.5. Range of Measurements.

The range of nominal conditions for the experiments are given in the following tables.

Skin friction

M_∞	0.6	0.8	1.4	1.7	2.0	2.4	2.8
$10^{-6} Re_t$	10	10	5 10 20	10	5 10 17	10	5 10

*Some comment on the effect of normal pressure gradients on the measured profiles is offered in Section 7.3.

Profiles

M_∞	0.6	1.4	1.7	2.0	2.4	2.8
$10^{-6} Re_t$	10	10 20	10	10	10	10

Profiles were measured at $x = 0.4, 0.475, 0.55, 0.7, 0.833, 0.983$ except for $M_\infty = 1.7, 2.4, 2.8$ where $x = 0.475$ was omitted.

3.6. Accuracy.

For a Reynolds number of 10^7 the pressure coefficients are estimated to have an accuracy of about ± 0.005 , about half of which arises from possible systematic error and about half from random error. Assuming that the razor blade calibration used is applicable to the conditions of the experiment, the skin-friction coefficients are estimated to be accurate to within ± 0.0002 . Part of this error is due to inaccuracies in measurement and part due to incorrect fore and aft positioning of the blades with respect to the static holes. The errors will be smaller at the higher Reynolds numbers and larger at the lower Reynolds numbers.

As noted in Section 3.3 the resolution of the system for measuring probe position was about 0.0013 inch. Since the wall was used as datum the accuracy of the distance from the wall was about 0.0026 inch.

The model shape was correct to within 0.01 inch with the slope maintained within 0.001 inch/inch. The maximum eccentricity was 0.006 inch.

4. Experimental Results.

Table 1 gives details of pressure, local Mach number and skin-friction distributions along the body. The pressure coefficient is referred to free stream static pressure and kinetic pressure but the skin-friction coefficient is referred to local kinetic pressure.

Table 2 lists the Mach numbers and velocity ratios in the boundary layers against the distance from the wall, y , measured in inches, with data evaluated both for $r = 1$ and $r = 0.89$ in the parabolic temperature distribution (equation (3.1)). The assumed edge of the boundary layer is indicated but some points are given beyond the edge. These points are included because they show normal gradients exist in the flow for supersonic speeds. (Pitot pressure outside the boundary layer is, of course, constant in principle for subsonic speeds.) The points are however incorrect because of the assumption of constant static pressure. For example at $M_\infty = 2.8$ and $x = 0.7$ if the total pressure outside the boundary layer is taken as constant the Mach number rises from 2.759 to 2.812 between $y = 0.630$ and $y = 1.193$ inches instead of falling from 2.759 to 2.695 as shown in the tabulation. Integral properties of the boundary layers are listed in Table 3.

The velocity profiles are plotted in Fig. 7 and the main results are summarised in Figs. 15 to 26 where comparisons with calculations are made.

5. Boundary-Layer Properties.

The experimental results are summarised in Fig. 6 which also illustrates the basic problem that the experiment was designed to study. In the figure, the measured values of local skin-friction coefficient are plotted against Reynolds number based on momentum thickness, with both expressed in intermediate temperature form, using the expression due to Eckert¹¹, which for zero heat transfer is

$$T^* = 0.28 T_\delta + 0.72 T_w. \quad (5.1)$$

For flat plate boundary layers the effects of compressibility are taken into account to within a small

percentage by the intermediate temperature hypothesis. It will be seen that for the present model the measurements at the model base fall within ± 10 per cent of the Prandtl-Schlichting line, and for Mach numbers of 1.4, 1.7 and 2.0 the measurements at $x = 0.4$ also fall near the line. For $M_\infty = 0.6$ the value at $x = 0.4$ is low but this might be expected since at subsonic speeds the adverse pressure gradient starts at $x = 0.3$. It is however surprising that the values for $x = 0.4$ fall well below the line at $M_\infty = 2.4$ and 2.8.

The main point of interest is the low values of skin-friction coefficient at the waist of the model. For all Mach numbers tested the value is approximately half that for a flat plate, and it is this feature particularly that the experiment was designed to study.

Velocity profiles are shown in Fig. 7. The profiles for Mach numbers up to 2 are as would be anticipated from Fig. 6, in that hollow profiles are obtained where the skin friction is low. At the highest two Mach numbers, however, the profiles remain full along the whole body.

For incompressible flows the Ludwig-Tillmann¹² formula relates skin friction to the velocity profile shape by expressing local skin-friction coefficient c_f as a function of Reynolds number based on momentum thickness $\frac{u_\delta \delta_2}{\nu}$ and shape parameter $H_{12} = \frac{\delta_1}{\delta_2}$ where δ_1, δ_2 are displacement and momentum thickness. This relationship cannot be used directly for compressible flows because H_{12} is strongly dependent upon the density distribution through the boundary layer. Walz¹³ has suggested instead the use of a parameter $H_{12}^i = \delta_1^i / \delta_2^i$ where δ_1^i, δ_2^i are evaluated from the velocity profiles as though the flow were incompressible, i.e. ignoring density terms. Walz also suggested that the Reynolds number based on momentum thickness should be modified by using a value of viscosity evaluated at wall conditions. The modified form of the Ludwig-Tillmann formula is then

$$c_f = 0.246 \left(\frac{\rho_\delta u_\delta \delta_2}{\mu_w} \right)^{-0.268} 10^{-0.678 H_{12}^i} \times k \quad (5.2)$$

where Walz takes $k = \frac{\delta_2}{\delta_2^i}$.

Fig. 8a shows k determined from the measurements of Ref. 8 at Reynolds numbers of the order of 50×10^6 . At such high Reynolds numbers the Ludwig-Tillmann formula gives low values of c_f but the results are nearly parallel to a line with twice the slope of the prediction of Walz, i.e.

$$k = 2 \frac{\delta_2}{\delta_2^i} - 1. \quad (5.3)$$

(There is obviously an upper limit to the Mach number for which the formula holds, otherwise at high Mach number negative skin friction would be predicted.) Fig. 8b shows the results on the body and though there is considerable scatter the same correlation is roughly applicable. In Fig. 8b the momentum thickness values used are evaluated in accord with the expression for a body of revolution and with the temperature distribution of equation (3.1) with $r = 0.89$.

Walz¹⁴ has utilised power law profiles together with a parabolic temperature distribution to calculate relationships between various profile parameters for compressible boundary layers and has suggested approximate general formulae fitting the results of his calculations. It is of interest to see how far his correlations can be applied to the present results. The use also of results of Ref. 8 gives a useful guide to the applicability of the correlations to flat plate conditions. The assumption of power law profiles implies that

$$H_{32}^i = \frac{4 H_{12}^i}{3 H_{12}^i - 1} \quad (5.4)$$

where $H_{32}^i = \frac{\delta_3^i}{\delta_2^i}$, the ratio of kinetic energy thickness to momentum thickness for constant density.

Fig. 9a shows that the flat plate profiles of Ref. 8 (which can be collapsed very closely by a summation of a logarithmic velocity distribution plus a constant wake term) can in fact also be represented well by power laws. The exponent is between 1/7 and 1/9. For the profiles on the body (Fig. 9b) there is much greater disparity with the power law line, particularly at the two higher Mach numbers (note change of scale between Figs. 9a and 9b). At other Mach numbers the points only at both ends of the body are far from the power law line.

In order to derive the compressible shape parameter H_{32} from the 'incompressible' value H_{32}^i Walz has suggested the approximation.

$$H_{32} = H_{32}^i [1 + (2 - H_{32}^i) b] \quad (5.5)$$

where b is primarily a function of Mach number but also from calculations shows a weak dependence upon H_{32}^i . Walz suggested as an approximation that

$$b = 0.004 M_\delta + 0.0075 M_\delta^2 - 0.00018 M_\delta^4. \quad (5.6)$$

Fig. 10a shows that for flat plate profiles a better fit is obtained if the linear term is omitted, i.e.

$$b = 0.0075 M_\delta^2 - 0.00018 M_\delta^4 \quad (5.7)$$

and the results on the body Fig. 10b are in fair agreement with equation (5.7).

For the ratio of 'incompressible' momentum thickness to actual momentum thickness the suggested correlation is

$$\frac{\delta_2^i}{\delta_2} = 1 + r \frac{\gamma - 1}{2} M_\delta^2 H_{32} (2 - H_{32}^i) a \quad (5.8)$$

where r is the recovery factor and a is a function both of H_{32}^i and M_δ , but with b , is only weakly dependent upon H_{32}^i and the dependence can be ignored. Fig. 11 shows that a better fit to both flat plate data and to the results on the body is obtained with

$$a = 1 - 0.043 M_\delta \quad (5.9)$$

rather than the form suggested by Walz. An even better fit would be obtained with a formula for which a tends to about 0.97 as $M_\delta \rightarrow 0$, as also given by the calculations of Ref. 5.

6. Details of Calculations.

The calculations are based upon the simultaneous integration of the momentum and kinetic energy equations of the boundary layer. For an isentropic flow over a surface with zero heat transfer these equations may be written

$$d \frac{\delta_2/l}{dx} + \frac{\delta_2}{l} \left[\frac{H_{12} + 2}{u_\delta} \frac{du_\delta}{dx} + \frac{1}{\rho_\delta} \frac{d\rho_\delta}{dx} + \frac{1}{\eta} \frac{d\eta}{dx} \right] = \frac{c_f}{2} \quad (6.1)$$

$$d \frac{\delta_3/l}{dx} + \frac{\delta_3}{l} \left[\frac{3}{u_\delta} \frac{du_\delta}{dx} + (2 - \gamma) \frac{1}{\rho_\delta} \frac{d\rho_\delta}{dx} + \frac{1}{\eta} \frac{d\eta}{dx} \right] = c_D \quad (6.2)$$

where lengths have been non-dimensionalised by dividing by the body length l . Strictly the streamwise distance should be measured along the body surface. The error involved in using the axial distance has been accepted. Providing the shape factor H_{12} , skin-friction coefficient c_f and dissipation coefficient c_D can be determined, the integration of the two equations can be performed. The basis for the determin-

ation of H_{12} is the set of relationships between the various parameters outlined in the preceding section. With the addition of the equation

$$H_{12} = H_{12}^i \frac{\delta_2^i}{\delta_2} + \frac{\gamma-1}{2} M_\delta^2 H_{32} \quad (6.3)$$

which is exact for a flow with zero heat transfer, H_{12} can be determined from the values of δ_2, δ_3 obtained from the integration. The skin-friction coefficient is given by the modified Ludwig-Tillmann formula (equation (5.2)). There remains to be obtained an expression for the dissipation coefficient. For incompressible flow Truckenbrodt¹⁵ has devised an approximate formula on the basis of the analysis of Rotta¹⁶. On the assumption that the shearing stress distribution is not altered in compressible flow, Walz modified the dissipation formula in the same way as the skin-friction formula. However, the shape of the shear stress distribution is somewhat fuller in compressible flow, and studies of the boundary layer on a flat plate suggested an increase in the ratio H_{32}/H_{32}^i . The following equation was therefore taken

$$c_D = 0.012 \left(\frac{\rho_\delta u_\delta \delta_2}{\mu_w} \right)^{-0.168} \left(2 \frac{\delta_2}{\delta_2^i} - 1 \right) \frac{H_{32}}{H_{32}^i}. \quad (6.4)$$

The multiplying factor was increased from 0.0112 (Ref. 14) to 0.012 in accord with the studies of Fernholz¹⁷.

The calculations were programmed for an IBM 650 computer, starting from the point $\frac{x}{l} = 0.1416$, the end of the conical nose, and assuming that viscosity is given by

$$\frac{\mu}{\mu_\infty} = \left(\frac{T}{T_\infty} \right)^{\frac{1}{2}}. \quad (6.5)$$

The initial values of δ_2 at the end of the conical nose were calculated in the following way. For supersonic flow with an attached shock wave (i.e. for $M_\infty \geq 1.4$) the pressure on the cone is constant and since $R \propto x$ the momentum equation simplifies to

$$\frac{1}{x} \frac{d \left(x \frac{\delta_2}{l} \right)}{dx} = \frac{c_f}{2}. \quad (6.6)$$

For a turbulent boundary layer the skin friction was calculated from the simple power law

$$c_f = 0.0256 \left(\frac{u_\delta \delta_2}{v_\delta} \right)^{-\frac{1}{4}} \left(\frac{c_f}{c_{fi}} \right) \quad (6.7)$$

with the ratio of skin friction for compressible flow to that for incompressible flow estimated from Eckert's intermediate temperature hypothesis. For laminar flow the Blasius formula gives

$$c_f = (0.664)^2 \frac{v_\delta}{u_\delta \delta_2} \quad (6.8)$$

for incompressible flow. Within the Mach number range under consideration this formula for incompressible flow can be used with little loss of accuracy. Using either equation (6.7) or (6.8) in (6.6) closed formulae can be obtained for δ_2 and c_f . The same formulae were used for subsonic flow although there is a strong favourable gradient with subsonic conditions.

Figs. 12a and b show the calculated values at $x = 0.05$ and $x = 0.1$ for a Reynolds number $Re_l = 10^7$.

For Mach numbers of 1.7 and greater the measured results at $x = 0.05$ (Fig. 12a) are close to the calculated line for laminar flow* and for lower Mach numbers are somewhat lower than the estimate for turbulent flow. As noted earlier the transition trip was of inadequate size at $M_\infty > 1.4$. At $x = 0.1$ the measurements are close to the calculated turbulent values except for $M_\infty = 2.8$ where the flow is still transitional. Fig. 13 shows the calculated values of momentum thickness at $x = 0.142$. No measurements are available for comparison.

The parameter H_{32} , in conjunction with δ_2 , is also needed to determine a starting value for δ_3 . The calculations are not very sensitive to the initial value of δ_3 and so the simplifying assumption was made that H_{32} is constant along the conical forebody. Equations (6.1) and (6.2) then reduce to the simple form.

$$H_{32} = \frac{2 c_D}{c_f}. \quad (6.9)$$

Substitution of equations (5.2) and (6.4) leads to

$$\left(\frac{\rho_\delta u_\delta \delta_2}{\mu_\delta} \right)^{0.1} = \frac{0.246}{0.024} \frac{H_{32}^i}{10^{0.678} H_{12}^i} \left(\frac{\mu_w}{\mu_\delta} \right)^{0.1} \quad (6.10)$$

from which H_{12}^i can be eliminated by equation (5.4). Use of equation (5.5) then enables H_{32} to be calculated. The values required were read from the chart shown in Fig. 14. The Reynolds number dependence invalidates the initial assumption but the variation of H_{32} is relatively small.

The calculations were made using two different assumptions for the initial conditions; firstly fully turbulent flow was taken over the conical nose and secondly the flow was assumed to be laminar with abrupt transition to turbulent flow at the end of the cone ($x = 0.142$). The differences between the two sets of calculations for δ_2 and δ_3 are small at the lower Mach numbers but increase with increase of Mach number. The effect of the different assumptions on skin-friction coefficient is generally small.

The normal definitions for two-dimensional flow of the various boundary-layer parameters in the momentum and kinetic energy equations are valid only if the boundary-layer thickness is small compared with the body radius. The boundary-layer thickness is certainly not small compared with the radius particularly at the waist of the body. However, equations (6.1), (6.2) are still correct provided the appropriate definitions for δ_1 , δ_2 , δ_3 and c_D are used. The definitions are as for two-dimensional flow with the factor $1 + \frac{y}{R}$ introduced in the integrands. It is not known how this procedure affects the formula (6.4) for

the dissipation coefficient but it is a reasonable assumption that $\left(1 + \frac{y}{R}\right)\tau$ does not change greatly with R , so that the equation may approximately be valid. The skin-friction formula, equation (5.2), may also be expected to be approximately correct even when axisymmetric definitions are used for the boundary-layer parameters. The power law relationship equation (5.4) will also be slightly modified by the introduction of the factor $1 + \frac{y}{R}$. The other short-coming of both the calculations and the experiment, the assumption of constant static pressure across the boundary layer, is likely to be increasingly inaccurate as the boundary layer becomes thicker with respect to the body radius in regions of high longitudinal curvature.

7. Discussion of Results.

7.1. General.

The main results of the experiment and comparisons with calculations are shown in Figs. 15 to 26 where schlieren photographs of the flow are also presented. As a check on the compatibility of the measured

*The razor blade calibration used is not necessarily valid in laminar flow.

values of skin-friction coefficient and momentum thickness an extra calculation was made in which the measured values of c_f and H_{12} were used in the momentum equation. This calculation took as a starting point the measured momentum thickness at $x = 0.4$, except for $M_\infty = 2.4$ where the measured value of δ_2 , appears to be inconsistently low. A starting value of $\frac{\delta_2}{l} = 2.3 \times 10^{-4}$ was taken instead of the measured value 1.8×10^{-4} . (Why this low value was obtained is not clear. The profile has some appearance of being laminar but skin-friction measurements taken, along a different generator, at the same time as the profiles show no change from the original measurements and there seems no reason why an asymmetry round the body should occur for one particular Mach number.) The calculations are shown as the chain dotted line in Figs. 15, 18, 19, 20, 22, 24, 26. At $M_\infty = 0.6$ (Fig. 15) the measured momentum thickness at the waist $x = 0.7$ is higher than calculated but it is in good agreement at the end of the body, suggesting that the measurement of skin friction is low up to the waist and possibly high thereafter. At other Mach numbers the calculations and the experiments are in excellent agreement up to $x = 0.7$ but the skin friction appears to be too large for $x > 0.7$ leading to high values of momentum thickness in the calculations. It must be remarked that the technique for the measurement of skin friction, has not been completely established for the flows in which it has been used.

All the experimental results can be described in the same general way. Up to $x = 0.4$ the boundary-layer thickness increases relatively slowly under the influence of a favourable pressure gradient and flow divergence. Between $x = 0.4$ and $x = 0.7$ the flow convergence and adverse pressure gradient lead to a rapid increase in thickness with a maximum thickness and minimum skin-friction coefficient near the waist, $x = 0.7$. The flow divergence downstream of $x = 0.7$ promotes a rapid thinning of the boundary layer and an increase in skin-friction coefficient. For $M_\infty = 1.4, 1.7$ and 2.0 the shape parameter, H_{12}^i , has a maximum at $x = 0.7$ but this feature is not shown at $M_\infty = 2.4$ and 2.8 . At $M_\infty = 0.6$ the peak value of H_{12}^i occurs at least as far forward as $x = 0.4$ where the adverse pressure gradient is strongest. In fact H_{12}^i appears to be correlated strongly with the pressure gradient.

There is good qualitative agreement generally between the calculations and the experiments but there are a number of features unexplained quantitatively. At $M_\infty = 0.6$ (Fig. 15) the momentum and energy thicknesses calculated are in fair agreement with the measured values but their ratio, H_{32} , is larger than measured. In turn the calculated 'incompressible' shape parameter, H_{12}^i , which has a powerful influence on the skin-friction coefficient, is too small and the calculated skin friction too high. Nevertheless the general shape of the curves is faithfully reproduced. The schlieren photograph merely illustrates the thickening of the boundary layer in the body waist. No profile measurements were made at $M_\infty = 0.8$ (Fig. 16) but the skin-friction comparison is similar to that at $M_\infty = 0.6$.

At $M_\infty = 1.4, 2.0$ and 2.8 (Figs. 17, 21, 25) measurements were made at a Reynolds number Re_l of approximately 5×10^6 , when transition did not occur until near the body waist. These results are discussed later (Section 7.4).

For $M_\infty = 1.4, 1.7$ and 2.0 and $Re_l \approx 10^7$ and also for $M_\infty = 1.4, 2.0$ and $Re_l \approx 2 \times 10^7$ the results are fairly similar. The calculations tend to underestimate δ_2 and δ_3 but the ratio, H_{32} , is well calculated. Despite poor agreement for H_{12}^i , for which a strong peak in the body waist is predicted but not measured, the skin friction is in remarkable agreement up to the body waist ($x = 0.7$) but the measured increase over the rear flare is underestimated.

At $M_\infty = 2.4$ and 2.8 with $Re_l \approx 10^7$ (Figs. 24 and 26) the experiments and calculations are in poor agreement. The calculations predict the same sort of behaviour as at lower Mach numbers, that is, sharp peaks in δ_2 and δ_3 at the waist with a low value of H_{32} and a peak in the value of H_{12}^i . In fact the peak in H_{12}^i is predicted to increase with increase of Mach number whereas the measurements show the opposite trend. The peak values of both δ_2 and δ_3 as measured at $M_\infty = 2.8$ occur downstream of the body waist. The measured skin-friction coefficient is considerably greater than estimated.

This failure of the calculations may arise from inaccuracy in the assumed form for the dissipation coefficient. As can be seen in Figs. 24 and 26 the calculations are very sensitive to the value of H_{32} and a small increase in the dissipation coefficient with increasing Mach number could produce a radical change in the results. Some assessment of the applicability of the formula taken for the dissipation coefficient can be made by calculating a sort of mean value. Equation (6.2) can be integrated to give

$$\int_{x_1}^x \frac{c_D}{\delta_3/l} dx = \ln(\delta_3 \rho_\delta^{2-\gamma} u_\delta^3 R)_x - \ln(\delta_3 \rho_\delta^{2-\gamma} u_\delta^3 R)_{x_1}. \quad (7.1)$$

By taking $x_1 = 0.4$ a 'mean' dissipation coefficient may be defined as

$$C_D = \frac{(\delta_3)_{0.4}}{x-0.4} \int_{0.4}^x \frac{c_D}{\delta_3} dx. \quad (7.2)$$

Values of C_D obtained from the measurements and from the calculations are compared in Fig. 27.

Up to $M_\infty = 2$ the experimental points have a fairly similar trend in that initially C_D is overestimated but at $x = 0.7$ the predicted C_D is too small. For $x > 0.7$ the prediction is too large. The points thus roughly follow the trends of H_{12}^i (Figs. 15 to 22), and it is thus indicated that the expression for the dissipation coefficient should be dependent upon this shape parameter. At $M_\infty = 2.4$ the high values of the experimental point can be partly attributed to the low values of δ_3 at $x = 0.4$, and remarked upon previously. Nevertheless both for $M_\infty = 2.4$ and 2.8 the change between $x = 0.55$ and $x = 0.7$ follows the trend of H_{12}^i (Figs. 24 and 26).

Some improvements in the details of the method of calculation could thus be made but the method used is essentially applicable only to two-dimensional flows with small streamwise curvature. In the experiment are included the effects of longitudinal and transverse curvature and of flow convergence and divergence. These effects may be expected to modify the basic structure of the boundary layers in ways of which no account is taken in the calculations. Some consideration of the effect of longitudinal curvature is given by one of the authors in Ref. 18.

7.2. The Influence of Pressure Gradient and Streamline Convergence.

The problem that the present work was intended to study was the combined influence of pressure gradient and streamline convergence on turbulent boundary-layer development. Though, as noted above, the method of calculation devised is not capable of taking into account fully the properties of the flow studied, some qualitative indication of the interaction of pressure gradient and streamline convergence can be obtained. Accordingly, further calculations have been made in which the surface pressure, p and the body radius, R have been taken as constant individually and together. The calculations start from $x = 0.3$ which is near the maximum diameter of the body. Results are shown in Figs. 28, 29 and 30 for the momentum thickness, skin-friction coefficient and shape parameter H_{12}^i .

With both p and R constant the boundary layer is as on a flat plate with momentum thickness growing, and skin friction and shape parameter falling, with increasing x . (H_{12}^i increases between $x = 0.3$ and 0.4 for supersonic speeds, presumably because of the slightly arbitrary choice of the starting values.) With the radius varying but p constant the boundary layer piles up in the body waist giving an increase in momentum thickness (Fig. 28) and a consequent small decrease in skin friction but the change in H_{12}^i is small. With p only varying the adverse pressure gradient up to the body waist causes an increase in momentum thickness over the flat plate values at $M_\infty = 0.6$ and 1.4. At $M_\infty = 2.8$ there is however a reduction because of the effect of the combined velocity and density gradient term in the momentum equation which changes sign at about $M = 2.4$. The dominating influence of the pressure gradient is on the shape parameter (Fig. 30) which is increased over most of the body and markedly so at the waist for $M_\infty = 1.4$ and 2.8. With both p and R varying the pressure gradient effects are amplified considerably. Thus though convergence and divergence of the flow alone produce almost solely geometric effects, appreciable changes in boundary-layer characteristics can be produced when convergence is combined with pressure gradient.

7.3. Comment on Velocity Profiles.

The shape parameters shown in Fig. 9b scatter considerably from the assumed power law line and it might be expected that the use of a two parameter family might give an improved correlation. The results of Ref. 8 show that flat plate velocity profiles in the Mach number range 0.2 to 2.8 correlate completely, both in a wall region and a wake region, at a given value of a Reynolds number $\frac{u_\delta \delta_2^i}{\nu_\delta}$ eliminating the scatter of Fig. 9a. It might be expected therefore that a similar correlation exists for boundary layers in pressure gradients with a family of lines with different values of the parameter $\frac{u_\delta \delta_2^i}{\nu_\delta}$. By varying the scale of a cosine wake term such a family has been constructed (Fig. 31). The dependence upon the Reynolds number is too small to explain the scatter of Fig. 9b and the only merit of the profiles is that the lines are rather steeper than a power law line (as are the experiments).

The failure of this approach is explained by plotting the experimental profiles in Clauser fashion (Figs. 32a to g). In these figures the 'law of the wall' lines are those of Ref. 8 but using freestream Mach number to determine the appropriate friction velocity. The feature that emerges from Fig. 32 is that the measured profiles are not all compatible with the wall law. This is so even at $M_\infty = 0.6$ for $x = 0.833$ and 0.983 and is thus not the fault of the compressibility factors used. The type of flattening of the profiles is similar to that found by Patel¹⁹ in favourable pressure gradients in incompressible flow.

The implication is that, in flows with favourable gradients or strong streamline divergence, calculation methods, such as that developed in this report which depends implicitly on the assumption of an equilibrium type flow, may prove to be unsatisfactory.

To check whether any of the conclusions regarding the behaviour of the velocity profiles are influenced by the assumption of constant static pressure in their evaluation some reappraisal has been undertaken. The pressure distribution through the boundary layer has been calculated utilising, by means of an iterative procedure, equilibrium between normal pressure gradient and local centrifugal acceleration. The calculations are slightly inconsistent, for supersonic speeds, with the profiles previously evaluated in that the constant of integration for the static pressure was determined at the wall rather than at the boundary-layer edge. Velocity profiles calculated using this pressure distribution and the measured pitot pressure are shown for $M_\infty = 0.6$ and 2.8 at $x = 0.4$ and 0.7 in Fig. 33 (to be compared with Figs. 32a and g). The two positions taken have normal pressure gradients of opposite sign. Though appreciable changes of the profiles result it will be seen that there is no significant improvement in the relationship with the 'law of the wall' lines. A further comparison (Fig. 34) of the shape parameter, $H_{1,2}^i$, determined with and without the normal pressure gradient confirms also that in respect of this important parameter the results are little influenced by the neglect of the normal pressure gradient.

7.4. Laminar Boundary-Layer Calculations.

At Reynolds number $Re_l \approx 5 \times 10^6$ at $M_\infty = 1.4, 2.0$ and 2.8 (Figs. 17, 21 and 25) the boundary layer over the body apparently remains laminar up to the point at which the adverse pressure gradient becomes steep. This is about $x = 0.5, 0.55$ and 0.65 at $M_\infty = 1.4, 2.0$ and 2.8 respectively. The change in character of the boundary layer is shown by the jump in the skin-friction coefficient and can also be detected on the schlieren photographs. (Note that the skin friction is deduced from a razor blade calibration for turbulent flow and this cannot be accepted as accurate for a laminar flow.) It is therefore of interest to make laminar boundary-layer calculations.

Such calculations can be made using the basic equations (6.1), (6.2), provided that relations can be established for the various profile parameters. By making use of the Stewartson-Illingworth transformation and writing

$$dY = \frac{\rho}{\rho_\delta} dy \quad (7.3)$$

it follows that the momentum thickness

$$\delta_2 = \int_0^{\infty} \frac{u}{u_\delta} \left(1 - \frac{u}{u_\delta}\right) dY \quad (7.4)$$

and energy thickness

$$\delta_3 = \int_0^{\infty} \frac{u}{u_\delta} \left\{1 - \left(\frac{u}{u_\delta}\right)^2\right\} dY. \quad (7.5)$$

A transformed displacement thickness δ_1^+ can be defined as

$$\delta_1^+ = \int_0^{\infty} \left(1 - \frac{u}{u_\delta}\right) dY. \quad (7.6)$$

For a Prandtl number of unity the total temperature through the boundary layer is constant so that, with $H_{12}^+ = \frac{\delta_1^+}{\delta_2}$,

$$H_{12} = \left(1 + \frac{\gamma-1}{2} M_\delta^2\right) H_{12}^+ + \frac{\gamma-1}{2} M_\delta^2. \quad (7.7)$$

Taking a one parameter family of profiles, H_{12}^+ and H_{32} are uniquely related independently of M_δ . Furthermore if two functions ε^+ and D^+ are defined as follows

$$\left[\begin{array}{c} \partial \left(\frac{u}{u_\delta} \right) \\ - \\ \partial \left(\frac{Y}{\delta_2} \right) \end{array} \right]_w = \varepsilon^+ (H_{32}) \quad (7.8)$$

and

$$\int_0^{\infty} \left[\begin{array}{c} \partial \left(\frac{u}{u_\delta} \right) \\ - \\ \partial \left(\frac{Y}{\delta_2} \right) \end{array} \right]^2 d \left(\frac{Y}{\delta_2} \right) = D^+ (H_{32}) \quad (7.9)$$

and assuming that $\mu\rho = \text{constant}$ then the skin friction and dissipation coefficients can be expressed as

$$c_f = \frac{2 v_\delta}{u_\delta \delta_2} \varepsilon^+ (H_{32}) \quad (7.10)$$

$$c_D = \frac{2 v_\delta}{u_\delta \delta_2} D^+ (H_{32}). \quad (7.11)$$

Using Hartree type profiles Walz²⁰ has developed the following approximate formulae

$$H_{12}^+ = 4.038 - 3.341 (H_{32} - 1.519)^{0.2879} \quad (7.12)$$

$$\varepsilon^+ = 1.299 (H_{32} - 1.519)^{0.6035} \quad (7.13)$$

$$D^+ = 0.1569 + 0.1411 (H_{32} - 1.519) + 3.810 (H_{32} - 1.519)^2 - 11.75 (H_{32} - 1.519)^3. \quad (7.14)$$

These formulae were used in equations (6.1), (6.2) with the starting point at $x = 0.142$, using equation (6.8) for the skin friction and taking a flat plate value of $H_{32} = 1.572$. The results agree qualitatively with the experimental values of skin friction (Figs. 17, 21, 25). Separation of the laminar boundary layer is predicted to occur close to the point at which transition to turbulence apparently occurs at $M_\infty = 1.4$ and 2.0. No separation is predicted at $M_\infty = 2.8$ though the measurements are similar to those at the lower Mach numbers but with transition slightly delayed.

Conclusions.

The measurements qualitatively confirm the findings for a delta wing³ on the effects of combined adverse pressure gradient and streamline convergence in promoting low values of skin friction. Some guidance on these low values can be obtained in terms of local flow conditions by using the Ludwig-Tillmann formula modified to take compressibility into account.

The calculation method developed, based on simultaneous integration of the momentum and kinetic energy equations, gives fair agreement with the experiments up to a Mach number of 2.0 but is less successful at higher Mach numbers. The main deficiencies of the method probably lie in the formula for the dissipation coefficient and in the single-parameter (power-law) representation of the velocity profiles; also no allowance is made, other than in the evaluation of the integral parameters and equations, for the effects of flow convergence or divergence or of surface curvatures both streamwise and transverse. Further work is needed to identify separately these effects, all of which are combined in the experiment.

The experiment could well be extended to higher Mach numbers and the measurement of temperature profiles through the boundary layers would add to its value.

