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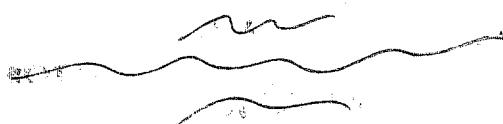


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Studies of the Turbulent Boundary Layer on a  
Waisted Body of Revolution in Subsonic and  
Supersonic Flow

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# Studies of the Turbulent Boundary Layer on a Waisted Body of Revolution in Subsonic and Supersonic Flow

By K. G. WINTER\*, J. C. ROTTA\*\* and K. G. SMITH\*\*\*

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## *Summary.*

The object of the study was to determine the influence of Mach number, pressure gradients and stream-line convergence and divergence on the development of turbulent boundary layers. Measurements were made of pressure distribution, local skin friction and boundary-layer profiles along the body, at Mach numbers between 0·6 and 2·8 and Reynolds numbers, based on the length of the body, between  $5 \times 10^6$  and  $2 \times 10^7$ . The results of comparative calculations based on simultaneous integration of the momentum and kinetic energy equations are generally in fair agreement with the experiments except at the two higher Mach numbers (2·4 and 2·8). The study was a result of collaboration between the Aerodynamische Versuchsanstalt, Göttingen and the Royal Aircraft Establishment, Bedford.

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\*Royal Aircraft Establishment, Bedford.

\*\*Aerodynamische Versuchsanstalt, Göttingen.

\*\*\*Formerly at R.A.E. Bedford now at University of Queensland.

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### 1. *Introduction.*

For a slender wing supersonic transport aircraft skin friction may contribute about a third of the total drag. Engines are likely to be installed on the wings and their intake design and performance will be strongly influenced by the local boundary-layer conditions on the wing surface. A detailed knowledge of the boundary-layer development over the wings is thus essential.

Following the ideas of Spence<sup>1</sup>, methods of calculation for turbulent boundary layers at supersonic speeds on slender wings were developed by Cooke<sup>2</sup>. One of the assumptions in this work was that the relationships between skin friction and Reynolds number based on local boundary-layer momentum thickness could be taken to be the same as on a flat plate, and in fact a power law was used. Calculations of this nature were found inadequate in predicting skin-friction coefficients measured on a cambered delta wing<sup>3</sup>. The inference taken from Ref. 3 was that the skin-friction law used was of a too simple form. The measurements showed that though the total skin-friction drag was fairly close to that of a flat plate, local values as low as half that on a flat plate at the same length Reynolds number were found. These low values occurred in regions where there was convergence of the flow combined with a mild adverse pressure gradient. In Ref. 3, skin friction only was measured and knowledge of the local boundary-layer profiles was clearly required to make any progress in understanding the flow. To avoid the experimental difficulties of boundary-layer exploration on the wing, which would arise from the crossflows, the present study was undertaken.

The main aim of the study was to produce an axisymmetric converging flow with an adverse pressure gradient. At the same time, it was appreciated that general information on the behaviour of turbulent boundary layers in compressible flows with pressure gradients could be of great value in developing and checking methods of calculation, which, in the present state of knowledge, must generally be based upon empirical correlations.

The study was a joint effort of the Aerodynamische Versuchsanstalt Göttingen and the Royal Aircraft Establishment Bedford. The measurements were made in the RAE 8ft × 8ft wind tunnel. A brief description of the work is contained in Ref. 4 and a more complete account in German in Ref. 5.

## 2. Model Design.

The obvious simple example of a supersonic flow with an adverse pressure gradient and converging streamlines is the aft end of a parabolic body of revolution. However, the convergence for a parabolic body increases as the tail is approached, and a more nearly constant value of the convergence parameters was felt to be desirable. (It was, in fact, visualised initially that a series of bodies with various values of convergence and divergence might be studied.) The starting point for the model design was thus a body approximating to a parabolic body over the forepart but with concavity introduced over the aft end. By adding a flare to the body it was hoped to obtain a diverging flow, whilst retaining for some part the adverse pressure gradient.

On the delta wing model of Ref. 3 the convergence of the external flow measured was about 0·04 radian per inch, and values of divergence up to 0·08 radian per inch were found. Since the intended model was to be of the same length (60 in.) as the delta wing and to be tested at the same conditions, it was reasonable to use the same dimensional values of convergence and divergence. This was taken to be 0·05 radian per inch, i.e.

$$\frac{1}{R} \frac{dR}{dX} = \pm 0·05 \quad (2.1)$$

when  $R$  and  $X$  the body radius and distance from the nose are measured in inches. Equation (2.1) implies an exponential variation of radius with distance but it was found that a cubic equation would give a sensibly constant value of  $\frac{1}{R} \frac{dR}{dX}$  over the regions of interest.

The final shape of the model is shown in Fig. 1. Its shape is specified in five sections with continuity of ordinate, slope and curvature at the junctions of the sections except at the end of the conical part of the nose where the curvature is discontinuous. The conical nose has an included angle of 40 degrees, being the largest angle to give an attached shock wave at the lowest supersonic speed of the test ( $M_\infty = 1·4$ ). This is followed by a shape defined by a quartic curve which joins the cubic giving approximately constant convergence. A mirror image of this cubic provides the final flare and a quartic fairing curve joins the converging and diverging regions.

The non-dimensional divergence parameter  $\frac{\eta'}{\eta}$  where  $\eta = \frac{R}{l}$  and the prime denotes differentiation with respect to  $x = \frac{X}{l}$ , is shown in Fig. 2, together with the non-dimensional longitudinal curvature. The pressure distribution is shown in Fig. 3, and by comparison with Fig. 2, it can be seen that combinations of streamline convergence or divergence, and sign of pressure gradient as in the following table are obtained.

### Supersonic speeds

$x$	0·0–1·42	1·42–3	3–4	4–7	7–1·0
Streamlines	divergent	divergent	convergent	convergent	divergent
Pressure gradient	zero	favourable	favourable	adverse	slightly adverse

### Subsonic speeds

$x$	0·0–3	3–7	7–1·0
Streamlines	divergent	convergent	divergent
Pressure gradient	favourable	adverse	favourable

All four possible combinations, the last only marginally, are obtained at supersonic speeds but only two at subsonic speed.

Fig. 4 compares the calculated pressure distribution at  $M_\infty = 1.4$ , using linear theory<sup>6</sup>, with the measured pressures. Despite the absence of any boundary-layer displacement correction in the calculations the comparison is good.

### 3. Experimental Details.

#### 3.1. Model Construction.

The model was constructed of fibreglass skin and bulkheads assembled over a steel core, and filled with foamed resin. The skin and bulkheads were 0.25 inch thick. Pressure tubes were built into the skin and emerged at the model base. 29 tubes were provided along each of two generators 30 degrees apart ( $\varphi = 0$  and  $\varphi = 30^\circ$ ) and extra holes at 90 degrees intervals were added at  $X = 6, 24, 42, 59$  inches. The pressure holes were 0.03 inch diameter. The hole at  $X = 9$  inches  $\varphi = 0$  became blocked early in the experiment and could not be cleared.

#### 3.2. Skin-Friction Measurement.

Skin friction was measured by the razor blade technique described in Ref. 7. The portions of razor blade (about 0.2 inch square) were mounted over the row of holes at  $\varphi = 30$  degrees, and the pressure difference taken from the static pressure measured on the row of holes at  $\varphi = 0$  degrees. The height of the razor blades was approximately 0.005 inch. That the presence of the razor blades did not influence the results was checked by repeating measurements with alternate blades removed. The calibration used differed from that given in Ref. 7 being based upon measurements taken during the tests of Ref. 8 in which surface shear was measured directly.

#### 3.3. Velocity Profiles.

Boundary-layer profiles were measured using the standard tunnel flow survey equipment. This is illustrated in Figs. 5a and b. Four remotely controlled motions are available with this equipment, a primary rotation coaxial with the model support sting, a secondary rotation about a parallel offset axis at the end of the primary arm, a tertiary rotation about an axis at the end of the secondary arm and a longitudinal motion along this axis. In addition the secondary arm can be adjusted manually through  $\pm 10$  degrees about two axes to change the direction of the longitudinal motion. The movement used for profile measurements was the tertiary rotation with an arm of length 3 inches. The probe thus traversed along circular arcs but the distance used in defining the profiles was the radial distance from the body. The survey probe used had five pitot tubes of 0.0195 inch outside diameter and 0.0103 inch inside diameter spaced 0.1 inch apart. The use of multiple tubes enabled a check to be made on any interference and backlash effects by repeating readings at a given point with different tubes, and also of course diminished the time necessary for a traverse. The angular setting was measured in steps of 0.05 degree, i.e. the error was less than or equal to 0.025 degree so that the positional accuracy was 0.0013 inch. The small backlash present in the gear train would give an error in excess of this. The backlash was however largely eliminated by using the surface of the model as datum, and little change in aerodynamic load on the probes would occur during the course of a traverse. Contact was determined electrically by using silver paint on the model surface and a sensitive relay circuit.

The fore and aft travel of the probe is limited to 24 inches so that different extension pieces were required for the forward and rearward parts of the body. Because of the shape of the body it was not possible to align the probes with the local direction of a generator of the body. The misalignment generally was about 5 degrees except for traverses in the waist of the body ( $x = 0.7$ ) when it was 11 degrees.

The pressures from the probes were measured using a strain gauge pressure transducer mounted in a pressure switch at the base of the secondary arm. The pressure switch had 24 ways with the connections arranged in four sequences of six each giving five pressures, from the five pitot tubes, plus either a calibration pressure or a zero. Velocities were evaluated from the measured pressures assuming the static pressure

to be constant across the boundary-layer thickness\*. At subsonic speeds the measured pressure at the wall was used. At supersonic speeds the static pressure was determined from the Mach number evaluated from the pitot reading at the assumed edge of the boundary layer using normal shock relations. A calculated total-pressure loss through the nose shock of the body was taken into account. For the temperature distribution the parabolic formula,

$$\frac{T}{T_\delta} = 1 + r \frac{\gamma - 1}{2} M_\delta^2 \left[ 1 - \left( \frac{u}{u_\delta} \right)^2 \right] \quad (3.1)$$

was used, and both  $r = 1$  (constant total temperature) and  $r = 0.89$  were taken. For the profiles measured by Nothwang<sup>9</sup> the use of equation (3.1) with  $r = 0.89$  has been found to give values of momentum thickness which are too high by about 9 per cent at  $M = 3$  compared with using his measured temperature distribution. Taking  $r = 1$  gives momentum thickness correctly to within about 1 per cent. For the present results Tables 3a and b show a difference at  $M_\infty = 2.8$  of 6 to 7 per cent for the two assumptions. Similar results are found in Ref. 8. It is interesting to note that the results of Ref. 8 show that the important parameter  $H_{12}^i$  has more nearly the correct value by taking  $r = 0.89$ ; the error at  $M = 2.8$  is about -0.3 per cent compared with -1.1 per cent for  $r = 1$ .

The various integral properties of the boundary layer, as defined in the list of symbols, were calculated taking into account the radius of the body. This of course is necessary in order that the quantities in the momentum integral equation do satisfy the equation. The application of the factor  $1 + \frac{y}{R}$  in the integrands of quantities such as  $\delta_1^i$  (see Section 5) may be questioned, since in some respects these quantities may be regarded merely as descriptive geometric parameters of the boundary-layer profiles. However, the correlation given in Ref. 8 for compressible boundary-layer profiles on the basis of similarity of 'incompressible' profiles implies some physical significance of the various  $\delta^i$ . Accordingly the factor  $1 + \frac{y}{R}$  in the integrals has been applied consistently throughout. In fact the influence of the factor on the shape parameters used is small.