LIST OF SYMBOLS

a	Defined by equation (5.8)
b	Defined by equation (5.5)
c_D	Local dissipation coefficient
C_D	'Mean' dissipation coefficient (equation (7.2))
c_f	Local skin-friction coefficient
c_{f_i}	Equivalent incompressible skin-friction coefficient
k	Defined by equation (5.2)
l	Body length (60 inches)
M	Mach number
R	Body radius (inches)
R_x	Radius of curvature in longitudinal direction
Re_l	Reynolds number based on free stream conditions and model length
Re_{δ_2}	Reynolds number based on local conditions outside boundary layer and momentum thickness
r	Temperature recovery factor
T	Temperature
u	Velocity
u_τ	Friction velocity
X	Distance along body axis from nose (inches)
x	$= \frac{X}{l}$
η	$= \frac{R}{l}$
y	Distance from body surface (inches)
Y	Defined by equation (7.3)
φ	Angular position round body
γ	Ratio of specific heats
μ	Viscosity
ν	Kinematic viscosity
ρ	Density
τ	Shearing stress

Boundary-layer parameters

δ	Total thickness
δ_1	$= \int_0^\delta \left(1 + \frac{y}{R}\right) \left(1 - \frac{\rho u}{\rho_\delta u_\delta}\right) dy$ displacement thickness

LIST OF SYMBOLS—*continued*

$$\delta_2 = \int_0^{\delta} \left(1 + \frac{y}{R}\right) \frac{\rho u}{\rho_{\delta} u_{\delta}} \left(1 - \frac{u}{u_{\delta}}\right) dy \quad \text{momentum thickness}$$

$$\delta_3 = \int_0^{\delta} \left(1 + \frac{y}{R}\right) \frac{\rho u}{\rho_{\delta} u_{\delta}} \left[1 - \left(\frac{u}{u_{\delta}}\right)^2\right] dy \quad \text{kinetic energy thickness}$$

$$\delta_1^i = \int_0^{\delta} \left(1 + \frac{y}{R}\right) \left(1 - \frac{u}{u_{\delta}}\right) dy$$

$$\delta_2^i = \int_0^{\delta} \left(1 + \frac{y}{R}\right) \frac{u}{u_{\delta}} \left(1 - \frac{u}{u_{\delta}}\right) dy$$

$$\delta_3^i = \int_0^{\delta} \left(1 + \frac{y}{R}\right) \frac{u}{u_{\delta}} \left[1 - \left(\frac{u}{u_{\delta}}\right)^2\right] dy$$

$$H_{12} = \frac{\delta_1}{\delta_2}$$

$$H_{32} = \frac{\delta_3}{\delta_2}$$

$$H_{12}^i = \frac{\delta_1^i}{\delta_2^i}$$

$$H_{32}^i = \frac{\delta_3^i}{\delta_2^i}$$

δ_1^+ Transformed laminar boundary-layer displacement thickness defined by equation (7.6)

$$H_{12}^+ = \frac{\delta_1^+}{\delta_2}$$

ε^+ Defined by equation (7.8)

D^+ Defined by equation (7.9)

Subscripts

- ∞ Refers to free stream
- δ Refers to conditions at edge of boundary layer
- w Refers to wall conditions
- t Refers to transition point

Superscript

- * Refers to intermediate temperature conditions

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TABLE 1

Pressure Distribution and Skin Friction.

x in	ϕ deg	$M_\infty = 0.597$ $Re_\ell = 9.85 \times 10^6$			$M_\infty = 0.801$ $Re_\ell = 9.98 \times 10^6$			$M_\infty = 1.390$ $Re_\ell = 5.04 \times 10^6$			$M_\infty = 1.398$ $Re_\ell = 10.2 \times 10^6$		
		C_p	M_δ	$10^3 c_f$	C_p	M_δ	$10^3 c_f$	C_p	M_δ	$10^3 c_f$	C_p	M_δ	$10^3 c_f$
3.0	0	0.311	0.493	3.92	0.371	0.631	3.66	0.413	1.050	2.52	0.417	1.053	3.88
3.0	90	0.310			0.369			0.407			0.406		
3.0	-180	0.314			0.374			0.409			0.402		
3.0	-90	0.310			0.368			0.411			0.401		
6.0	0	0.202	0.530	3.70	0.262	0.681	3.70	0.427	1.040	1.91	0.433	1.042	3.79
12.0	0	-0.222	0.666	3.59	-0.218	0.900	3.87	0.153	1.251	0.68	0.151	1.260	1.01
15.0	0	-0.382	0.715	2.80	-0.458	1.012	3.37	-0.040	1.427	2.24	-0.042	1.438	3.56
18.0	0	-0.399	0.720	2.37	-0.499	1.032	2.72	-0.180	1.582	1.78	-0.181	1.593	3.17
21.0	0	-0.313	0.694	2.45	-0.349	0.960	2.37	-0.281	1.715	1.69	-0.281	1.727	3.37
21.0	90	-0.313			-0.348			-0.280			-0.284		
21.0	-180	-0.310			-0.346			-0.279			-0.275		
21.0	-90	-0.313			-0.350			-0.279			-0.280		
24.0	0	-0.145	0.642	1.83	-0.133	0.861	1.62	-0.273			-0.302	1.759	2.72
27.0	0	-0.004	0.598	1.53	0.027	0.788	1.27	-0.256	1.679	0.65	-0.258	1.695	2.23
28.5	0	0.037	0.585	1.42	0.068	0.770	1.25	-0.248	1.669	0.71	-0.208	1.626	1.92
30.0	0	0.058	0.578	1.35	0.095	0.758	1.20	-0.204	1.611	0.74	-0.154	1.561	1.54
31.5	0	0.073	0.573	1.59	0.108	0.752	1.48	-0.116	1.508	1.97	-0.109	1.509	1.58
33.0	0	0.084	0.569	1.47	0.117	0.748	1.39	-0.062	1.450	2.99	-0.070	1.467	1.43
34.5	0	0.090	0.567	1.47	0.123	0.745	1.42	-0.021	1.409	2.90	-0.038	1.434	1.34
36.0	0	0.103	0.563	1.48	0.137	0.739	1.44	0.009	1.379	2.90	-0.010	1.406	1.31
37.5	0	0.115	0.559	1.31	0.149	0.733	1.35	0.034	1.356	2.58	0.016	1.381	1.16
40.0	0	0.158	0.545	1.31	0.197	0.711	1.19	0.091	1.304	2.24	0.093	1.310	1.00
42.0	0	0.183	0.537	1.43	0.221	0.700	1.38	0.196	1.215	1.73	0.166	1.247	0.83
42.0	90	0.181			0.218			0.191			0.166		
42.0	-180	0.182			0.222			0.198			0.168		
42.0	-90	0.178			0.219			0.191			0.165		
44.0	0	0.168	0.542	1.40	0.208	0.707	1.29	0.249	1.173	1.75	0.200	1.219	0.91
45.5	0	0.138	0.552	1.62	0.178	0.720	1.53	0.228	1.182	2.02	0.198	1.221	1.14
47.0	0	0.118	0.558	1.72	0.150	0.733	1.74	0.208	1.206	2.24	0.188	1.229	1.33
48.5	0	0.103	0.563	1.76	0.133	0.740	1.79	0.191	1.219	2.46	0.178	1.237	1.56
50.0	0	0.092	0.567	1.85	0.128	0.743	1.84	0.188	1.222	2.50	0.176	1.238	1.71
51.5	0	0.086	0.569	1.79	0.124	0.745	1.70	0.186	1.223	2.30	0.178	1.237	1.70
53.0	0	0.074	0.573	2.12	0.116	0.748	2.02	0.197	1.215	2.63	0.188	1.229	1.97
54.5	0	0.058	0.578	2.10	0.097	0.757	2.06	0.197	1.215	2.63	0.190	1.227	2.05
56.0	0	0.037	0.585	2.10	0.077	0.766	2.09	0.218	1.197	2.44	0.207	1.213	2.00
57.5	0	-0.000	0.597	2.27	0.038	0.783	2.30	0.229	1.189	2.63	0.222	1.201	2.09
59.0	0	-0.083	0.623	2.47	-0.047	0.822	2.54	0.248	1.174	2.56	0.236	1.189	2.17
59.0	90	-0.074			-0.037			0.254			0.244		
59.0	-180	-0.080			-0.044			0.246			0.237		
59.0	-90	-0.081			-0.045			0.253			0.237		

TABLE 1—continued

x in	φ deg	$M_\infty = 1.404$ $Re_\ell = 19.97 \times 10^6$			$M_\infty = 1.700$ $Re_\ell = 10.08 \times 10^6$			$M_\infty = 1.996$ $Re_\ell = 4.98 \times 10^6$			$M_\infty = 2.000$ $Re_\ell = 9.96 \times 10^6$		
		C_p	M_δ	$10^3 c_f$	C_p	M_δ	$10^3 c_f$	C_p	M_δ	$10^3 c_f$	C_p	M_δ	$10^3 c_f$
3.0	0	0.417	1.057	3.95	0.360	1.319	1.40	0.333	1.553	1.91	0.325	1.567	1.27
3.0	90	0.403			0.354			0.334			0.327		
3.0	-180	0.400			0.350			0.330			0.324		
3.0	-90	0.408			0.350			0.329			0.323		
6.0	0	0.437	1.043	3.20	0.368	1.311	3.93	0.333	1.553	1.44	0.336	1.556	3.63
12.0	0	0.155	1.261	0.91	0.166	1.501	3.69	0.166	1.737	1.42	0.163	1.749	3.20
15.0	0	-0.040	1.442		0.000	1.696		0.029	1.933	1.46	0.022	1.954	2.54
18.0	0	-0.179	1.598	2.76	-0.115	1.870	2.58	-0.075	2.130	1.12	-0.080	2.154	2.10
21.0	0	-0.282	1.738	2.99	-0.201	2.036	2.75	-0.141	2.298	1.14	-0.150	2.341	2.19
21.0	90	-0.284			-0.199			-0.140			-0.149		
21.0	-180	-0.279			-0.198			-0.141			-0.149		
21.0	-90	-0.277			-0.196			-0.140			-0.148		
24.0	0	-0.299	1.763	2.31	-0.223	2.086	2.34	-0.162	2.360	0.29	-0.173	2.416	1.88
27.0	0	-0.253	1.695	1.93	-0.196	2.025	1.96	-0.139	2.291	0.36	-0.160	2.372	1.73
28.5	0	-0.206	1.632	1.73	-0.168	1.966	1.90	-0.138			-0.140	2.310	1.69
30.0	0	-0.156	1.570	1.46	-0.134	1.903	1.60	-0.134			-0.116	2.244	1.50
31.5	0	-0.110	1.517	1.59	-0.104	1.852	1.67	-0.115			-0.094	2.187	1.47
33.0	0	-0.069	1.472	1.40	-0.074	1.803	1.47	-0.083	2.149	0.30	-0.070	2.134	1.44
34.5	0	-0.038	1.441	1.40	-0.050	1.767	1.38	-0.056	2.089	1.56	-0.051	2.093	1.34
36.0	0	-0.010	1.412	1.45	-0.029	1.737	1.38	-0.025	2.029	2.60	-0.033	2.054	1.33
37.5	0	0.016	1.386	1.26	-0.007	1.706	1.20	0.001	1.981	2.38	-0.015	2.021	1.16
40.0	0	0.089	1.318	1.13	0.046	1.637	1.07	0.038	1.917	2.49	0.024	1.951	1.11
42.0	0	0.174	1.245	0.86	0.123	1.547	0.83	0.118	1.799	2.24	0.095	1.840	0.85
42.0	90	0.171			0.122			0.106			0.092		
42.0	-180	0.174			0.125			0.112			0.100		
42.0	-90	0.169			0.122			0.108			0.093		
44.0	0	0.211	1.215	0.90	0.169	1.498	0.92	0.181	1.718	2.20	0.147	1.770	0.94
45.5	0	0.205	1.219	1.17	0.172	1.495	1.18	0.181	1.719	2.51	0.154	1.761	1.23
47.0	0	0.191	1.231	1.40	0.163	1.504	1.46	0.173	1.728	2.45	0.150	1.765	1.53
48.5	0	0.180	1.241	1.54	0.156	1.512	1.75	0.163	1.740	2.60	0.145	1.772	1.82
50.0	0	0.181	1.239	1.65	0.156	1.512	1.93	0.157	1.748	2.64	0.144	1.773	1.98
51.5	0	0.182	1.239	1.56	0.154	1.513	1.94	0.153	1.753	2.44	0.142	1.776	1.96
53.0	0	0.194	1.229	1.83	0.164	1.504	2.23	0.157	1.748	2.75	0.148	1.767	2.26
54.5	0	0.194	1.229	1.87	0.162	1.505	2.38	0.160	1.744	2.69	0.150	1.766	2.35
56.0	0	0.210	1.216	1.83	0.178	1.489	2.27	0.174	1.727	2.44	0.165	1.746	2.17
57.5	0	0.224	1.204	1.90	0.190	1.476	2.38	0.184	1.715	2.59	0.175	1.734	2.33
59.0	0	0.239	1.192	1.55	0.202	1.464	2.43	0.194	1.702	2.58	0.185	1.721	2.37
59.0	90	0.249			0.211			0.199			0.188		
59.0	-180	0.240			0.204			0.191			0.181		
59.0	-90	0.245			0.206			0.194			0.184		

TABLE 1—continued

x in	ϕ deg	$M_\infty = 2.002$ $Re_\ell = 16.85 \times 10^6$			$M_\infty = 2.401$ $Re_\ell = 10.03 \times 10^6$			$M_\infty = 2.793$ $Re_\ell = 5.03 \times 10^6$			$M_\infty = 2.799$ $Re_\ell = 10.05 \times 10^6$		
		C_p	M_δ	$10^3 c_f$	C_p	M_δ	$10^3 c_f$	C_p	M_δ	$10^3 c_f$	C_p	M_δ	$10^3 c_f$
3.0	0	0.330	1.564	3.50	0.307	1.868	1.11	0.300	2.133	1.49	0.291	2.153	1.06
3.0	90	0.331			0.306			0.298			0.289		
3.0	-180	0.323			0.304			0.299			0.288		
3.0	-90	0.322			0.302			0.294			0.286		
6.0	0	0.337	1.557	2.99	0.312	1.862	3.35	0.301	2.132	1.10	0.292	2.151	2.34
12.0	0	0.162	1.752	2.83	0.165	2.058	2.73	0.168	2.336	1.12	0.158	2.364	2.35
15.0	0	0.019	1.962	2.40	0.038	2.292	2.05	0.056	2.580	0.85	0.040	2.636	1.83
18.0	0	-0.081	2.162	2.01	-0.050	2.528	1.73	-0.028	2.859	0.93	-0.036	2.908	1.57
21.0	0	-0.153	2.354	2.17	-0.109	2.756	1.78	-0.048	2.950	1.06	-0.082	3.162	1.45
21.0	90	-0.152			-0.108			-0.049			-0.080		
21.0	-180	-0.150			-0.110			-0.046			-0.080		
21.0	-90	-0.151			-0.106			-0.041			-0.078		
24.0	0	-0.176	2.430	1.82	-0.130	2.865	1.50	-0.074			-0.111	3.301	1.13
27.0	0	-0.163	2.385	1.60	-0.123	2.826	1.39	-0.065			-0.096	3.261	1.04
28.5	0	-0.142	2.321	1.58	-0.111	2.766	1.39	-0.068	3.050	0.35	-0.089	3.208	1.09
30.0	0	-0.118	2.252	1.35	-0.094	2.691	1.31	-0.066	3.043	0.45	-0.077	3.131	1.21
31.5	0	-0.096	2.196	1.42	-0.080	2.633	1.29	-0.068	3.051	0.87	-0.066	3.064	1.14
33.0	0	-0.074	2.143	1.35	-0.063	2.571	1.24	-0.066	3.039	0.41	-0.056	3.005	1.13
34.5	0	-0.053	2.099	1.27	-0.048	2.522	1.18	-0.061	3.011	0.31	-0.045	2.954	1.23
36.0	0	-0.035	2.061	1.26	-0.036	2.484	1.22	-0.050			-0.031	2.890	1.03
37.5	0	-0.017	2.026	1.11	-0.022	2.444	1.09	-0.037			-0.021	2.844	0.95
40.0	0	0.022	1.957	1.11	0.005	2.361	1.04	0.008	2.724	0.63	0.004	2.751	0.98
42.0	0	0.095	1.842	0.93	0.066	2.233	0.91	0.068	2.547	1.55	0.053	2.600	0.83
42.0	90	0.091			0.064			0.066			0.048		
42.0	-180	0.093			0.069			0.070			0.052		
42.0	-90	0.090			0.064			0.069			0.050		
44.0	0	0.147	1.771	0.88	0.119	2.134	1.00	0.131	2.407	1.96	0.106	2.468	0.93
45.5	0	0.153	1.763	1.22	0.131	2.114	1.33	0.147	2.376	2.19	0.122	2.435	1.21
47.0	0	0.148	1.769	1.55	0.132	2.112	1.53	0.145	2.378	2.06	0.125	2.429	1.36
48.5	0	0.143	1.776	1.79	0.127	2.120	1.78	0.137	2.395	2.18	0.120	2.438	1.56
50.0	0	0.143	1.776	1.93	0.128	2.118	1.90	0.136	2.397	2.20	0.121	2.437	1.68
51.5	0	0.140	1.780	1.87	0.129	2.117	1.77	0.138	2.393	1.73	0.122	2.435	1.51
53.0	0	0.147	1.771	2.13	0.133	2.110	2.08	0.140	2.389	2.06	0.126	2.426	1.77
54.5	0	0.148	1.770	2.20	0.135	2.106	2.12	0.136	2.397	2.20	0.127	2.424	1.83
56.0	0	0.162	1.752	2.04	0.148	2.086	1.94	0.149	2.372	2.01	0.137	2.404	1.72
57.5	0	0.174	1.737	2.14	0.157	2.070	2.09	0.152	2.366	2.19	0.144	2.390	1.87
59.0	0	0.183	1.726	2.14	0.167	2.056	2.15	0.167	2.337	2.05	0.155	2.369	1.88
59.0	90	0.186			0.170			0.172			0.159		
59.0	-180	0.176			0.164			0.168			0.152		
59.0	-90	0.181			0.167			0.166			0.156		

TABLE 2

Velocity Profiles.

Table 2a $M_\infty = 0.597$ $Re_\delta = 9.98 \times 10^6$

$x = 0.4$

$x = 0.475$

$x = 0.55$

$x = 0.4$				$x = 0.475$				$x = 0.55$			
y in	M	$\frac{u}{u_\delta}$	$\frac{u}{u_\delta}$	y in	M	$\frac{u}{u_\delta}$	$\frac{u}{u_\delta}$	y in	M	$\frac{u}{u_\delta}$	$\frac{u}{u_\delta}$
		$r = 0.89$	$r = 1$			$r = 0.89$	$r = 1$			$r = 0.89$	$r = 1$
0.0010	0.3251	0.5201	0.5217	0.0010	0.2795	0.4702	0.4715	0.0010	0.2512	0.4505	0.4517
0.0013	0.3276	0.5240	0.5256	0.0013	0.2835	0.4774	0.4787	0.0013	0.2583	0.4631	0.4643
0.0015	0.3303	0.5283	0.5299	0.0018	0.2914	0.4914	0.4927	0.0015	0.2639	0.4730	0.4742
0.0020	0.3441	0.5498	0.5514	0.0043	0.3170	0.5367	0.5381	0.0018	0.2735	0.4900	0.4912
0.0030	0.3624	0.5784	0.5800	0.0058	0.3338	0.5665	0.5678	0.0020	0.2748	0.4922	0.4934
0.0045	0.3847	0.6132	0.6148	0.0074	0.3447	0.5854	0.5868	0.0025	0.2788	0.4993	0.5005
0.0060	0.4091	0.6510	0.6525	0.0090	0.3592	0.6107	0.6121	0.0035	0.2890	0.5174	0.5186
0.0075	0.4321	0.6864	0.6879	0.0104	0.3692	0.6281	0.6295	0.0051	0.3034	0.5427	0.5440
0.0090	0.4553	0.7219	0.7233	0.0105	0.3701	0.6297	0.6310	0.0065	0.3142	0.5616	0.5629
0.0098	0.4728	0.7487	0.7500	0.0107	0.3692	0.6281	0.6295	0.0081	0.3245	0.5797	0.5810
0.0100	0.4744	0.7511	0.7525	0.0112	0.3721	0.6333	0.6346	0.0097	0.3332	0.5950	0.5963
0.0103	0.4762	0.7538	0.7552	0.0120	0.3864	0.6579	0.6592	0.0105	0.3297	0.5888	0.5901
0.0105	0.4771	0.7552	0.7565	0.0122	0.3846	0.6548	0.6562	0.0108	0.3340	0.5964	0.5977
0.0108	0.4830	0.7642	0.7656	0.0138	0.3975	0.6770	0.6783	0.0110	0.3400	0.6069	0.6081
0.0115	0.4882	0.7721	0.7734	0.0148	0.4072	0.6938	0.6951	0.0112	0.3417	0.6099	0.6112
0.0117	0.4969	0.7852	0.7865	0.0152	0.4143	0.7059	0.7072	0.0113	0.3422	0.6107	0.6120
0.0132	0.5146	0.8121	0.8132	0.0168	0.4252	0.7245	0.7257	0.0115	0.3432	0.6124	0.6137
0.0140	0.5215	0.8224	0.8235	0.0174	0.4302	0.7331	0.7343	0.0120	0.3412	0.6090	0.6103
0.0146	0.5355	0.8434	0.8444	0.0184	0.4376	0.7457	0.7469	0.0131	0.3485	0.6218	0.6231
0.0162	0.5535	0.8703	0.8712	0.0199	0.4519	0.7698	0.7709	0.0140	0.3545	0.6322	0.6335
0.0165	0.5498	0.8648	0.8657	0.0200	0.4519	0.7698	0.7709	0.0147	0.3573	0.6371	0.6384
0.0176	0.5707	0.8960	0.8967	0.0203	0.4565	0.7777	0.7788	0.0162	0.3663	0.6528	0.6540
0.0190	0.5883	0.9219	0.9225	0.0206	0.4580	0.7801	0.7812	0.0170	0.3692	0.6579	0.6592
0.0190	0.5786	0.9076	0.9082	0.0207	0.5050	0.8157	0.8170	0.0177	0.3759	0.6695	0.6708
0.0192	0.5845	0.9163	0.9169	0.0211	0.4642	0.7906	0.7916	0.0193	0.3853	0.6858	0.6870
0.0193	0.5890	0.9229	0.9235	0.0215	0.4678	0.7967	0.7978	0.0196	0.3836	0.6828	0.6840
0.0195	0.5902	0.9247	0.9253	0.0221	0.4716	0.8031	0.8042	0.0207	0.3862	0.6873	0.6885
0.0200	0.5959	0.9332	0.9337	0.0236	0.4875	0.8297	0.8307	0.0209	0.3915	0.6965	0.6977
0.0202	0.5937	0.9299	0.9304	0.0240	0.4875	0.8297	0.8307	0.0209	0.3925	0.6983	0.6995
0.0210	0.6050	0.9466	0.9470	0.0252	0.4973	0.8461	0.8470	0.0211	0.3946	0.7019	0.7031
0.0215	0.6019	0.9420	0.9424	0.0266	0.5082	0.8644	0.8652	0.0215	0.3973	0.7066	0.7078
0.0225	0.6150	0.9612	0.9615	0.0267	0.5082	0.8644	0.8652	0.0216	0.3982	0.7081	0.7093
0.0226	0.6145	0.9604	0.9607	0.0282	0.5182	0.8809	0.8816	0.0222	0.3982	0.7081	0.7093
0.0239	0.6253	0.9763	0.9765	0.0293	0.5260	0.8940	0.8946	0.0232	0.4035	0.7173	0.7185
0.0239	0.6223	0.9719	0.9721	0.0298	0.5292	0.8992	0.8998	0.0237	0.4059	0.7215	0.7227
0.0252	0.6291	0.9818	0.9819	0.0300	0.5356	0.9097	0.9102	0.0248	0.4128	0.7333	0.7344
0.0253	0.6344	0.9895	0.9896	0.0303	0.5344	0.9077	0.9083	0.0263	0.4220	0.7491	0.7502
0.0269	0.6380	0.9948	0.9948	0.0308	0.5375	0.9128	0.9134	0.0265	0.4229	0.7508	0.7519
0.0275	0.6385	0.9955	0.9955	0.0314	0.5418	0.9200	0.9205	0.0278	0.4311	0.7649	0.7659
0.0281	0.6404	0.9983	0.9983	0.0317	0.5424	0.9210	0.9215	0.0292	0.4384	0.7774	0.7784
0.0282	0.6410	0.9992	0.9992	0.0333	0.5528	0.9381	0.9385	0.0295	0.4415	0.7827	0.7837
0.0283	0.6404	0.9983	0.9983	0.0340	0.5589	0.9480	0.9483	0.0304	0.4395	0.7793	0.7803
0.0286	0.6401	0.9978	0.9978	0.0348	0.5625	0.9539	0.9542	0.0307	0.4448	0.7883	0.7894
0.0290	0.6410	0.9992	0.9992	0.0363	0.5707	0.9673	0.9675	0.0310	0.4472	0.7924	0.7934
0.0292	0.6410	0.9992	0.9992	0.0365	0.5719	0.9693	0.9695	0.0310	0.4484	0.7945	0.7955
0.0300	0.6410	0.9992	0.9992	0.0379	0.5764	0.9767	0.9769	0.0312	0.4495	0.7964	0.7974
0.0300	0.6408	0.9988	0.9988	0.0390	0.5821	0.9860	0.9861	0.0315	0.4479	0.7936	0.7946
0.0315	0.6421	1.0008	1.0008	0.0394	0.5833	0.9879	0.9880	0.0320	0.4517	0.8001	0.8010
0.0413	0.6418	1.0002	1.0002	0.0400	0.5839	0.9888	0.9889	0.0330	0.4563	0.8079	0.8089
0.0522	0.6421	1.0008	1.0008	0.0403	0.5861	0.9924	0.9925	0.0338	0.4660	0.8246	0.8254
0.0595	0.6418	1.0002	1.0002	0.0408	0.5861	0.9924	0.9925	0.0346	0.4645	0.8219	0.8228
				0.0408	0.5866	0.9933	0.9933	0.0362	0.4790	0.8467	0.8475
				0.0418	0.5873	0.9943	0.9944	0.0367	0.4819	0.8515	0.8522
				0.0434	0.5900	0.9988	0.9988	0.0377	0.4874	0.8609	0.8617
				0.0435	0.5895	0.9979	0.9979	0.0392	0.4910	0.8669	0.8677
				0.0449	0.5900	0.9988	0.9988	0.0394	0.4916	0.8680	0.8688
				0.0460	0.5900	0.9988	0.9988	0.0401	0.4936	0.8713	0.8720
				0.0460	0.5900	0.9988	0.9988	0.0404	0.4980	0.8788	0.8795
				0.0464	0.5905	0.9996	0.9996	0.0406	0.4987	0.8799	0.8806
				0.0561	0.5905	0.9996	0.9996	0.0408	0.5026	0.8866	0.8872
				0.0646	0.5912	1.0006	1.0006	0.0408	0.4979	0.8786	0.8792
				0.0740	0.5912	1.0006	1.0006	0.0411	0.5005	0.8831	0.8838
				0.0840	0.5917	1.0015	1.0015	0.0416	0.5020	0.8855	0.8861
								0.0427	0.5066	0.8934	0.8941
								0.0437	0.5126	0.9035	0.9041
								0.0442	0.5158	0.9089	0.9094
								0.0457	0.5248	0.9240	0.9245
								0.0465	0.5223	0.9198	0.9202
								0.0466	0.5254	0.9250	0.9255
								0.0473	0.5306	0.9337	0.9341
								0.0489	0.5380	0.9460	0.9464
								0.0492	0.5374	0.9451	0.9454
								0.0505	0.5441	0.9563	0.9566
								0.0533	0.5561	0.9763	0.9765
								0.0559	0.5592	0.9814	0.9815
								0.0562	0.5633	0.9882	0.9882
								0.0588	0.5673	0.9949	0.9949
								0.0622	0.5685	0.9969	0.9969
								0.0660	0.5708	1.0006	1.0006
								0.0716	0.5696	0.9986	0.9987
								0.0726	0.5690	0.9978	0.9978
								0.0726	0.5678	0.9958	0.9958
								0.0757	0.5708	1.0006	1.0006
								0.0855	0.5708	1.0006	1.0006
								0.0921	0.5690	0.9978	0.9978
								0.1012	0.5703	0.9998	0.9998
								0.1115	0.5703	0.9998	0.9998

Table 2b $M_{\infty} = 1.398$ $Re_x = 10.08 \times 10^6$

x = 0.4

x = 0.475

x = 0.55

y_{in}	M	$\frac{u}{u_0}$		y_{in}	M	$\frac{u}{u_0}$		y_{in}	M	$\frac{u}{u_0}$	
		r = 0.89	r = 1			r = 0.89	r = 1			r = 0.89	r = 1
00010	08772	05888	05891	00010	07068	05036	05109	00010	05293	04168	04225
00013	08877	05869	05952	00013	07107	05061	05135	00013	05338	04201	04259
00015	09078	05985	06068	00015	07633	05402	05476	00015	05515	04333	04392
00017	09240	06078	06161	00018	07527	05334	05408	00018	05602	04398	04457
00020	09520	06237	06319	00033	08393	05882	05957	00023	05848	04580	04641
00025	09929	06466	06547	00049	08956	06229	06303	00028	06040	04721	04783
00030	10258	06647	06726	00065	09553	06588	06661	00042	06479	05042	05104
00045	11103	07099	07174	00081	10003	06852	06923	00057	06851	05312	05375
00060	11905	07511	07581	00096	10586	07187	07254	00073	07165	05533	05597
00075	12622	07866	07930	00104	10823	07320	07386	00089	07540	05797	05861
00090	13274	08177	08235	00107	10881	07353	07418	00105	07779	05963	06026
00098	13838	08437	08489	00109	10960	07397	07461	00108	07857	06016	06080
00100	13873	08453	08504	00112	11076	07461	07525	00109	08002	06116	06180
00103	13961	08493	08543	00112	11122	07486	07550	00110	07936	06071	06134
00105	14014	08511	08567	00127	11635	07765	07825	00113	07986	06105	06169
00108	14118	08564	08612	00143	12129	08028	08083	00118	08036	06140	06203
00110	14031	08525	08574	00143	12242	08087	08141	00123	08185	06242	06305
00112	14309	08649	08695	00158	12627	08286	08336	00138	08519	06467	06530
00117	14444	08708	08753	00169	12955	08452	08499	00140	08602	06523	06586
00130	14729	08832	08874	00174	13054	08502	08547	00154	08903	06724	06785
00132	14893	08903	08942	00190	13541	08742	08782	00167	09201	06919	06979
00146	15390	09113	09146	00195	13658	08799	08837	00170	09235	06942	07001
00155	15516	09165	09197	00203	13874	08903	08938	00185	09584	07168	07226
00162	15764	09267	09295	00205	13922	08925	08960	00206	10025	07449	07504
00176	15948	09342	09367	00206	13860	08896	08931	00207	10013	07441	07496
00180	16068	09390	09413	00203	13974	08950	08985	00209	10064	07473	07528
00190	16629	09611	09627	00211	14018	08971	09005	00211	10150	07527	07581
00193	16645	09617	09632	00221	14415	09157	09186	00215	10150	07527	07581
00195	16702	09639	09653	00226	14550	09220	09246	00220	10301	07622	07674
00197	16615	09606	09621	00236	14808	09338	09361	00225	10447	07712	07764
00198	16731	09650	09664	00242	14920	09388	09409	00237	10682	07856	07906
00200	16789	09673	09686	00248	15050	09446	09466	00240	10748	07897	07946
00205	16845	09694	09707	00257	15249	09535	09552	00255	11115	08118	08164
00205	16687	09634	09648	00262	15375	09591	09605	00263	11209	08174	08219
00205	16687	09634	09648	00273	15546	09665	09677	00270	11447	08315	08358
00210	16974	09743	09754	00274	15595	09686	09698	00286	11738	08486	08525
00216	17017	09759	09769	00288	15861	09801	09808	00304	12054	08668	08703
00225	17185	09823	09830	00288	15833	09789	09797	00307	12040	08660	08695
00229	17129	09802	09810	00300	16006	09863	09868	00307	12169	08733	08767
00239	17380	09896	09900	00300	16033	09874	09879	00310	12184	08742	08776
00241	17353	09885	09890	00303	16032	09873	09878	00312	12197	08749	08783
00253	17533	09952	09954	00304	16073	09891	09895	00317	12326	08822	08854
00266	17587	09971	09973	00305	16044	09879	09883	00322	12453	08894	08924
00269	17628	09987	09987	00308	16130	09915	09918	00338	12789	09080	09106
00281	17615	09982	09982	00314	16192	09941	09943	00338	12836	09106	09131
00283	17628	09987	09987	00323	16228	09956	09957	00353	13094	09246	09268
00286	17628	09987	09987	00335	16337	10001	10001	00365	13360	09389	09407
00287	17670	10002	10002	00338	16293	09983	09984	00369	13414	09418	09435
00388	17670	10002	10002	00340	16278	09977	09977	00385	13665	09550	09564
00489	17737	10026	10025	00354	16317	09993	09993	00401	13916	09681	09691
00585	17777	10041	10039	00360	16324	09996	09996	00404	13916	09681	09691
				00464	16325	09996	09997	00406	13993	09721	09730
				00558	16290	09982	09982	00406	13981	09715	09724
				00660	16313	09991	09992	00408	13982	09715	09724
								00414	14081	09766	09773
								00418	14190	09822	09827
								00430	14199	09827	09832
								00435	14308	09882	09886
								00437	14308	09882	09886
								00450	14409	09933	09935
								00463	14468	09963	09964
								00465	14496	09976	09977
								00480	14570	10014	10013
								00502	14553	10005	10005
								00524	14520	09989	09989
								00626	14499	09978	09979
								00723	14478	09967	09968
								00820	14499	09978	09979

Table 20 $M_{\infty} = 1.404$ $Re_{\xi} = 19.34 \times 10^6$

$x = 0.4$				$x = 0.475$				$x = 0.55$			
y	M	$\frac{u}{u_0}$	$\frac{u}{u_0}$	y	M	$\frac{u}{u_0}$	$\frac{u}{u_0}$	y	M	$\frac{u}{u_0}$	$\frac{u}{u_0}$
in		$r = 0.89$	$r = 1$	in		$r = 0.89$	$r = 1$	in		$r = 0.89$	$r = 1$
00.010	0.9116	0.5985	0.6068	00.010	0.7468	0.5268	0.5344	00.010	0.6009	0.4663	0.4725
00.013	0.9396	0.6144	0.6227	00.013	0.7693	0.5413	0.5488	00.013	0.5970	0.4635	0.4697
00.016	0.9490	0.6198	0.6280	00.015	0.7873	0.5526	0.5602	00.015	0.6061	0.4701	0.4763
00.017	0.9704	0.6317	0.6400	00.018	0.8007	0.5611	0.5687	00.018	0.6252	0.4840	0.4902
00.022	1.0165	0.6572	0.6653	00.033	0.8792	0.6097	0.6173	00.023	0.6328	0.4895	0.4958
00.028	1.0502	0.6754	0.6834	00.049	0.9452	0.6494	0.6568	00.023	0.6403	0.4949	0.5012
00.042	1.1387	0.7220	0.7295	00.065	1.0038	0.6837	0.6909	00.039	0.6953	0.5341	0.5406
00.058	1.2223	0.7642	0.7710	00.081	1.0653	0.7188	0.7256	00.054	0.7326	0.5604	0.5668
00.073	1.2958	0.7998	0.8060	00.096	1.1295	0.7542	0.7606	00.070	0.7648	0.5827	0.5892
00.088	1.3607	0.8301	0.8357	00.104	1.1413	0.7606	0.7669	00.085	0.7943	0.6030	0.6094
00.098	1.4364	0.8641	0.8688	00.107	1.1545	0.7677	0.7739	00.105	0.8449	0.6371	0.6435
00.100	1.4497	0.8700	0.8745	00.109	1.1638	0.7728	0.7788	00.108	0.8472	0.6387	0.6451
00.103	1.4515	0.8708	0.8753	00.112	1.1726	0.7774	0.7834	00.109	0.8397	0.6337	0.6401
00.103	1.3345	0.8180	0.8238	00.112	1.1874	0.7853	0.7911	00.110	0.8502	0.6407	0.6470
00.105	1.4619	0.8752	0.8796	00.127	1.2154	0.8000	0.8056	00.113	0.8596	0.6470	0.6533
00.110	1.4839	0.8847	0.8889	00.143	1.2812	0.8337	0.8386	00.118	0.8621	0.6486	0.6549
00.115	1.4994	0.8914	0.8953	00.143	1.2975	0.8419	0.8466	00.118	0.8666	0.6516	0.6579
00.123	1.4922	0.8883	0.8923	00.158	1.3369	0.8613	0.8657	00.130	0.9016	0.6747	0.6808
00.130	1.5467	0.9112	0.9145	00.169	1.3798	0.8821	0.8859	00.134	0.9111	0.6808	0.6870
00.144	1.5877	0.9279	0.9307	00.174	1.3930	0.8882	0.8920	00.149	0.9479	0.7047	0.7106
00.159	1.6309	0.9451	0.9473	00.190	1.4452	0.9127	0.9157	00.165	0.9806	0.7254	0.7312
00.173	1.6425	0.9497	0.9517	00.195	1.4623	0.9205	0.9233	00.181	1.0060	0.7414	0.7470
00.174	1.6699	0.9603	0.9619	00.203	1.4781	0.9277	0.9302	00.204	1.0633	0.7767	0.7819
00.190	1.7141	0.9771	0.9780	00.205	1.4943	0.9350	0.9373	00.207	1.0830	0.7886	0.7936
00.193	1.7197	0.9791	0.9800	00.206	1.4835	0.9301	0.9326	00.210	1.0862	0.7906	0.7955
00.195	1.7227	0.9802	0.9811	00.208	1.4929	0.9344	0.9367	00.212	1.0911	0.7935	0.7984
00.198	1.7254	0.9813	0.9820	00.211	1.5008	0.9379	0.9401	00.215	1.1004	0.7991	0.8039
00.202	1.7340	0.9845	0.9851	00.221	1.5245	0.9484	0.9503	00.220	1.1050	0.8018	0.8066
00.207	1.7469	0.9882	0.9897	00.226	1.5385	0.9546	0.9562	00.220	1.1095	0.8045	0.8092
00.209	1.7319	0.9837	0.9843	00.236	1.5637	0.9655	0.9668	00.227	1.1271	0.8149	0.8195
00.222	1.7636	0.9953	0.9955	00.242	1.5726	0.9693	0.9704	00.229	1.1421	0.8237	0.8281
00.222	1.7392	0.9864	0.9869	00.248	1.5810	0.9729	0.9739	00.236	1.1540	0.8307	0.8350
00.236	1.7704	0.9977	0.9978	00.257	1.5995	0.9807	0.9814	00.251	1.1935	0.8534	0.8573
00.237	1.7577	0.9932	0.9935	00.262	1.6100	0.9851	0.9857	00.267	1.2273	0.8725	0.8760
00.251	1.7744	0.9992	0.9992	00.273	1.6259	0.9918	0.9921	00.282	1.2624	0.8921	0.8951
00.259	1.7740	0.9991	0.9991	00.288	1.6384	0.9969	0.9970	00.304	1.3105	0.9182	0.9206
00.266	1.7772	1.0002	1.0002	00.288	1.6364	0.9961	0.9962	00.306	1.3051	0.9153	0.9177
00.349	1.7798	1.0012	1.0011	00.300	1.6426	0.9987	0.9987	00.307	1.3116	0.9188	0.9212
00.462	1.7813	1.0017	1.0016	00.303	1.6425	0.9986	0.9987	00.309	1.3153	0.9207	0.9231
00.530	1.7837	1.0026	1.0025	00.304	1.6436	0.9991	0.9991	00.312	1.3250	0.9259	0.9281
00.592	1.7936	1.0061	1.0058	00.305	1.6448	0.9996	0.9996	00.317	1.3310	0.9292	0.9313
				00.308	1.6446	0.9995	0.9995	00.317	1.3347	0.9311	0.9331
				00.314	1.6454	0.9998	0.9998	00.326	1.3641	0.9466	0.9482
				00.412	1.6454	0.9998	0.9998	00.328	1.3639	0.9465	0.9481
				00.500	1.6484	1.0010	1.0010	00.330	1.3582	0.9435	0.9452
				00.607	1.6430	0.9988	0.9988	00.333	1.3725	0.9509	0.9524
								00.348	1.4058	0.9680	0.9690
								00.364	1.4259	0.9782	0.9789
								00.380	1.4424	0.9865	0.9869
								00.383	1.4370	0.9838	0.9843
								00.401	1.4626	0.9965	0.9966
								00.403	1.4586	0.9945	0.9947
								00.404	1.4623	0.9963	0.9965
								00.405	1.4623	0.9963	0.9965
								00.409	1.4645	0.9974	0.9975
								00.414	1.4655	0.9979	0.9980
								00.414	1.4655	0.9979	0.9980
								00.425	1.4674	0.9989	0.9989
								00.427	1.4686	0.9995	0.9995
								00.427	1.4686	0.9995	0.9995
								00.430	1.4698	1.0001	1.0001
								00.526	1.4696	1.0000	1.0000
								00.625	1.4674	0.9989	0.9989
								00.726	1.4664	0.9984	0.9984