### 3.4. Transition Trip.

For all experiments a transition trip was attached 1.5 inches from the nose of the body. The trip was of Ballotini of size 0.005 inch. The size proved to be inadequate at Mach numbers above 1.4. Using the criterion of Ref. 10 (established after the initial experiments) a trip of size, 0.013 inch would be required to bring transition forward to the roughness band at  $M_\infty = 2.8$  and a unit Reynolds number of 1 million per foot.

### 3.5. Range of Measurements.

The range of nominal conditions for the experiments are given in the following tables.

#### Skin friction

$M_\infty$	0.6	0.8	1.4	1.7	2.0	2.4	2.8
$10^{-6} Re_l$	10	10	5 10 20	10	5 10 17	10	5 10

\*Some comment on the effect of normal pressure gradients on the measured profiles is offered in Section 7.3.

## Profiles

$M_\infty$	0·6	1·4	1·7	2·0	2·4	2·8
$10^{-6} Re_l$	10	10 20	10	10	10	10

Profiles were measured at  $x = 0·4, 0·475, 0·55, 0·7, 0·833, 0·983$  except for  $M_\infty = 1·7, 2·4, 2·8$  where  $x = 0·475$  was omitted.

### 3.6. Accuracy.

For a Reynolds number of  $10^7$  the pressure coefficients are estimated to have an accuracy of about  $\pm 0·005$ , about half of which arises from possible systematic error and about half from random error. Assuming that the razor blade calibration used is applicable to the conditions of the experiment, the skin-friction coefficients are estimated to be accurate to within  $\pm 0·0002$ . Part of this error is due to inaccuracies in measurement and part due to incorrect fore and aft positioning of the blades with respect to the static holes. The errors will be smaller at the higher Reynolds numbers and larger at the lower Reynolds numbers.

As noted in Section 3.3 the resolution of the system for measuring probe position was about 0·0013 inch. Since the wall was used as datum the accuracy of the distance from the wall was about 0·0026 inch.

The model shape was correct to within 0·01 inch with the slope maintained within 0·001 inch/inch. The maximum eccentricity was 0·006 inch.

## 4. Experimental Results.

Table 1 gives details of pressure, local Mach number and skin-friction distributions along the body. The pressure coefficient is referred to free stream static pressure and kinetic pressure but the skin-friction coefficient is referred to local kinetic pressure.

Table 2 lists the Mach numbers and velocity ratios in the boundary layers against the distance from the wall,  $y$ , measured in inches, with data evaluated both for  $r = 1$  and  $r = 0·89$  in the parabolic temperature distribution (equation (3.1)). The assumed edge of the boundary layer is indicated but some points are given beyond the edge. These points are included because they show normal gradients exist in the flow for supersonic speeds. (Pitot pressure outside the boundary layer is, of course, constant in principle for subsonic speeds.) The points are however incorrect because of the assumption of constant static pressure. For example at  $M_\infty = 2·8$  and  $x = 0·7$  if the total pressure outside the boundary layer is taken as constant the Mach number rises from 2·759 to 2·812 between  $y = 0·630$  and  $y = 1·193$  inches instead of falling from 2·759 to 2·695 as shown in the tabulation. Integral properties of the boundary layers are listed in Table 3.

The velocity profiles are plotted in Fig. 7 and the main results are summarised in Figs. 15 to 26 where comparisons with calculations are made.

### 5. Boundary-Layer Properties.

The experimental results are summarised in Fig. 6 which also illustrates the basic problem that the experiment was designed to study. In the figure, the measured values of local skin-friction coefficient are plotted against Reynolds number based on momentum thickness, with both expressed in intermediate temperature form, using the expression due to Eckert<sup>11</sup>, which for zero heat transfer is

$$T^* = 0·28 T_\delta + 0·72 T_w. \quad (5.1)$$

For flat plate boundary layers the effects of compressibility are taken into account to within a small

percentage by the intermediate temperature hypothesis. It will be seen that for the present model the measurements at the model base fall within  $\pm 10$  per cent of the Prandtl-Schlichting line, and for Mach numbers of 1.4, 1.7 and 2.0 the measurements at  $x = 0.4$  also fall near the line. For  $M_\infty = 0.6$  the value at  $x = 0.4$  is low but this might be expected since at subsonic speeds the adverse pressure gradient starts at  $x = 0.3$ . It is however surprising that the values for  $x = 0.4$  fall well below the line at  $M_\infty = 2.4$  and 2.8.

The main point of interest is the low values of skin-friction coefficient at the waist of the model. For all Mach numbers tested the value is approximately half that for a flat plate, and it is this feature particularly that the experiment was designed to study.

Velocity profiles are shown in Fig. 7. The profiles for Mach numbers up to 2 are as would be anticipated from Fig. 6, in that hollow profiles are obtained where the skin friction is low. At the highest two Mach numbers, however, the profiles remain full along the whole body.

For incompressible flows the Ludwig-Tillmann<sup>12</sup> formula relates skin friction to the velocity profile shape by expressing local skin-friction coefficient  $c_f$  as a function of Reynolds number based on momentum thickness  $\frac{u_\delta \delta_2}{v}$  and shape parameter  $H_{12} = \frac{\delta_1}{\delta_2}$  where  $\delta_1, \delta_2$  are displacement and momentum thickness. This relationship cannot be used directly for compressible flows because  $H_{12}$  is strongly dependent upon the density distribution through the boundary layer. Walz<sup>13</sup> has suggested instead the use of a parameter  $H_{12}^i = \delta_1^i/\delta_2^i$  where  $\delta_1^i, \delta_2^i$  are evaluated from the velocity profiles as though the flow were incompressible, i.e. ignoring density terms. Walz also suggested that the Reynolds number based on momentum thickness should be modified by using a value of viscosity evaluated at wall conditions. The modified form of the Ludwig-Tillmann formula is then

$$c_f = 0.246 \left( \frac{\rho_\delta u_\delta \delta_2}{\mu_w} \right)^{-0.268} 10^{-0.678 H_{12}^i} \times k \quad (5.2)$$

where Walz takes  $k = \frac{\delta_2}{\delta_2^i}$ .

Fig. 8a shows  $k$  determined from the measurements of Ref. 8 at Reynolds numbers of the order of  $50 \times 10^6$ . At such high Reynolds numbers the Ludwig-Tillmann formula gives low values of  $c_f$  but the results are nearly parallel to a line with twice the slope of the prediction of Walz, i.e.

$$k = 2 \frac{\delta_2}{\delta_2^i} - 1. \quad (5.3)$$

(There is obviously an upper limit to the Mach number for which the formula holds, otherwise at high Mach number negative skin friction would be predicted.) Fig. 8b shows the results on the body and though there is considerable scatter the same correlation is roughly applicable. In Fig. 8b the momentum thickness values used are evaluated in accord with the expression for a body of revolution and with the temperature distribution of equation (3.1) with  $r = 0.89$ .

Walz<sup>14</sup> has utilised power law profiles together with a parabolic temperature distribution to calculate relationships between various profile parameters for compressible boundary layers and has suggested approximate general formulae fitting the results of his calculations. It is of interest to see how far his correlations can be applied to the present results. The use also of results of Ref. 8 gives a useful guide to the applicability of the correlations to flat plate conditions. The assumption of power law profiles implies that

$$H_{32}^i = \frac{4 H_{12}^i}{3 H_{12}^i - 1} \quad (5.4)$$

where  $H_{32}^i = \frac{\delta_3^i}{\delta_2^i}$ , the ratio of kinetic energy thickness to momentum thickness for constant density.

Fig. 9a shows that the flat plate profiles of Ref. 8 (which can be collapsed very closely by a summation of a logarithmic velocity distribution plus a constant wake term) can in fact also be represented well by power laws. The exponent is between 1/7 and 1/9. For the profiles on the body (Fig. 9b) there is much greater disparity with the power law line, particularly at the two higher Mach numbers (note change of scale between Figs. 9a and 9b). At other Mach numbers the points only at both ends of the body are far from the power law line.

In order to derive the compressible shape parameter  $H_{32}$  from the ‘incompressible’ value  $H_{32}^i$  Walz has suggested the approximation.

$$H_{32} = H_{32}^i [1 + (2 - H_{32}^i) b] \quad (5.5)$$

where  $b$  is primarily a function of Mach number but also from calculations shows a weak dependence upon  $H_{32}^i$ . Walz suggested as an approximation that

$$b = 0.004 M_\delta + 0.0075 M_\delta^2 - 0.00018 M_\delta^4. \quad (5.6)$$

Fig. 10a shows that for flat plate profiles a better fit is obtained if the linear term is omitted, i.e.

$$b = 0.0075 M_\delta^2 - 0.00018 M_\delta^4 \quad (5.7)$$

and the results on the body Fig. 10b are in fair agreement with equation (5.7).

For the ratio of ‘incompressible’ momentum thickness to actual momentum thickness the suggested correlation is

$$\frac{\delta_2^i}{\delta_2} = 1 + r \frac{\gamma-1}{2} M_\delta^2 H_{32} (2 - H_{32}^i) a \quad (5.8)$$

where  $r$  is the recovery factor and  $a$  is a function both of  $H_{32}^i$  and  $M_\delta$ , but with  $b$ , is only weakly dependent upon  $H_{32}^i$  and the dependence can be ignored. Fig. 11 shows that a better fit to both flat plate data and to the results on the body is obtained with

$$a = 1 - 0.043 M_\delta \quad (5.9)$$

rather than the form suggested by Walz. An even better fit would be obtained with a formula for which  $a$  tends to about 0.97 as  $M_\delta \rightarrow 0$ , as also given by the calculations of Ref. 5.

### 6. Details of Calculations.

The calculations are based upon the simultaneous integration of the momentum and kinetic energy equations of the boundary layer. For an isentropic flow over a surface with zero heat transfer these equations may be written

$$d \frac{\delta_2/l}{dx} + \frac{\delta_2}{l} \left[ \frac{H_{12} + 2}{u_\delta} \frac{du_\delta}{dx} + \frac{1}{\rho_\delta} \frac{d\rho_\delta}{dx} + \frac{1}{\eta} \frac{d\eta}{dx} \right] = \frac{c_f}{2} \quad (6.1)$$

$$d \frac{\delta_3/l}{dx} + \frac{\delta_3}{l} \left[ \frac{3}{u_\delta} \frac{du_\delta}{dx} + (2-\gamma) \frac{1}{\rho_\delta} \frac{d\rho_\delta}{dx} + \frac{1}{\eta} \frac{d\eta}{dx} \right] = c_D \quad (6.2)$$

where lengths have been non-dimensionalised by dividing by the body length  $l$ . Strictly the streamwise distance should be measured along the body surface. The error involved in using the axial distance has been accepted. Providing the shape factor  $H_{12}$ , skin-friction coefficient  $c_f$  and dissipation coefficient  $c_D$  can be determined, the integration of the two equations can be performed. The basis for the determin-

ation of  $H_{12}$  is the set of relationships between the various parameters outlined in the preceding section. With the addition of the equation

$$H_{12} = H_{12}^i \frac{\delta_2^i}{\delta_2} + \frac{\gamma-1}{2} M_\delta^2 H_{32} \quad (6.3)$$

which is exact for a flow with zero heat transfer,  $H_{12}$  can be determined from the values of  $\delta_2, \delta_3$  obtained from the integration. The skin-friction coefficient is given by the modified Ludwig-Tillmann formula (equation (5.2)). There remains to be obtained an expression for the dissipation coefficient. For incompressible flow Truckenbrodt<sup>15</sup> has devised an approximate formula on the basis of the analysis of Rotta<sup>16</sup>. On the assumption that the shearing stress distribution is not altered in compressible flow, Walz modified the dissipation formula in the same way as the skin-friction formula. However, the shape of the shear stress distribution is somewhat fuller in compressible flow, and studies of the boundary layer on a flat plate suggested an increase in the ratio  $H_{32}/H_{32}^i$ . The following equation was therefore taken

$$c_D = 0.012 \left( \frac{\rho_\delta u_\delta \delta_2}{\mu_w} \right)^{-0.168} \left( 2 \frac{\delta_2}{\delta_2^i} - 1 \right) \frac{H_{32}}{H_{32}^i}. \quad (6.4)$$

The multiplying factor was increased from 0.0112 (Ref. 14) to 0.012 in accord with the studies of Fernholz<sup>17</sup>.