Table 2a $M_\infty = 1.700$ $Re_\ell = 10,00 \times 10^6$

Table.2d

x = 0,4

y in	M	$\frac{u}{u_0}$ r = 0,89	$\frac{u}{u_0}$ r = 1
00,010	0,9728	0,5746	0,5847
00,013	0,9859	0,5812	0,5913
00,015	0,9991	0,5878	0,5979
00,017	1,0242	0,6003	0,6104
00,020	1,0562	0,6160	0,6260
00,022	1,0756	0,6253	0,6353
00,025	1,1091	0,6414	0,6512
00,028	1,1281	0,6504	0,6602
00,030	1,1598	0,6651	0,6748
00,037	1,1947	0,6811	0,6907
00,048	1,2657	0,7128	0,7220
00,057	1,3251	0,7385	0,7472
00,073	1,4040	0,7712	0,7794
00,088	1,4786	0,8010	0,8084
00,098	1,5607	0,8322	0,8389
00,100	1,5678	0,8349	0,8414
00,103	1,5678	0,8349	0,8414
00,105	1,5775	0,8395	0,8449
00,108	1,5874	0,8421	0,8484
00,108	1,5725	0,8366	0,8431
00,110	1,5945	0,8447	0,8510
00,112	1,6039	0,8481	0,8542
00,115	1,6140	0,8518	0,8578
00,117	1,6278	0,8567	0,8626
00,125	1,6475	0,8637	0,8694
00,128	1,6496	0,8645	0,8701
00,135	1,6866	0,8774	0,8826
00,145	1,7194	0,8886	0,8934
00,148	1,7186	0,8883	0,8931
00,160	1,7758	0,9074	0,9115
00,168	1,7932	0,9130	0,9169
00,174	1,8201	0,9217	0,9253
00,188	1,8507	0,9313	0,9345
00,190	1,8876	0,9427	0,9454
00,193	1,8915	0,9439	0,9466
00,194	1,8807	0,9406	0,9434
00,195	1,8954	0,9451	0,9477
00,198	1,8993	0,9463	0,9489
00,200	1,9060	0,9483	0,9508
00,202	1,9099	0,9495	0,9519
00,205	1,9196	0,9524	0,9547
00,207	1,9242	0,9538	0,9560
00,210	1,9339	0,9567	0,9588
00,212	1,9159	0,9513	0,9536
00,215	1,9335	0,9566	0,9587
00,217	1,9523	0,9621	0,9640
00,225	1,9720	0,9679	0,9695
00,235	1,9735	0,9683	0,9698
00,236	1,9870	0,9722	0,9736
00,237	1,9735	0,9683	0,9698
00,250	2,0213	0,9820	0,9829
00,254	2,0128	0,9796	0,9806
00,256	2,0476	0,9893	0,9898
00,273	2,0457	0,9888	0,9893
00,281	2,0659	0,9943	0,9946
00,283	2,0659	0,9943	0,9946
00,285	2,0657	0,9943	0,9946
00,286	2,0659	0,9943	0,9946
00,288	2,0694	0,9953	0,9955
00,290	2,0723	0,9961	0,9963
00,293	2,0723	0,9961	0,9963
00,295	2,0728	0,9962	0,9964
00,298	2,0747	0,9967	0,9969
00,298	2,0676	0,9948	0,9950
00,300	2,0766	0,9972	0,9974
00,305	2,0782	0,9977	0,9978
00,307	2,0760	0,9971	0,9972
00,310	2,0771	0,9974	0,9975
00,316	2,0820	0,9987	0,9988
00,322	2,0801	0,9982	0,9983
00,325	2,0818	0,9986	0,9987
00,326	2,0820	0,9987	0,9988
00,341	2,0830	0,9990	0,9990
00,344	2,0836	0,9991	0,9992
00,355	2,0855	0,9996	0,9997
00,363	2,0872	1,0001	1,0001
00,466	2,0914	1,0012	1,0012
00,568	2,0996	1,0034	1,0033
00,661	2,1091	1,0060	1,0057
00,731	2,1108	1,0064	1,0061

x = 0,55

y in	M	$\frac{u}{u_0}$ r = 0,89	$\frac{u}{u_0}$ r = 1
00,010	0,7222	0,4794	0,4877
00,013	0,7285	0,4832	0,4915
00,015	0,7330	0,4859	0,4943
00,018	0,7436	0,4923	0,5007
00,023	0,7632	0,5041	0,5126
00,028	0,7834	0,5162	0,5246
00,028	0,7882	0,5190	0,5275
00,033	0,8051	0,5290	0,5375
00,038	0,8251	0,5408	0,5493
00,042	0,8405	0,5497	0,5583
00,048	0,8593	0,5606	0,5692
00,053	0,8720	0,5679	0,5765
00,057	0,8884	0,5773	0,5859
00,063	1,1678	0,7269	0,7346
00,073	0,9319	0,6019	0,6104
00,083	0,9571	0,6159	0,6244
00,094	0,9867	0,6321	0,6406
00,104	1,0147	0,6473	0,6557
00,105	1,0300	0,6557	0,6641
00,108	1,0314	0,6563	0,6646
00,108	1,0319	0,6566	0,6649
00,113	1,0394	0,6601	0,6683
00,118	1,0471	0,6647	0,6729
00,120	1,0494	0,6659	0,6741
00,120	1,0494	0,6659	0,6741
00,123	1,0567	0,6698	0,6780
00,123	1,0569	0,6699	0,6781
00,128	1,0697	0,6766	0,6848
00,133	1,0846	0,6844	0,6925
00,138	1,0920	0,6883	0,6963
00,143	1,1065	0,6958	0,7037
00,150	1,1195	0,7025	1,2056
00,154	1,1345	0,7101	0,7180
00,159	1,1499	0,7180	0,7257
00,170	1,1797	0,7329	0,7404
00,172	1,1797	0,7329	0,7404
00,180	1,2057	0,7458	0,7531
00,191	1,2330	0,7590	0,7662
00,200	1,2614	0,7727	0,7796
00,207	1,2964	0,7893	0,7959
00,209	1,2970	0,7896	0,7961
00,209	1,2981	0,7901	0,7967
00,215	1,3051	0,7933	0,7998
00,216	1,2970	0,7896	0,7961
00,216	1,2970	0,7896	0,7961
00,220	1,3115	0,7963	0,8028
00,225	1,3243	0,8023	0,8086
00,225	1,3243	0,8023	0,8086
00,225	1,3104	0,7958	0,8023
00,230	1,3395	0,8093	0,8154
00,235	1,3526	0,8152	0,8213
00,240	1,3617	0,8195	0,8253
00,245	1,3745	0,8251	0,8309
00,250	1,3878	0,8311	0,8368
00,255	1,4027	0,8377	0,8432
00,260	1,4145	0,8429	0,8483
00,268	1,4290	0,8493	0,8545
00,270	1,4480	0,8575	0,8625
00,277	1,4376	0,8530	0,8581
00,281	1,4734	0,8684	0,8731
00,293	1,4984	0,8789	0,8833
00,302	1,5325	0,8931	0,8970
00,304	1,5432	0,8974	0,9013
00,304	1,4963	0,8780	0,8825
00,307	1,5447	0,8980	0,9019
00,307	1,5451	0,8982	0,9020
00,312	1,5528	0,9014	0,9051
00,317	1,5582	0,9036	0,9072
00,317	1,5612	0,9048	0,9084
00,317	1,5581	0,9035	0,9071
00,322	1,5691	0,9080	0,9115
00,322	1,5702	0,9084	0,9119
00,322	1,5533	0,9015	0,9053
00,327	1,5842	0,9140	0,9173
00,330	1,5549	0,9022	0,9059
00,330	1,5581	0,9035	0,9071
00,333	1,5965	0,9189	0,9220
00,338	1,6042	0,9219	0,9250
00,344	1,6154	0,9263	0,9292
00,349	1,6320	0,9328	0,9355
00,356	1,6229	0,9292	0,9320
00,358	1,6514	0,9403	0,9427
00,369	1,6909	0,9552	0,9571
00,370	1,6749	0,9492	0,9513
00,373	1,6677	0,9465	0,9486
00,380	1,7010	0,9590	0,9607
00,383	1,6764	0,9498	0,9518
00,383	1,6764	0,9498	0,9518
00,390	1,7225	0,9669	0,9683
00,399	1,7266	0,9685	0,9698
00,400	1,7506	0,9772	0,9782
00,401	1,7541	0,9784	0,9794
00,404	1,5462	0,8987	0,9025
00,404	1,7551	0,9788	0,9797
00,408	1,7649	0,9823	0,9831
00,414	1,7625	0,9815	0,9823
00,417	1,7645	0,9822	0,9829
00,417	1,7617	0,9812	0,9820
00,418	1,7692	0,9839	0,9846
00,418	1,7701	0,9842	0,9849
00,422	1,7687	0,9837	0,9844
00,424	1,7771	0,9867	0,9872
00,425	1,7576	0,9797	0,9806
00,425	1,7604	0,9807	0,9815
00,430	1,7852	0,9896	0,9900
00,435	1,7894	0,9910	0,9914
00,440	1,8032	0,9959	0,9961
00,445	1,8032	0,9959	0,9961
00,450	1,8059	0,9968	0,9970
00,451	1,7934	0,9924	0,9928
00,455	1,8123	0,9991	0,9991
00,465	1,8164	1,0005	1,0005
00,564	1,8150	1,0000	1,0000
00,668	1,8137	0,9995	0,9996
00,773	1,8110	0,9986	0,9987
00,895	1,8106	0,9985	0,9985
00,989	1,8065	0,9970	0,9972

Table 2d (Contd)

x = 0.7				x = 0.833				x = 0.983			
y	M	$\frac{u}{u_0}$	$\frac{u}{u_0}$	y	M	$\frac{u}{u_0}$	$\frac{u}{u_0}$	y	M	$\frac{u}{u_0}$	$\frac{u}{u_0}$
in		$r = 0.89$	$r = 1$	in		$r = 0.89$	$r = 1$	in		$r = 0.89$	$r = 1$
00010	05813	04263	04329	00010	07795	05763	05832	00010	08605	06397	06462
00012	05905	04327	04394	00015	08010	05906	05974	00012	08736	06483	06548
00015	05996	04389	04456	00017	08252	06066	06134	00015	08996	06652	06716
00018	06130	04481	04549	00022	08405	06165	06233	00017	09125	06735	06798
00020	06171	04509	04577	00027	08598	06291	06359	00020	09318	06858	06921
00028	06344	04627	04696	00035	08865	06463	06530	00025	09586	07028	07089
00035	06426	04683	04752	00048	09142	06638	06704	00030	09875	07209	07269
00043	06544	04763	04833	00060	09350	06769	06835	00035	09985	07278	07337
00057	06780	04922	04993	00081	09667	06966	07030	00045	10380	07520	07576
00072	07001	05070	05141	00108	09967	07151	07213	00056	10633	07673	07727
00087	07180	05188	05260	00108	09929	07127	07190	00066	10816	07782	07835
00101	07418	05346	05418	00111	09978	07157	07219	00077	11025	07906	07957
00104	07418	05346	05418	00114	10040	07195	07257	00092	11227	08025	08074
00105	07418	05346	05418	00120	10095	07229	07290	00108	11473	08167	08214
00106	07484	05389	05461	00125	10131	07251	07312	00108	11397	08124	08171
00109	07484	05389	05461	00132	10229	07310	07370	00112	11449	08153	08200
00111	07515	05409	05482	00145	10342	07377	07437	00115	11481	08172	08218
00119	07646	05495	05567	00159	10443	07438	07497	00116	11544	08208	08254
00126	07676	05514	05587	00179	10654	07563	07620	00120	11567	08221	08267
00134	07801	05595	05668	00205	11755	08196	08244	00125	11621	08252	08297
00148	08012	05731	05804	00205	10965	07745	07800	00130	11702	08299	08343
00153	08188	05844	05917	00210	10930	07725	07780	00135	11706	08301	08345
00178	08385	05969	06041	00212	10998	07764	07819	00145	11807	08358	08401
00195	08599	06104	06176	00218	11015	07775	07829	00155	11913	08418	08460
00195	08651	06136	06209	00222	11066	07804	07858	00166	11991	08462	08503
00197	08651	06136	06209	00230	11147	07851	07904	00176	12070	08507	08547
00200	08678	06153	06226	00243	11309	07944	07996	00192	12224	08592	08631
00203	08730	06186	06258	00255	11432	08014	08065	00206	12442	08633	08682
00205	08730	06186	06258	00276	11644	08134	08183	00209	12351	08662	08699
00212	08881	06280	06352	00303	11978	08320	08365	00210	12266	08615	08653
00220	08931	06310	06382	00306	11982	08322	08367	00212	12297	08633	08671
00228	09079	06402	06473	00310	12036	08352	08397	00215	12379	08678	08714
00243	09267	06517	06588	00314	12087	08380	08425	00215	12358	08666	08703
00258	09473	06642	06712	00318	12118	08398	08441	00217	12381	08679	08716
00272	09693	05774	06843	00324	12192	08438	08481	00223	12434	08708	08744
00290	09924	06912	06980	00331	12279	08486	08528	00227	12480	08733	08769
00293	10065	06995	07062	00345	12424	08564	08605	00232	12505	08747	08782
00295	10106	07020	07087	00357	12549	08632	08670	00243	12600	08799	08833
00298	10146	07043	07110	00370	12649	08686	08723	00253	12648	08825	08859
00301	10185	07066	07132	00376	12798	08765	08801	00264	12795	08904	08936
00303	10204	07077	07143	00402	13044	08894	08927	00274	12819	08918	08949
00310	10339	07156	07222	00405	13086	08916	08948	00290	12915	08969	08999
00317	10417	07201	07266	00405	13095	08921	08953	00306	13040	09036	09064
00326	10529	07266	07330	00408	13126	08937	08969	00306	13010	09020	09048
00340	10766	07401	07464	00413	13181	08965	08996	00308	13018	09024	09053
00353	10856	07452	07515	00418	13224	08988	09018	00311	13050	09041	09069
00355	10979	07522	07584	00426	13319	09037	09066	00314	13122	09079	09106
00370	11202	07647	07707	00439	13464	09112	09139	00314	13088	09061	09089
00385	11436	07777	07835	00452	13589	09175	09201	00316	13109	09073	09100
00387	11468	07795	07852	00466	13755	09259	09282	00321	13159	09099	09126
00388	11468	07795	07852	00473	13796	09280	09303	00326	13178	09109	09135
00390	11516	07821	07878	00499	14098	09430	09449	00331	13225	09134	09160
00394	11550	07840	07897	00563	14612	09681	09692	00342	13290	09168	09193
00396	11598	07866	07922	00630	14983	09857	09862	00353	13358	09204	09228
00403	11695	07919	07975	00665	15132	09927	09929	00363	13428	09240	09263
00410	11806	07979	08034	00724	15238	09976	09977	00370	13451	09252	09275
00418	11931	08047	08100	00760	15270	09990	09991	00373	13495	09275	09297
00433	12160	08170	08221	00820	15291	10001	10001	00390	13608	09334	09354
00441	12282	08234	08284	00921	15291	10001	10001	00400	13672	09366	09386
00448	12371	08281	08330	01016	15291	10001	10001	00403	13653	09356	09376
00462	12605	08404	08450	01176	15280	09996	09996	00405	13686	09373	09393
00479	12891	08551	08594	01270	15270	09991	09991	00408	13729	09385	09414
00534	13668	08941	08974					00408	13707	09384	09404
00598	14557	09366	09388					00408	13698	09379	09399
00630	15086	09610	09623					00410	13727	09394	09413
00685	15596	09837	09843					00415	13772	09418	09436
00720	15832	09941	09943					00420	13791	09427	09445
00775	15954	09994	09994					00425	13813	09438	09456
00841	15954	09994	09994					00436	13874	09470	09486
00960	15932	09984	09985					00447	13940	09503	09519
01075	15865	09955	09957					00457	14006	09536	09551
01156	15854	09950	09952					00468	14092	09580	09593
01243	15809	09931	09933					00470	14070	09569	09583
01335	15809	09931	09933					00484	14135	09601	09614
01420	15764	09911	09914					00500	14220	09644	09655
								00567	14516	09790	09797
								00632	14717	09888	09892
								00667	14784	09921	09923
								00728	14880	09967	09968
								00763	14926	09989	09989
								00827	14940	09996	09996
								00892	14966	10008	10008
								00988	14976	09999	09999
								01087	14943	09997	09997
								01187	14943	09997	09997
								01283	14943	09997	09997

Table 2f $M_{\infty} = 2.401$ $Re_{\rho} = 9.92 \times 10^6$

$x = 0.4$

y in	M	$\frac{u}{u_6}$	$\frac{u}{u_6}$
		$r = 0.89$	$r = 1$
00.010	0.9932	0.5004	0.5138
00.013	1.1145	0.5510	0.5646
00.015	1.1263	0.5558	0.5694
00.017	1.1587	0.5687	0.5824
00.022	1.2178	0.5918	0.6054
00.028	1.2974	0.6217	0.6352
00.032	1.4140	0.6634	0.6765
00.043	1.5902	0.7214	0.7336
00.052	1.8174	0.7879	0.7984
00.065	2.0977	0.8582	0.8660
00.078	2.3424	0.9102	0.9156
00.090	2.5096	0.9414	0.9451
00.098	2.6048	0.9577	0.9604
00.100	2.6486	0.9649	0.9672
00.100	2.6044	0.9576	0.9604
00.103	2.6537	0.9657	0.9680
00.105	2.6744	0.9690	0.9711
00.110	2.6858	0.9709	0.9728
00.113	2.6767	0.9694	0.9714
00.115	2.7216	0.9765	0.9780
00.120	2.7430	0.9798	0.9811
00.125	2.7310	0.9779	0.9794
00.130	2.7564	0.9818	0.9830
00.140	2.7745	0.9845	0.9856
00.152	2.7895	0.9868	0.9876
00.165	2.7969	0.9879	0.9887
00.176	2.8026	0.9887	0.9895
00.187	2.8096	0.9897	0.9904
00.190	2.8235	0.9917	0.9923
00.193	2.8248	0.9919	0.9925
00.195	2.8231	0.9917	0.9922
00.198	2.8291	0.9926	0.9931
00.200	2.8179	0.9909	0.9915
00.202	2.8274	0.9923	0.9928
00.207	2.8352	0.9934	0.9939
00.212	2.8429	0.9945	0.9949
00.212	2.8308	0.9928	0.9933
00.222	2.8494	0.9955	0.9958
00.232	2.8537	0.9961	0.9963
00.243	2.8554	0.9963	0.9966
00.256	2.8626	0.9974	0.9975
00.269	2.8678	0.9981	0.9982
00.278	2.8682	0.9981	0.9983
00.281	2.8754	0.9992	0.9992
00.283	2.8767	0.9993	0.9994
00.286	2.8746	0.9990	0.9991
00.288	2.8720	0.9987	0.9988
00.290	2.8763	0.9993	0.9993
00.293	2.8793	0.9997	0.9997
00.298	2.8805	0.9999	0.9999
00.302	2.8818	1.0001	1.0001
00.405	2.9008	1.0027	1.0025
00.541	2.9273	1.0063	1.0059
00.628	2.9398	1.0080	1.0075
00.719	2.9589	1.0106	1.0099
00.842	2.9819	1.0137	1.0127
00.920	2.9946	1.0153	1.0142
00.999	3.0190	1.0185	1.0172
01.081	3.0312	1.0200	1.0186
01.167	3.0436	1.0216	1.0201

$x = 0.55$

y in	M	$\frac{u}{u_6}$	$\frac{u}{u_6}$
		$r = 0.89$	$r = 1$
00.010	1.1337	0.5844	0.5971
00.013	1.1933	0.6069	0.6194
00.015	1.2365	0.6242	0.6367
00.018	1.2571	0.6323	0.6448
00.020	1.2905	0.6453	0.6577
00.023	1.2983	0.6484	0.6606
00.025	1.3475	0.6670	0.6791
00.028	1.3636	0.6730	0.6850
00.030	1.3910	0.6831	0.6950
00.042	1.4642	0.7093	0.7207
00.056	1.5383	0.7347	0.7457
00.068	1.5948	0.7534	0.7640
00.094	1.7110	0.7899	0.7995
00.105	1.7802	0.8105	0.8195
00.107	1.7668	0.8066	0.8157
00.108	1.7926	0.8141	0.8230
00.110	1.7995	0.8161	0.8249
00.113	1.8068	0.8182	0.8263
00.115	1.8154	0.8206	0.8293
00.118	1.8208	0.8222	0.8308
00.120	1.8419	0.8281	0.8365
00.123	1.8538	0.8315	0.8397
00.125	1.8671	0.8351	0.8433
00.138	1.9143	0.8480	0.8556
00.153	1.9645	0.8612	0.8684
00.165	2.0207	0.8756	0.8822
00.191	2.1183	0.8993	0.9048
00.203	2.1750	0.9125	0.9174
00.207	2.2029	0.9188	0.9234
00.209	2.2129	0.9210	0.9255
00.211	2.2239	0.9235	0.9278
00.215	2.2239	0.9235	0.9278
00.216	2.2309	0.9250	0.9293
00.220	2.2356	0.9260	0.9303
00.222	2.2582	0.9309	0.9349
00.225	2.2574	0.9308	0.9348
00.227	2.2682	0.9331	0.9370
00.240	2.3068	0.9413	0.9447
00.252	2.3429	0.9488	0.9518
00.266	2.3798	0.9562	0.9589
00.293	2.4424	0.9685	0.9704
00.304	2.4818	0.9760	0.9775
00.305	2.4772	0.9751	0.9767
00.307	2.4811	0.9759	0.9773
00.310	2.4860	0.9768	0.9782
00.312	2.4860	0.9768	0.9782
00.315	2.4919	0.9779	0.9793
00.317	2.4968	0.9788	0.9801
00.320	2.5024	0.9798	0.9811
00.322	2.5111	0.9815	0.9826
00.325	2.5111	0.9815	0.9826
00.338	2.5312	0.9851	0.9860
00.351	2.5456	0.9877	0.9885
00.370	2.5603	0.9904	0.9910
00.377	2.5749	0.9930	0.9934
00.390	2.5843	0.9946	0.9950
00.401	2.5985	0.9971	0.9973
00.403	2.5925	0.9961	0.9963
00.404	2.5975	0.9969	0.9971
00.406	2.5975	0.9969	0.9971
00.408	2.5975	0.9969	0.9971
00.411	2.5985	0.9971	0.9973
00.414	2.5985	0.9971	0.9973
00.416	2.6038	0.9980	0.9982
00.418	2.6029	0.9979	0.9980
00.422	2.6076	0.9987	0.9988
00.433	2.6026	0.9978	0.9980
00.435	2.6079	0.9987	0.9988
00.447	2.6126	0.9995	0.9996
00.465	2.6129	0.9996	0.9996
00.473	2.6129	0.9996	0.9996
00.487	2.6129	0.9996	0.9996
00.500	2.6160	1.0001	1.0001
00.664	2.8026	0.9978	0.9980
00.727	2.5975	0.9969	0.9971
00.827	2.5928	0.9961	0.9964
00.923	2.5881	0.9953	0.9956
01.023	2.5834	0.9945	0.9948

Table 2g $M_{\infty} = 2.799$ $Re_{\ell} = 10.10 \times 10^6$

$x = 0.4$

$x = 0.55$

y_{in}	M	$\frac{u}{u_0}$	$\frac{u}{u_0}$
		$r = 0.89$	$r = 1$
00010	1.1790	0.5468	0.5620
00013	1.2365	0.5679	0.5831
00015	1.2790	0.5831	0.5982
00017	1.3425	0.6051	0.6202
00022	1.4584	0.6435	0.6582
00028	1.5135	0.6608	0.6754
00037	1.6506	0.7017	0.7156
00048	1.7931	0.7408	0.7538
00057	1.9536	0.7809	0.7928
00073	2.2044	0.8362	0.8459
00088	2.4281	0.8786	0.8863
00098	2.6057	0.9083	0.9144
00100	2.6428	0.9141	0.9198
00103	2.6620	0.9170	0.9226
00105	2.7045	0.9234	0.9286
00105	2.6811	0.9199	0.9253
00110	2.7833	0.9348	0.9393
00115	2.8128	0.9389	0.9432
00123	2.8573	0.9450	0.9489
00125	2.8986	0.9505	0.9540
00135	2.9501	0.9572	0.9602
00138	2.9722	0.9600	0.9629
00145	3.0200	0.9659	0.9684
00153	3.0424	0.9686	0.9709
00160	3.0702	0.9719	0.9740
00174	3.1188	0.9776	0.9792
00190	3.1351	0.9794	0.9810
00192	3.1606	0.9823	0.9836
00193	3.1467	0.9808	0.9822
00195	3.1537	0.9815	0.9829
00198	3.1698	0.9833	0.9846
00202	3.1812	0.9846	0.9858
00207	3.1881	0.9854	0.9865
00210	3.1987	0.9865	0.9875
00217	3.2071	0.9874	0.9884
00224	3.2176	0.9886	0.9894
00226	3.2169	0.9885	0.9894
00236	3.2432	0.9913	0.9920
00240	3.2454	0.9916	0.9922
00250	3.2618	0.9933	0.9938
00266	3.2804	0.9952	0.9956
00281	3.3061	0.9979	0.9981
00282	3.3017	0.9975	0.9976
00283	3.3039	0.9977	0.9979
00286	3.3135	0.9987	0.9988
00288	3.3120	0.9985	0.9986
00293	3.3193	0.9993	0.9993
00298	3.3193	0.9993	0.9993
00300	3.3201	0.9993	0.9994
00307	3.3193	0.9993	0.9993
00315	3.3201	0.9993	0.9994
00316	3.3171	0.9990	0.9991
00326	3.3266	1.0000	1.0000
00329	3.3288	1.0002	1.0002
00341	3.3354	1.0009	1.0008
00433	3.3629	1.0036	1.0033
00510	3.3830	1.0056	1.0052
00631	3.4222	1.0094	1.0087
00710	3.4484	1.0119	1.0110
00862	3.5007	1.0167	1.0154
00940	3.5180	1.0183	1.0169
01019	3.5359	1.0199	1.0184
01186	3.5869	1.0244	1.0225

y_{in}	M	$\frac{u}{u_0}$	$\frac{u}{u_0}$
		$r = 0.89$	$r = 1$
00010	1.2604	0.5944	0.6086
00013	1.2831	0.6027	0.6169
00015	1.3584	0.6295	0.6435
00018	1.3889	0.6400	0.6540
00020	1.4186	0.6501	0.6640
00023	1.4761	0.6692	0.6828
00028	1.5203	0.6835	0.6969
00038	1.6079	0.7107	0.7236
00048	1.6711	0.7295	0.7420
00063	1.7685	0.7570	0.7689
00079	1.8455	0.7777	0.7890
00094	1.9463	0.8034	0.8138
00105	1.9713	0.8095	0.8197
00107	2.0284	0.8231	0.8328
00108	2.0300	0.8235	0.8332
00110	2.0476	0.8276	0.8371
00113	2.0560	0.8300	0.8394
00115	2.0777	0.8345	0.8437
00118	2.0972	0.8389	0.8479
00123	2.1372	0.8478	0.8564
00133	2.1810	0.8572	0.8655
00143	2.2180	0.8650	0.8729
00159	2.3184	0.8852	0.8922
00175	2.3773	0.8965	0.9029
00191	2.4220	0.9048	0.9107
00203	2.4967	0.9181	0.9233
00207	2.4314	0.9065	0.9123
00209	2.4980	0.9183	0.9235
00211	2.5130	0.9209	0.9260
00215	2.5207	0.9223	0.9272
00216	2.5368	0.9250	0.9298
00220	2.5451	0.9264	0.9312
00225	2.5863	0.9333	0.9376
00235	2.6069	0.9367	0.9408
00245	2.6459	0.9429	0.9467
00260	2.6843	0.9489	0.9523
00276	2.7429	0.9579	0.9607
00293	2.7817	0.9636	0.9661
00304	2.7841	0.9639	0.9664
00305	2.8108	0.9678	0.9700
00307	2.8183	0.9689	0.9710
00310	2.8258	0.9699	0.9720
00312	2.8327	0.9709	0.9729
00315	2.8401	0.9719	0.9739
00317	2.8555	0.9741	0.9759
00322	2.8612	0.9749	0.9766
00335	2.8815	0.9777	0.9792
00344	2.9023	0.9805	0.9819
00358	2.9379	0.9853	0.9863
00370	2.9406	0.9856	0.9866
00375	2.9643	0.9887	0.9895
00390	2.9867	0.9916	0.9922
00401	3.0078	0.9943	0.9947
00403	3.0067	0.9942	0.9946
00404	3.0137	0.9951	0.9954
00406	3.0137	0.9951	0.9954
00408	3.0137	0.9951	0.9954
00411	3.0207	0.9959	0.9962
00414	3.0218	0.9961	0.9964
00418	3.0271	0.9968	0.9970
00430	3.0325	0.9974	0.9976
00440	3.0395	0.9983	0.9984
00455	3.0464	0.9991	0.9992
00465	3.0427	0.9987	0.9988
00470	3.0522	0.9999	0.9999
00487	3.0538	1.0001	1.0001
00500	3.0602	1.0008	1.0008
00633	3.0427	0.9987	0.9988
00727	3.0357	0.9978	0.9980
00827	3.0293	0.9970	0.9972
00923	3.0293	0.9970	0.9972
01023	3.0223	0.9961	0.9964

Table 2g (Contd)

x = 0.7

x = 0.833

x = 0.983

y in	M	u u ₀		y in	M	u u ₀		y in	M	u u ₀	
		r = 0.89	r = 1			r = 0.89	r = 1			r = 0.89	r = 1
00010	13326	06461	06589	00010	13350	06794	06907	00010	13477	06908	07018
00012	13621	06569	06696	00012	14048	07058	07168	00012	13769	07021	07129
00015	14009	06708	06834	00015	14248	07132	07241	00015	14343	07236	07341
00020	14751	06966	07088	00017	15000	07403	07507	00017	14616	07336	07439
00035	16044	07390	07504	00020	15245	07489	07590	00022	15359	07600	07698
00050	16845	07637	07745	00025	16001	07746	07841	00025	15717	07724	07819
00065	17536	07841	07943	00030	16372	07868	07960	00030	16115	07858	07949
00080	18113	08005	08102	00035	16729	07983	08072	00030	16115	07858	07949
00092	18610	08141	08234	00045	17343	08175	08258	00035	16456	07971	08059
00101	19039	08256	08344	00055	17863	08332	08410	00045	17157	08195	08277
00104	19110	08275	08363	00071	18562	08536	08607	00060	17921	08429	08503
00105	19028	08253	08342	00086	19012	08662	08728	00077	18685	08653	08718
00106	19176	08292	08379	00108	19573	08815	08875	00092	19234	08807	08866
00111	19311	08327	08413	00108	19451	08782	08844	00108	19872	08979	09032
00125	19846	08463	08544	00109	19614	08826	08885	00108	19755	08948	09002
00140	20366	08592	08677	00111	19583	08817	08878	00112	19913	08990	09042
00155	20937	08728	08808	00114	19703	08850	08908	00115	19991	09011	09062
00170	21479	08852	08917	00117	19714	08852	08911	00116	20028	09021	09071
00183	21783	08921	08982	00122	19751	08862	08920	00122	20147	09052	09101
00195	22092	08989	09046	00127	19877	08896	08952	00125	20224	09072	09120
00195	22373	09049	09104	00132	19962	08918	08974	00130	20302	09092	09139
00197	22148	09001	09058	00143	20140	08964	09018	00130	20302	09092	09139
00200	22327	09039	09095	00153	20301	09005	09057	00135	20378	09112	09158
00205	22327	09039	09095	00169	20591	09079	09128	00145	20571	09161	09205
00220	22844	09148	09198	00184	20754	09120	09167	00160	20798	09218	09260
00235	23183	09218	09265	00205	21028	09187	09231	00176	21090	09291	09332
00250	23677	09317	09358	00205	20996	09180	09224	00192	21317	09346	09382
00265	23957	09372	09410	00207	21028	09187	09231	00206	21489	09388	09421
00278	24221	09422	09458	00210	20990	09178	09222	00208	21536	09399	09432
00290	24486	09472	09505	00212	21070	09198	09241	00210	21498	09390	09423
00293	24601	09494	09525	00215	21159	09219	09261	00212	21571	09407	09440
00295	24601	09494	09525	00220	21239	09239	09280	00215	21536	09399	09432
00298	24656	09504	09535	00225	21233	09237	09278	00220	21608	09416	09448
00303	24706	09513	09543	00230	21312	09256	09296	00223	21680	09433	09464
00317	24971	09562	09589	00241	21400	09277	09317	00227	21715	09441	09472
00333	25178	09599	09624	00252	21588	09322	09359	00232	21790	09459	09489
00349	25478	09652	09674	00266	21784	09368	09403	00243	21895	09484	09512
00353	25552	09665	09686	00282	21938	09404	09437	00259	22038	09517	09544
00363	25843	09716	09734	00303	22243	09473	09503	00274	22215	09558	09583
00375	25884	09723	09740	00306	22276	09481	09510	00290	22392	09598	09621
00385	25992	09741	09758	00308	22276	09481	09510	00305	22450	09611	09633
00387	26036	09749	09765	00310	22276	09481	09510	00306	22522	09628	09649
00388	25944	09733	09750	00314	22276	09481	09510	00308	22459	09613	09635
00390	26044	09750	09766	00316	22361	09500	09528	00311	22528	09629	09650
00396	25992	09741	09758	00321	22400	09509	09536	00314	22564	09637	09657
00410	26291	09792	09805	00326	22466	09523	09550	00319	22633	09652	09672
00425	26441	09816	09828	00331	22541	09540	09566	00321	22666	09660	09679
00440	26531	09831	09842	00342	22624	09559	09584	00326	22672	09661	09680
00441	26602	09843	09853	00352	22728	09581	09605	00326	22638	09654	09673
00455	26734	09865	09873	00368	22949	09630	09651	00326	22702	09668	09686
00468	26773	09871	09879	00370	22914	09622	09644	00331	22702	09668	09686
00479	26870	09887	09894	00383	23060	09654	09674	00342	22803	09690	09708
00534	27209	09941	09944	00402	23241	09692	09710	00357	22907	09713	09729
00598	27369	09966	09968	00403	23165	09676	09695	00370	23002	09734	09749
00630	27589	10000	10000	00405	23203	09684	09702	00373	23010	09735	09751
00720	27494	09985	09986	00405	23244	09693	09711	00390	23111	09757	09771
00839	27282	09952	09955	00408	23275	09700	09717	00400	23070	09748	09763
00922	27186	09937	09941	00410	23247	09693	09711	00403	23111	09757	09771
01010	27090	09922	09927	00415	23319	09709	09726	00405	23143	09764	09778
01193	26948	09899	09906	00420	23278	09700	09718	00408	23178	09772	09785
				00426	23313	09708	09725	00408	23205	09778	09790
				00436	23500	09747	09762	00413	23245	09786	09799
				00447	23531	09753	09768	00415	23245	09786	09799
				00463	23708	09790	09802	00420	23285	09795	09807
				00463	23708	09790	09802	00420	23280	09794	09806
				00478	23779	09805	09816	00425	23280	09794	09806
				00499	23920	09834	09843	00436	23379	09815	09826
				00549	24236	09897	09903	00451	23414	09822	09833
				00630	24512	09952	09955	00468	23512	09843	09852
				00685	24580	09965	09967	00470	23507	09842	09851
				00784	24681	09985	09986	00484	23546	09850	09859
				00740	24481	09985	09986	00500	23673	09877	09884
				00880	24749	09998	09998	00567	23870	09918	09923
				00921	24749	09998	09998	00632	24037	09952	09955
				01018	24749	09998	09998	00667	24096	09964	09966
				01270	24681	09985	09986	00728	24169	09979	09980
								00763	24195	09984	09985
								00827	24264	09998	09998
								00931	24264	09998	09998
								01024	24264	09998	09998
								01187	24200	09985	09986
								01283	24135	09972	09974

TABLE 3

Integral Properties of the Boundary Layers.