The calculations were programmed for an IBM 650 computer, starting from the point  $\frac{x}{l} = 0.1416$ , the end of the conical nose, and assuming that viscosity is given by

$$\frac{\mu}{\mu_\infty} = \left( \frac{T}{T_\infty} \right)^{\frac{1}{k}}. \quad (6.5)$$

The initial values of  $\delta_2$  at the end of the conical nose were calculated in the following way. For supersonic flow with an attached shock wave (i.e. for  $M_\infty \geq 1.4$ ) the pressure on the cone is constant and since  $R \propto x$  the momentum equation simplifies to

$$\frac{1}{x} \frac{d \left( x \frac{\delta_2}{l} \right)}{dx} = \frac{c_f}{2}. \quad (6.6)$$

For a turbulent boundary layer the skin friction was calculated from the simple power law

$$c_f = 0.0256 \left( \frac{u_\delta \delta_2}{v_\delta} \right)^{-\frac{1}{4}} \left( \frac{c_f}{c_{fi}} \right) \quad (6.7)$$

with the ratio of skin friction for compressible flow to that for incompressible flow estimated from Eckert's intermediate temperature hypothesis. For laminar flow the Blasius formula gives

$$c_f = (0.664)^2 \frac{v_\delta}{u_\delta \delta_2} \quad (6.8)$$

for incompressible flow. Within the Mach number range under consideration this formula for incompressible flow can be used with little loss of accuracy. Using either equation (6.7) or (6.8) in (6.6) closed formulae can be obtained for  $\delta_2$  and  $c_f$ . The same formulae were used for subsonic flow although there is a strong favourable gradient with subsonic conditions.

Figs. 12a and b show the calculated values at  $x = 0.05$  and  $x = 0.1$  for a Reynolds number  $Re_l = 10^7$ .

For Mach numbers of 1·7 and greater the measured results at  $x = 0\cdot05$  (Fig. 12a) are close to the calculated line for laminar flow\* and for lower Mach numbers are somewhat lower than the estimate for turbulent flow. As noted earlier the transition trip was of inadequate size at  $M_\infty > 1\cdot4$ . At  $x = 0\cdot1$  the measurements are close to the calculated turbulent values except for  $M_\infty = 2\cdot8$  where the flow is still transitional. Fig. 13 shows the calculated values of momentum thickness at  $x = 0\cdot142$ . No measurements are available for comparison.

The parameter  $H_{32}$ , in conjunction with  $\delta_2$ , is also needed to determine a starting value for  $\delta_3$ . The calculations are not very sensitive to the initial value of  $\delta_3$  and so the simplifying assumption was made that  $H_{32}$  is constant along the conical forebody. Equations (6.1) and (6.2) then reduce to the simple form.

$$H_{32} = \frac{2c_D}{c_f}. \quad (6.9)$$

Substitution of equations (5.2) and (6.4) leads to

$$\left( \frac{\rho_\delta u_\delta \delta_2}{\mu_\delta} \right)^{0\cdot1} = \frac{0\cdot246}{0\cdot024} \frac{H_{32}^i}{10^{0\cdot678} H_{12}^i} \left( \frac{\mu_w}{\mu_\delta} \right)^{0\cdot1} \quad (6.10)$$

from which  $H_{12}^i$  can be eliminated by equation (5.4). Use of equation (5.5) then enables  $H_{32}$  to be calculated. The values required were read from the chart shown in Fig. 14. The Reynolds number dependence invalidates the initial assumption but the variation of  $H_{32}$  is relatively small.

The calculations were made using two different assumptions for the initial conditions; firstly fully turbulent flow was taken over the conical nose and secondly the flow was assumed to be laminar with abrupt transition to turbulent flow at the end of the cone ( $x = 0\cdot142$ ). The differences between the two sets of calculations for  $\delta_2$  and  $\delta_3$  are small at the lower Mach numbers but increase with increase of Mach number. The effect of the different assumptions on skin-friction coefficient is generally small.

The normal definitions for two-dimensional flow of the various boundary-layer parameters in the momentum and kinetic energy equations are valid only if the boundary-layer thickness is small compared with the body radius. The boundary-layer thickness is certainly not small compared with the radius particularly at the waist of the body. However, equations (6.1), (6.2) are still correct provided the appropriate definitions for  $\delta_1$ ,  $\delta_2$ ,  $\delta_3$  and  $c_D$  are used. The definitions are as for two-dimensional flow with the factor  $1 + \frac{y}{R}$  introduced in the integrands. It is not known how this procedure affects the formula (6.4) for

the dissipation coefficient but it is a reasonable assumption that  $\left( 1 + \frac{y}{R} \right) \tau$  does not change greatly with  $R$ , so that the equation may approximately be valid. The skin-friction formula, equation (5.2), may also be expected to be approximately correct even when axisymmetric definitions are used for the boundary-layer parameters. The power law relationship equation (5.4) will also be slightly modified by the introduction of the factor  $1 + \frac{y}{R}$ . The other short-coming of both the calculations and the experiment, the assumption of constant static pressure across the boundary layer, is likely to be increasingly inaccurate as the boundary layer becomes thicker with respect to the body radius in regions of high longitudinal curvature.

## 7. Discussion of Results.

### 7.1. General.

The main results of the experiment and comparisons with calculations are shown in Figs. 15 to 26 where schlieren photographs of the flow are also presented. As a check on the compatibility of the measured

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\*The razor blade calibration used is not necessarily valid in laminar flow.

values of skin-friction coefficient and momentum thickness an extra calculation was made in which the measured values of  $c_f$  and  $H_{12}$  were used in the momentum equation. This calculation took as a starting point the measured momentum thickness at  $x = 0.4$ , except for  $M_\infty = 2.4$  where the measured value of  $\delta_2$ , appears to be inconsistently low. A starting value of  $\frac{\delta_2}{l} = 2.3 \times 10^{-4}$  was taken instead of the measured value  $1.8 \times 10^{-4}$ . (Why this low value was obtained is not clear. The profile has some appearance of being laminar but skin-friction measurements taken, along a different generator, at the same time as the profiles show no change from the original measurements and there seems no reason why an asymmetry round the body should occur for one particular Mach number.) The calculations are shown as the chain dotted line in Figs. 15, 18, 19, 20, 22, 24, 26. At  $M_\infty = 0.6$  (Fig. 15) the measured momentum thickness at the waist  $x = 0.7$  is higher than calculated but it is in good agreement at the end of the body, suggesting that the measurement of skin friction is low up to the waist and possibly high thereafter. At other Mach numbers the calculations and the experiments are in excellent agreement up to  $x = 0.7$  but the skin friction appears to be too large for  $x > 0.7$  leading to high values of momentum thickness in the calculations. It must be remarked that the technique for the measurement of skin friction, has not been completely established for the flows in which it has been used.

All the experimental results can be described in the same general way. Up to  $x = 0.4$  the boundary-layer thickness increases relatively slowly under the influence of a favourable pressure gradient and flow divergence. Between  $x = 0.4$  and  $x = 0.7$  the flow convergence and adverse pressure gradient lead to a rapid increase in thickness with a maximum thickness and minimum skin-friction coefficient near the waist,  $x = 0.7$ . The flow divergence downstream of  $x = 0.7$  promotes a rapid thinning of the boundary layer and an increase in skin-friction coefficient. For  $M_\infty = 1.4, 1.7$  and  $2.0$  the shape parameter,  $H_{12}^i$ , has a maximum at  $x = 0.7$  but this feature is not shown at  $M_\infty = 2.4$  and  $2.8$ . At  $M_\infty = 0.6$  the peak value of  $H_{12}^i$  occurs at least as far forward as  $x = 0.4$  where the adverse pressure gradient is strongest. In fact  $H_{12}^i$  appears to be correlated strongly with the pressure gradient.

There is good qualitative agreement generally between the calculations and the experiments but there are a number of features unexplained quantitatively. At  $M_\infty = 0.6$  (Fig. 15) the momentum and energy thicknesses calculated are in fair agreement with the measured values but their ratio,  $H_{32}$ , is larger than measured. In turn the calculated 'incompressible' shape parameter,  $H_{12}^i$ , which has a powerful influence on the skin-friction coefficient, is too small and the calculated skin friction too high. Nevertheless the general shape of the curves is faithfully reproduced. The schlieren photograph merely illustrates the thickening of the boundary layer in the body waist. No profile measurements were made at  $M_\infty = 0.8$  (Fig. 16) but the skin-friction comparison is similar to that at  $M_\infty = 0.6$ .

At  $M_\infty = 1.4, 2.0$  and  $2.8$  (Figs. 17, 21, 25) measurements were made at a Reynolds number  $Re_l$  of approximately  $5 \times 10^6$ , when transition did not occur until near the body waist. These results are discussed later (Section 7.4).

For  $M_\infty = 1.4, 1.7$  and  $2.0$  and  $Re_l \approx 10^7$  and also for  $M_\infty = 1.4, 2.0$  and  $Re_l \approx 2 \times 10^7$  the results are fairly similar. The calculations tend to underestimate  $\delta_2$  and  $\delta_3$  but the ratio,  $H_{32}$ , is well calculated. Despite poor agreement for  $H_{12}^i$ , for which a strong peak in the body waist is predicted but not measured, the skin friction is in remarkable agreement up to the body waist ( $x = 0.7$ ) but the measured increase over the rear flare is underestimated.

At  $M_\infty = 2.4$  and  $2.8$  with  $Re_l \approx 10^7$  (Figs. 24 and 26) the experiments and calculations are in poor agreement. The calculations predict the same sort of behaviour as at lower Mach numbers, that is, sharp peaks in  $\delta_2$  and  $\delta_3$  at the waist with a low value of  $H_{32}$  and a peak in the value of  $H_{12}^i$ . In fact the peak in  $H_{12}^i$  is predicted to increase with increase of Mach number whereas the measurements show the opposite trend. The peak values of both  $\delta_2$  and  $\delta_3$  as measured at  $M_\infty = 2.8$  occur downstream of the body waist. The measured skin-friction coefficient is considerably greater than estimated.

This failure of the calculations may arise from inaccuracy in the assumed form for the dissipation coefficient. As can be seen in Figs. 24 and 26 the calculations are very sensitive to the value of  $H_{32}$  and a small increase in the dissipation coefficient with increasing Mach number could produce a radical change in the results. Some assessment of the applicability of the formula taken for the dissipation coefficient can be made by calculating a sort of mean value. Equation (6.2) can be integrated to give

$$\int_{x_1}^x \frac{c_D}{\delta_3/l} dx = \ln(\delta_3 \rho_\delta^{2-\gamma} u_\delta^3 R)_x - \ln(\delta_3 \rho_\delta^{2-\gamma} u_\delta^3 R)_{x_1}. \quad (7.1)$$

By taking  $x_1 = 0.4$  a 'mean' dissipation coefficient may be defined as

$$C_D = \frac{(\delta_3)_{0.4}}{x-0.4} \int_{0.4}^x \frac{c_D}{\delta_3} dx. \quad (7.2)$$

Values of  $C_D$  obtained from the measurements and from the calculations are compared in Fig. 27.

Up to  $M_\infty = 2$  the experimental points have a fairly similar trend in that initially  $C_D$  is overestimated but at  $x = 0.7$  the predicted  $C_D$  is too small. For  $x > 0.7$  the prediction is too large. The points thus roughly follow the trends of  $H_{12}^i$  (Figs. 15 to 22), and it is thus indicated that the expression for the dissipation coefficient should be dependent upon this shape parameter. At  $M_\infty = 2.4$  the high values of the experimental point can be partly attributed to the low values of  $\delta_3$  at  $x = 0.4$ , and remarked upon previously. Nevertheless both for  $M_\infty = 2.4$  and 2.8 the change between  $x = 0.55$  and  $x = 0.7$  follows the trend of  $H_{12}^i$  (Figs. 24 and 26).