(a) $r = 0.89$

x	δ_1 in	δ_2 in	δ_3 in	δ_1^i in	δ_2^i in	δ_3^i in	H_{12}	H_{32}	H_{12}^i	H_{32}^i	$\frac{u_\delta}{v_\delta}$ $\times 10^5/\text{in}$	M_δ
$M_\infty = 0.597 \quad Re_\ell = 9.98 \times 10^6$												
0.4	0.0635	0.0363	0.0624	0.0590	0.0375	0.0645	1.751	1.720	1.571	1.718	1.752	0.642
0.475	0.1095	0.0630	0.1064	0.1030	0.0649	0.1096	1.739	1.690	1.587	1.689	1.644	0.586
0.55	0.1572	0.0939	0.1597	0.1480	0.0965	0.1641	1.675	1.701	1.533	1.700	1.612	0.570
0.7	0.3059	0.1858	0.3157	0.2897	0.1906	0.3235	1.646	1.699	1.520	1.697	1.472	0.538
0.833	0.1683	0.1142	0.2037	0.1566	0.1166	0.2080	1.473	1.784	1.343	1.783	1.543	0.566
0.983	0.0859	0.0609	0.1130	0.0781	0.0620	0.1149	1.411	1.856	1.261	1.855	1.662	0.622
$M_\infty = 1.398 \quad Re_\ell = 10.08 \times 10^6$												
0.4	0.0654	0.0234	0.0417	0.0422	0.0282	0.0500	2.799	1.784	1.499	1.775	1.516	1.766
0.475	0.0970	0.0362	0.0628	0.0671	0.0437	0.0755	2.681	1.737	1.535	1.727	1.592	1.633
0.55	0.1581	0.0618	0.1043	0.1189	0.0736	0.1234	2.559	1.687	1.616	1.678	1.647	1.454
0.7	0.3244	0.1359	0.2263	0.2576	0.1573	0.2607	2.388	1.665	1.638	1.658	1.702	1.288
0.833	0.1837	0.0916	0.1629	0.1381	0.1014	0.1799	2.006	1.779	1.362	1.775	1.706	1.254
0.983	0.1233	0.0665	0.1224	0.0912	0.0714	0.1313	1.855	1.842	1.276	1.839	1.695	1.215
$M_\infty = 1.404 \quad Re_\ell = 19.34 \times 10^6$												
0.4	0.0584	0.0207	0.0370	0.0376	0.0249	0.0443	2.824	1.789	1.509	1.779	2.922	1.777
0.475	0.0840	0.0312	0.0544	0.0578	0.0377	0.0654	2.692	1.744	1.533	1.735	3.051	1.646
0.55	0.1356	0.0534	0.0906	0.1008	0.0635	0.1073	2.542	1.698	1.587	1.689	3.219	1.470
0.7	0.2866	0.1234	0.2077	0.2252	0.1421	0.2382	2.322	1.683	1.584	1.676	3.219	1.289
0.833	0.1594	0.0806	0.1450	0.1179	0.0887	0.1593	1.979	1.799	1.329	1.796	3.218	1.269
0.983	0.1112	0.0605	0.1120	0.0820	0.0647	0.1197	1.839	1.851	1.267	1.849	3.303	1.211

TABLE 3(a)—continued

x	δ_1 in	δ_2 in	δ_3 in	δ_1^i in	δ_2^i in	δ_3^i in	H_{12}	H_{32}	H_{12}^i	H_{32}^i	$\frac{u_\delta}{v_\delta}$ $\times 10^5/\text{in}$	M_δ
$M_\infty = 1.700 \quad Re_\ell = 10.00 \times 10^6$												
0.4	0.0800	0.0244	0.0438	0.0461	0.0312	0.0556	3.273	1.792	1.474	1.779	1.419	2.087
0.55	0.1594	0.0538	0.0925	0.1051	0.0684	0.1168	2.963	1.720	1.537	1.708	1.592	1.815
0.7	0.2901	0.1070	0.1807	0.2081	0.1315	0.2206	2.712	1.689	1.583	1.678	1.712	1.597
0.833	0.1763	0.0764	0.1365	0.1195	0.0881	0.1570	2.309	1.788	1.356	1.782	1.712	1.529
0.983	0.1172	0.0545	0.1009	0.0770	0.0603	0.1114	2.149	1.851	1.276	1.847	1.768	1.495
$M_\infty = 2.000 \quad Re_\ell = 9.88 \times 10^6$												
0.4	0.0916	0.0238	0.0429	0.0471	0.0322	0.0575	3.851	1.802	1.462	1.785	1.311	2.414
0.475	0.1232	0.0329	0.0583	0.0668	0.0453	0.0795	3.746	1.770	1.473	1.754	1.363	2.333
0.55	0.1678	0.0482	0.0839	0.0986	0.0656	0.1131	3.481	1.739	1.504	1.724	1.487	2.153
0.7	0.2736	0.0878	0.1505	0.1751	0.1149	0.1954	3.117	1.714	1.524	1.701	1.693	1.918
0.833	0.1689	0.0636	0.1148	0.1023	0.0764	0.1372	2.654	1.804	1.340	1.796	1.778	1.804
0.983	0.1180	0.0478	0.0888	0.0695	0.0544	0.1008	2.469	1.858	1.277	1.853	1.816	1.751
$M_\infty = 2.401 \quad Re_\ell = 9.92 \times 10^6$												
0.4	0.0582	0.0110	0.0194	0.0296	0.0172	0.0297	5.312	1.768	1.723	1.731	1.266	2.881
0.55	0.1170	0.0281	0.0510	0.0549	0.0392	0.0705	4.165	1.815	1.403	1.800	1.453	2.615
0.7	0.1903	0.0527	0.0950	0.0965	0.0707	0.1264	3.608	1.802	1.365	1.788	1.631	2.354
0.833	0.1447	0.0475	0.0885	0.0722	0.0569	0.1058	3.048	1.865	1.267	1.858	1.813	2.145
0.983	0.0959	0.0322	0.0606	0.0485	0.0375	0.0704	2.977	1.883	1.292	1.874	1.849	2.096
$M_\infty = 2.799 \quad Re_\ell = 10.10 \times 10^6$												
0.4	0.0796	0.0129	0.0233	0.0337	0.0214	0.0379	6.167	1.804	1.576	1.770	1.216	3.3-7
0.55	0.1323	0.0259	0.0474	0.0537	0.0387	0.0701	5.112	1.830	1.387	1.810	1.411	3.053
0.7	0.1410	0.0329	0.0611	0.0581	0.0443	0.0816	4.285	1.858	1.313	1.844	1.608	2.759
0.833	0.1199	0.0333	0.0631	0.0510	0.0404	0.0763	3.599	1.895	1.262	1.885	1.866	2.476
0.983	0.0998	0.0283	0.0536	0.0436	0.0339	0.0639	3.531	1.896	1.286	1.886	1.922	2.427

TABLE 3—continued

(b) $r = 1$

x	δ_1 in	δ_2 in	δ_3 in	δ_1^i in	δ_2^i in	δ_3^i in	H_{12}	H_{32}	H_{12}^i	H_{32}^i	$\frac{u_\delta}{v_\delta}$ $\times 10^5/\text{in}$	M_δ
$M_\infty = 0.597 \quad Re_\ell = 9.98 \times 10^6$												
0.4	0.0638	0.0360	0.0620	0.0587	0.0374	0.0643	1.771	1.721	1.569	1.719	1.752	0.642
0.475	0.1099	0.0626	0.1059	0.1026	0.0647	0.1094	1.756	1.692	1.585	1.690	1.644	0.586
0.55	0.1578	0.0933	0.1588	0.1474	0.0963	0.1638	1.691	1.702	1.531	1.701	1.612	0.570
0.7	0.3069	0.1849	0.3143	0.2887	0.1902	0.3229	1.660	1.700	1.518	1.698	1.472	0.538
0.833	0.1689	0.1135	0.2026	0.1559	0.1162	0.2073	1.488	1.785	1.341	1.784	1.543	0.566
0.983	0.0863	0.0604	0.1122	0.0777	0.0616	0.1144	1.429	1.856	1.260	1.865	1.662	0.622
$M_\infty = 1.398 \quad Re_\ell = 10.08 \times 10^6$												
0.4	0.0663	0.0225	0.0403	0.0412	0.0276	0.0491	2.948	1.789	1.493	1.779	1.516	1.766
0.475	0.0982	0.0350	0.0609	0.0657	0.0430	0.0745	2.808	1.742	1.526	1.732	1.592	1.633
0.55	0.1599	0.0601	0.1017	0.1168	0.0728	0.1224	2.661	1.692	1.606	1.682	1.647	1.454
0.7	0.3275	0.1328	0.2217	0.2541	0.1560	0.2591	2.467	1.670	1.628	1.661	1.702	1.288
0.833	0.1858	0.0894	0.1594	0.1357	0.1000	0.1778	2.078	1.783	1.357	1.778	1.706	1.254
0.983	0.1263	0.0656	0.1208	0.0907	0.0710	0.1306	1.926	1.842	1.276	1.839	1.695	1.215
$M_\infty = 1.404 \quad Re_\ell = 19.34 \times 10^6$												
0.4	0.0591	0.0199	0.0356	0.0366	0.0243	0.0434	2.977	1.794	1.505	1.784	2.922	1.777
0.475	0.0851	0.0301	0.0527	0.0565	0.0370	0.0645	2.822	1.749	1.525	1.740	3.051	1.646
0.55	0.1371	0.0518	0.0882	0.0989	0.0627	0.1062	2.645	1.703	1.578	1.693	3.219	1.470
0.7	0.2895	0.1205	0.2034	0.2219	0.1409	0.2365	2.401	1.687	1.575	1.679	3.219	1.289
0.833	0.1611	0.0782	0.1409	0.1157	0.0870	0.1564	2.059	1.802	1.329	1.797	3.218	1.269
0.983	0.1126	0.0591	0.1095	0.0805	0.0637	0.1179	1.906	1.854	1.264	1.851	3.303	1.211

TABLE 3(b)—continued

x	δ_1 in	δ_2 in	δ_3 in	δ_1^i in	δ_2^i in	δ_3^i in	H_{12}	H_{32}	H_{12}^i	H_{32}^i	$\frac{u_\delta}{v_\delta}$ $\times 10^5/\text{in}$	M_δ
$M_\infty = 1.700 \quad Re_\ell = 10.00 \times 10^6$												
0.4	0.0811	0.0233	0.0419	0.0446	0.0304	0.0543	3.480	1.799	1.468	1.784	1.419	2.087
0.55	0.1535	0.0487	0.0833	0.0986	0.0643	0.1097	3.152	1.711	1.534	1.707	1.592	1.815
0.7	0.2935	0.1036	0.1755	0.2040	0.1299	0.2185	2.832	1.694	1.570	1.682	1.712	1.597
0.833	0.1779	0.0737	0.1322	0.1161	0.0861	0.1539	2.414	1.793	1.348	1.787	1.712	1.529
0.983	0.1197	0.0531	0.0984	0.0757	0.0594	0.1098	2.254	1.853	1.275	1.849	1.768	1.495
$M_\infty = 2.000 \quad Re_\ell = 9.88 \times 10^6$												
0.4	0.0929	0.0225	0.0407	0.0454	0.0312	0.0559	4.125	1.809	1.454	1.791	1.311	2.414
0.475	0.1249	0.0312	0.0555	0.0645	0.0441	0.0777	4.002	1.778	1.462	1.761	1.363	2.333
0.55	0.1701	0.0460	0.0803	0.0956	0.0641	0.1110	3.698	1.747	1.491	1.731	1.487	2.153
0.7	0.2772	0.0843	0.1451	0.1705	0.1129	0.1927	3.289	1.721	1.510	1.707	1.698	1.918
0.833	0.1714	0.0612	0.1106	0.0993	0.0746	0.1343	2.802	1.809	1.332	1.801	1.778	1.804
0.983	0.1197	0.0459	0.0855	0.0673	0.0528	0.0981	2.610	1.863	1.274	1.857	1.816	1.751
$M_\infty = 2.401 \quad Re_\ell = 9.92 \times 10^6$												
0.4	0.0589	0.0103	0.0183	0.0285	0.0166	0.0289	5.723	1.776	1.714	1.739	1.266	2.881
0.55	0.1257	0.0283	0.0520	0.0546	0.0397	0.0720	4.435	1.836	1.375	1.815	1.453	2.615
0.7	0.1930	0.0500	0.0904	0.0928	0.0685	0.1229	3.862	1.809	1.355	1.795	1.631	2.354
0.833	0.1476	0.0453	0.0846	0.0697	0.0551	0.1026	3.261	1.870	1.264	1.861	1.813	2.145
0.983	0.0974	0.0306	0.0578	0.0467	0.0361	0.0679	3.181	1.887	1.290	1.878	1.849	2.096
$M_\infty = 2.799 \quad Re_\ell = 10.10 \times 10^6$												
0.4	0.0805	0.0120	0.0218	0.0323	0.0206	0.0365	6.696	1.813	1.568	1.777	1.216	3.327
0.55	0.1340	0.0242	0.0445	0.0512	0.0371	0.0674	5.543	1.838	1.379	1.818	1.411	3.053
0.7	0.1430	0.0309	0.0575	0.0554	0.0423	0.0783	4.633	1.865	1.308	1.850	1.608	2.759
0.833	0.1219	0.0314	0.0597	0.0487	0.0386	0.0730	3.879	1.898	1.261	1.889	1.866	2.476
0.983	0.1014	0.0267	0.0507	0.0417	0.0324	0.0612	3.803	1.901	1.286	1.890	1.922	2.427

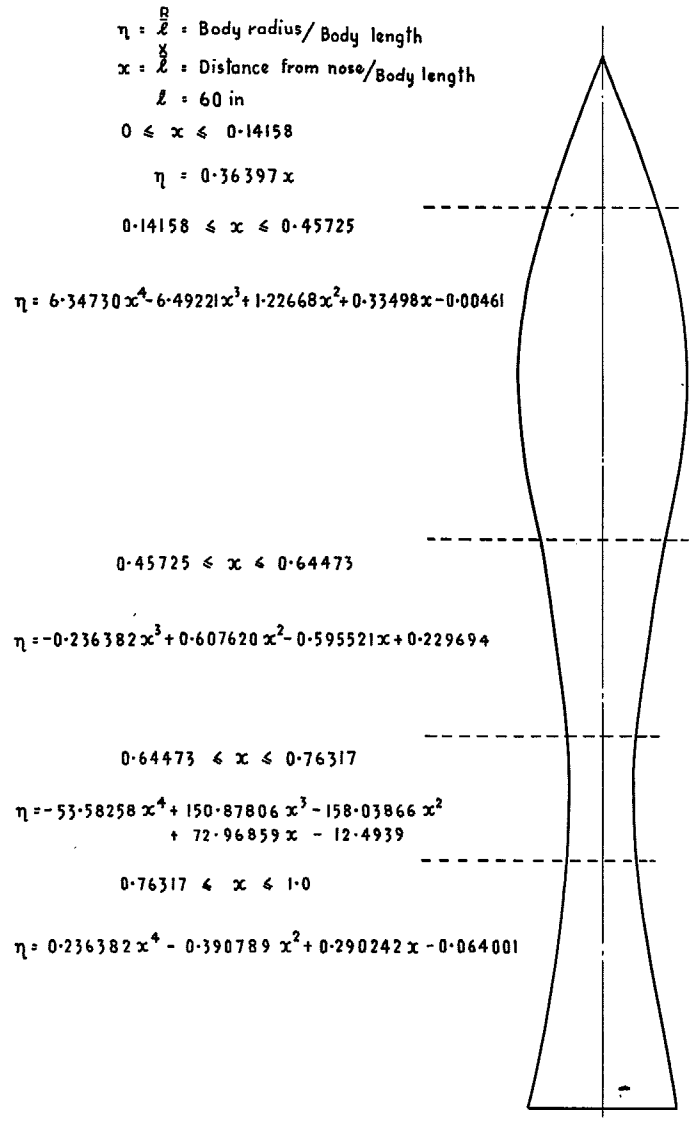


FIG. 1. Geometry of body.

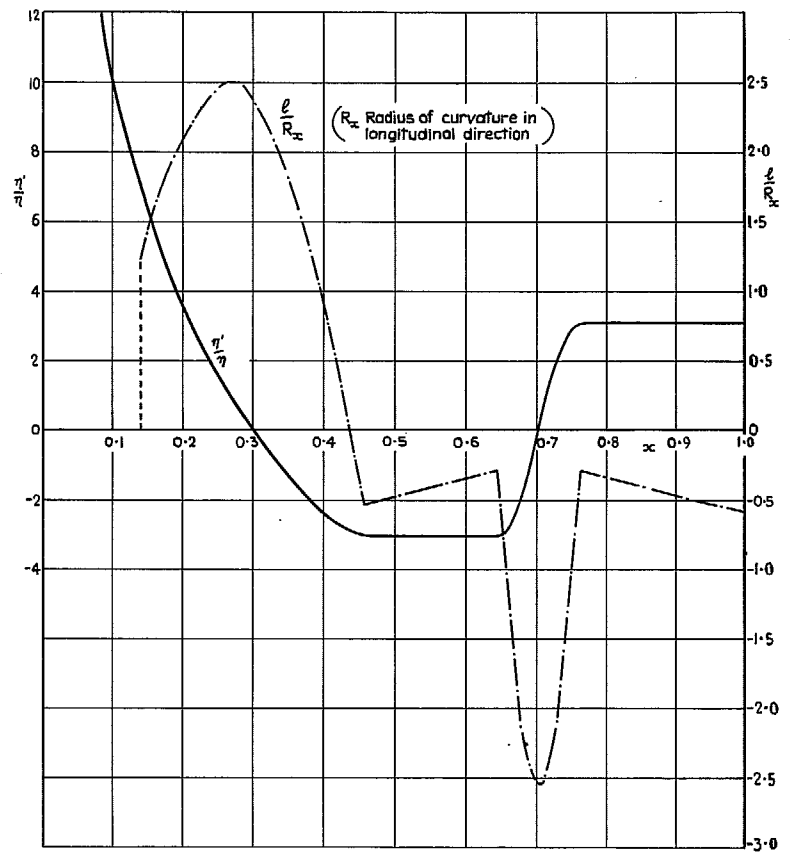


FIG. 2. Divergence parameter and longitudinal curvature.

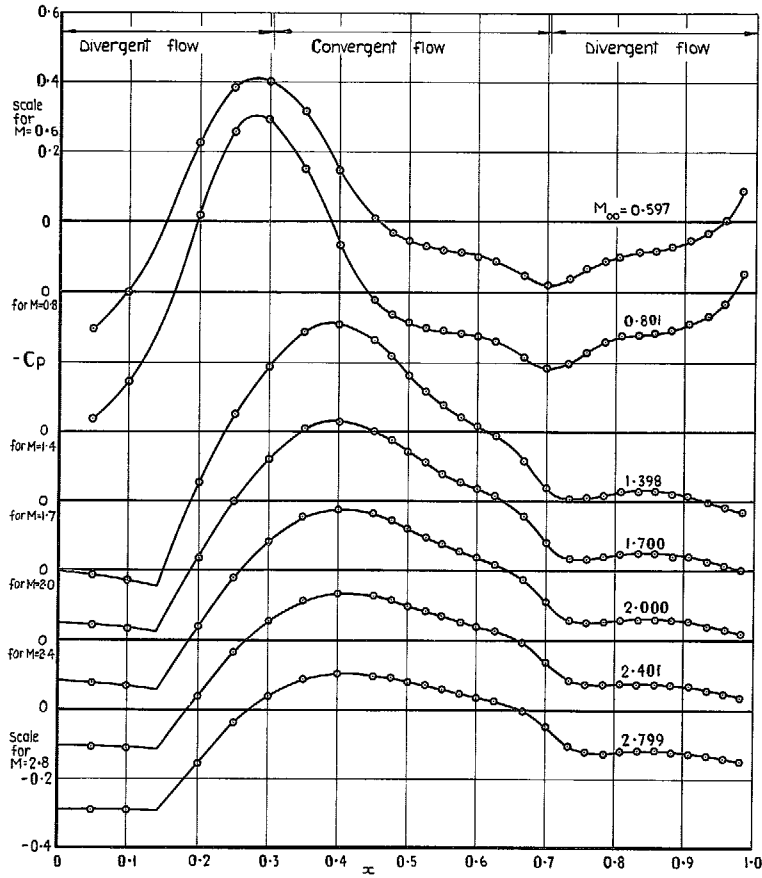


FIG. 3. Pressure distribution $Re_l \approx 10^7$.

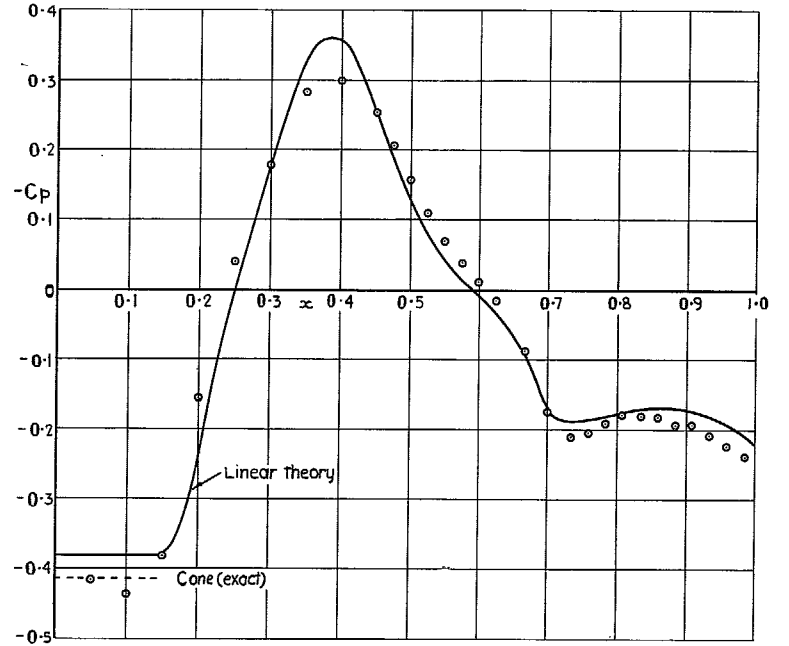


FIG. 4. Comparison of predicted (inviscid) and measured pressure distribution $M = 1.404$
 $Re_l = 19.97 \times 10^6$.

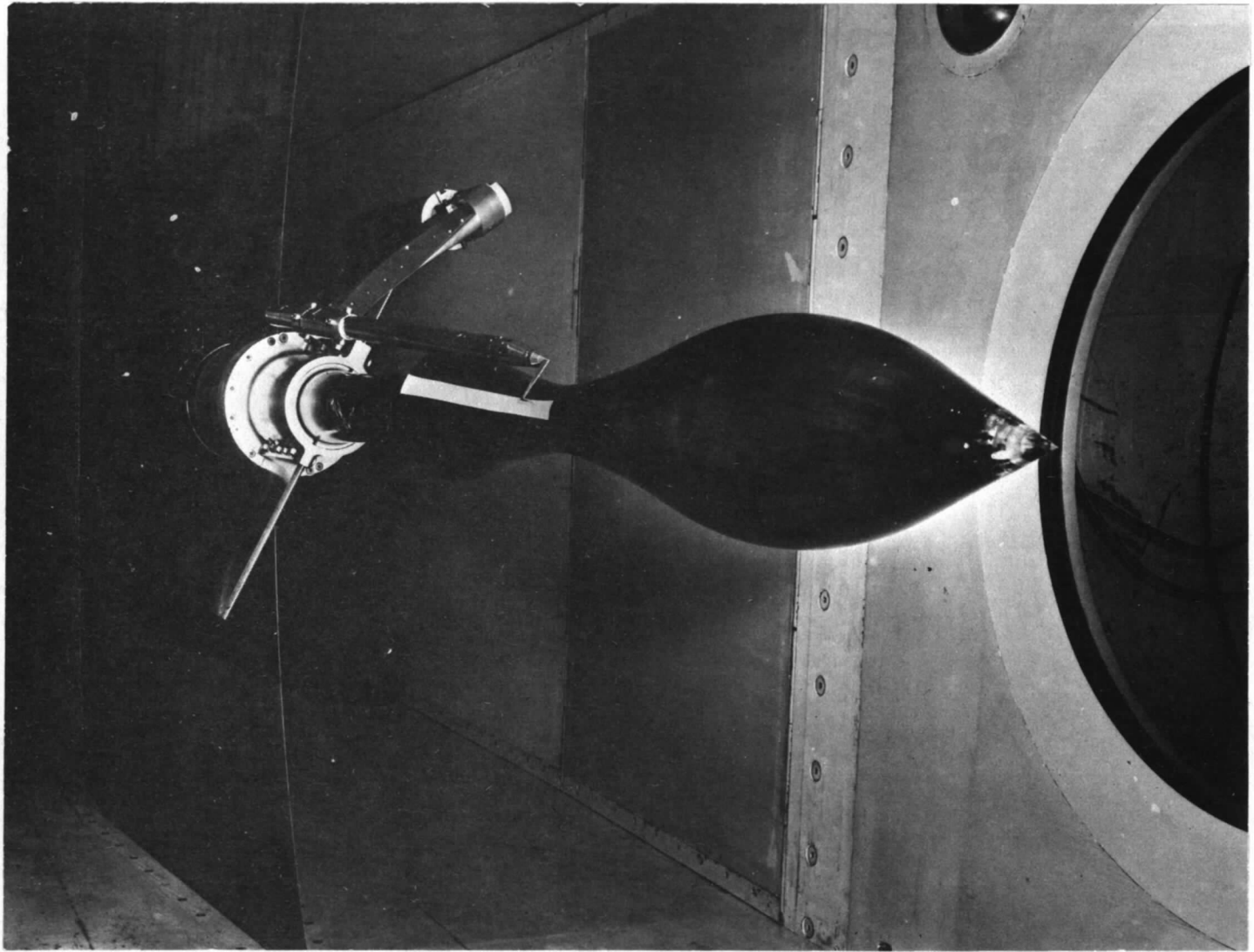


FIG. 5a. Model with boundary-layer survey equipment.

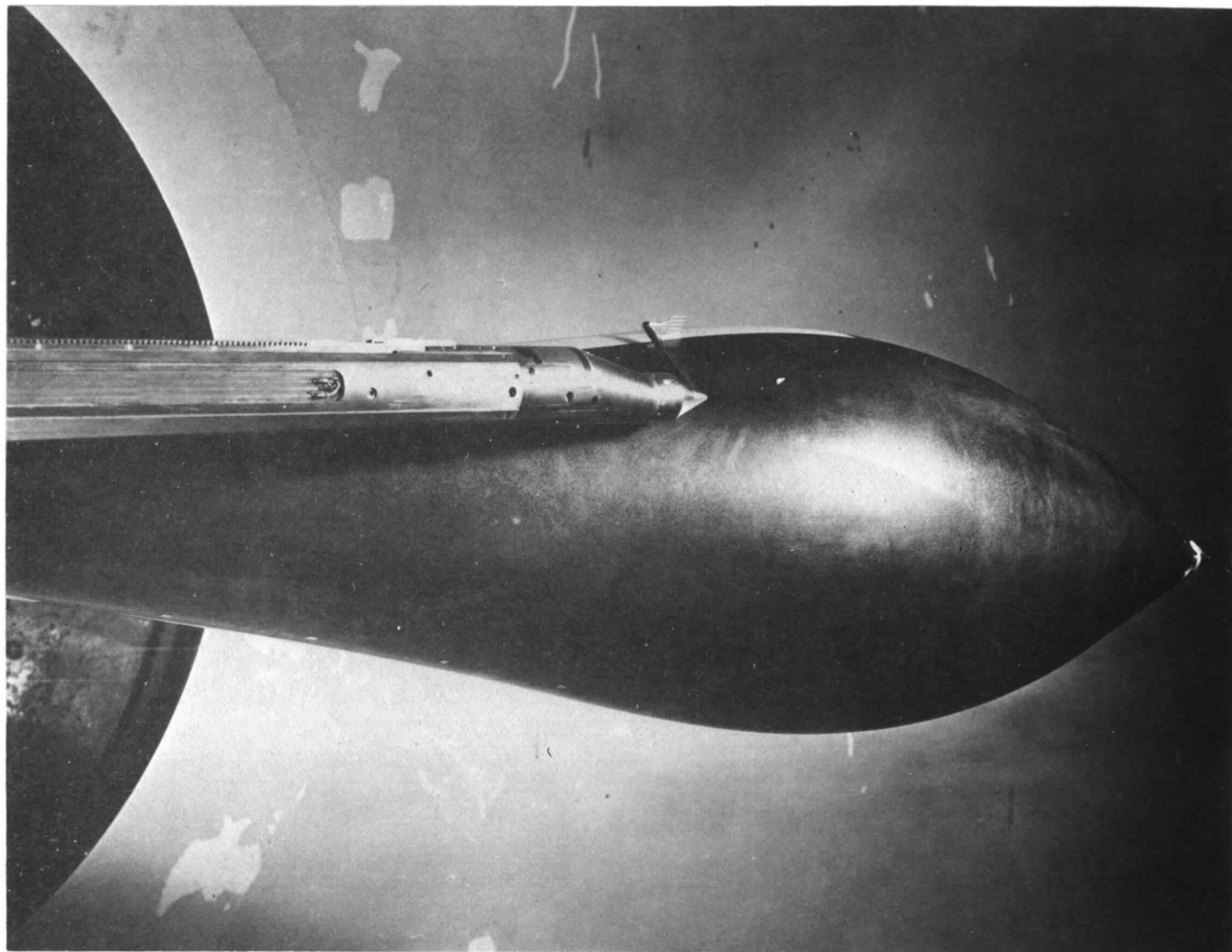


FIG. 5b. Detail of model with rake.

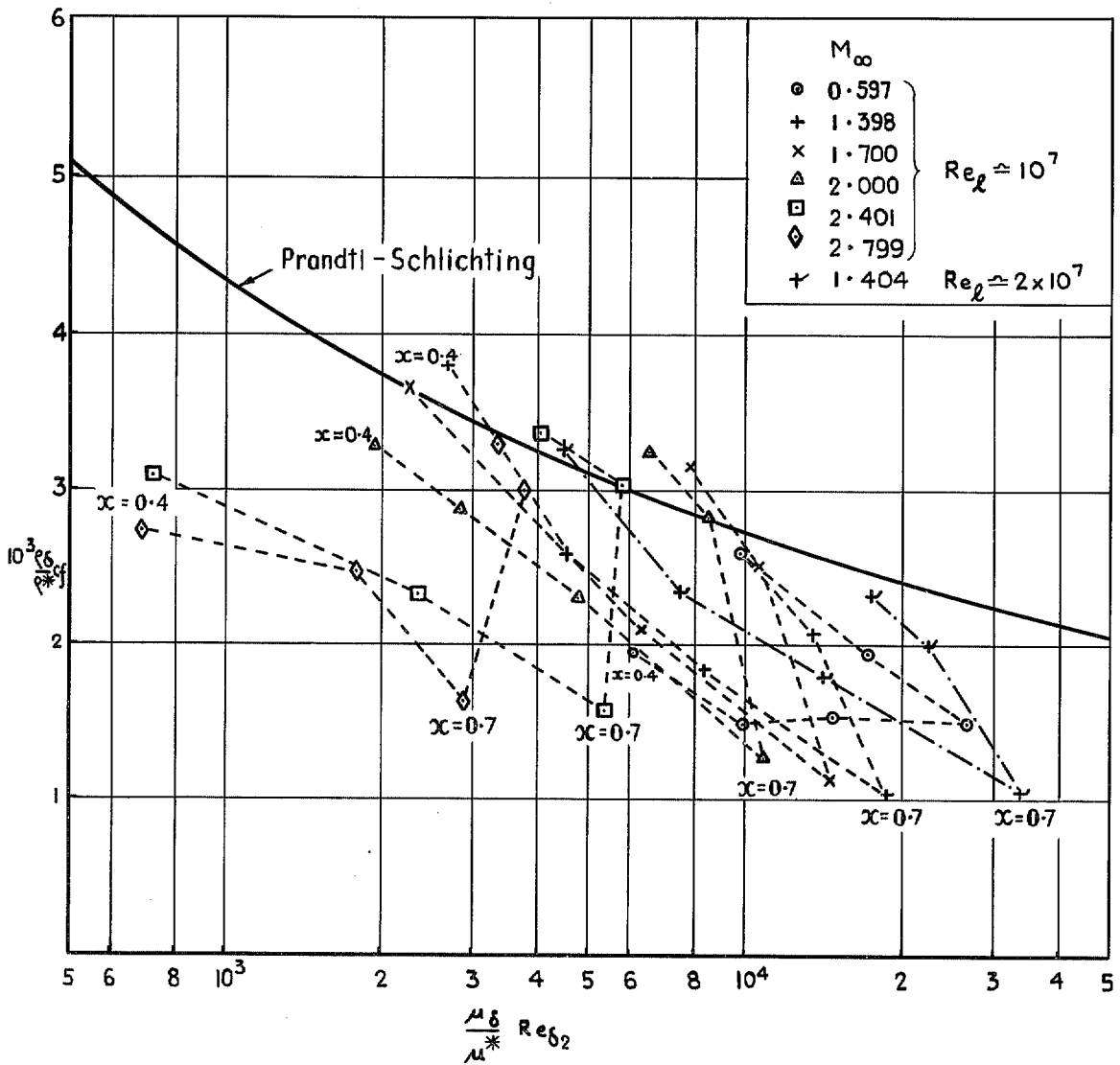


FIG. 6. Local skin friction as a function of momentum thickness Reynolds number in intermediate temperature form.

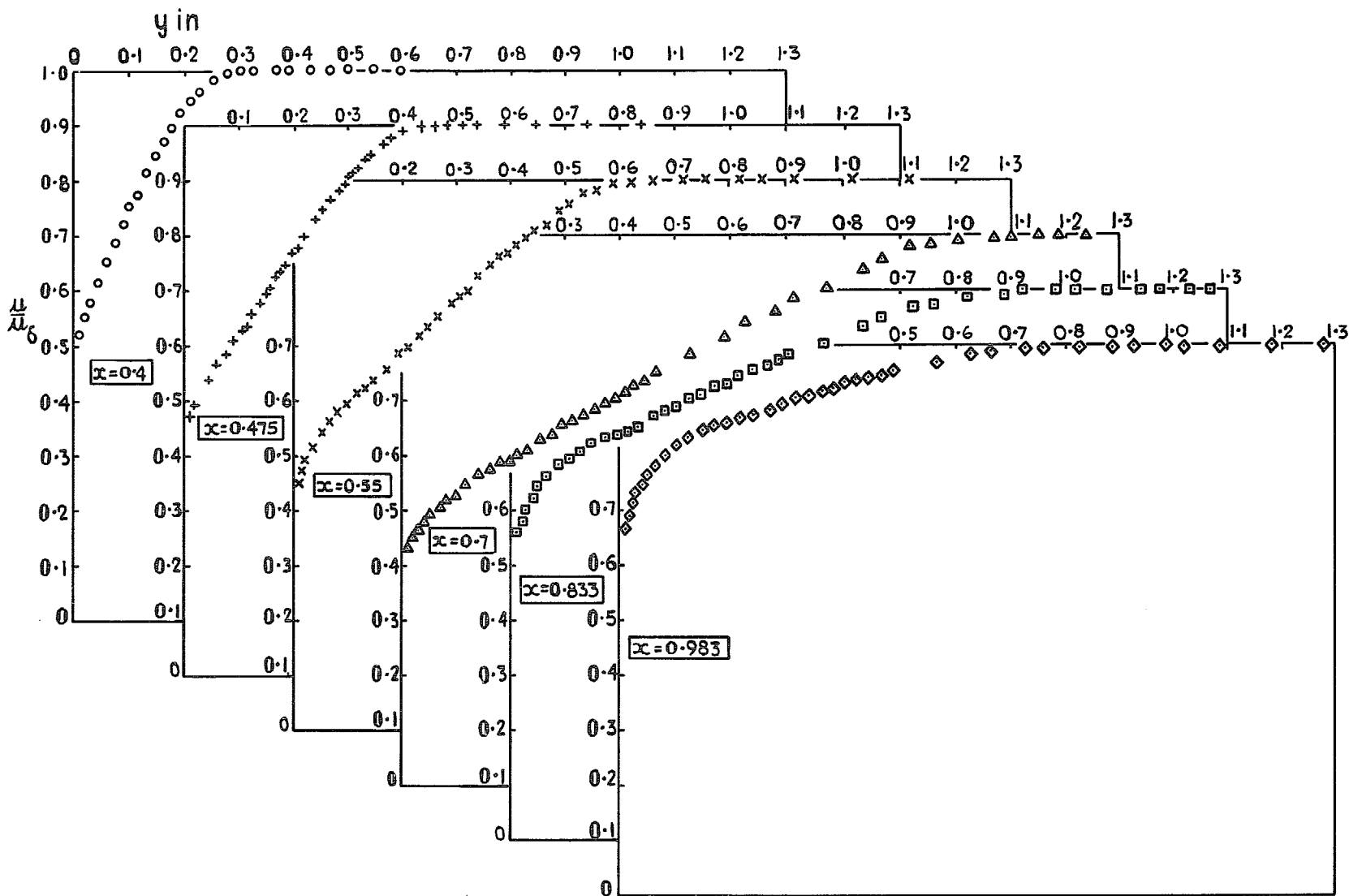
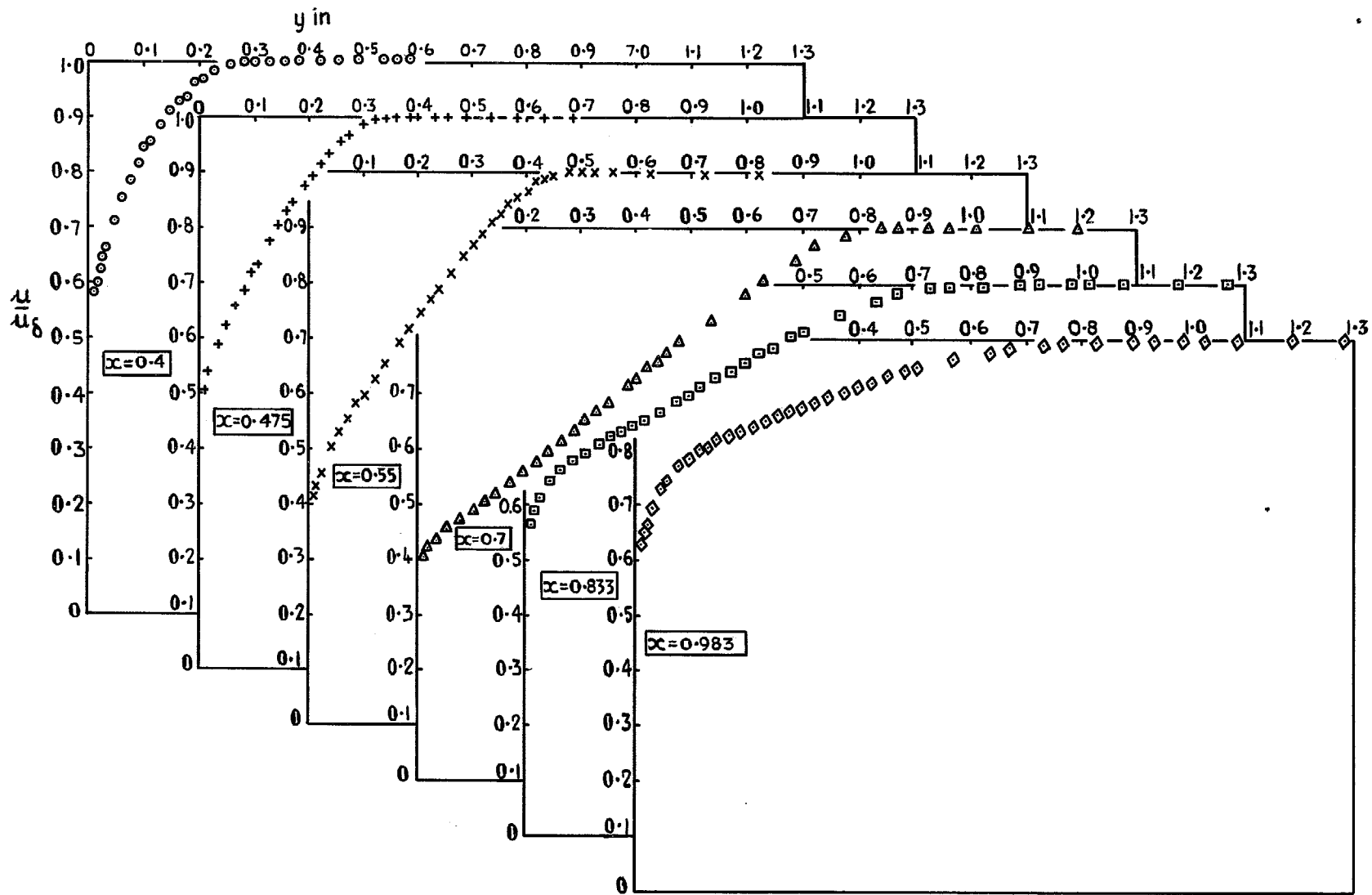


FIG. 7a. Velocity profiles $M_\infty = 0.597$ $Re_t = 9.98 \times 10^6$.



47.

FIG. 7b. Velocity profiles $M_\infty = 1.398$ $Re_t = 10.1 \times 10^6$.

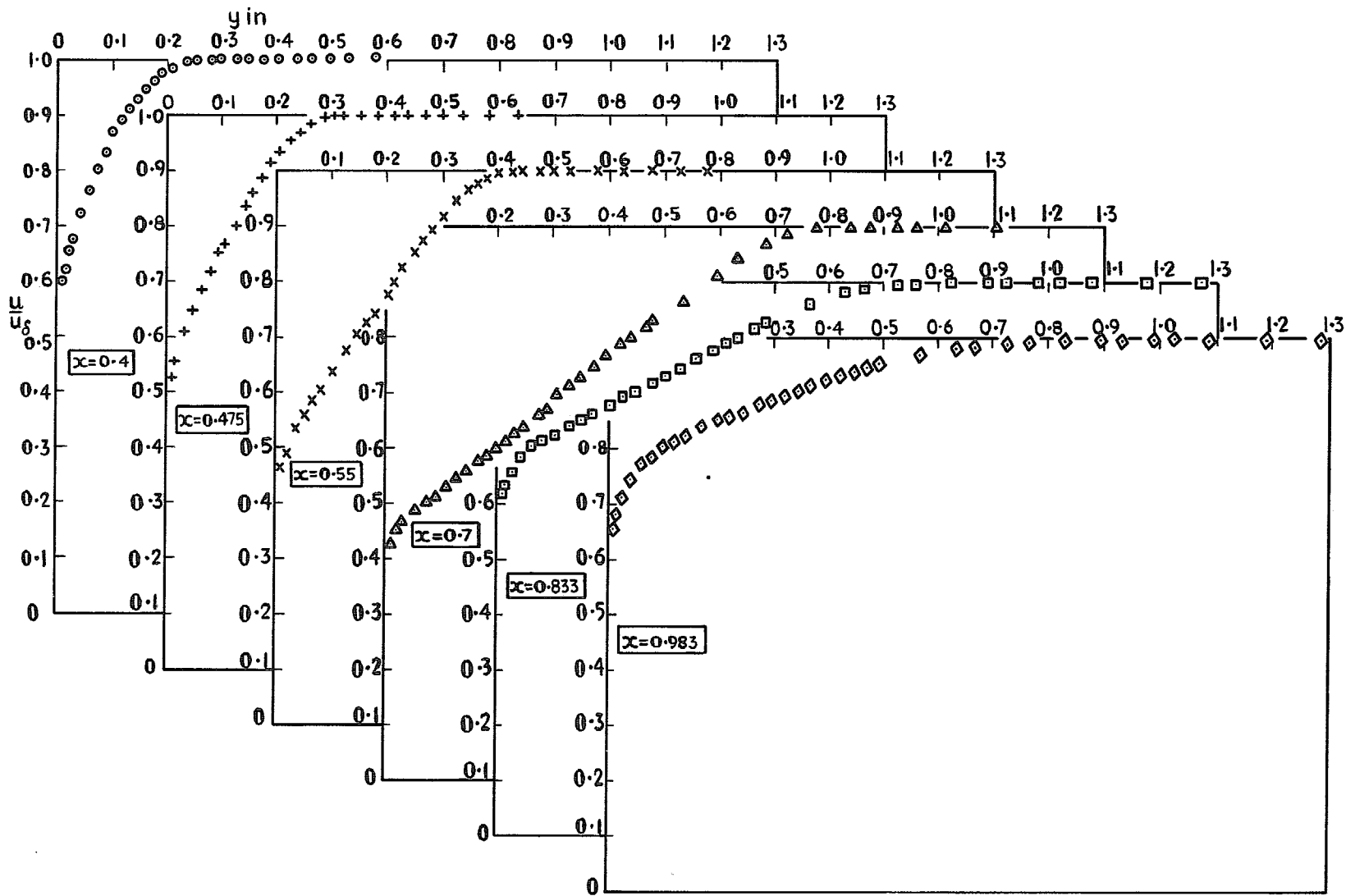


FIG. 7c. Velocity profiles $M_\infty = 1.404$ $Re_l = 19.34 \times 10^6$.

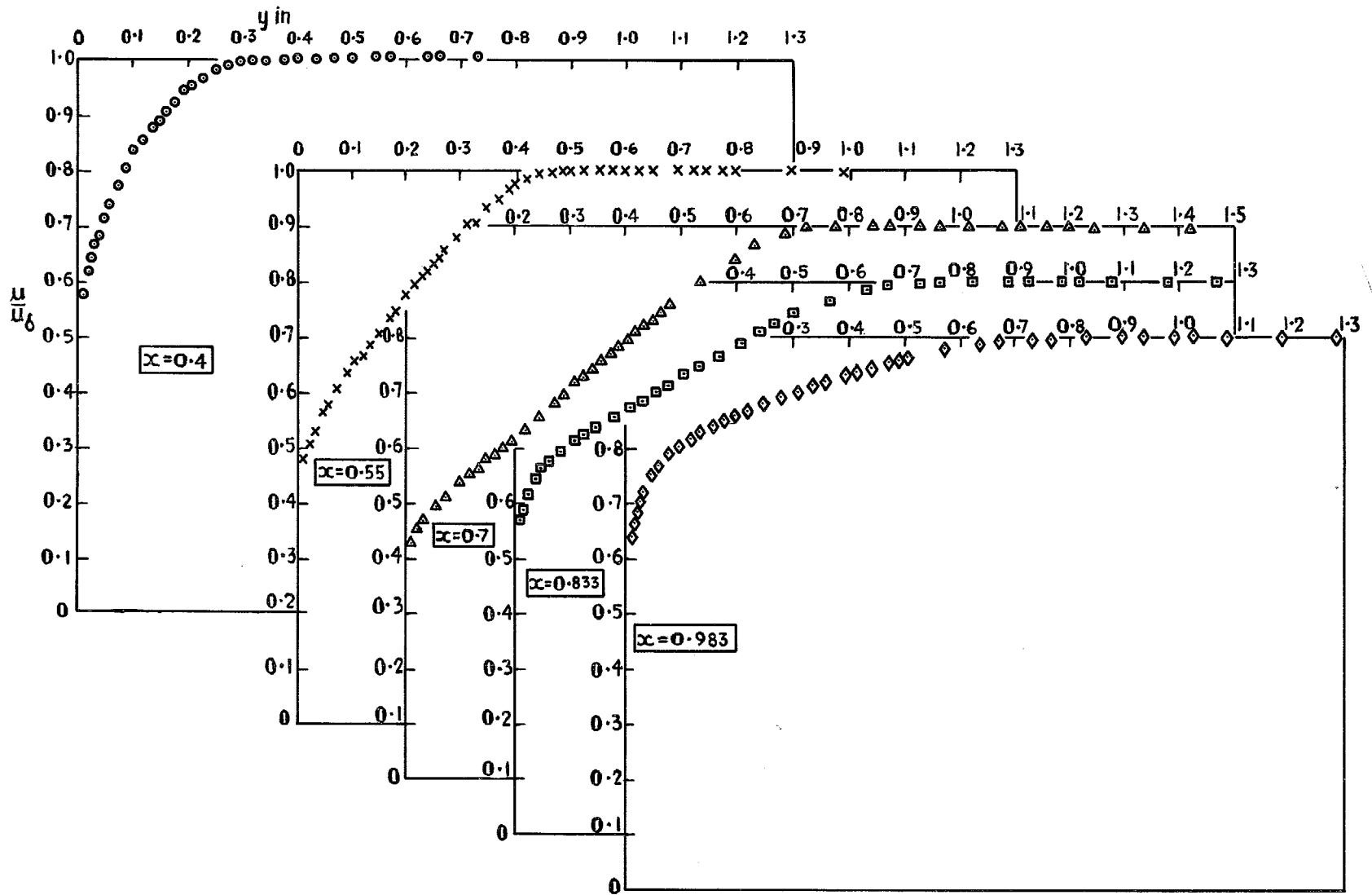


FIG. 7d. Velocity profiles $M_\infty = 1.700$ $Re_l = 10.00 \times 10^6$.

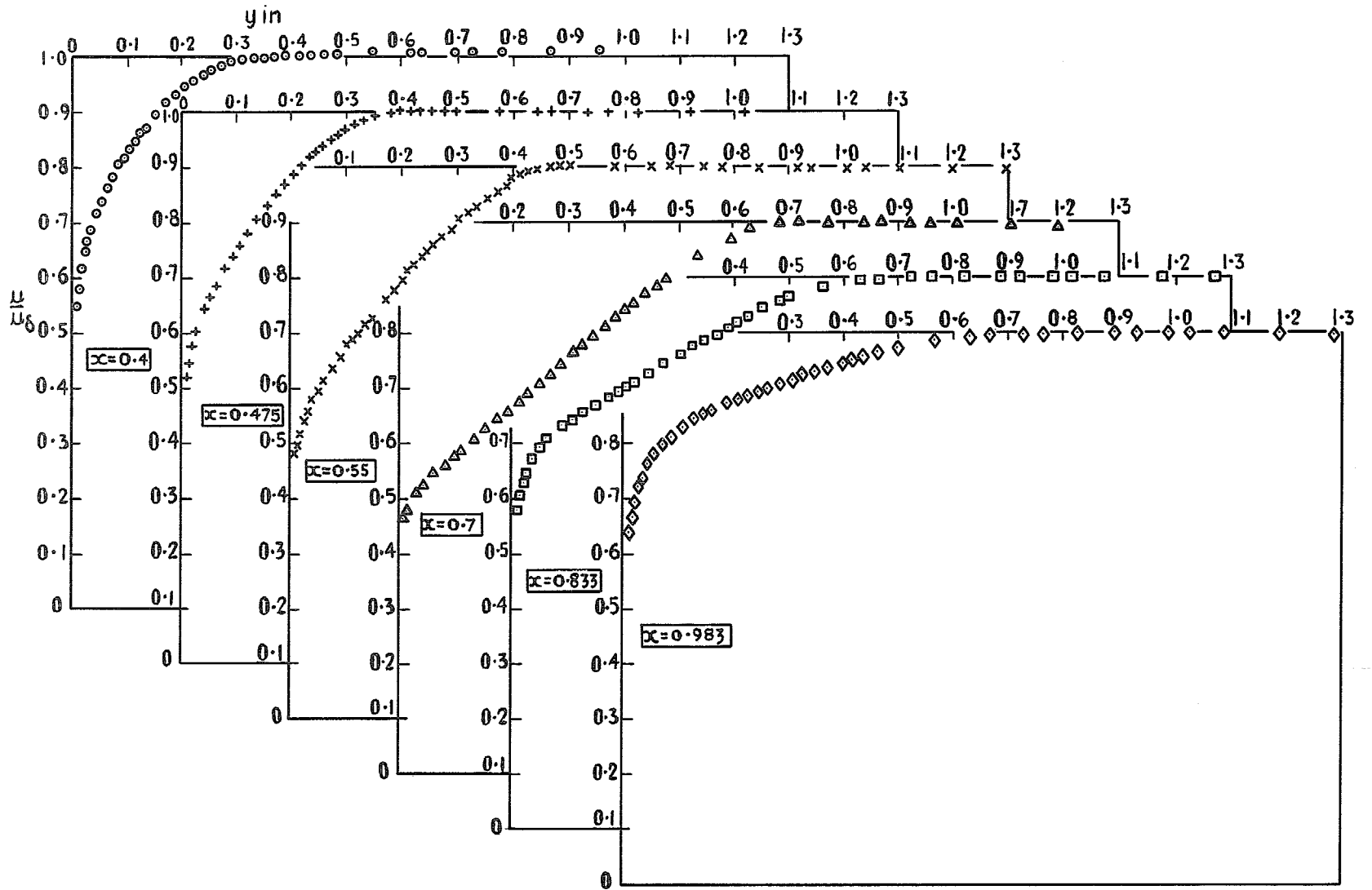


FIG. 7e. Velocity profiles $M_y = 2.001 Re_l = 9.88 \times 10^6$.

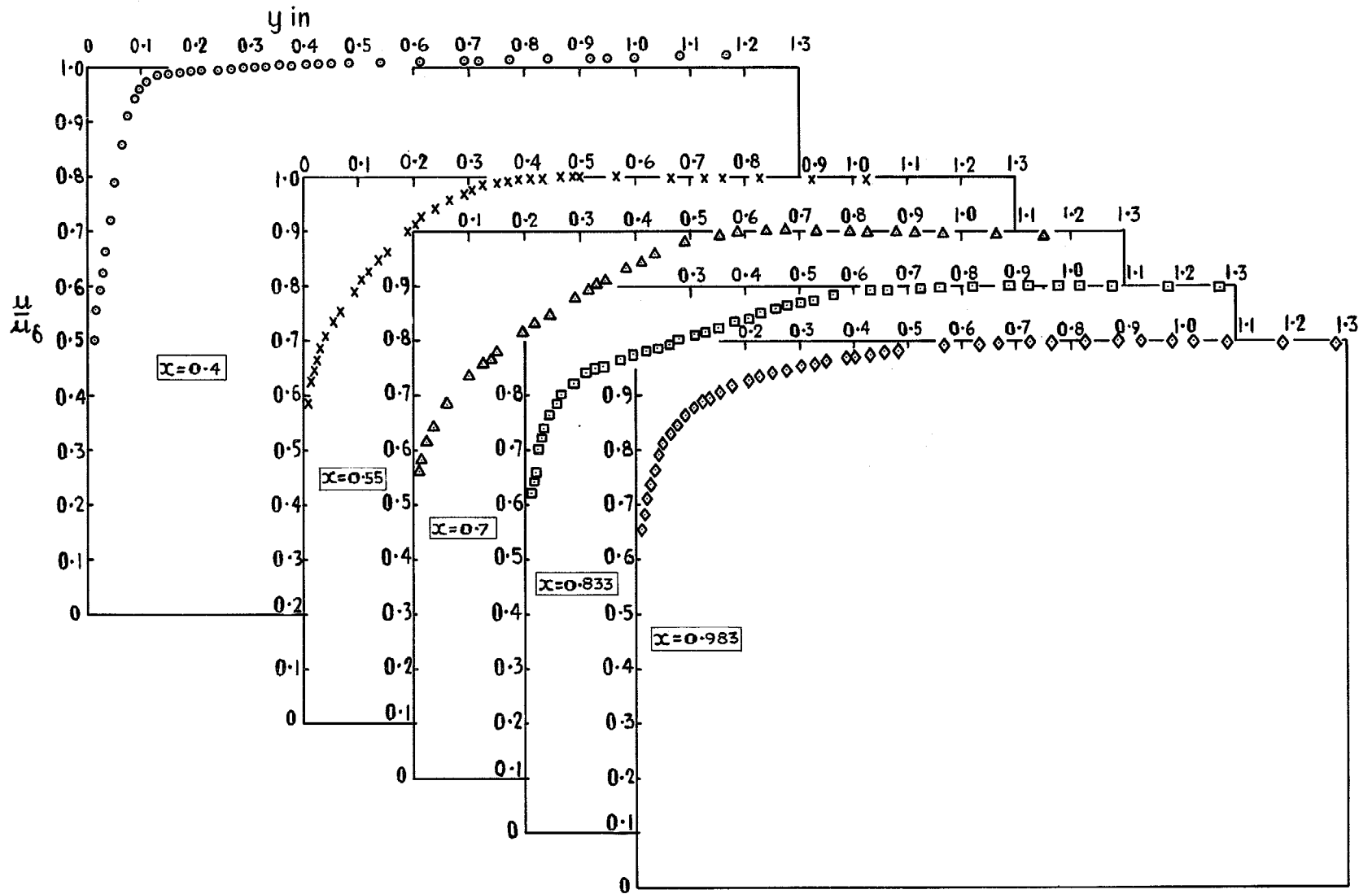


FIG. 7f. Velocity profiles $M_\tau = 2.401$ $Re_l = 9.92 \times 10^6$.

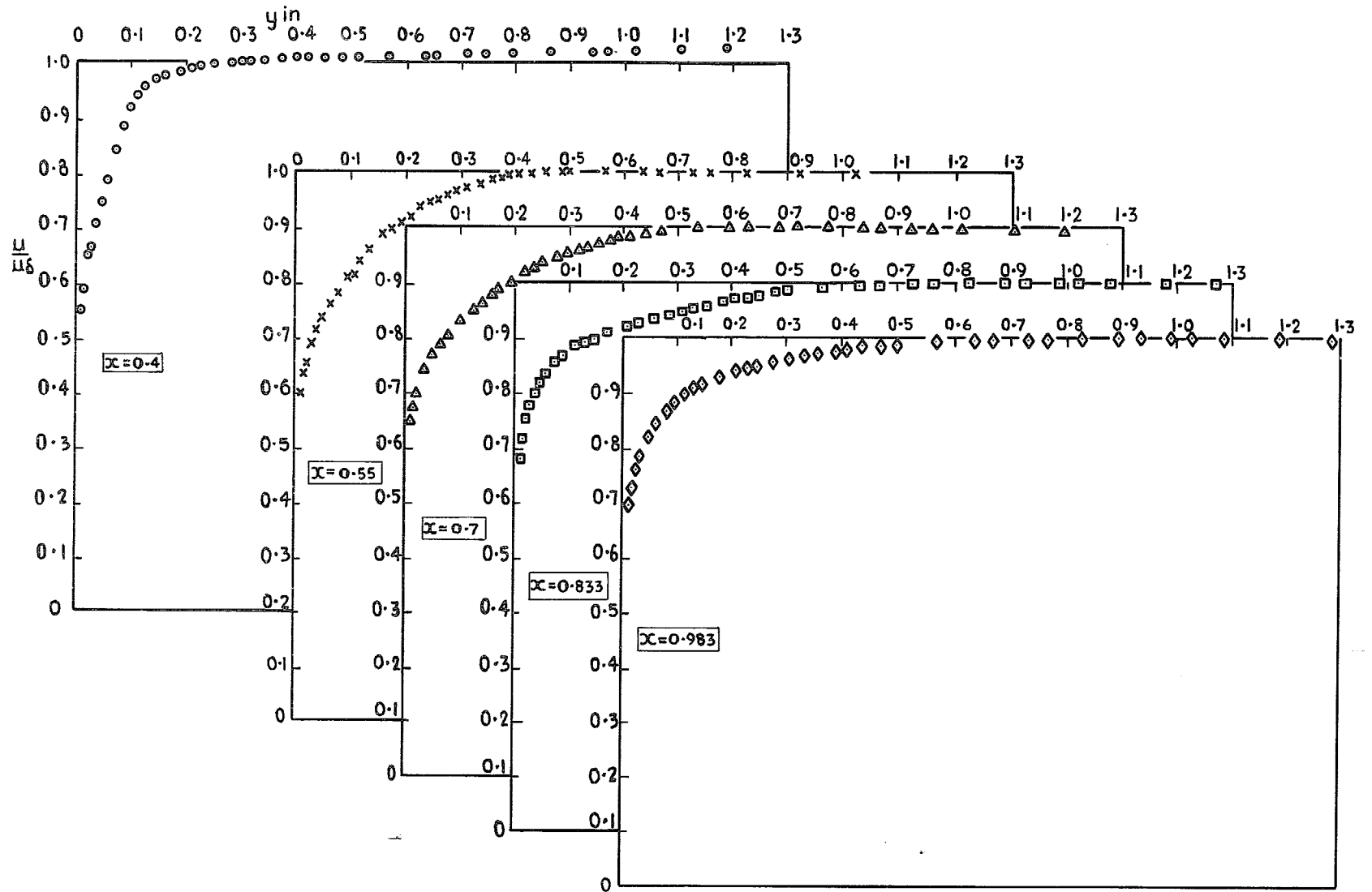
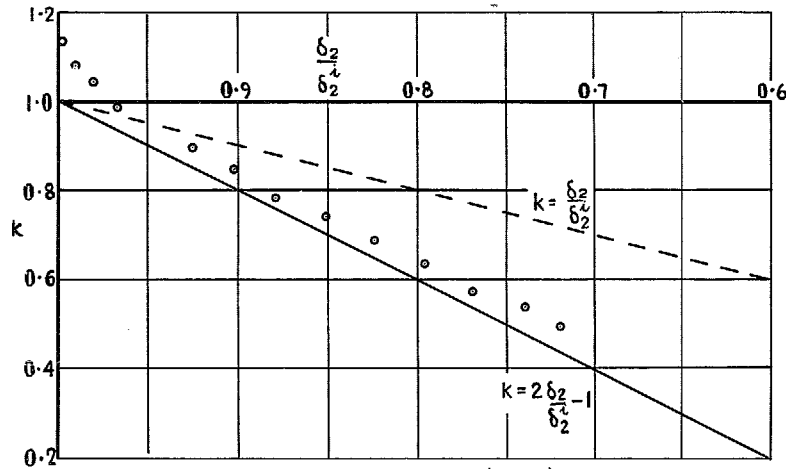
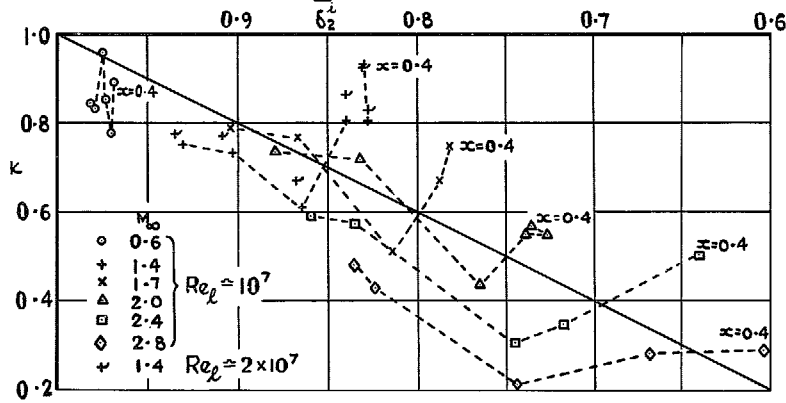


FIG. 7g. Velocity profiles $M_x = 2.798$ $Re_l = 10.10 \times 10^6$.



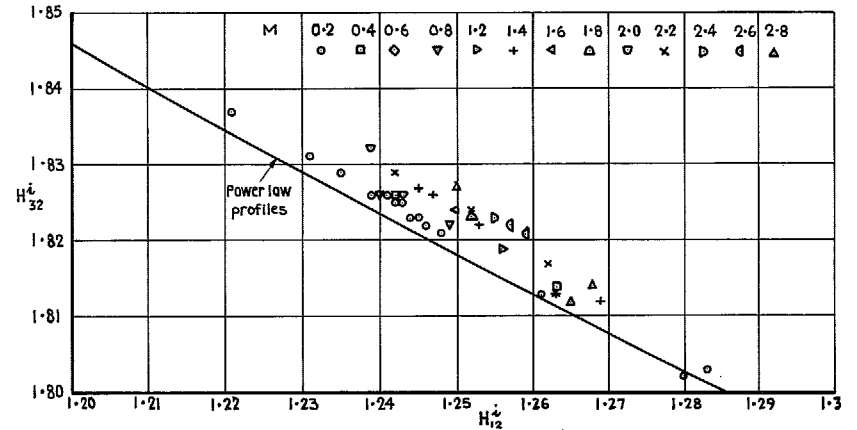
(a) Flat plate results (ref 8)

$$k = \frac{c_f}{0.246 \left(\frac{\rho_0 u_\infty \delta_2}{\mu_w} \right)^{-0.268} 10^{-0.678} H_{12}^+}$$

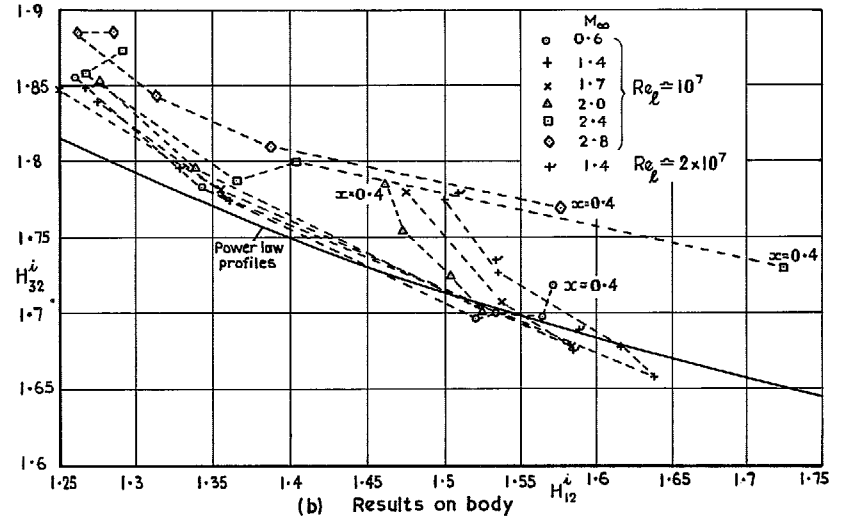


(b) Results on body

FIG. 8 a & b. Compressibility correction to Ludwig-Tillman formula.