Some improvements in the details of the method of calculation could thus be made but the method used is essentially applicable only to two-dimensional flows with small streamwise curvature. In the experiment are included the effects of longitudinal and transverse curvature and of flow convergence and divergence. These effects may be expected to modify the basic structure of the boundary layers in ways of which no account is taken in the calculations. Some consideration of the effect of longitudinal curvature is given by one of the authors in Ref. 18.

## 7.2. The Influence of Pressure Gradient and Streamline Convergence.

The problem that the present work was intended to study was the combined influence of pressure gradient and streamline convergence on turbulent boundary-layer development. Though, as noted above, the method of calculation devised is not capable of taking into account fully the properties of the flow studied, some qualitative indication of the interaction of pressure gradient and streamline convergence can be obtained. Accordingly, further calculations have been made in which the surface pressure,  $p$  and the body radius,  $R$  have been taken as constant individually and together. The calculations start from  $x = 0.3$  which is near the maximum diameter of the body. Results are shown in Figs. 28, 29 and 30 for the momentum thickness, skin-friction coefficient and shape parameter  $H_{12}^i$ .

With both  $p$  and  $R$  constant the boundary layer is as on a flat plate with momentum thickness growing, and skin friction and shape parameter falling, with increasing  $x$ . ( $H_{12}^i$  increases between  $x = 0.3$  and 0.4 for supersonic speeds, presumably because of the slightly arbitrary choice of the starting values.) With the radius varying but  $p$  constant the boundary layer piles up in the body waist giving an increase in momentum thickness (Fig. 28) and a consequent small decrease in skin friction but the change in  $H_{12}^i$  is small. With  $p$  only varying the adverse pressure gradient up to the body waist causes an increase in momentum thickness over the flat plate values at  $M_\infty = 0.6$  and 1.4. At  $M_\infty = 2.8$  there is however a reduction because of the effect of the combined velocity and density gradient term in the momentum equation which changes sign at about  $M = 2.4$ . The dominating influence of the pressure gradient is on the shape parameter (Fig. 30) which is increased over most of the body and markedly so at the waist for  $M_\infty = 1.4$  and 2.8. With both  $p$  and  $R$  varying the pressure gradient effects are amplified considerably. Thus though convergence and divergence of the flow alone produce almost solely geometric effects, appreciable changes in boundary-layer characteristics can be produced when convergence is combined with pressure gradient.

### 7.3. Comment on Velocity Profiles.

The shape parameters shown in Fig. 9b scatter considerably from the assumed power law line and it might be expected that the use of a two parameter family might give an improved correlation. The results of Ref. 8 show that flat plate velocity profiles in the Mach number range 0·2 to 2·8 correlate completely, both in a wall region and a wake region, at a given value of a Reynolds number  $\frac{u_\delta \delta^i_2}{v_\delta}$  eliminating the scatter of Fig. 9a. It might be expected therefore that a similar correlation exists for boundary layers in pressure gradients with a family of lines with different values of the parameter  $\frac{u_\delta \delta^i_2}{v_\delta}$ . By varying the scale of a cosine wake term such a family has been constructed (Fig. 31). The dependence upon the Reynolds number is too small to explain the scatter of Fig. 9b and the only merit of the profiles is that the lines are rather steeper than a power law line (as are the experiments).

The failure of this approach is explained by plotting the experimental profiles in Clauser fashion (Figs. 32a to g). In these figures the 'law of the wall' lines are those of Ref. 8 but using freestream Mach number to determine the appropriate friction velocity. The feature that emerges from Fig. 32 is that the measured profiles are not all compatible with the wall law. This is so even at  $M_\infty = 0\cdot6$  for  $x = 0\cdot833$  and  $0\cdot983$  and is thus not the fault of the compressibility factors used. The type of flattening of the profiles is similar to that found by Patel<sup>19</sup> in favourable pressure gradients in incompressible flow.

The implication is that, in flows with favourable gradients or strong streamline divergence, calculation methods, such as that developed in this report which depends implicitly on the assumption of an equilibrium type flow, may prove to be unsatisfactory.

To check whether any of the conclusions regarding the behaviour of the velocity profiles are influenced by the assumption of constant static pressure in their evaluation some reappraisal has been undertaken. The pressure distribution through the boundary layer has been calculated utilising, by means of an iterative procedure, equilibrium between normal pressure gradient and local centrifugal acceleration. The calculations are slightly inconsistent, for supersonic speeds, with the profiles previously evaluated in that the constant of integration for the static pressure was determined at the wall rather than at the boundary-layer edge. Velocity profiles calculated using this pressure distribution and the measured pitot pressure are shown for  $M_\infty = 0\cdot6$  and  $2\cdot8$  at  $x = 0\cdot4$  and  $0\cdot7$  in Fig. 33 (to be compared with Figs. 32a and g). The two positions taken have normal pressure gradients of opposite sign. Though appreciable changes of the profiles result it will be seen that there is no significant improvement in the relationship with the 'law of the wall' lines. A further comparison (Fig. 34) of the shape parameter,  $H_{12}^i$ , determined with and without the normal pressure gradient confirms also that in respect of this important parameter the results are little influenced by the neglect of the normal pressure gradient.

### 7.4. Laminar Boundary-Layer Calculations.

At Reynolds number  $Re_l \approx 5 \times 10^6$  at  $M_\infty = 1\cdot4$ ,  $2\cdot0$  and  $2\cdot8$  (Figs. 17, 21 and 25) the boundary layer over the body apparently remains laminar up to the point at which the adverse pressure gradient becomes steep. This is about  $x = 0\cdot5$ ,  $0\cdot55$  and  $0\cdot65$  at  $M_\infty = 1\cdot4$ ,  $2\cdot0$  and  $2\cdot8$  respectively. The change in character of the boundary layer is shown by the jump in the skin-friction coefficient and can also be detected on the schlieren photographs. (Note that the skin friction is deduced from a razor blade calibration for turbulent flow and this cannot be accepted as accurate for a laminar flow.) It is therefore of interest to make laminar boundary-layer calculations.

Such calculations can be made using the basic equations (6.1), (6.2), provided that relations can be established for the various profile parameters. By making use of the Stewartson-Illingworth transformation and writing

$$dY = \frac{\rho}{\rho_\delta} dy \quad (7.3)$$

it follows that the momentum thickness

$$\delta_2 = \int_0^\infty \frac{u}{u_\delta} \left( 1 - \frac{u}{u_\delta} \right) dY \quad (7.4)$$

and energy thickness

$$\delta_3 = \int_0^\infty \frac{u}{u_\delta} \left\{ 1 - \left( \frac{u}{u_\delta} \right)^2 \right\} dY. \quad (7.5)$$

A transformed displacement thickness  $\delta_1^+$  can be defined as

$$\delta_1^+ = \int_0^\infty \left( 1 - \frac{u}{u_\delta} \right) dY. \quad (7.6)$$

For a Prandtl number of unity the total temperature through the boundary layer is constant so that, with  $H_{12}^+ = \frac{\delta_1^+}{\delta_2}$ ,

$$H_{12} = \left( 1 + \frac{\gamma-1}{2} M_\delta^2 \right) H_{12}^+ + \frac{\gamma-1}{2} M_\delta^2. \quad (7.7)$$

Taking a one parameter family of profiles,  $H_{12}^+$  and  $H_{32}$  are uniquely related independently of  $M_\delta$ . Furthermore if two functions  $\varepsilon^+$  and  $D^+$  are defined as follows

$$\left[ \frac{\partial \left( \frac{u}{u_\delta} \right)}{\partial \left( \frac{Y}{\delta_2} \right)} \right]_w = \varepsilon^+(H_{32}) \quad (7.8)$$

and

$$\int_0^\infty \left[ \frac{\partial \left( \frac{u}{u_\delta} \right)}{\partial \left( \frac{Y}{\delta_2} \right)} \right]^2 d\left( \frac{Y}{\delta_2} \right) = D^+(H_{32}) \quad (7.9)$$

and assuming that  $\mu\rho = \text{constant}$  then the skin friction and dissipation coefficients can be expressed as

$$c_f = \frac{2 v_\delta}{u_\delta \delta_2} \varepsilon^+(H_{32}) \quad (7.10)$$

$$c_D = \frac{2 v_\delta}{u_\delta \delta_2} D^+(H_{32}). \quad (7.11)$$

Using Hartree type profiles Walz<sup>20</sup> has developed the following approximate formulae

$$H_{12}^+ = 4.038 - 3.341 (H_{32} - 1.519)^{0.2879} \quad (7.12)$$

$$\varepsilon^+ = 1.299 (H_{32} - 1.519)^{0.6035} \quad (7.13)$$

$$D^+ = 0.1569 + 0.1411 (H_{32} - 1.519) + 3.810 (H_{32} - 1.519)^2 - 11.75 (H_{32} - 1.519)^3. \quad (7.14)$$

These formulae were used in equations (6.1), (6.2) with the starting point at  $x = 0.142$ , using equation (6.8) for the skin friction and taking a flat plate value of  $H_{32} = 1.572$ . The results agree qualitatively with the experimental values of skin friction (Figs. 17, 21, 25). Separation of the laminar boundary layer is predicted to occur close to the point at which transition to turbulence apparently occurs at  $M_\infty = 1.4$  and 2.0. No separation is predicted at  $M_\infty = 2.8$  though the measurements are similar to those at the lower Mach numbers but with transition slightly delayed.

#### *Conclusions.*

The measurements qualitatively confirm the findings for a delta wing<sup>3</sup> on the effects of combined adverse pressure gradient and streamline convergence in promoting low values of skin friction. Some guidance on these low values can be obtained in terms of local flow conditions by using the Ludwig-Tillmann formula modified to take compressibility into account.

The calculation method developed, based on simultaneous integration of the momentum and kinetic energy equations, gives fair agreement with the experiments up to a Mach number of 2.0 but is less successful at higher Mach numbers. The main deficiencies of the method probably lie in the formula for the dissipation coefficient and in the single-parameter (power-low) representation of the velocity profiles; also no allowance is made, other than in the evaluation of the integral parameters and equations, for the effects of flow convergence or divergence or of surface curvatures both streamwise and transverse. Further work is needed to identify separately these effects, all of which are combined in the experiment.

The experiment could well be extended to higher Mach numbers and the measurement of temperature profiles through the boundary layers would add to its value.