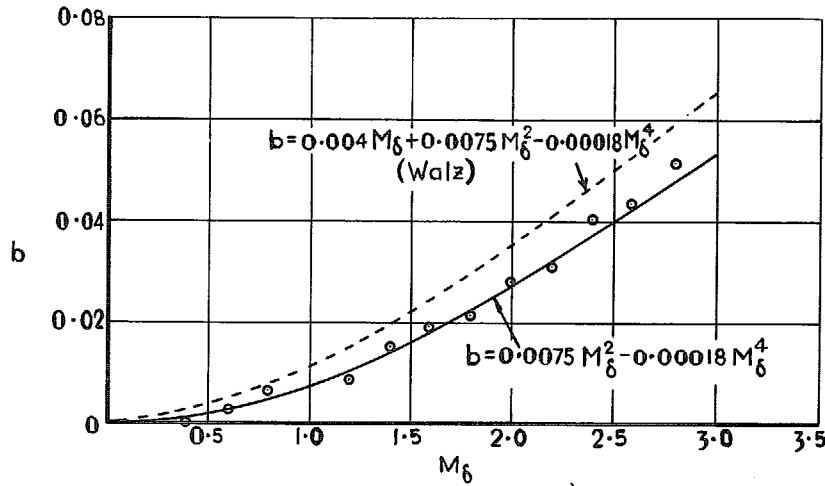


(a) Flat plate results (ref 8)



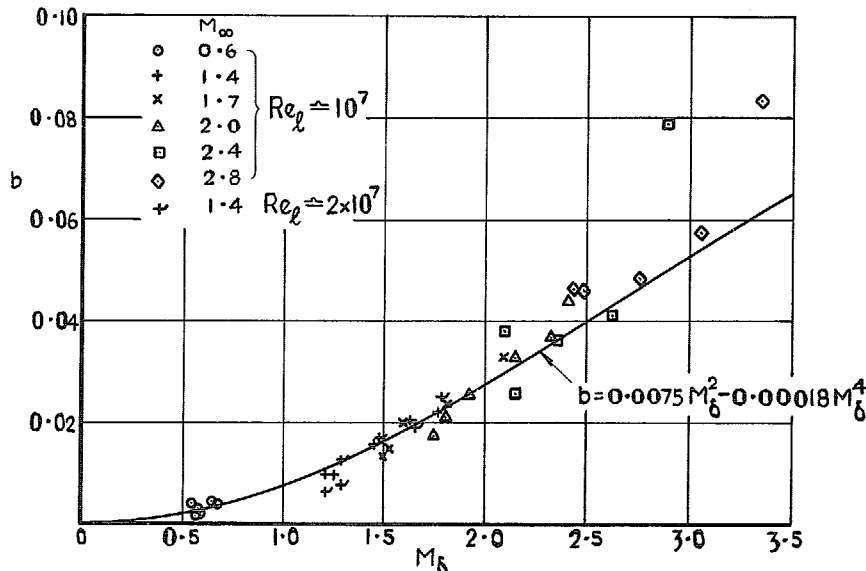
(b) Results on body

FIG. 9 a & b. Relationship between 'incompressible' shape parameters.

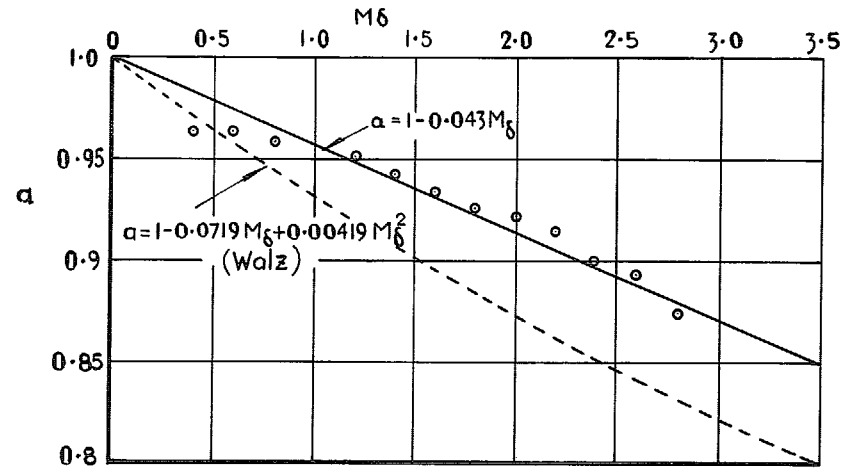


(a) Flat plate results (ref 8)

$$H_{32} = H_{32}^i [1 + (2 - H_{32}^i) b]$$

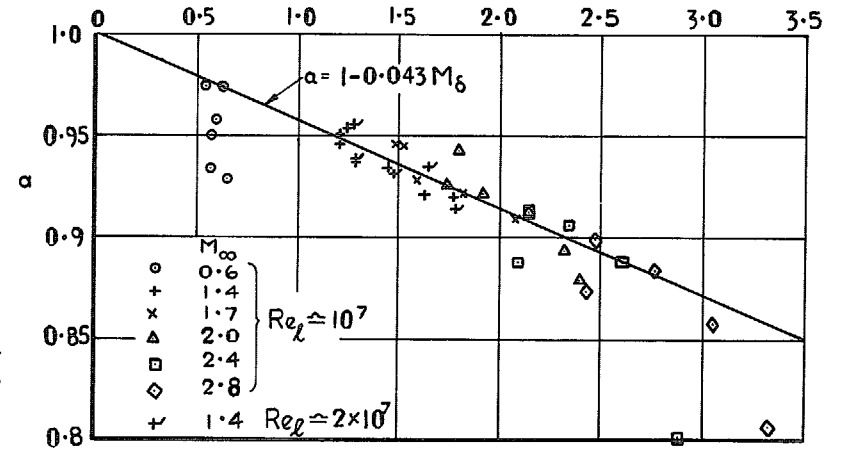


(b) Results on body



(a) Flat plate results (ref 8)

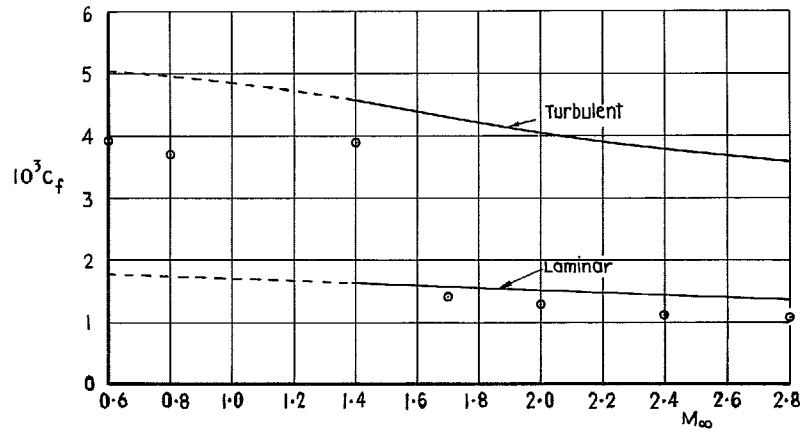
$$\frac{\delta_2^i}{\delta_2} = 1 + \tau \frac{\gamma - 1}{2} M_6^2 H_{32} (2 - H_{32}^i) a$$



(b) Results on body

FIG. 10 a & b. Relationship between H_{32} and H_{32}^i .

FIG. 11 a & b. Determination of $\frac{\delta_2^i}{\delta_2}$.



(a) $x = 0.05$ $Re_x = 10^7$

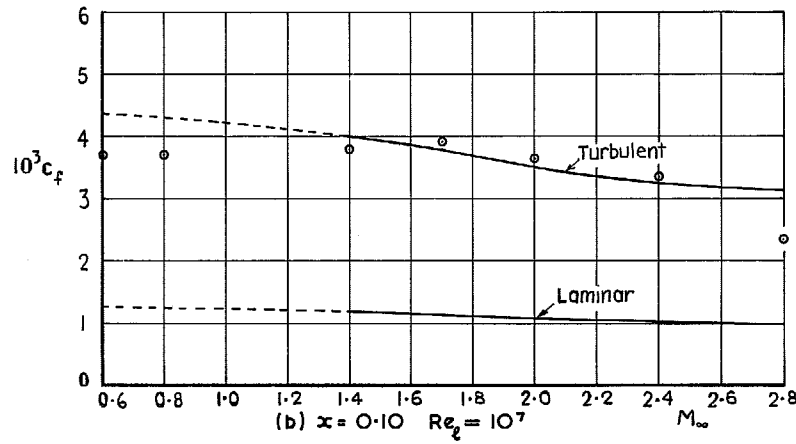


FIG. 12 a & b. Skin friction on conical nose.

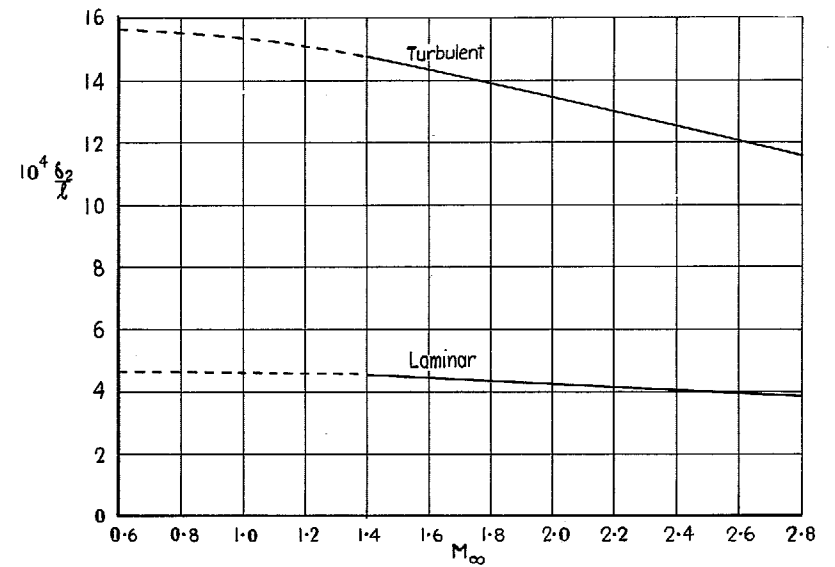


FIG. 13. Calculated momentum thickness
 $x = 0.1416$ $Re_x = 10^7$.

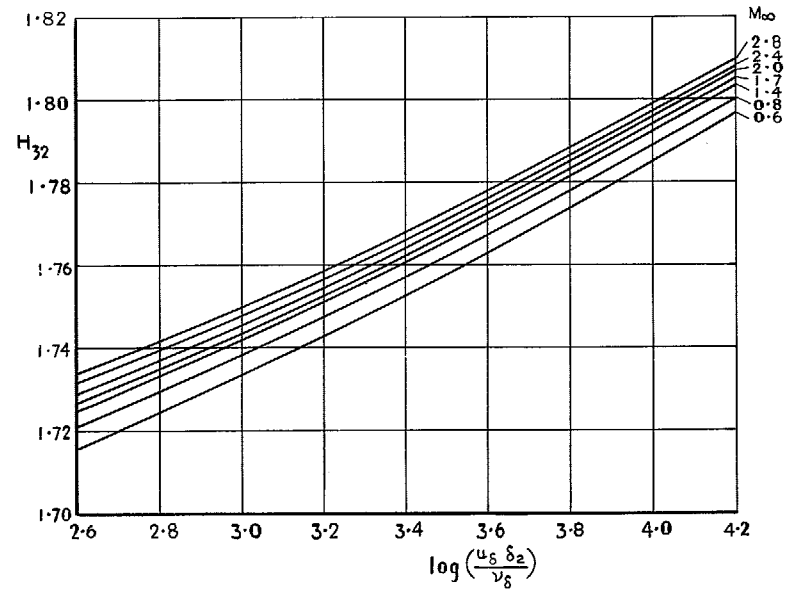


FIG. 14. Chart for determination of H_{32} at
 $x = 0.1416$.

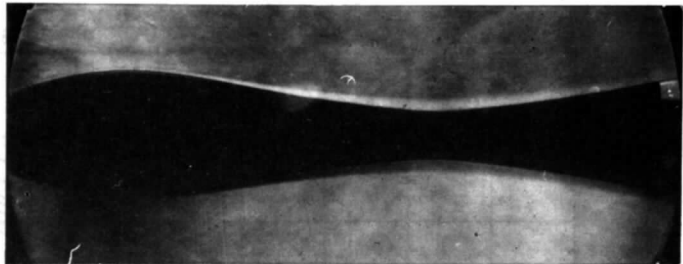
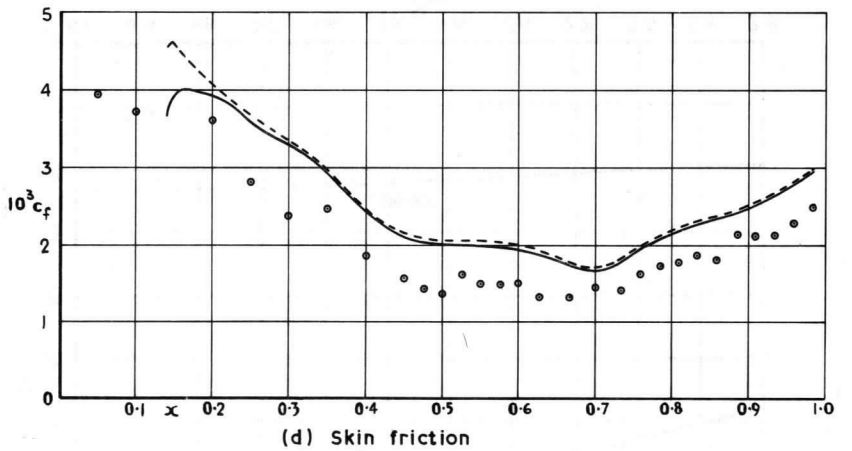
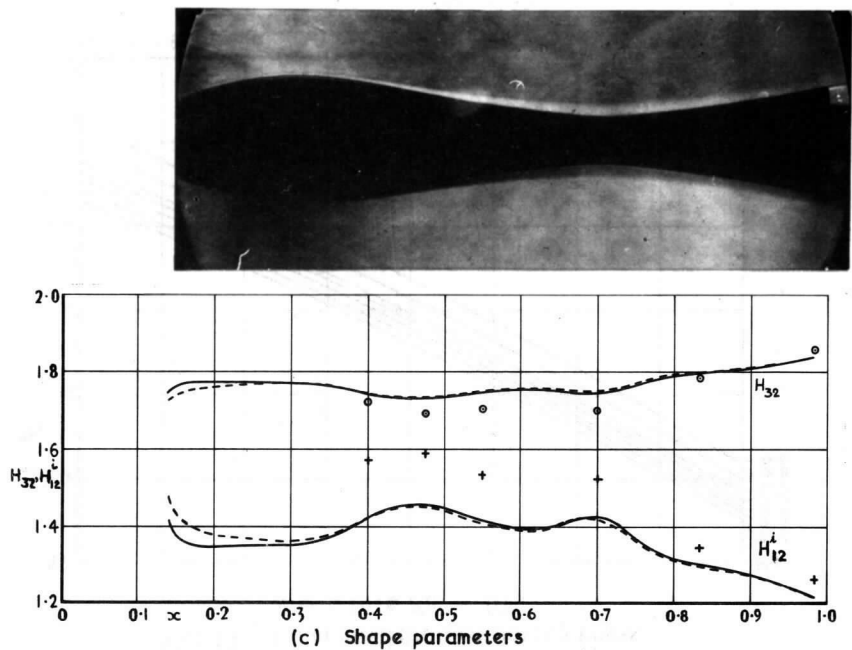
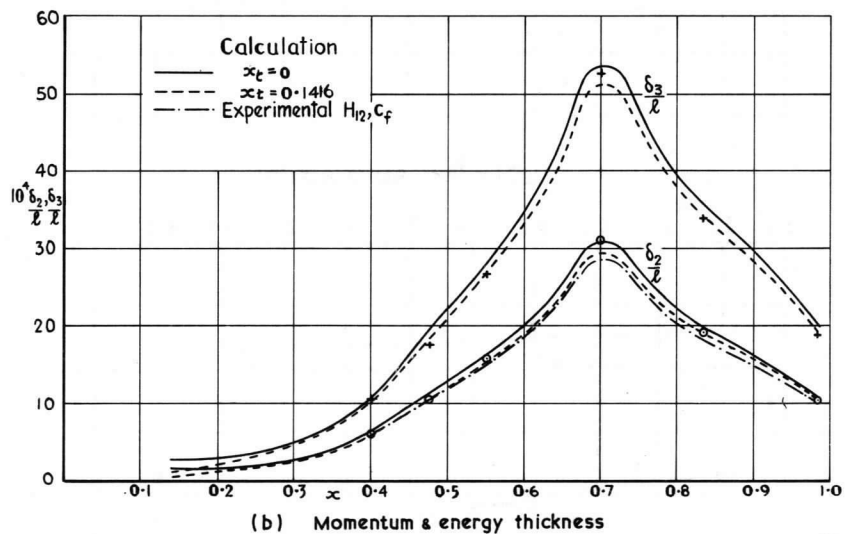
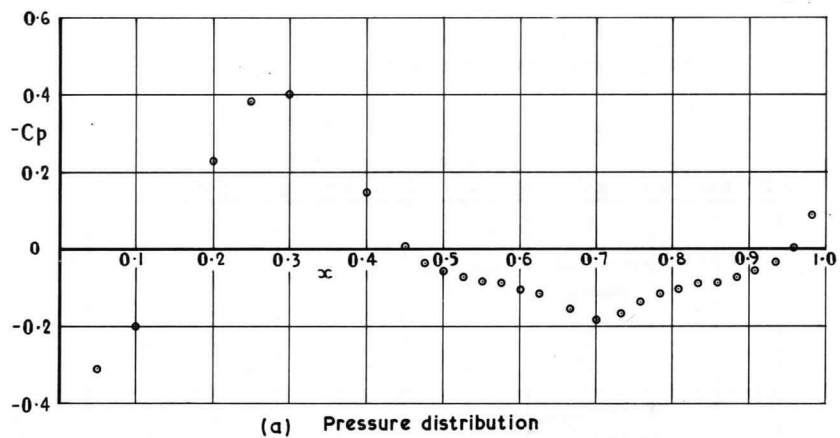
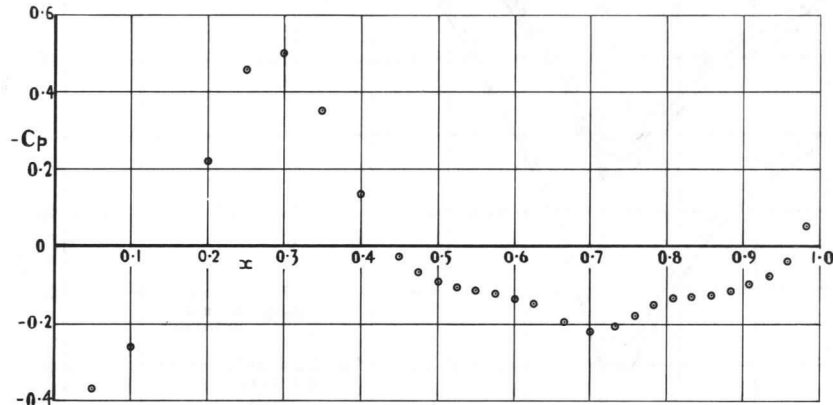
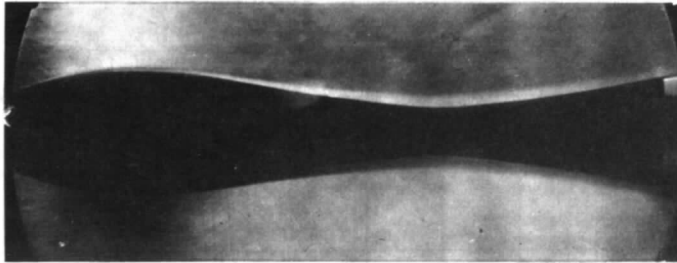
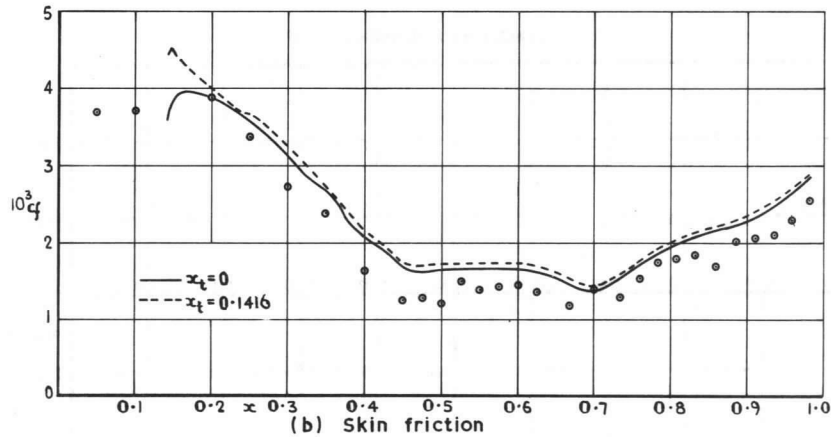


FIG. 15. Comparison of calculation and experiment $M_\infty = 0.597$ $Re_l \approx 10^7$.

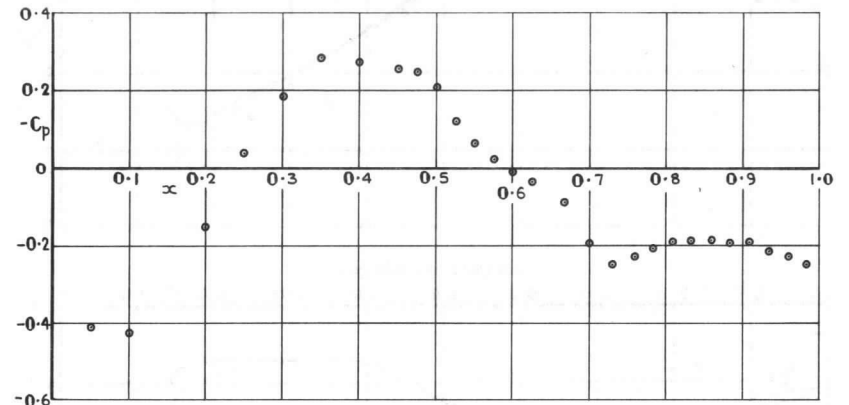
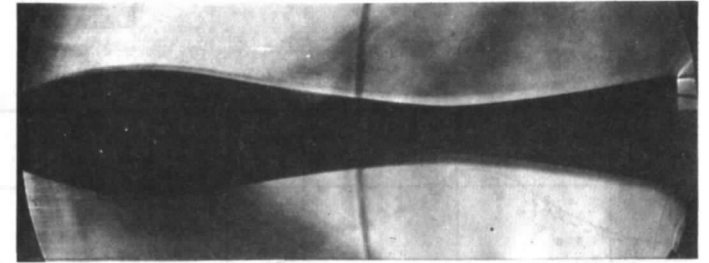


(a) Pressure coefficient

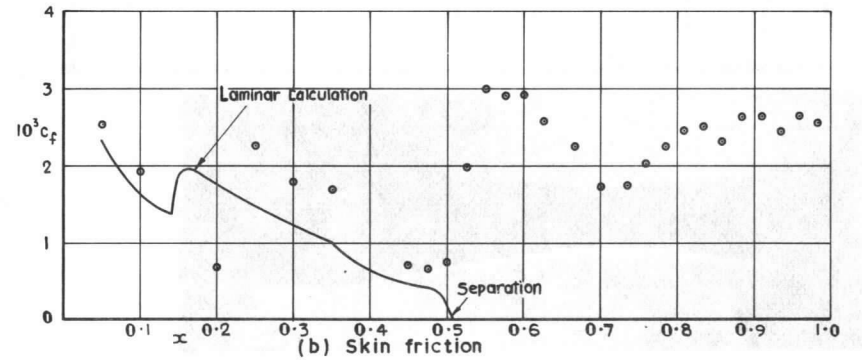


(b) Skin friction

FIG. 16 a & b. Comparison of experiment and calculation $M_\infty = 0.801$ $Re_l \approx 10^7$.

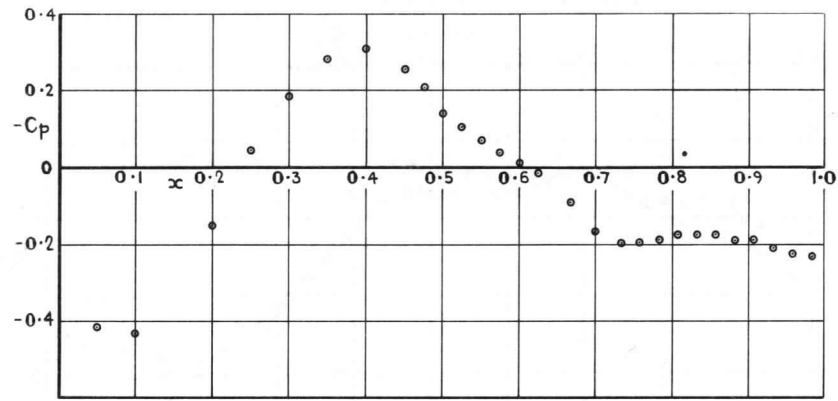


(a) Pressure coefficient

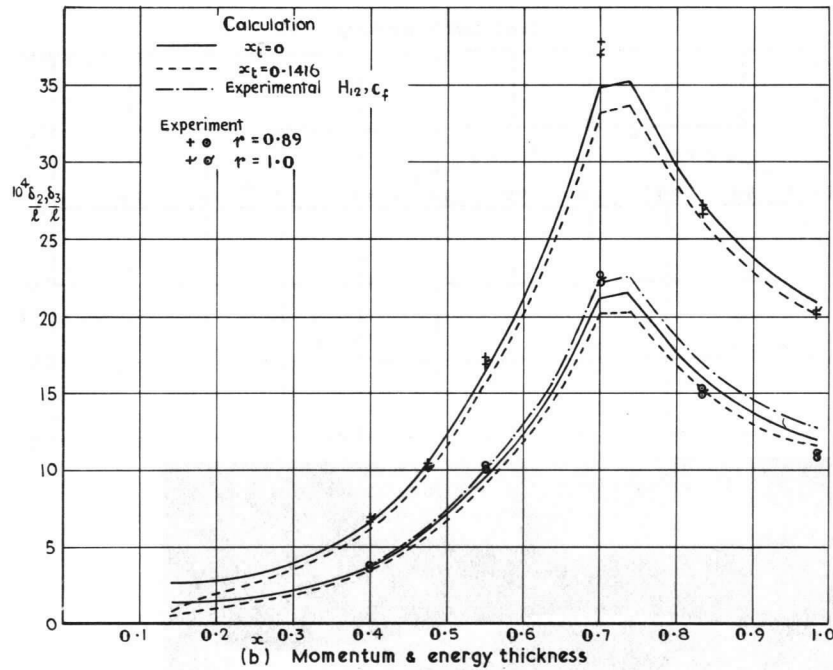


(b) Skin friction

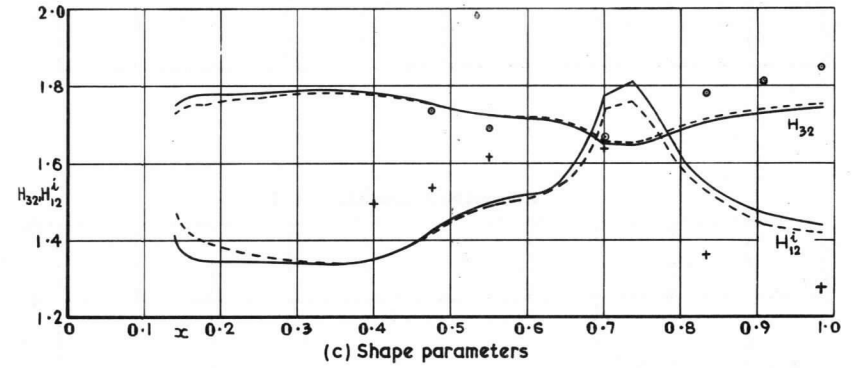
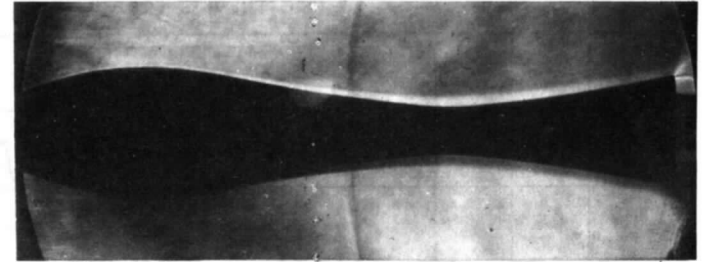
FIG. 17 a & b. Comparison of experiment and calculation $M_\infty = 1.390$ $Re_l \approx 5 \times 10^6$.



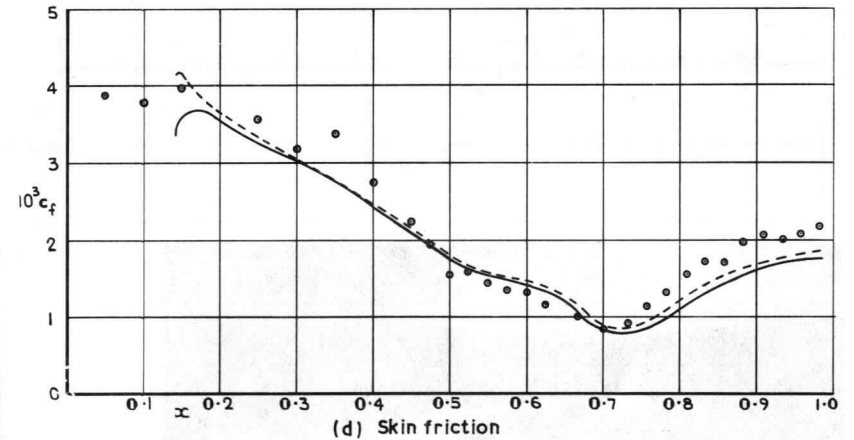
(a) Pressure coefficient



(b) Momentum & energy thickness

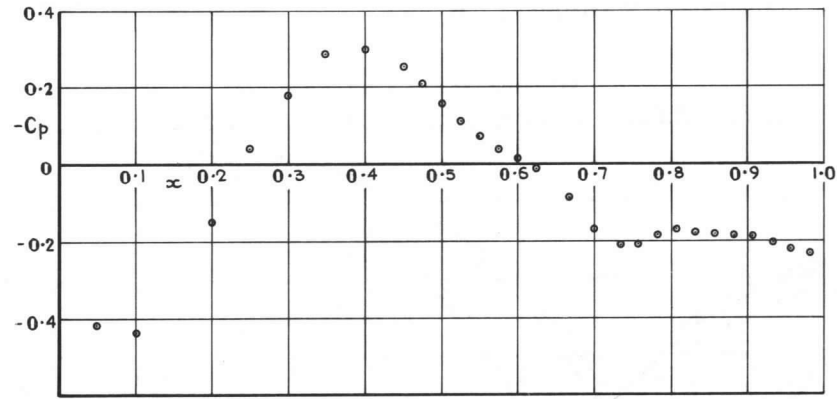


(c) Shape parameters

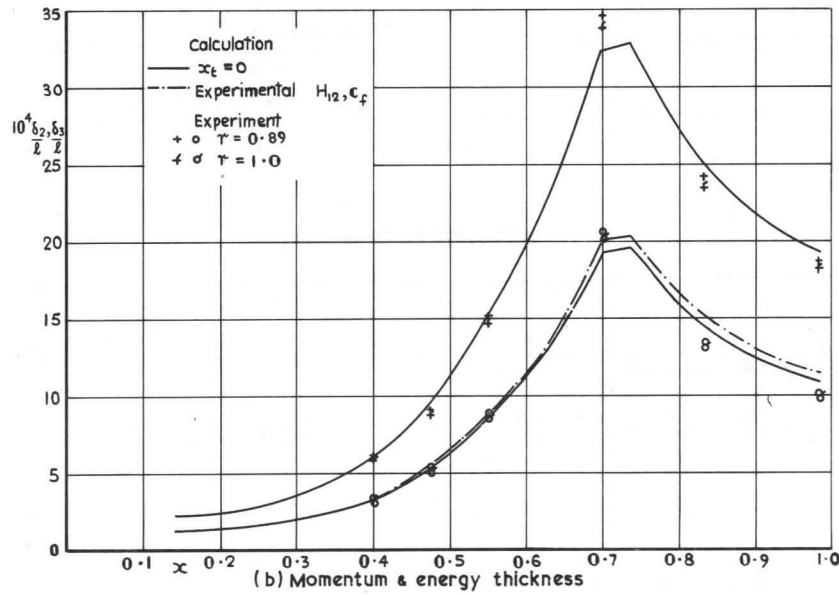


(d) Skin friction

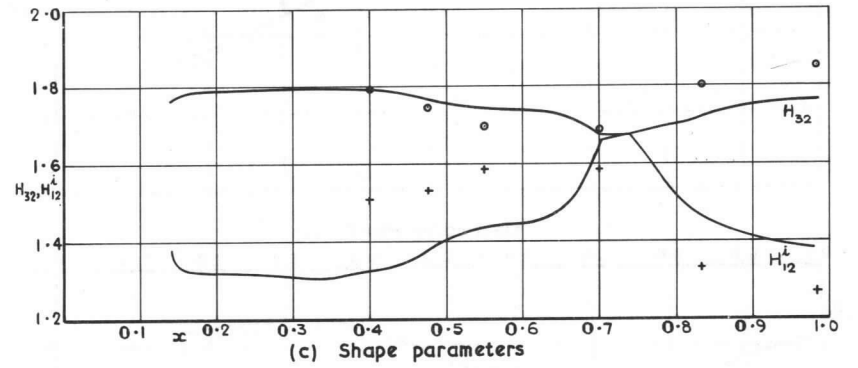
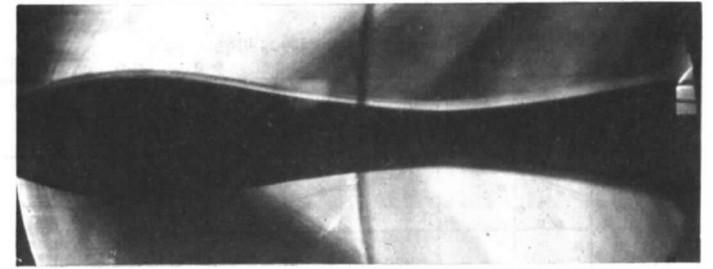
FIG. 18. Comparison of experiment and calculation $M_\infty = 1.398 Re_l \approx 10^7$.



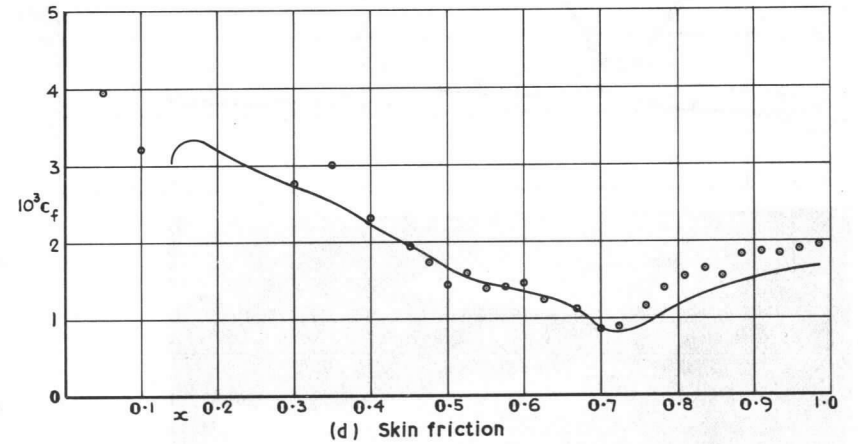
(a) Pressure coefficient



(b) Momentum & energy thickness

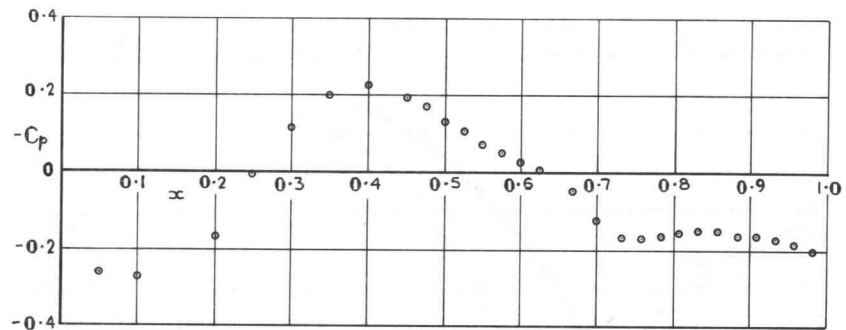


(c) Shape parameters

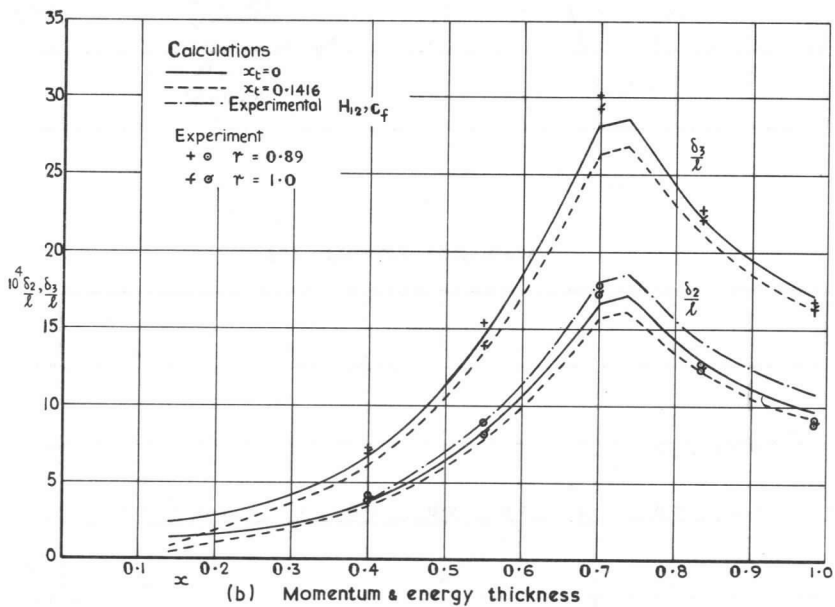


(d) Skin friction

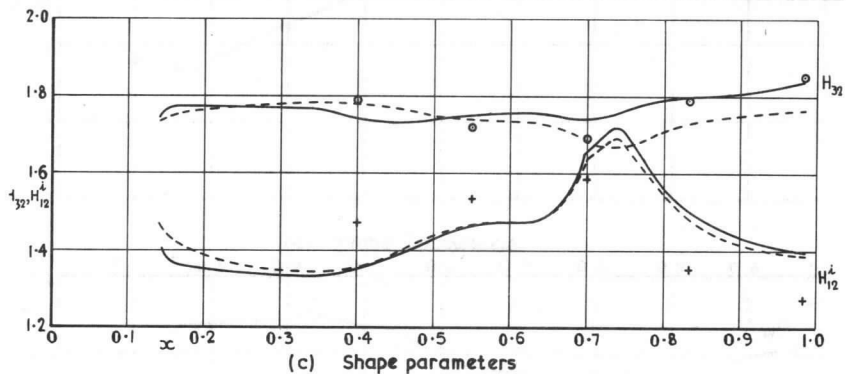
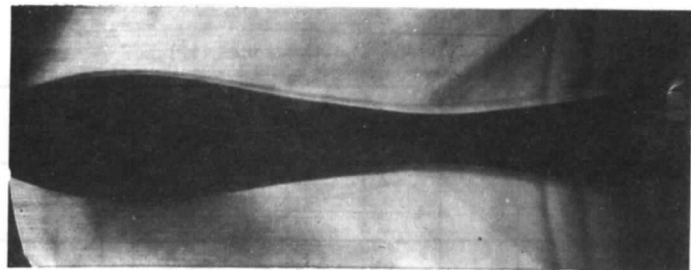
FIG. 19. Comparison of calculation and experiment $M_\infty = 1.404 Re_l \approx 2 \times 10^7$.



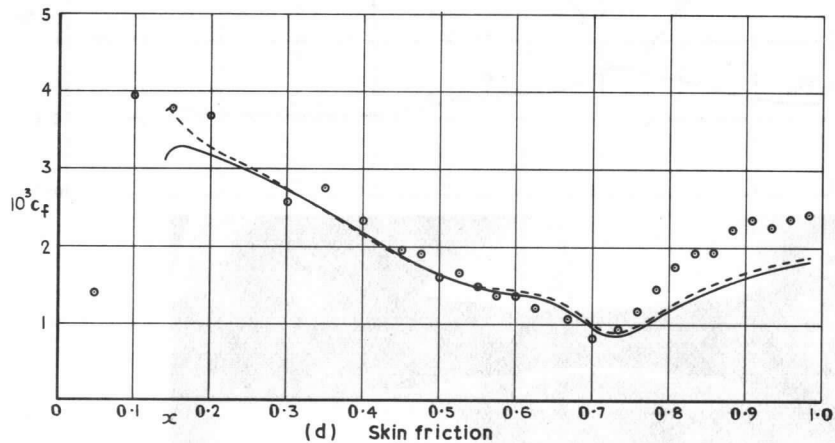
(a) Pressure coefficient



(b) Momentum & energy thickness

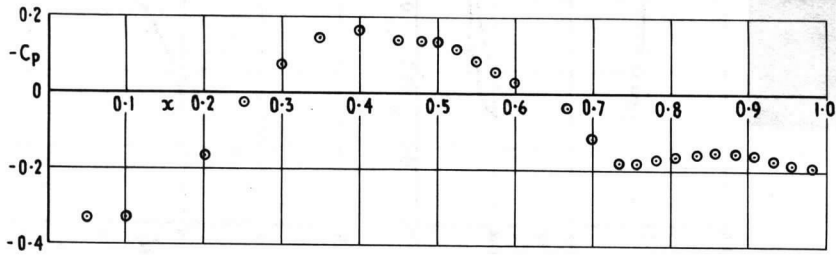
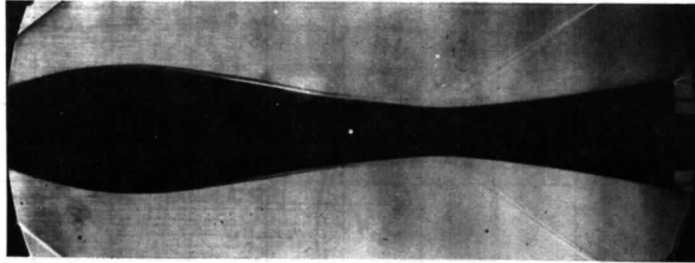


(c) Shape parameters

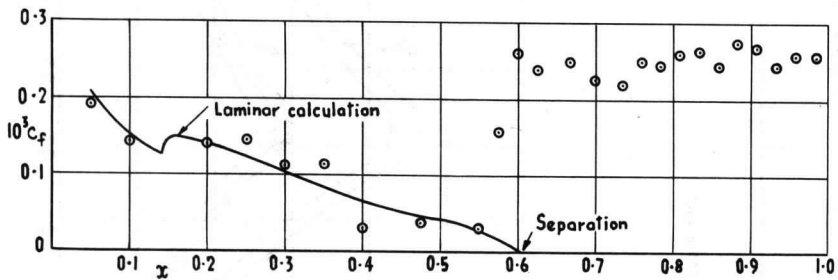


(d) Skin friction

FIG. 20. Comparison of calculation and experiment $M_\infty = 1.700$ $Re_l \approx 10^7$.

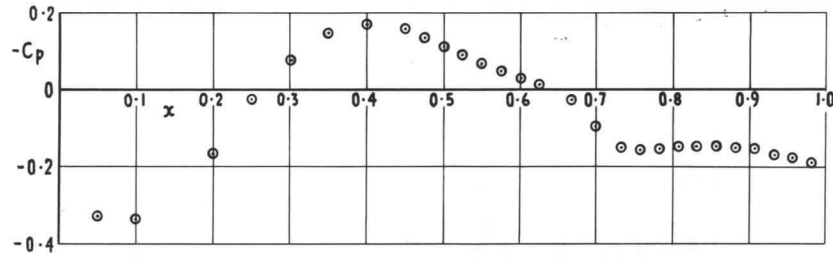


(a) Pressure coefficient

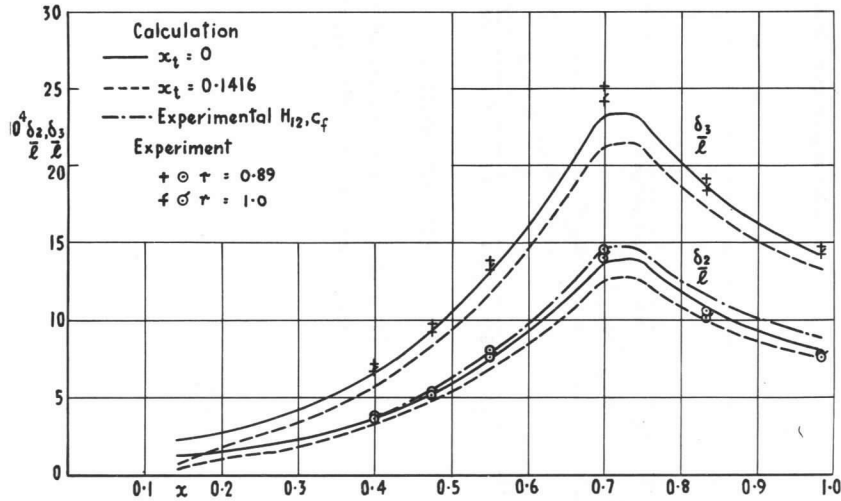


(b) Skin friction

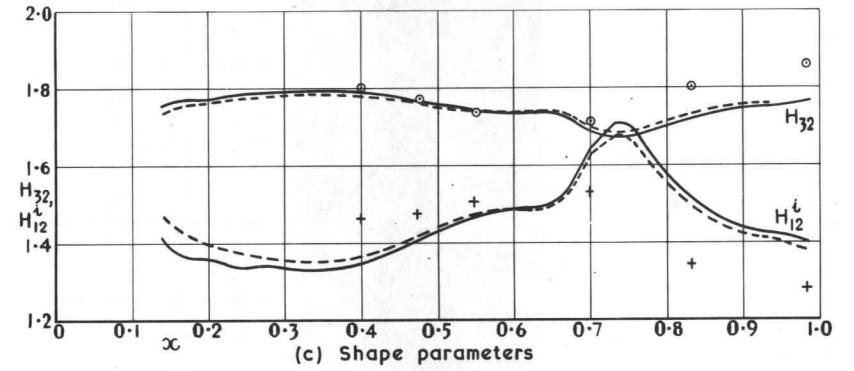
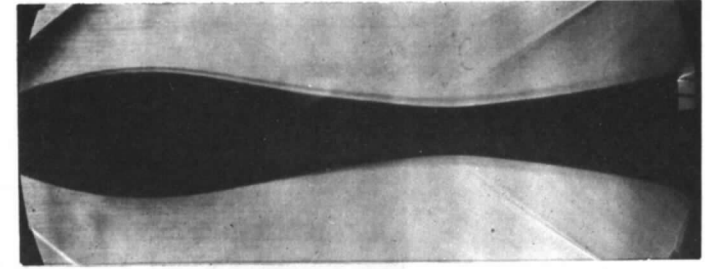
FIG. 21 a & b. Comparison of calculation and experiment $M_\infty = 1.996$ $Re_l \approx 5 \times 10^6$.



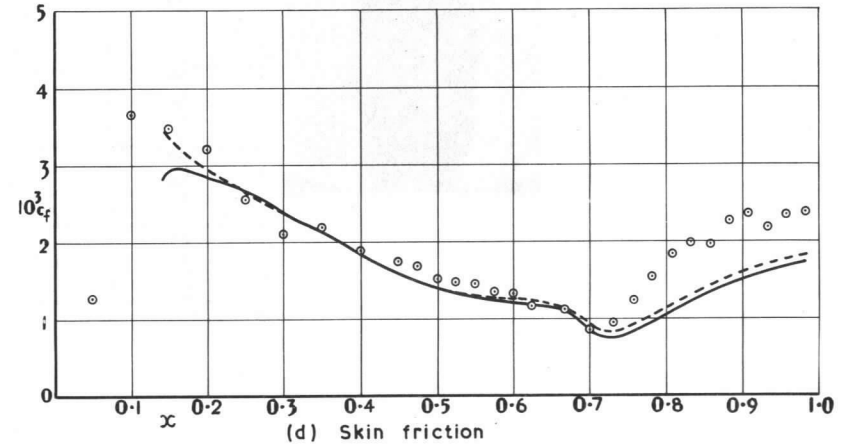
(a) Pressure coefficient



(b) Momentum & energy thickness

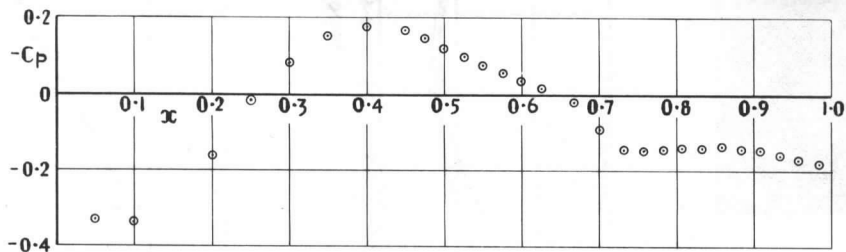
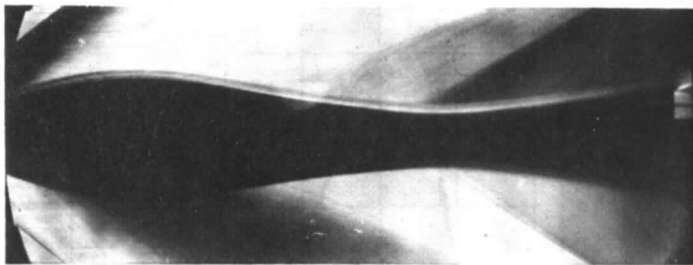


(c) Shape parameters

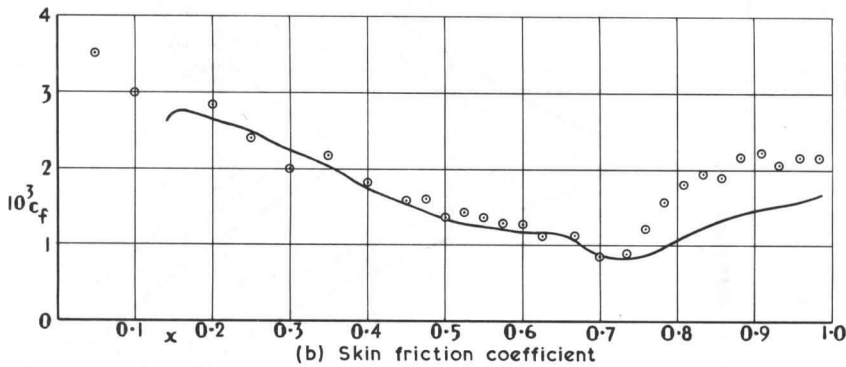


(d) Skin friction

FIG. 22. Comparison of calculation and experiment $M_\infty = 2.000$ $Re_l \approx 10^7$.

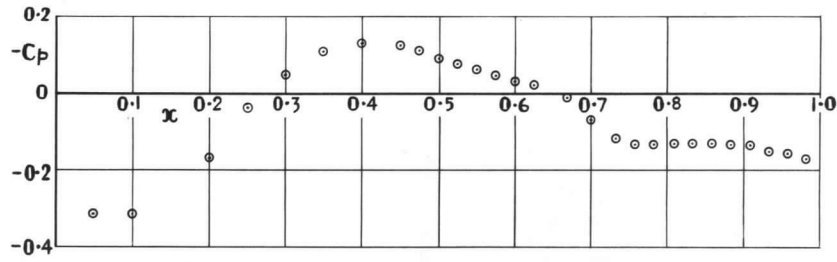


(a) Pressure coefficient

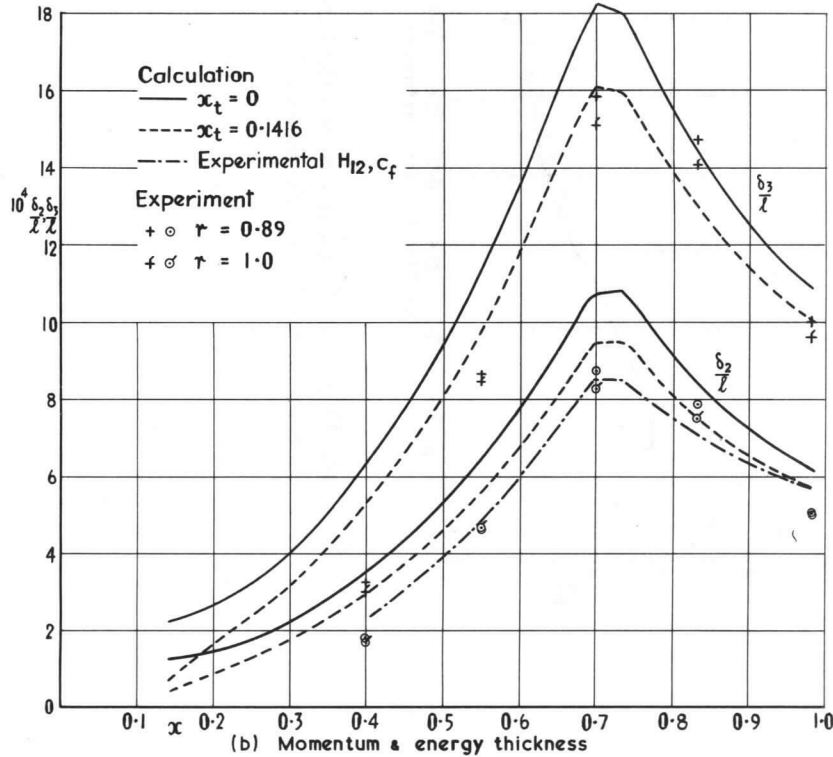
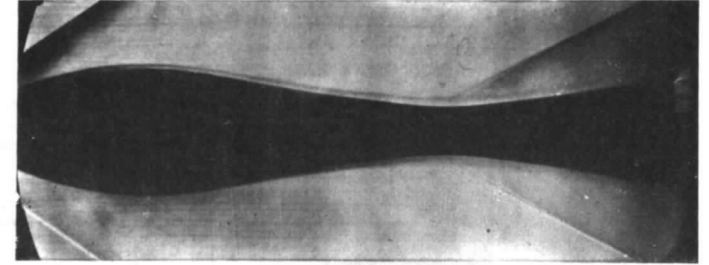


(b) Skin friction coefficient

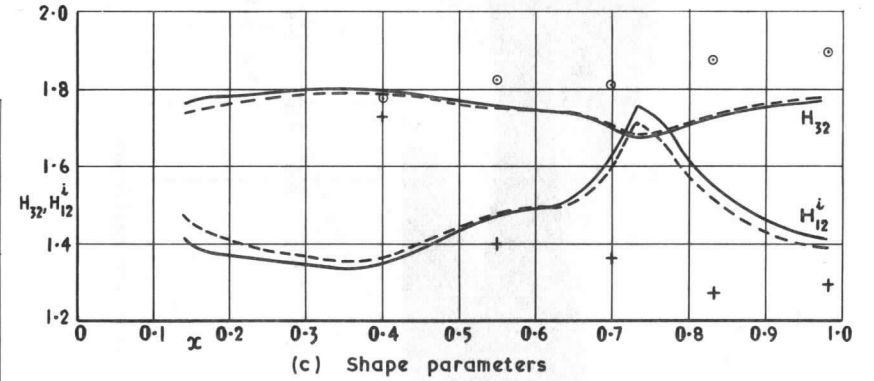
FIG. 23 a & b. Comparison of calculation and experiment $M_\infty = 2.002$ $Re_l \approx 1.7 \times 10^7$.



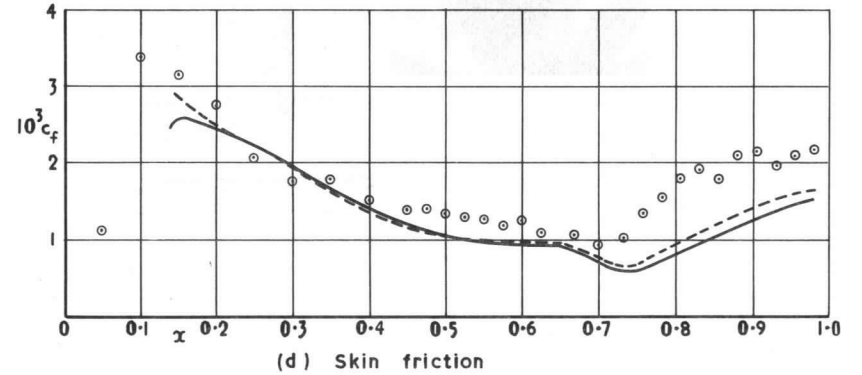
(a) Pressure coefficient



(b) Momentum & energy thickness

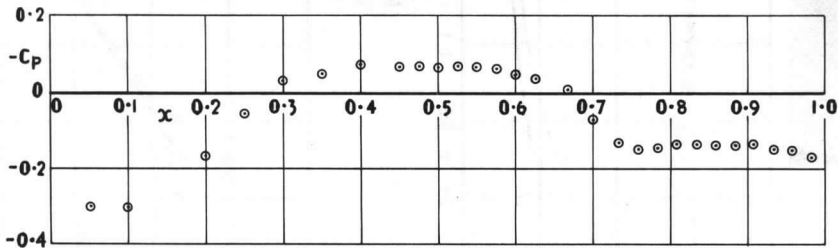
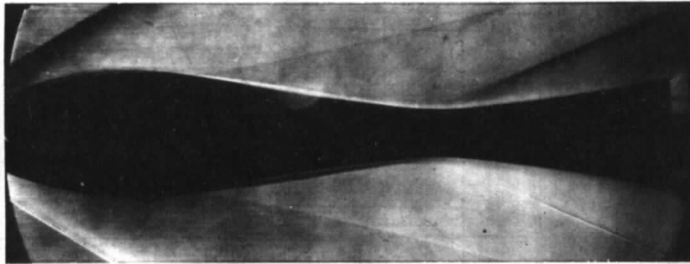


(c) Shape parameters

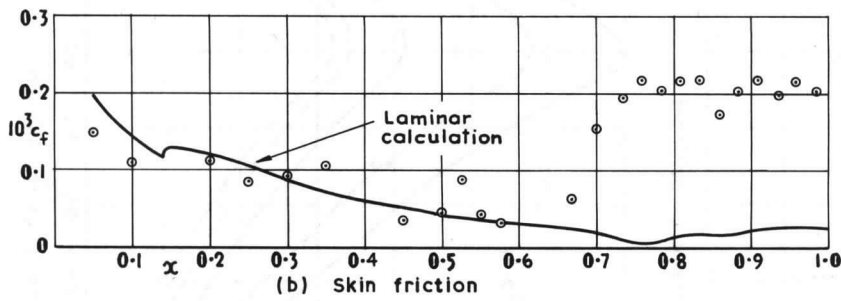


(d) Skin friction

FIG. 24. Comparison of calculation and experiment $M_\infty = 2.401$ $Re_l \approx 10^7$.

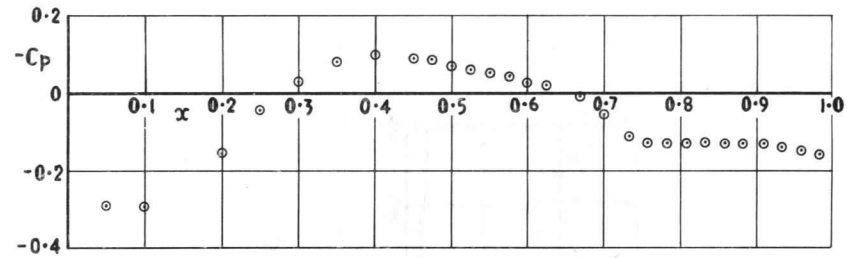


(a) Pressure coefficient

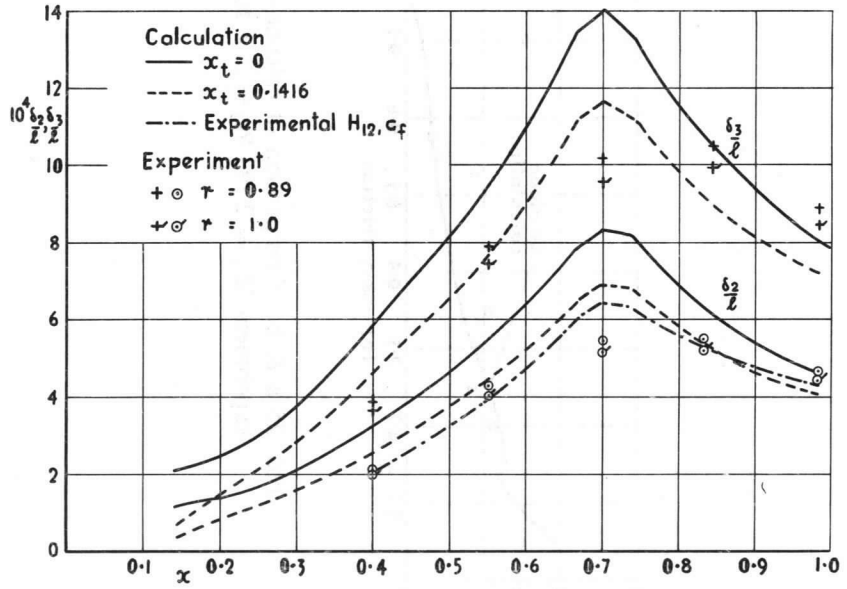


(b) Skin friction

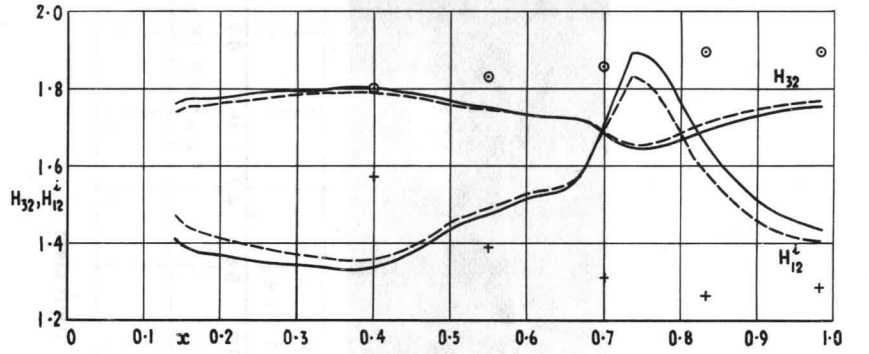
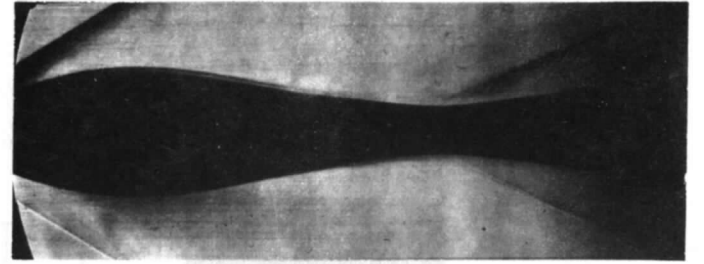
FIG. 25 a & b. Comparison of calculation and experiment $M_\infty = 2.793$ $Re_l \approx 5 \times 10^6$.



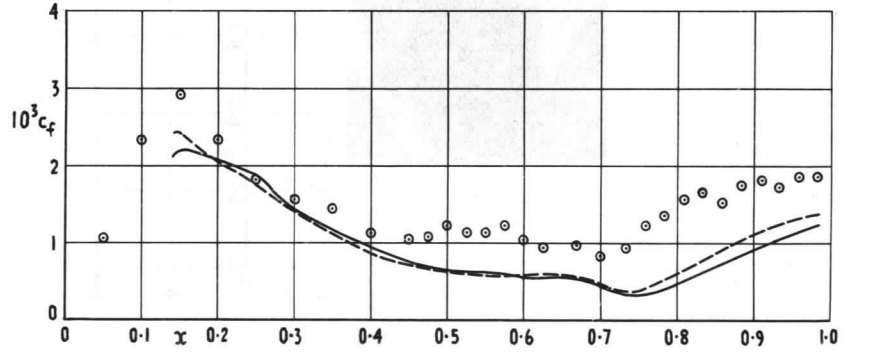
(a) Pressure coefficient



(b) Momentum & energy thickness



(c) Shape parameters



(d) Skin friction

FIG. 26. Comparison of calculation and experiment $M_\infty = 2.799$ $Re_l \approx 10^7$.

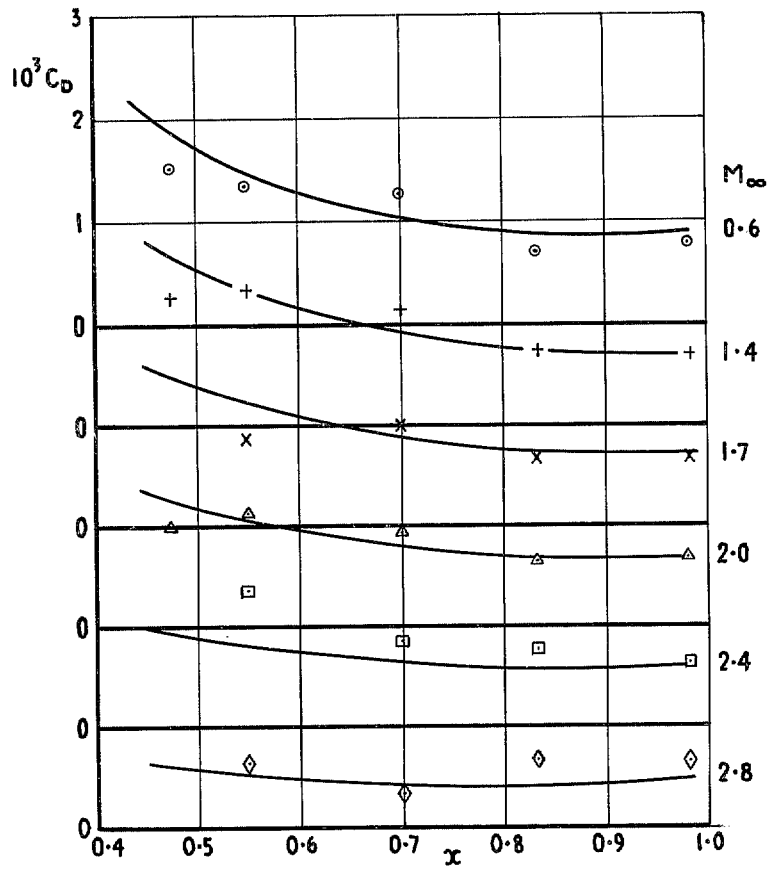


FIG. 27. 'Mean' dissipation coefficient $Re_t \approx 10^7$.