## LIST OF SYMBOLS

<i>a</i>	Defined by equation (5.8)
<i>b</i>	Defined by equation (5.5)
<i>c<sub>D</sub></i>	Local dissipation coefficient
<i>C<sub>D</sub></i>	'Mean' dissipation coefficient (equation (7.2))
<i>c<sub>f</sub></i>	Local skin-friction coefficient
<i>c<sub>f<i>i</i></sub></i>	Equivalent incompressible skin-friction coefficient
<i>k</i>	Defined by equation (5.2)
<i>l</i>	Body length (60 inches)
<i>M</i>	Mach number
<i>R</i>	Body radius (inches)
<i>R<sub>x</sub></i>	Radius of curvature in longitudinal direction
<i>Re<sub>l</sub></i>	Reynolds number based on free stream conditions and model length
<i>Re<sub>δ<sub>2</sub></sub></i>	Reynolds number based on local conditions outside boundary layer and momentum thickness
<i>r</i>	Temperature recovery factor
<i>T</i>	Temperature
<i>u</i>	Velocity
<i>u<sub>t</sub></i>	Friction velocity
<i>X</i>	Distance along body axis from nose (inches)
<i>x</i> = $\frac{X}{l}$	
<i>η</i> = $\frac{R}{l}$	
<i>y</i>	Distance from body surface (inches)
<i>Y</i>	Defined by equation (7.3)
<i>φ</i>	Angular position round body
<i>γ</i>	Ratio of specific heats
<i>μ</i>	Viscosity
<i>v</i>	Kinematic viscosity
<i>ρ</i>	Density
<i>τ</i>	Shearing stress
<i>Boundary-layer parameters</i>	
<i>δ</i>	Total thickness
<i>δ<sub>1</sub></i> = $\int_0^\delta \left( 1 + \frac{y}{R} \right) \left( 1 - \frac{\rho u}{\rho_\delta u_\delta} \right) dy$	displacement thickness

LIST OF SYMBOLS—*continued*

$$\delta_2 = \int_0^\delta \left( 1 + \frac{y}{R} \right) \frac{\rho u}{\rho_\delta u_\delta} \left( 1 - \frac{u}{u_\delta} \right) dy \quad \text{momentum thickness}$$

$$\delta_3 = \int_0^\delta \left( 1 + \frac{y}{R} \right) \frac{\rho u}{\rho_\delta u_\delta} \left[ 1 - \left( \frac{u}{u_\delta} \right)^2 \right] dy \quad \text{kinetic energy thickness}$$

$$\delta_1^i = \int_0^\delta \left( 1 + \frac{y}{R} \right) \left( 1 - \frac{u}{u_\delta} \right) dy$$

$$\delta_2^i = \int_0^\delta \left( 1 + \frac{y}{R} \right) \frac{u}{u_\delta} \left( 1 - \frac{u}{u_\delta} \right) dy$$

$$\delta_3^i = \int_0^\delta \left( 1 + \frac{y}{R} \right) \frac{u}{u_\delta} \left[ 1 - \left( \frac{u}{u_\delta} \right)^2 \right] dy$$

$$H_{12} = \frac{\delta_1}{\delta_2}$$

$$H_{32} = \frac{\delta_3}{\delta_2}$$

$$H_{12}^i = \frac{\delta_1^i}{\delta_2^i}$$

$$H_{32}^i = \frac{\delta_3^i}{\delta_2^i}$$

$\delta_1^+$  Transformed laminar boundary-layer displacement thickness defined by equation (7.6)

$$H_{12}^+ = \frac{\delta_1^+}{\delta_2}$$

$\epsilon^+$  Defined by equation (7.8)

$D^+$  Defined by equation (7.9)

*Subscripts*

$\infty$  Refers to free stream

$\delta$  Refers to conditions at edge of boundary layer

$w$  Refers to wall conditions

$t$  Refers to transition point

*Superscript*

\* Refers to intermediate temperature conditions

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TABLE 1

Pressure Distribution and Skin Friction.

x in	$\varphi$ deg	$M_\infty = 0.597$			$M_\infty = 0.801$			$M_\infty = 1.390$			$M_\infty = 1.398$		
		$C_p$	$M_\delta$	$10^3 c_f$									
3.0	0	0.311	0.493	3.92	0.371	0.631	3.66	0.413	1.050	2.52	0.417	1.053	3.88
3.0	90	0.310	0.369		0.374			0.407			0.406		
3.0	-180	0.314			0.368			0.409			0.402		
3.0	-90	0.310			0.368			0.411			0.401		
6.0	0	0.202	0.530	3.70	0.262	0.681	3.70	0.427	1.040	1.91	0.433	1.042	3.79
12.0	0	-0.222	0.666	3.59	-0.218	0.900	3.87	0.153	1.251	0.68	0.151	1.260	1.01
15.0	0	-0.382	0.715	2.80	-0.458	1.012	3.37	-0.040	1.427	2.24	-0.042	1.438	3.56
18.0	0	-0.399	0.720	2.37	-0.499	1.032	2.72	-0.180	1.582	1.78	-0.181	1.593	3.17
21.0	0	-0.313	0.694	2.45	-0.349	0.960	2.37	-0.281	1.715	1.69	-0.281	1.727	3.37
21.0	90	-0.313			-0.348			-0.280			-0.284		
21.0	-180	-0.310			-0.346			-0.279			-0.275		
21.0	-90	-0.313			-0.350			-0.279			-0.280		
24.0	0	-0.145	0.642	1.83	-0.133	0.861	1.62	-0.273			-0.302	1.759	2.72
27.0	0	-0.004	0.598	1.53	0.027	0.788	1.27	-0.256	1.679	0.65	-0.258	1.695	2.23
28.5	0	0.037	0.585	1.42	0.068	0.770	1.25	-0.248	1.669	0.71	-0.208	1.626	1.92
30.0	0	0.058	0.578	1.35	0.095	0.758	1.20	-0.204	1.611	0.74	-0.154	1.561	1.54
31.5	0	0.073	0.573	1.59	0.108	0.752	1.48	-0.116	1.508	1.97	-0.109	1.509	1.58
33.0	0	0.084	0.569	1.47	0.117	0.748	1.39	-0.062	1.450	2.99	-0.070	1.467	1.43
34.5	0	0.090	0.567	1.47	0.123	0.745	1.42	-0.021	1.409	2.90	-0.038	1.434	1.34
36.0	0	0.103	0.563	1.48	0.137	0.739	1.44	0.009	1.379	2.90	-0.010	1.406	1.31
37.5	0	0.115	0.559	1.31	0.149	0.733	1.35	0.034	1.356	2.58	0.016	1.381	1.16
40.0	0	0.158	0.545	1.31	0.197	0.711	1.19	0.091	1.304	2.24	0.093	1.310	1.00
42.0	0	0.183	0.537	1.43	0.221	0.700	1.38	0.196	1.215	1.73	0.166	1.247	0.83
42.0	90	0.181			0.218			0.191			0.166		
42.0	-180	0.182			0.222			0.198			0.168		
42.0	-90	0.178			0.219			0.191			0.165		
44.0	0	0.168	0.542	1.40	0.208	0.707	1.29	0.249	1.173	1.75	0.200	1.219	0.91
45.5	0	0.138	0.552	1.62	0.178	0.720	1.53	0.228	1.182	2.02	0.198	1.221	1.14
47.0	0	0.118	0.558	1.72	0.150	0.733	1.74	0.208	1.206	2.24	0.188	1.229	1.33
48.5	0	0.103	0.563	1.76	0.133	0.740	1.79	0.191	1.219	2.46	0.178	1.237	1.56
50.0	0	0.092	0.567	1.85	0.128	0.743	1.84	0.188	1.222	2.50	0.176	1.238	1.71
51.5	0	0.086	0.569	1.79	0.124	0.745	1.70	0.186	1.223	2.30	0.178	1.237	1.70
53.0	0	0.074	0.573	2.12	0.116	0.748	2.02	0.197	1.215	2.63	0.188	1.229	1.97
54.5	0	0.058	0.578	2.10	0.097	0.757	2.06	0.197	1.215	2.63	0.190	1.227	2.05
56.0	0	0.037	0.585	2.10	0.077	0.766	2.09	0.218	1.197	2.44	0.207	1.213	2.00
57.5	0	-0.000	0.597	2.27	0.038	0.783	2.30	0.229	1.189	2.63	0.222	1.201	2.09
59.0	0	-0.083	0.625	2.47	-0.047	0.822	2.54	0.248	1.174	2.56	0.236	1.189	2.17
59.0	90	-0.074			-0.037			0.254			0.244		
59.0	-180	-0.080			-0.044			0.246			0.237		
59.0	-90	-0.081			-0.045			0.253			0.237		

TABLE 1—continued

x in	$\phi$ deg	$M_\infty = 1.404$			$M_\infty = 1.700$			$M_\infty = 1.996$			$M_\infty = 2.000$		
		$C_p$	$M_\delta$	$10^3 c_f$									
3.0	0	0.417	1.057	3.95	0.360	1.319	1.40	0.333	1.553	1.91	0.325	1.567	1.27
3.0	90	0.403			0.354			0.334			0.327		
3.0	-180	0.400			0.350			0.330			0.324		
3.0	-90	0.408			0.350			0.329			0.323		
6.0	0	0.437	1.043	3.20	0.368	1.311	3.93	0.333	1.553	1.44	0.336	1.556	3.63
12.0	0	0.155	1.261	0.91	0.166	1.501	3.69	0.166	1.737	1.42	0.163	1.749	3.20
15.0	0	-0.040	1.442		0.000	1.696		0.029	1.933	1.46	0.022	1.954	2.54
18.0	0	-0.179	1.598	2.76	-0.115	1.870	2.58	-0.075	2.130	1.12	-0.080	2.154	2.10
21.0	0	-0.282	1.738	2.99	-0.201	2.036	2.75	-0.141	2.298	1.14	-0.150	2.341	2.19
21.0	90	-0.284			-0.199			-0.140			-0.149		
21.0	-180	-0.279			-0.198			-0.141			-0.149		
21.0	-90	-0.277			-0.196			-0.140			-0.148		
24.0	0	-0.299	1.763	2.31	-0.223	2.086	2.34	-0.162	2.360	0.29	-0.173	2.416	1.88
27.0	0	-0.253	1.695	1.93	-0.196	2.025	1.96	-0.139	2.291	0.36	-0.160	2.372	1.73
28.5	0	-0.206	1.632	1.73	-0.168	1.966	1.90	-0.138			-0.140	2.310	1.69
30.0	0	-0.156	1.570	1.46	-0.134	1.903	1.60	-0.134			-0.116	2.244	1.50
31.0	0	-0.110	1.517	1.59	-0.104	1.852	1.67	-0.115			-0.094	2.187	1.47
33.0	0	-0.069	1.472	1.40	-0.074	1.803	1.47	-0.083	2.149	0.30	-0.070	2.134	1.44
34.5	0	-0.038	1.441	1.40	-0.050	1.767	1.38	-0.056	2.089	1.56	-0.051	2.093	1.34
36.0	0	-0.010	1.412	1.45	-0.029	1.737	1.38	-0.025	2.029	2.60	-0.033	2.054	1.33
37.5	0	0.016	1.386	1.26	-0.007	1.706	1.20	0.001	1.981	2.38	-0.015	2.021	1.16
40.0	0	0.089	1.318	1.13	0.046	1.637	1.07	0.038	1.917	2.49	0.024	1.951	1.11
42.0	0	0.174	1.245	0.86	0.123	1.547	0.83	0.118	1.799	2.24	0.095	1.840	0.85
42.0	90	0.171			0.122			0.106			0.092		
42.0	-180	0.174			0.125			0.112			0.100		
42.0	-90	0.169			0.122			0.108			0.093		
44.0	0	0.211	1.215	0.90	0.169	1.498	0.92	0.181	1.718	2.20	0.147	1.770	0.94
45.5	0	0.205	1.219	1.17	0.172	1.495	1.18	0.181	1.719	2.51	0.154	1.761	1.23
47.0	0	0.191	1.231	1.40	0.163	1.504	1.46	0.173	1.728	2.45	0.150	1.765	1.53
48.5	0	0.180	1.241	1.54	0.156	1.512	1.75	0.163	1.740	2.60	0.145	1.772	1.82
50.0	0	0.181	1.239	1.65	0.156	1.512	1.93	0.157	1.748	2.64	0.144	1.773	1.98
51.0	0	0.182	1.239	1.56	0.154	1.513	1.94	0.153	1.753	2.44	0.142	1.776	1.96
53.0	0	0.194	1.229	1.83	0.164	1.504	2.23	0.157	1.748	2.75	0.148	1.767	2.26
54.5	0	0.194	1.229	1.87	0.162	1.505	2.38	0.160	1.744	2.69	0.150	1.766	2.35
56.0	0	0.210	1.216	1.83	0.178	1.489	2.27	0.174	1.727	2.44	0.165	1.746	2.17
57.5	0	0.224	1.204	1.90	0.190	1.476	2.38	0.184	1.715	2.59	0.175	1.734	2.33
59.0	0	0.239	1.192	1.95	0.202	1.464	2.43	0.194	1.702	2.58	0.185	1.721	2.37
59.0	90	0.249			0.211			0.199			0.188		
59.0	-180	0.240			0.204			0.191			0.181		
59.0	-90	0.245			0.206			0.194			0.184		

TABLE 1—*continued*

		$M_{\infty} = 2.002$ $Re_{\ell} = 16.85 \times 10^6$			$M_{\infty} = 2.401$ $Re_{\ell} = 10.03 \times 10^6$			$M_{\infty} = 2.793$ $Re_{\ell} = 5.03 \times 10^6$			$M_{\infty} = 2.799$ $Re_{\ell} = 10.05 \times 10^6$		
x in	$\phi$ deg	$c_p$	$M_{\delta}$	$10^3 c_f$	$c_p$	$M_{\delta}$	$10^3 c_f$	$c_p$	$M_{\delta}$	$10^3 c_f$	$c_p$	$M_{\delta}$	$10^3 c_f$
3.0	0	0.330	1.564	3.50	0.307	1.868	1.11	0.300	2.133	1.49	0.291	2.153	1.06
3.0	90	0.331			0.306			0.298			0.289		
3.0	-180	0.323			0.304			0.299			0.288		
3.0	-90	0.322			0.302			0.294			0.286		
6.0	0	0.337	1.557	2.99	0.312	1.862	3.35	0.301	2.132	1.10	0.292	2.151	2.34
12.0	0	0.162	1.752	2.83	0.165	2.058	2.73	0.168	2.336	1.12	0.158	2.364	2.35
15.0	0	0.019	1.962	2.40	0.038	2.292	2.05	0.056	2.580	0.85	0.040	2.636	1.83
18.0	0	-0.081	2.162	2.01	-0.050	2.528	1.73	-0.028	2.859	0.93	-0.036	2.908	1.57
21.0	0	-0.153	2.354	2.17	-0.109	2.756	1.78	-0.048	2.950	1.06	-0.082	3.162	1.45
21.0	90	-0.152			-0.108			-0.049			-0.080		
21.0	-180	-0.150			-0.110			-0.046			-0.080		
21.0	-90	-0.151			-0.106			-0.041			-0.078		
24.0	0	-0.176	2.430	1.82	-0.130	2.865	1.50	-0.074			-0.111	3.301	1.13
27.0	0	-0.163	2.385	1.60	-0.125	2.626	1.39	-0.065			-0.096	3.261	1.04
28.5	0	-0.142	2.321	1.58	-0.111	2.766	1.39	-0.068	3.050	0.35	-0.089	3.208	1.09
30.0	0	-0.118	2.252	1.35	-0.094	2.691	1.31	-0.066	3.043	0.45	-0.077	3.131	1.21
31.5	0	-0.096	2.196	1.42	-0.080	2.633	1.29	-0.068	3.051	0.87	-0.066	3.064	1.14
33.0	0	-0.074	2.143	1.35	-0.063	2.571	1.24	-0.066	3.039	0.41	-0.056	3.005	1.13
34.5	0	-0.053	2.099	1.27	-0.048	2.522	1.18	-0.061	3.011	0.31	-0.045	2.554	1.23
36.0	0	-0.035	2.061	1.26	-0.036	2.484	1.22	-0.050			-0.031	2.390	1.03
37.5	0	-0.017	2.026	1.11	-0.022	2.444	1.09	-0.037			-0.021	2.844	0.95
40.0	0	0.022	1.957	1.11	0.009	2.361	1.04	0.008	2.724	0.63	0.004	2.751	0.98
42.0	0	0.095	1.842	0.83	0.066	2.233	0.91	0.068	2.547	1.55	0.053	2.600	0.83
42.0	90	0.091			0.064			0.066			0.048		
42.0	-180	0.093			0.069			0.070			0.052		
42.0	-90	0.090			0.064			0.069			0.050		
44.0	0	0.147	1.771	0.88	0.119	2.134	1.00	0.131	2.407	1.96	0.136	2.468	0.93
45.5	0	0.153	1.763	1.22	0.131	2.114	1.33	0.147	2.376	2.19	0.122	2.435	1.21
47.0	0	0.148	1.769	1.55	0.132	2.112	1.53	0.145	2.378	2.06	0.125	2.429	1.36
48.5	0	0.143	1.776	1.79	0.127	2.120	1.78	0.137	2.395	2.18	0.120	2.438	1.56
50.0	0	0.143	1.776	1.93	0.128	2.118	1.90	0.136	2.397	2.20	0.121	2.437	1.68
51.5	0	0.140	1.780	1.87	0.129	2.117	1.77	0.138	2.393	1.73	0.122	2.435	1.51
53.0	0	0.147	1.771	2.13	0.133	2.110	2.08	0.140	2.389	2.06	0.126	2.426	1.77
54.5	0	0.148	1.770	2.20	0.135	2.106	2.12	0.136	2.397	2.20	0.127	2.424	1.83
56.0	0	0.162	1.752	2.04	0.148	2.086	1.94	0.149	2.372	2.01	0.137	2.404	1.72
57.5	0	0.174	1.737	2.14	0.157	2.070	2.09	0.152	2.366	2.19	0.144	2.390	1.87
59.0	0	0.183	1.726	2.14	0.167	2.056	2.15	0.167	2.337	2.05	0.155	2.369	1.88
59.0	90	0.186			0.170			0.172			0.159		
59.0	-180	0.176			0.164			0.168			0.152		
59.0	-90	0.181			0.167			0.166			0.156		

TABLE 2

## Velocity Profiles.

Table 2a  $M_\infty = 0.597$   $Re_\delta = 9.98 \times 10^6$ 

$x = 0.4$		$x = 0.475$		$x = 0.55$							
$y$ in	$M$	$\frac{u}{u_\delta}$	$\frac{u}{u_\delta}$	$y$ in	$M$	$\frac{u}{u_\delta}$	$\frac{u}{u_\delta}$	$y$ in	$M$	$\frac{u}{u_\delta}$	$\frac{u}{u_\delta}$
0.0010	0.3251	0.5201	0.5217	0.0010	0.2795	0.4702	0.4715	0.0010	0.2512	0.4505	0.4517
0.0013	0.3276	0.5240	0.5256	0.0013	0.2835	0.4774	0.4787	0.0013	0.2583	0.4631	0.4643
0.0015	0.3303	0.5283	0.5299	0.0018	0.2914	0.4914	0.4927	0.0015	0.2639	0.4730	0.4742
0.0020	0.3441	0.5498	0.5514	0.0043	0.3170	0.5367	0.5381	0.0018	0.2735	0.4900	0.4912
0.0030	0.3624	0.5784	0.5800	0.0058	0.3338	0.5665	0.5678	0.0020	0.2748	0.4922	0.4934
0.0045	0.3847	0.6132	0.6148	0.0074	0.3447	0.5854	0.5868	0.0025	0.2788	0.4993	0.5005
0.0060	0.4091	0.6510	0.6525	0.0090	0.3592	0.6107	0.6121	0.0035	0.2890	0.5174	0.5186
0.0075	0.4321	0.6864	0.6879	0.0104	0.3692	0.6281	0.6295	0.0051	0.3034	0.5427	0.5440
0.0090	0.4553	0.7219	0.7233	0.0105	0.3701	0.6297	0.6310	0.0065	0.3142	0.5616	0.5629
0.0098	0.4728	0.7487	0.7500	0.0107	0.3692	0.6281	0.6295	0.0081	0.3245	0.5797	0.5810
0.0100	0.4744	0.7511	0.7525	0.0112	0.3721	0.6333	0.6346	0.0097	0.3332	0.5950	0.5963
0.0103	0.4762	0.7538	0.7552	0.0120	0.3864	0.6579	0.6592	0.0105	0.3297	0.5888	0.5901
0.0105	0.4771	0.7552	0.7565	0.0122	0.3846	0.6548	0.6562	0.0108	0.3340	0.5964	0.5977
0.0108	0.4830	0.7642	0.7656	0.0138	0.3975	0.6770	0.6783	0.0110	0.3400	0.6069	0.6081
0.0115	0.4882	0.7721	0.7734	0.0148	0.4072	0.6938	0.6951	0.0112	0.3417	0.6099	0.6112
0.0117	0.4969	0.7852	0.7865	0.0152	0.4143	0.7059	0.7072	0.0113	0.3422	0.6107	0.6120
0.0132	0.5146	0.8121	0.8132	0.0168	0.4252	0.7245	0.7257	0.0115	0.3432	0.6124	0.6137
0.0140	0.5215	0.8224	0.8235	0.0174	0.4302	0.7331	0.7343	0.0120	0.3412	0.6090	0.6103
0.0146	0.5355	0.8434	0.8444	0.0184	0.4376	0.7457	0.7469	0.0131	0.3485	0.6218	0.6231
0.0162	0.5535	0.8703	0.8712	0.0199	0.4519	0.7698	0.7709	0.0140	0.3545	0.6322	0.6335
0.0165	0.5498	0.8648	0.8657	0.0200	0.4519	0.7698	0.7709	0.0147	0.3573	0.6371	0.6384
0.0176	0.5707	0.8960	0.8967	0.0203	0.4565	0.7777	0.7788	0.0162	0.3663	0.6528	0.6540
0.0190	0.5883	0.9219	0.9225	0.0206	0.4580	0.7801	0.7812	0.0170	0.3692	0.6579	0.6592
0.0190	0.5786	0.9076	0.9082	0.0207	0.3050	0.5157	0.5170	0.0177	0.3759	0.6695	0.6708
0.0192	0.5845	0.9163	0.9169	0.0211	0.4642	0.7906	0.7916	0.0193	0.3853	0.6858	0.6870
0.0193	0.5890	0.9229	0.9235	0.0215	0.4678	0.7967	0.7978	0.0196	0.3836	0.6828	0.6840
0.0195	0.5902	0.9247	0.9253	0.0221	0.4716	0.8031	0.8042	0.0207	0.3862	0.6873	0.6885
0.0200	0.5959	0.9332	0.9337	0.0236	0.4875	0.8297	0.8307	0.0209	0.3915	0.6965	0.6977
0.0202	0.5937	0.9299	0.9304	0.0240	0.4875	0.8297	0.8307	0.0209	0.3925	0.6983	0.6995
0.0210	0.6050	0.9466	0.9470	0.0252	0.4973	0.8461	0.8470	0.0211	0.3946	0.7019	0.7031
0.0215	0.6019	0.9420	0.9424	0.0266	0.5082	0.8644	0.8652	0.0215	0.3973	0.7066	0.7078
0.0225	0.6150	0.9612	0.9615	0.0267	0.5082	0.8644	0.8652	0.0216	0.3982	0.7081	0.7093
0.0226	0.6145	0.9604	0.9607	0.0282	0.5182	0.8809	0.8816	0.0222	0.3982	0.7081	0.7093
0.0239	0.6253	0.9763	0.9765	0.0293	0.5260	0.8940	0.8946	0.0232	0.4035	0.7173	0.7185
0.0239	0.6223	0.9719	0.9721	0.0298	0.5292	0.8992	0.8998	0.0237	0.4059	0.7215	0.7227
0.0252	0.6291	0.9818	0.9819	0.0300	0.5356	0.9097	0.9102	0.0248	0.4128	0.7333	0.7344
0.0253	0.6344	0.9895	0.9896	0.0303	0.5344	0.9077	0.9083	0.0263	0.4220	0.7491	0.7502
0.0269	0.6380	0.9948	0.9948	0.0308	0.5375	0.9128	0.9134	0.0265	0.4229	0.7508	0.7519
0.0275	0.6385	0.9955	0.9955	0.0314	0.5418	0.9200	0.9205	0.0278	0.4311	0.7649	0.7659
0.0281	0.6404	0.9983	0.9983	0.0317	0.5424	0.9210	0.9215	0.0292	0.4384	0.7774	0.7784
0.0282	0.6410	0.9992	0.9992	0.0333	0.5528	0.9381	0.9385	0.0295	0.4415	0.7827	0.7837
0.0283	0.6404	0.9983	0.9983	0.0340	0.5589	0.9480	0.9483	0.0304	0.4395	0.7793	0.7803
0.0286	0.6401	0.9978	0.9978	0.0348	0.5625	0.9539	0.9542	0.0307	0.4448	0.7883	0.7894
0.0290	0.6410	0.9992	0.9992	0.0363	0.5707	0.9673	0.9675	0.0310	0.4472	0.7924	0.7934
0.0292	0.6410	0.9992	0.9992	0.0365	0.5719	0.9693	0.9695	0.0310	0.4484	0.7945	0.7955
0.0300	0.6410	0.9992	0.9992	0.0379	0.5764	0.9767	0.9769	0.0312	0.4495	0.7964	0.7974
0.0300	0.6408	0.9988	0.9988	0.0390	0.5821	0.9860	0.9861	0.0315	0.4479	0.7936	0.7946
0.0315	0.6421	1.0008	1.0008	0.0394	0.5833	0.9879	0.9880	0.0320	0.4517	0.8001	0.8010
0.0413	0.6418	1.0002	1.0002	0.0400	0.5839	0.9888	0.9889	0.0330	0.4563	0.8079	0.8089
0.0522	0.6421	1.0008	1.0008	0.0403	0.5861	0.9924	0.9925	0.0338	0.4660	0.8246	0.8254
0.0595	0.6418	1.0002	1.0002	0.0408	0.5861	0.9924	0.9925	0.0346	0.4645	0.8219	0.8228
				0.0408	0.5866	0.9933	0.9933	0.0362	0.4790	0.8467	0.8475
				0.0418	0.5873	0.9943	0.9944	0.0367	0.4819	0.8515	0.8522
				0.0434	0.5900	0.9988	0.9988	0.0377	0.4874	0.8609	0.8617
				0.0435	0.5895	0.9979	0.9979	0.0392	0.4910	0.8669	0.8677
				0.0449	0.5900	0.9988	0.9988	0.0394	0.4916	0.8680	0.8688
				0.0460	0.5900	0.9988	0.9988	0.0401	0.4936	0.8713	0.8720
				0.0460	0.5900	0.9988	0.9988	0.0404	0.4980	0.8788	0.8795
				0.0464	0.5905	0.9996	0.9996	0.0406	0.4987	0.8799	0.8806
				0.0561	0.5905	0.9996	0.9996	0.0408	0.5026	0.8866	0.8872
				0.0646	0.5912	1.0006	1.0006	0.0408	0.4979	0.8786	0.8792
				0.0740	0.5912	1.0006	1.0006	0.0411	0.5005	0.8831	0.8838
				0.0840	0.5917	1.0015	1.0015	0.0416	0.5020	0.8855	0.8861
								0.0427	0.5066	0.8934	0.8940
								0.0437	0.5126	0.9035	0.9041
								0.0442	0.5158	0.9089	0.9094
								0.0457	0.5248	0.9240	0.9245
								0.0465	0.5223	0.9198	0.9202
								0.0466	0.5254	0.9250	0.9255
								0.0473	0.5306	0.9337	0.9341
								0.0489	0.5380	0.9460	0.9464
								0.0492	0.5374	0.9451	0.9454
								0.0505	0.5441	0.9563	0.9566
								0.0533	0.5561	0.9763	0.9765
								0.0559	0.5592	0.9814	0.9815
								0.0562	0.5633	0.9882	0.9882
								0.0588	0.5673	0.9949	0.9949
								0.0622	0.5685	0.9969	0.9969
								0.0660	0.5708	1.0006	1.0006
								0.0716	0.5696	0.9985	0.9987
								0.0726	0.5690	0.9978	0.9978
								0.0726	0.5678	0.9958	0.9958
								0.0757	0.5708	1.0006	1.0006
								0.0855	0.5708	1.0006	1.0006
								0.0921	0.5690	0.9978	0.9978
								0.1012	0.5703	0.9998	0.9998
								0.1115	0.5703	0.9998	0.9998