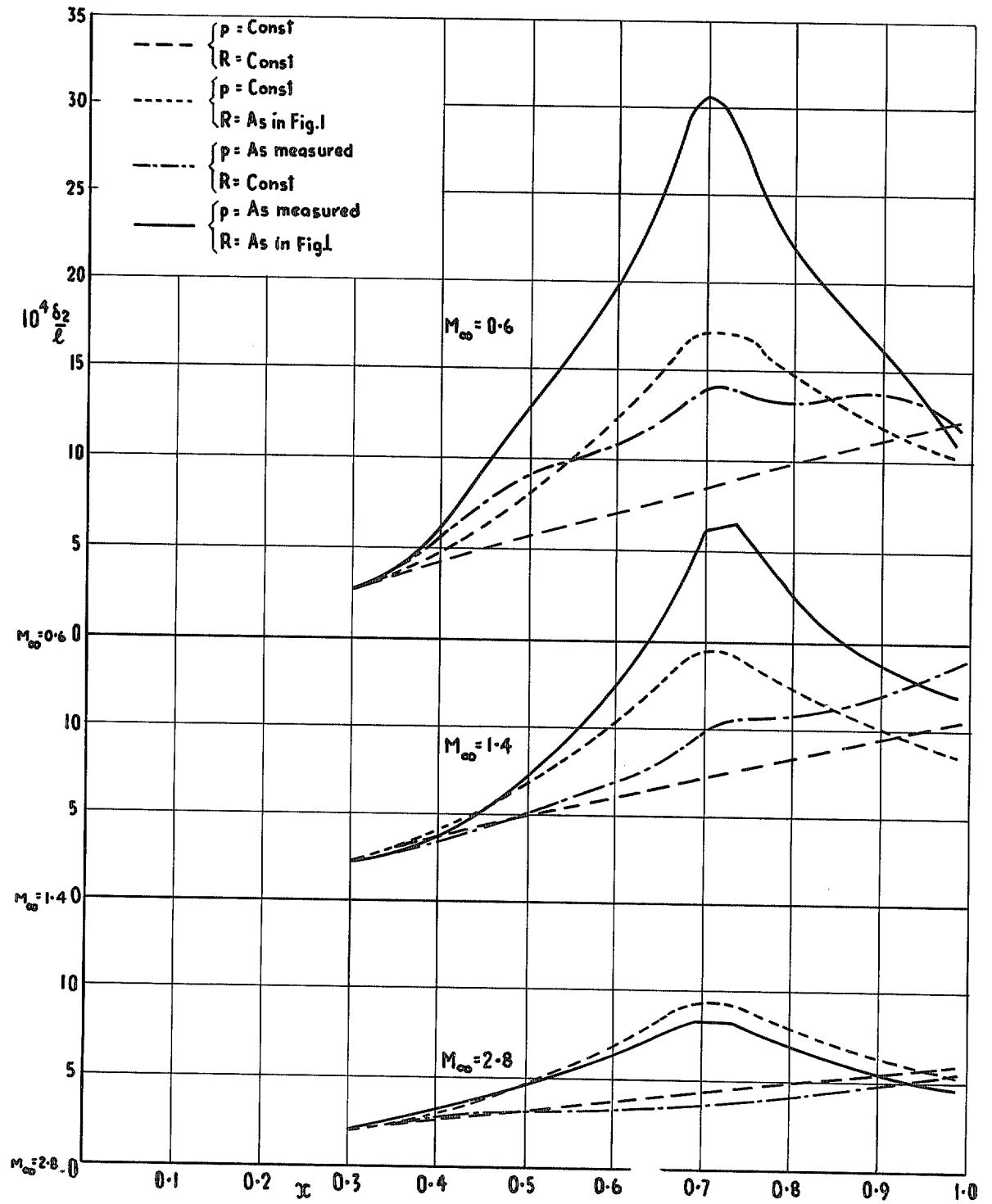


FIG 28. Influence of pressure gradient and streamline convergence on momentum thickness $Re_l = 10^7$.

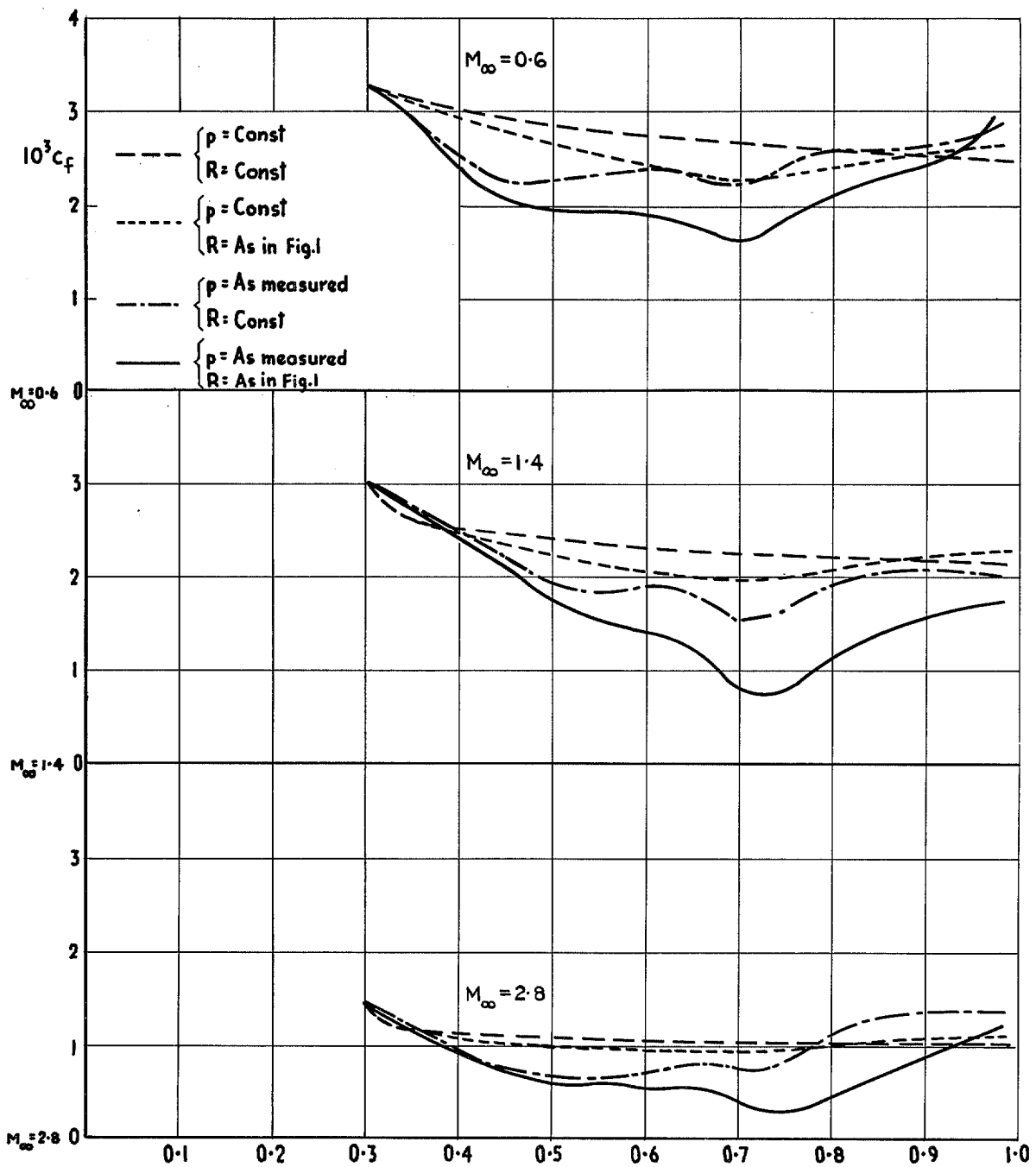


FIG. 29. Influence of pressure gradient and streamline convergence on skin friction $Re_t = 10^7$.

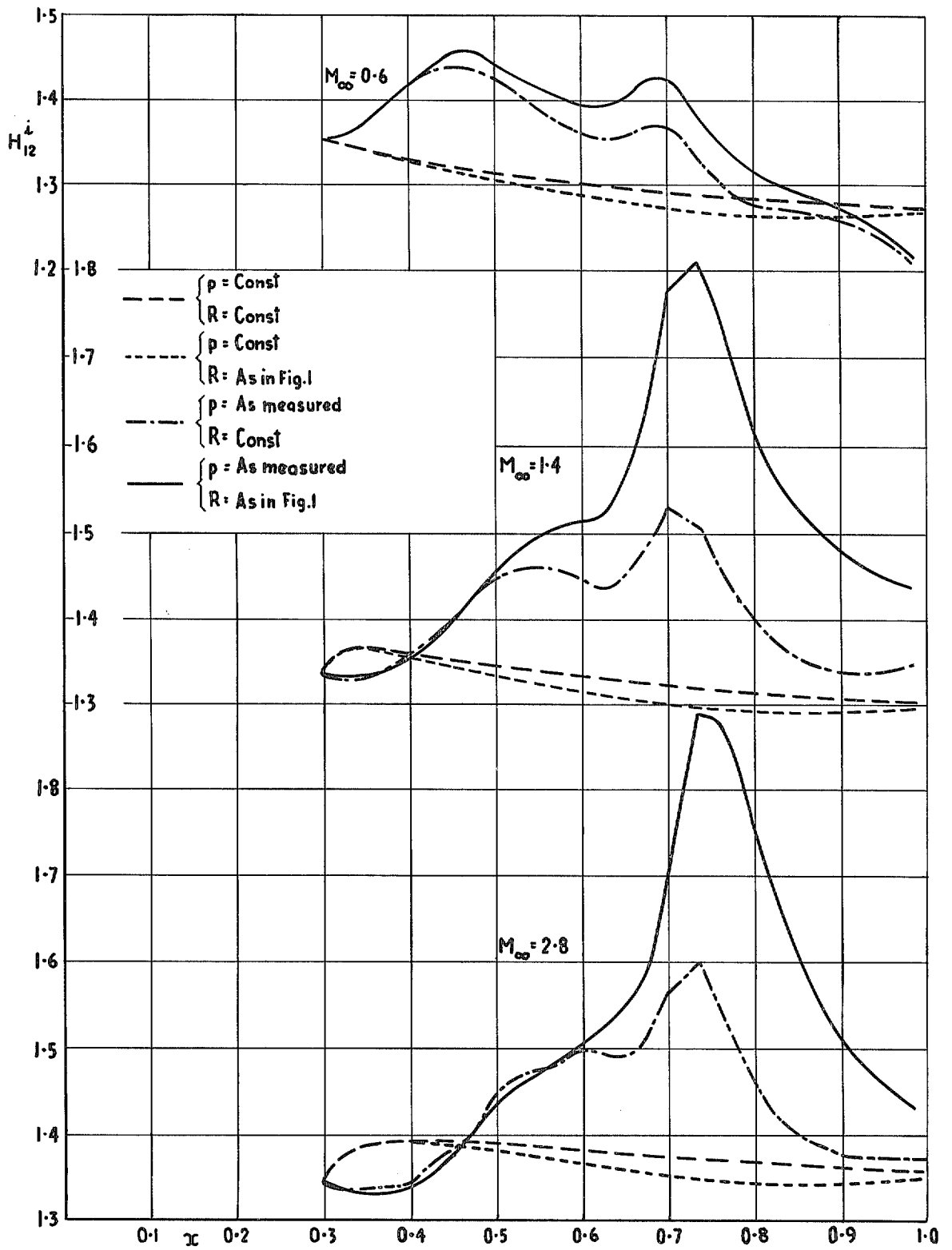


FIG. 30. Influence of pressure gradient and streamline convergence on shape parameter H_{12}^i $Re_l = 10^7$.

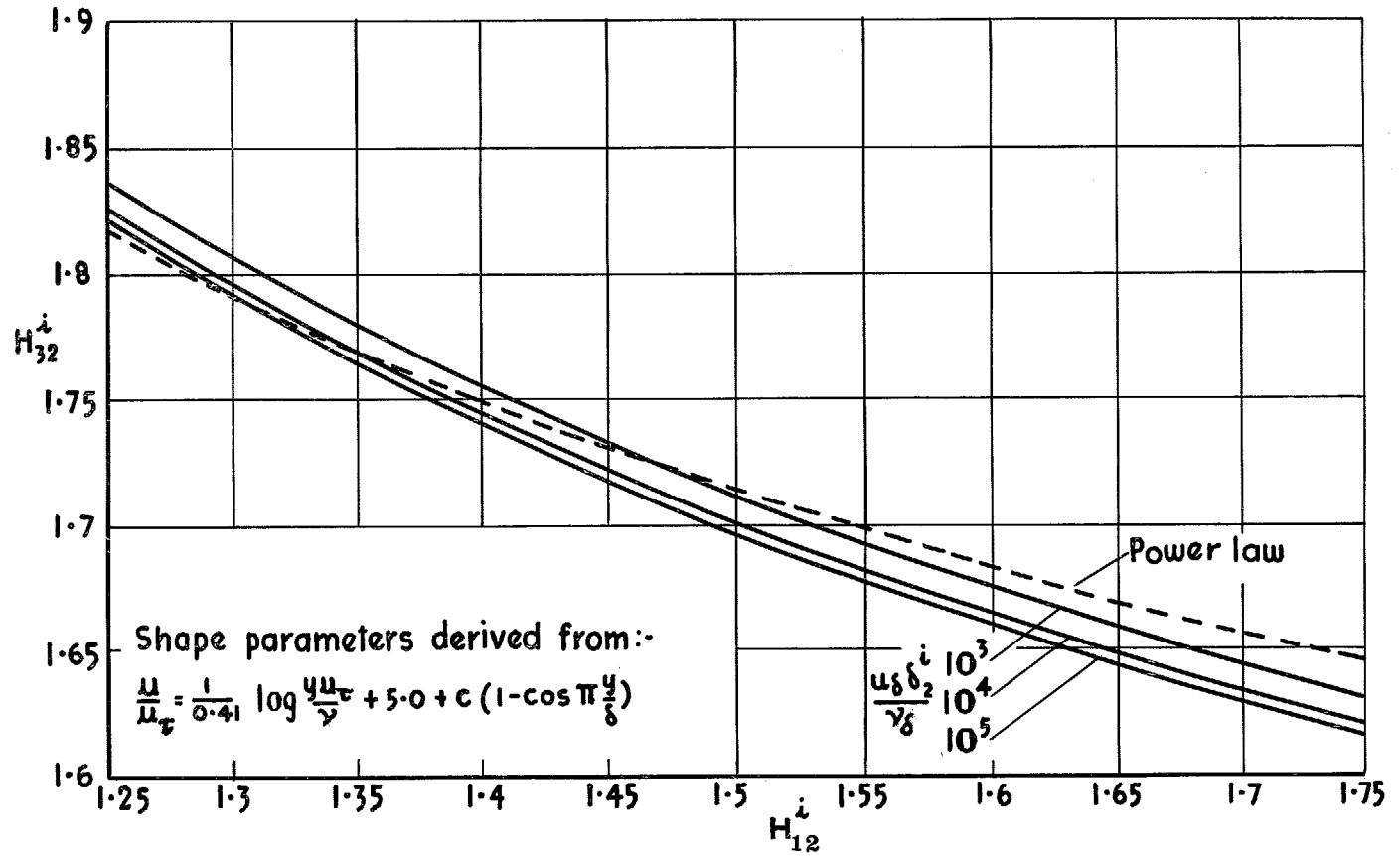


FIG. 31. Alternative shape parameter correlation.

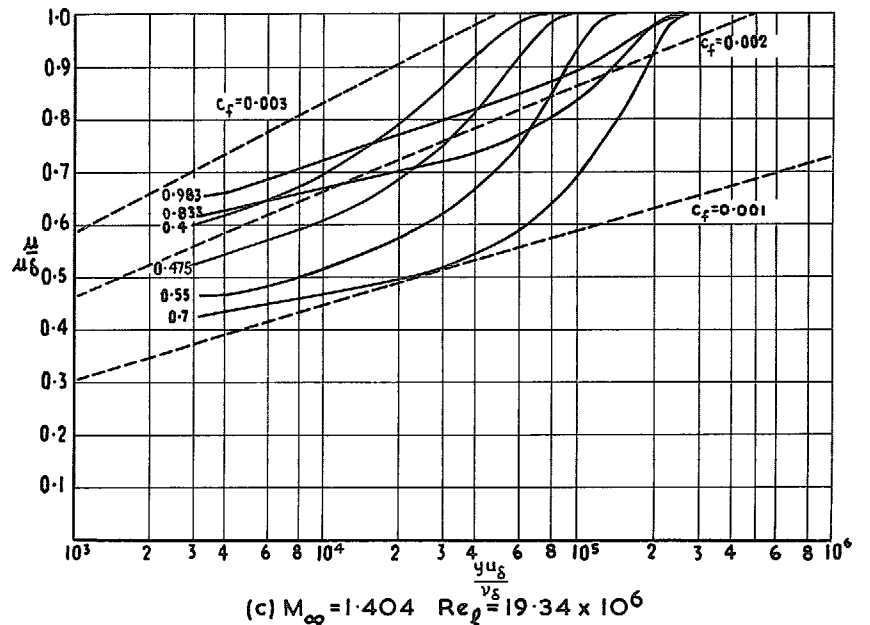
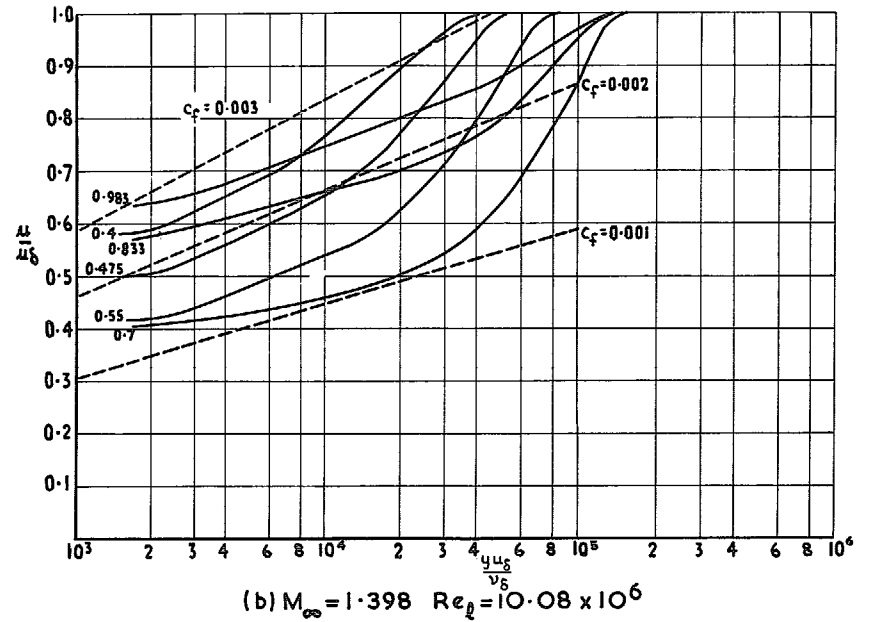
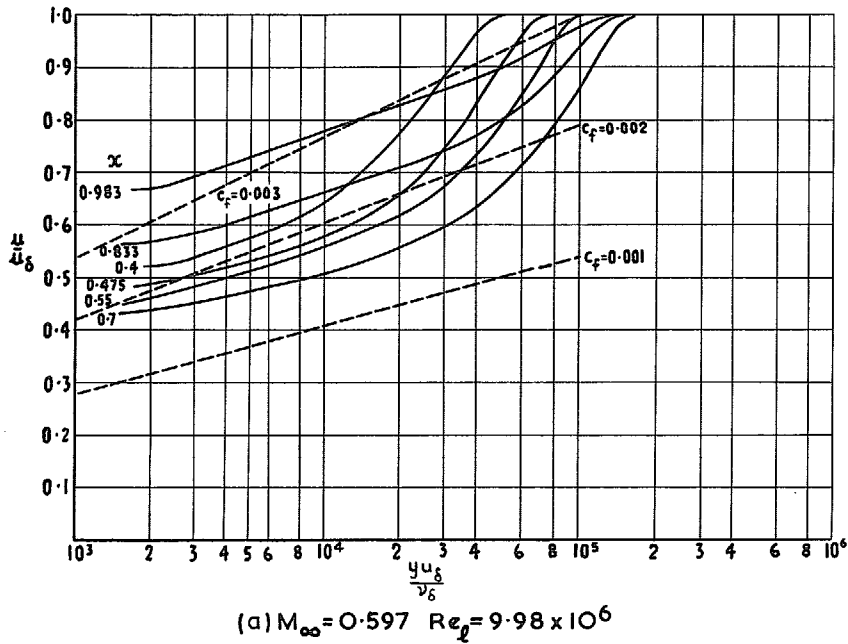


FIG. 32 a to c. Semi-logarithmic plot of velocity profiles.

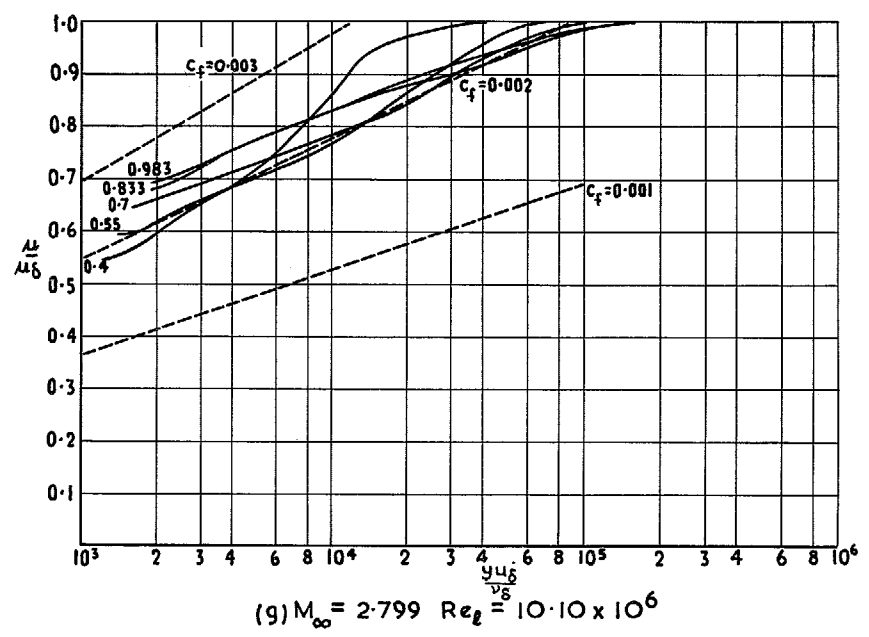
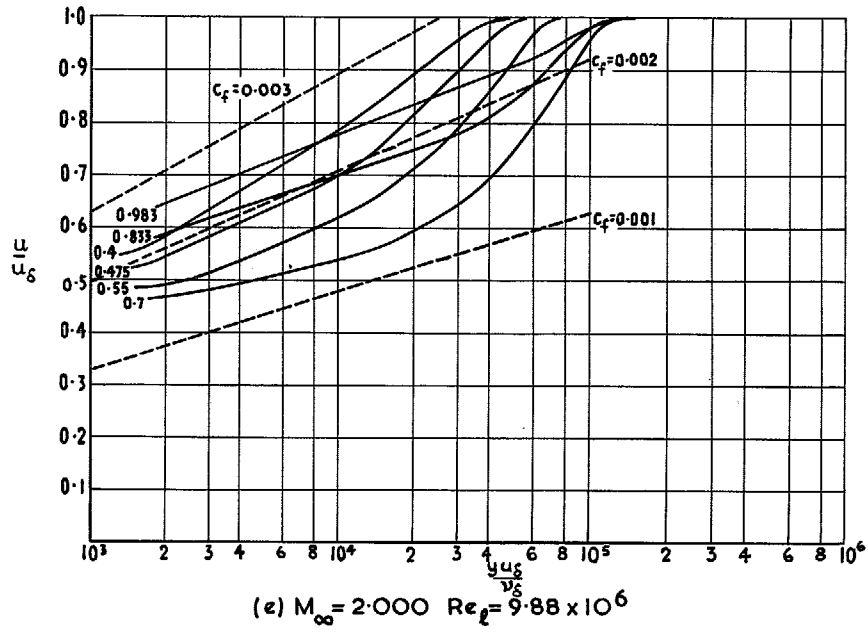
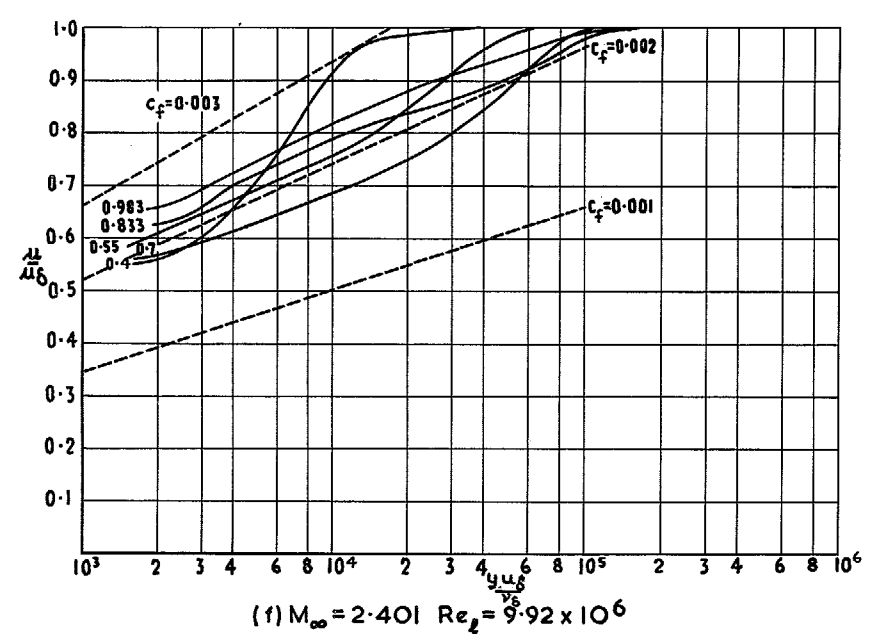
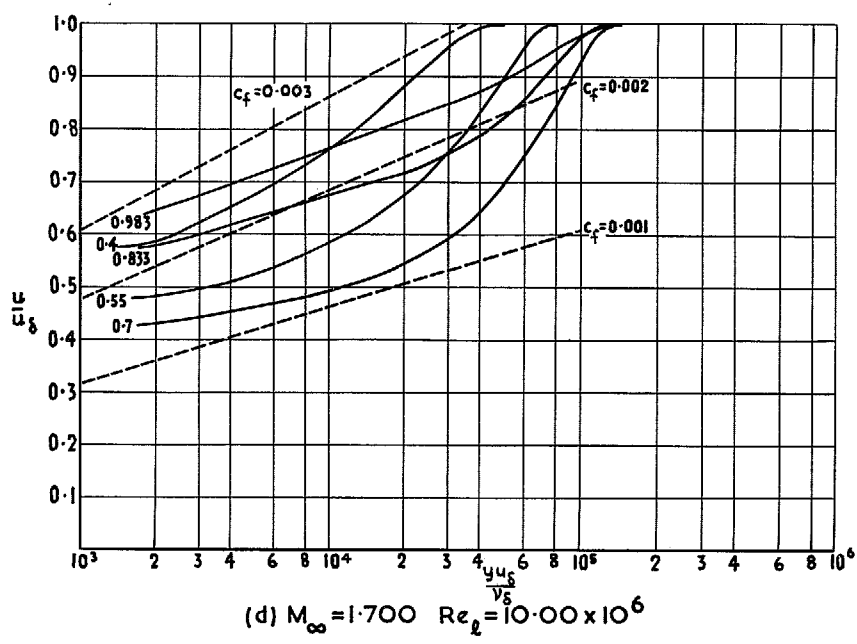


FIG. 32d to g. Semi-logarithmic plot of velocity profiles.

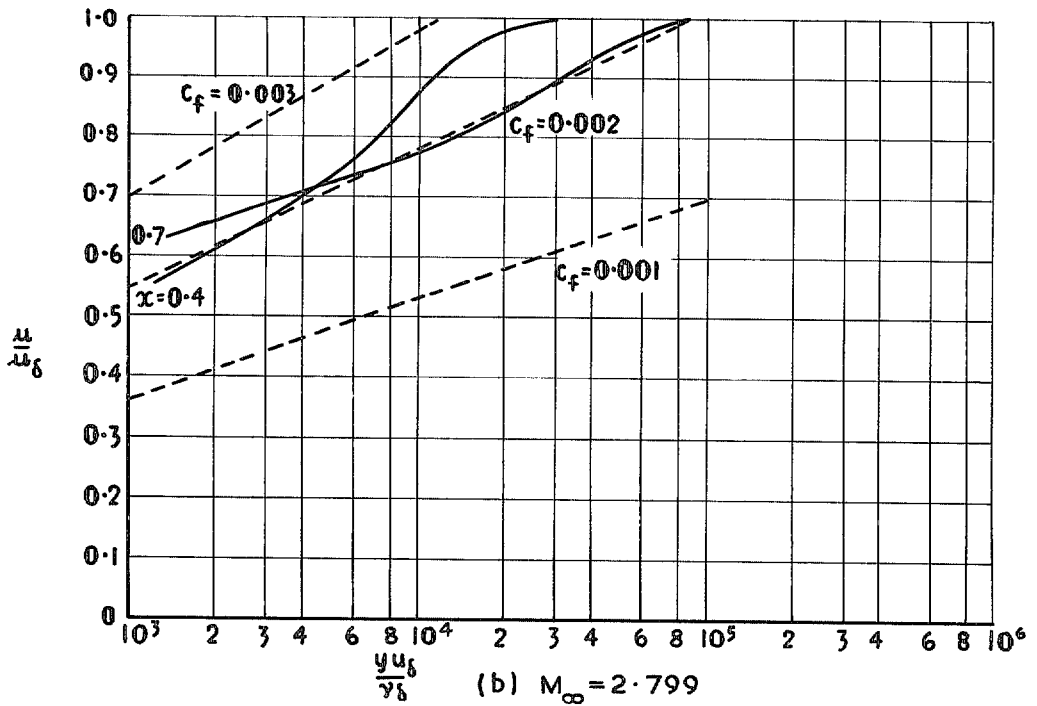
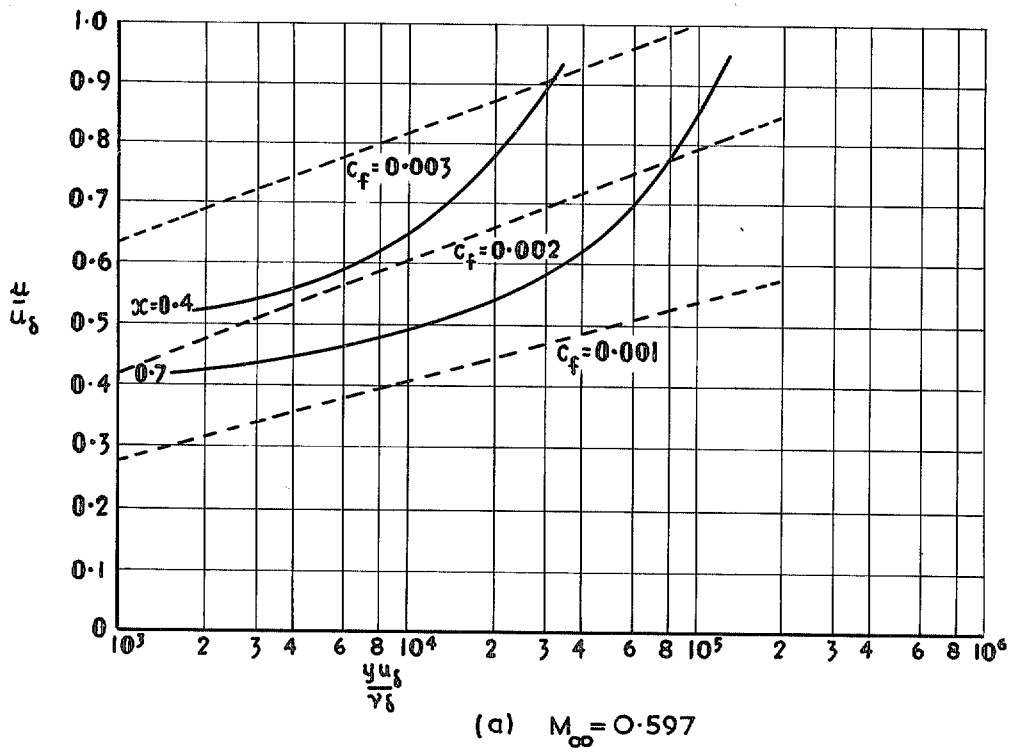
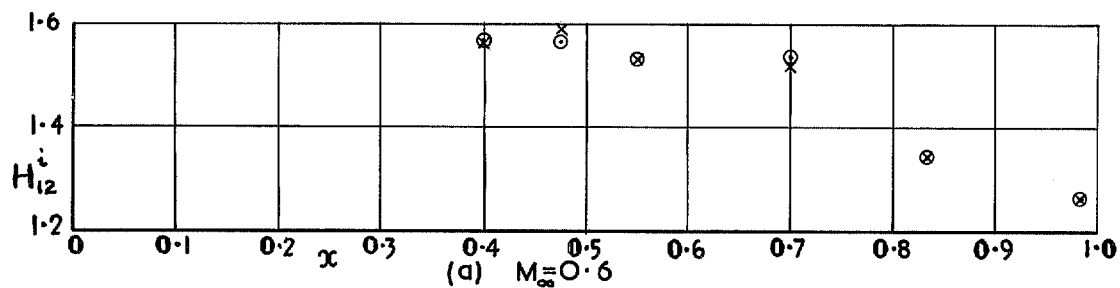


FIG. 33 a & b. Velocity profiles corrected for normal pressure gradient.



x Static pressure constant
o With calculated normal pressure variation

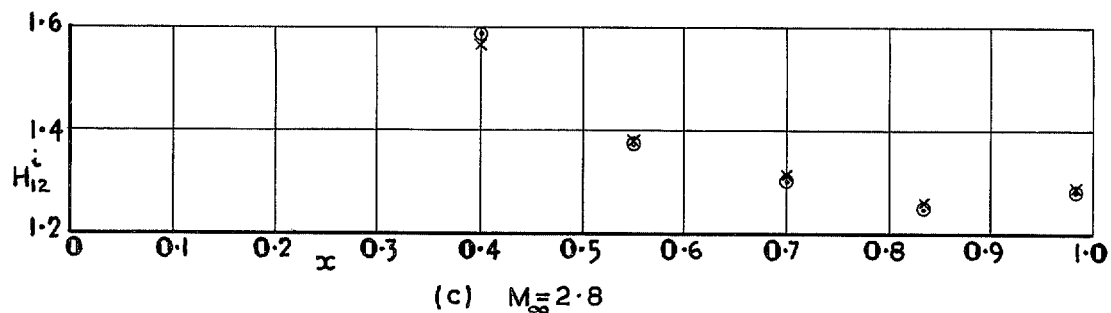
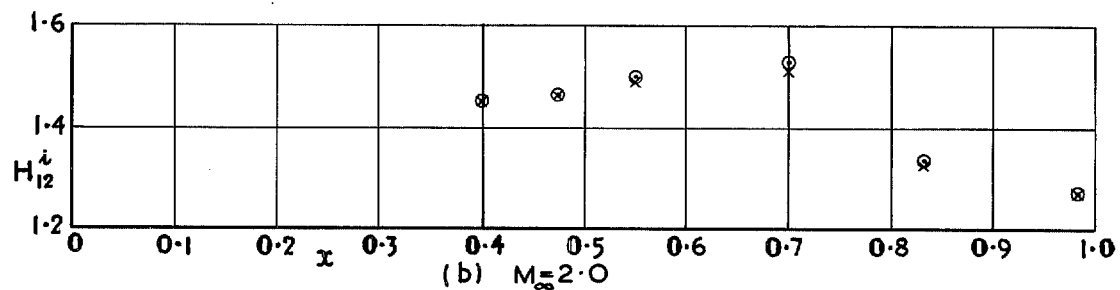


FIG. 34 a to c. Calculated effect of normal pressure gradients on shape parameter H_{12}^i ($r = 1$).

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