Table 2a (Contd)

x = 0.7				x = 0.833				x = 0.983			
y in	M	$\frac{u}{u_0}$	$\frac{u}{u_0}$	y in	M	$\frac{u}{u_0}$	$\frac{u}{u_0}$	y in	M	$\frac{u}{u_0}$	$\frac{u}{u_0}$
		r = 0.89	r = 1			r = 0.89	r = 1			r = 0.89	r = 1
0.0010	0.2271	0.4312	0.4322	0.0010	0.3129	0.5631	0.5644	0.0010	0.4084	0.6688	0.6702
0.0012	0.2282	0.4333	0.4343	0.0015	0.3204	0.5763	0.5776	0.0012	0.4088	0.6694	0.6709
0.0015	0.2315	0.4395	0.4406	0.0017	0.3172	0.5707	0.5720	0.0015	0.4152	0.6796	0.6811
0.0018	0.2341	0.4443	0.4454	0.0020	0.3232	0.5814	0.5827	0.0020	0.4223	0.6909	0.6923
0.0020	0.2373	0.4504	0.4515	0.0022	0.3289	0.5914	0.5927	0.0020	0.4275	0.6991	0.7005
0.0025	0.2436	0.4623	0.4634	0.0027	0.3348	0.6017	0.6030	0.0025	0.4389	0.7170	0.7184
0.0030	0.2454	0.4655	0.4666	0.0031	0.3415	0.6135	0.6148	0.0030	0.4508	0.7358	0.7372
0.0035	0.2498	0.4738	0.4749	0.0038	0.3480	0.6250	0.6263	0.0035	0.4541	0.7411	0.7424
0.0040	0.2528	0.4795	0.4806	0.0043	0.3544	0.6363	0.6376	0.0040	0.4592	0.7492	0.7505
0.0045	0.2545	0.4826	0.4837	0.0048	0.3605	0.6470	0.6482	0.0050	0.4713	0.7680	0.7693
0.0050	0.2587	0.4906	0.4917	0.0054	0.3637	0.6526	0.6539	0.0060	0.4791	0.7803	0.7816
0.0060	0.2632	0.4990	0.5001	0.0063	0.3707	0.6649	0.6661	0.0072	0.4890	0.7958	0.7970
0.0070	0.2674	0.5067	0.5079	0.0074	0.3747	0.6719	0.6731	0.0082	0.4927	0.8016	0.8027
0.0080	0.2729	0.5172	0.5183	0.0085	0.3826	0.6856	0.6869	0.0092	0.4972	0.8086	0.8097
0.0090	0.2757	0.5225	0.5235	0.0095	0.3845	0.6890	0.6902	0.0103	0.5038	0.8188	0.8199
0.0100	0.2775	0.5257	0.5269	0.0105	0.3873	0.6939	0.6951	0.0108	0.5105	0.8293	0.8304
0.0101	0.2846	0.5390	0.5402	0.0108	0.3941	0.7056	0.7068	0.0112	0.5125	0.8323	0.8333
0.0104	0.2841	0.5379	0.5391	0.0111	0.3913	0.7009	0.7021	0.0115	0.5125	0.8323	0.8333
0.0105	0.2867	0.5429	0.5440	0.0114	0.3918	0.7016	0.7028	0.0120	0.5102	0.8288	0.8299
0.0109	0.2849	0.5396	0.5407	0.0117	0.3928	0.7035	0.7046	0.0120	0.5144	0.8353	0.8363
0.0111	0.2849	0.5396	0.5407	0.0120	0.3937	0.7049	0.7061	0.0125	0.5129	0.8330	0.8341
0.0116	0.2902	0.5493	0.5505	0.0125	0.3947	0.7076	0.7079	0.0130	0.5150	0.8362	0.8372
0.0120	0.2876	0.5445	0.5456	0.0130	0.3984	0.7132	0.7144	0.0135	0.5186	0.8419	0.8428
0.0125	0.2902	0.5493	0.5505	0.0135	0.4013	0.7182	0.7194	0.0140	0.5182	0.8411	0.8421
0.0130	0.2916	0.5520	0.5532	0.0140	0.4003	0.7165	0.7176	0.0150	0.5216	0.8465	0.8474
0.0136	0.2902	0.5493	0.5505	0.0145	0.4039	0.7228	0.7240	0.0160	0.5228	0.8498	0.8508
0.0140	0.2978	0.5636	0.5648	0.0151	0.4021	0.7197	0.7208	0.0170	0.5258	0.8529	0.8538
0.0150	0.2978	0.5636	0.5648	0.0161	0.4058	0.7260	0.7271	0.0181	0.5299	0.8593	0.8602
0.0160	0.3028	0.5729	0.5740	0.0171	0.4112	0.7354	0.7365	0.0192	0.5313	0.8614	0.8623
0.0170	0.3028	0.5729	0.5740	0.0182	0.4147	0.7416	0.7427	0.0203	0.5333	0.8645	0.8654
0.0180	0.3090	0.5845	0.5857	0.0193	0.4130	0.7385	0.7396	0.0206	0.5336	0.8650	0.8658
0.0190	0.3104	0.5870	0.5881	0.0202	0.4200	0.7507	0.7518	0.0210	0.5355	0.8680	0.8698
0.0195	0.3096	0.5855	0.5867	0.0205	0.4192	0.7494	0.7505	0.0212	0.5354	0.8678	0.8686
0.0197	0.3128	0.5914	0.5926	0.0207	0.4167	0.7450	0.7461	0.0217	0.5366	0.8696	0.8704
0.0200	0.3104	0.5870	0.5881	0.0210	0.4175	0.7463	0.7474	0.0217	0.5378	0.8715	0.8723
0.0203	0.3149	0.5954	0.5965	0.0212	0.4185	0.7480	0.7491	0.0223	0.5385	0.8726	0.8734
0.0205	0.3136	0.5929	0.5941	0.0215	0.4181	0.7474	0.7484	0.0227	0.5399	0.8747	0.8755
0.0210	0.3172	0.5997	0.6009	0.0218	0.4206	0.7517	0.7528	0.0232	0.5378	0.8715	0.8723
0.0215	0.3159	0.5973	0.5985	0.0222	0.4216	0.7534	0.7545	0.0239	0.5387	0.8728	0.8737
0.0220	0.3206	0.6060	0.6072	0.0227	0.4225	0.7551	0.7562	0.0248	0.5433	0.8799	0.8807
0.0225	0.3196	0.6041	0.6052	0.0230	0.4250	0.7594	0.7605	0.0259	0.5454	0.8831	0.8839
0.0230	0.3206	0.6060	0.6072	0.0233	0.4225	0.7551	0.7562	0.0270	0.5440	0.8811	0.8819
0.0235	0.3219	0.6084	0.6095	0.0243	0.4284	0.7653	0.7664	0.0280	0.5512	0.8921	0.8928
0.0245	0.3275	0.6188	0.6199	0.0249	0.4294	0.7670	0.7680	0.0290	0.5519	0.8932	0.8939
0.0255	0.3320	0.6271	0.6282	0.0260	0.4318	0.7712	0.7722	0.0300	0.5525	0.8941	0.8948
0.0265	0.3332	0.6294	0.6305	0.0270	0.4352	0.7770	0.7780	0.0306	0.5584	0.9031	0.9038
0.0275	0.3364	0.6353	0.6364	0.0280	0.4369	0.7799	0.7809	0.0308	0.5591	0.9042	0.9049
0.0285	0.3386	0.5394	0.6405	0.0290	0.4393	0.7840	0.7850	0.0311	0.5584	0.9031	0.9038
0.0293	0.3477	0.6562	0.6573	0.0301	0.4426	0.7897	0.7907	0.0316	0.5594	0.9047	0.9053
0.0295	0.3453	0.6518	0.6529	0.0306	0.4460	0.7956	0.7966	0.0316	0.5594	0.9047	0.9053
0.0298	0.3432	0.6478	0.6490	0.0308	0.4469	0.7972	0.7982	0.0321	0.5600	0.9055	0.9062
0.0301	0.3482	0.6570	0.6581	0.0310	0.4476	0.7984	0.7994	0.0326	0.5612	0.9075	0.9081
0.0303	0.3482	0.6570	0.6581	0.0314	0.4469	0.7972	0.7982	0.0331	0.5620	0.9086	0.9092
0.0308	0.3482	0.6570	0.6581	0.0316	0.4456	0.7950	0.7960	0.0337	0.5628	0.9099	0.9106
0.0313	0.3503	0.6609	0.6620	0.0318	0.4456	0.7950	0.7960	0.0347	0.5672	0.9166	0.9171
0.0317	0.3535	0.6669	0.6680	0.0324	0.4491	0.8009	0.8019	0.0357	0.5666	0.9157	0.9163
0.0323	0.3556	0.6708	0.6719	0.0329	0.4514	0.8049	0.8058	0.0365	0.5691	0.9195	0.9201
0.0328	0.3556	0.6708	0.6719	0.0335	0.4521	0.8061	0.8071	0.0368	0.5690	0.9193	0.9199
0.0333	0.3565	0.6724	0.6736	0.0340	0.4537	0.8089	0.8098	0.0379	0.5709	0.9223	0.9228
0.0343	0.3597	0.6783	0.6794	0.0345	0.4546	0.8104	0.8113	0.0390	0.5734	0.9261	0.9266
0.0349	0.3579	0.6750	0.6761	0.0350	0.4595	0.8185	0.8194	0.0400	0.5778	0.9328	0.9333
0.0352	0.3617	0.6821	0.6832	0.0360	0.4600	0.8197	0.8206	0.0400	0.5764	0.9307	0.9312
0.0363	0.3647	0.6874	0.6885	0.0367	0.4605	0.8206	0.8215	0.0403	0.5790	0.9347	0.9351
0.0373	0.3675	0.6928	0.6939	0.0370	0.4631	0.8251	0.8260	0.0405	0.5783	0.9336	0.9341
0.0382	0.3735	0.7037	0.7047	0.0380	0.4654	0.8289	0.8298	0.0410	0.5805	0.9369	0.9374
0.0385	0.3741	0.7049	0.7059	0.0392	0.4662	0.8304	0.8313	0.0410	0.5793	0.9351	0.9355
0.0388	0.3728	0.7025	0.7035	0.0402	0.4718	0.8400	0.8408	0.0415	0.5805	0.9369	0.9374
0.0390	0.3719	0.7009	0.7019	0.0402	0.4700	0.8368	0.8377	0.0420	0.5805	0.9369	0.9374
0.0394	0.3735	0.7037	0.7047	0.0403	0.4725	0.8412	0.8420	0.0425	0.5811	0.9378	0.9382
0.0396	0.3735	0.7037	0.7047	0.0405	0.4733	0.8426	0.8434	0.0430	0.5813	0.9382	0.9386
0.0401	0.3765	0.7092	0.7103	0.0408	0.4718	0.8400	0.8408	0.0441	0.5831	0.9409	0.9413
0.0405	0.3784	0.7128	0.7138	0.0410	0.4713	0.8391	0.8400	0.0451	0.5855	0.9445	0.9449
0.0410	0.3793	0.7144	0.7154	0.0413	0.4728	0.8417	0.8426	0.0463	0.5874	0.9474	0.9478
0.0415	0.3804	0.7163	0.7174	0.0418	0.4745	0.8446	0.8454	0.0465	0.5886	0.9492	0.9496
0.0420	0.3842	0.7233	0.7243	0.0423	0.4767	0.8483	0.8491	0.0473	0.5898	0.9510	0.9514
0.0425	0.3861	0.7268	0.7278	0.0429	0.4750	0.8472	0.8480	0.0484	0.5932	0.9563	0.9566
0.0435	0.3861	0.7268	0.7278	0.0434	0.4775	0.8498	0.8505	0.0494	0.5934	0.9565	0.9568
0.0437	0.3900	0.7340	0.7350	0.0439	0.4803	0.8546	0.8553	0.0562	0.6017	0.9691	0.9693
0.0445	0.3896	0.7333	0.7343	0.0445	0.4812	0.8560	0.8567	0.0626	0.6115	0.9838	0.9839
0.0455	0.3906	0.7351	0.7362	0.0455	0.4833	0.8596	0.8604	0.0661	0.6149	0.9890	0.9890
0.0465	0.3980	0.7486</td									

Table 2b  $\frac{U}{U_\infty} = 1.398$   $Re_\delta = 10.08 \times 10^6$ 

$x = 0.4$												$x = 0.475$												$x = 0.55$																																																																																																																																																																																																																																																																																																																																																																																																																																																																																				
$y$	$in$	$M$	$\frac{u}{u_\delta}$	$\frac{u}{u_\delta}$	$y$	$in$	$M$	$\frac{u}{u_\delta}$	$\frac{u}{u_\delta}$	$y$	$in$	$M$	$\frac{u}{u_\delta}$	$\frac{u}{u_\delta}$	$y$	$in$	$M$	$\frac{u}{u_\delta}$	$\frac{u}{u_\delta}$	$y$	$in$	$M$	$\frac{u}{u_\delta}$	$\frac{u}{u_\delta}$	$y$	$in$	$M$	$\frac{u}{u_\delta}$	$\frac{u}{u_\delta}$																																																																																																																																																																																																																																																																																																																																																																																																																																																																															
00010	0.8772	0.5808	0.5891	0.0010	0.7068	0.5036	0.5109	0.0010	0.5293	0.4168	0.4225	0.0013	0.8877	0.5869	0.5952	0.0013	0.7107	0.5061	0.5135	0.0013	0.5338	0.4201	0.4259	0.0015	0.9078	0.5985	0.6068	0.0015	0.7633	0.5402	0.5476	0.0015	0.5515	0.4333	0.4392																																																																																																																																																																																																																																																																																																																																																																																																																																																																									
00017	0.9240	0.6078	0.6161	0.0018	0.7527	0.5334	0.5408	0.0018	0.5602	0.4398	0.4457	0.0020	0.9520	0.6237	0.6319	0.0033	0.8393	0.5882	0.5957	0.0023	0.5848	0.4580	0.4641	0.0025	0.9929	0.6466	0.6547	0.0049	0.8956	0.6229	0.6303	0.0028	0.6040	0.4721	0.4783																																																																																																																																																																																																																																																																																																																																																																																																																																																																									
00030	1.0258	0.6647	0.6726	0.0065	0.9553	0.6588	0.6661	0.0042	0.6479	0.5042	0.5104	0.0045	1.1103	0.7099	0.7174	0.0081	1.0003	0.6852	0.6923	0.0057	0.6854	0.5312	0.5375	00060	1.1905	0.7511	0.7581	0.0096	1.0586	0.7187	0.7254	0.0073	0.7165	0.5533	0.5597																																																																																																																																																																																																																																																																																																																																																																																																																																																																									
00075	1.2622	0.7866	0.7930	0.0104	1.0823	0.7320	0.7386	0.0089	0.7540	0.5797	0.5861	00090	1.3274	0.8177	0.8235	0.0107	1.0881	0.7353	0.7418	0.0105	0.7779	0.5963	0.6026	00098	1.3838	0.8437	0.8489	0.0109	1.0960	0.7397	0.7461	0.0108	0.7857	0.6016	0.6080	00100	1.3873	0.8453	0.8504	0.0112	1.1076	0.7461	0.7525	0.0109	0.8002	0.6116	0.6180																																																																																																																																																																																																																																																																																																																																																																																																																																																													
00103	1.3961	0.8493	0.8543	0.0112	1.1122	0.7486	0.7550	0.0110	0.7936	0.6071	0.6134	00105	1.4014	0.8517	0.8567	0.0127	1.1635	0.7765	0.7825	0.0113	0.7986	0.6105	0.6169	00108	1.4118	0.8564	0.8612	0.0143	1.2129	0.8028	0.8083	0.0118	0.8036	0.6140	0.6203	00110	1.4031	0.8525	0.8574	0.0143	1.2242	0.8087	0.8141	0.0123	0.8185	0.6242	0.6305																																																																																																																																																																																																																																																																																																																																																																																																																																																													
00112	1.4309	0.8649	0.8695	0.0158	1.2627	0.8286	0.8336	0.0138	0.8519	0.6467	0.6530	00117	1.4444	0.8708	0.8753	0.0169	1.2955	0.8452	0.8499	0.0140	0.8602	0.6523	0.6586	00130	1.4729	0.8832	0.8874	0.0174	1.3054	0.8502	0.8547	0.0154	0.8903	0.6724	0.6785	00132	1.4893	0.8903	0.8942	0.0190	1.3541	0.8742	0.8782	0.0167	0.9201	0.6919	0.6979	00146	1.5390	0.9113	0.9146	0.0195	1.3658	0.8799	0.8837	0.0170	0.9235	0.6942	0.7001	00155	1.5516	0.9165	0.9197	0.0203	1.3874	0.8903	0.8938	0.0185	0.9584	0.7168	0.7226	00162	1.5764	0.9267	0.9295	0.0205	1.3922	0.8925	0.8960	0.0206	1.0025	0.7449	0.7504	00176	1.5948	0.9342	0.9367	0.0206	1.3860	0.8896	0.8931	0.0207	1.0013	0.7441	0.7496	00180	1.6068	0.9390	0.9413	0.0203	1.3974	0.8950	0.8985	0.0209	1.0064	0.7473	0.7528	00190	1.6629	0.9611	0.9627	0.0211	1.4018	0.8971	0.9005	0.0211	1.0150	0.7527	0.7581	00193	1.6645	0.9617	0.9632	0.0221	1.4415	0.9157	0.9186	0.0215	1.0150	0.7527	0.7581	00195	1.6702	0.9639	0.9653	0.0226	1.4550	0.9220	0.9246	0.0220	1.0301	0.7622	0.7674	00197	1.6615	0.9606	0.9621	0.0236	1.4808	0.9338	0.9361	0.0225	1.0447	0.7712	0.7764	00200	1.6789	0.9673	0.9685	0.0248	1.5050	0.9446	0.9466	0.0240	1.0748	0.7897	0.7946	00205	1.6845	0.9694	0.9707	0.0257	1.5249	0.9535	0.9552	0.0255	1.1115	0.8118	0.8164	00205	1.6687	0.9634	0.9648	0.0262	1.5375	0.9591	0.9605	0.0263	1.1209	0.8174	0.8219	00205	1.6687	0.9634	0.9648	0.0273	1.5546	0.9665	0.9677	0.0270	1.1447	0.8315	0.8358	00210	1.6974	0.9743	0.9754	0.0274	1.5595	0.9686	0.9698	0.0286	1.1738	0.8486	0.8525	00216	1.7017	0.9759	0.9769	0.0288	1.5861	0.9801	0.9808	0.0304	1.2054	0.8668	0.8703	00225	1.7185	0.9823	0.9830	0.0288	1.5833	0.9789	0.9797	0.0307	1.2040	0.8650	0.8695	00229	1.7129	0.9802	0.9810	0.0300	1.6006	0.9863	0.9868	0.0307	1.2169	0.8733	0.8767	00239	1.7380	0.9896	0.9900	0.0300	1.6033	0.9874	0.9879	0.0310	1.2184	0.8742	0.8776	00241	1.7353	0.9885	0.9890	0.0303	1.6032	0.9873	0.9878	0.0312	1.2197	0.8749	0.8783	00253	1.7533	0.9952	0.9954	0.0304	1.6073	0.9891	0.9895	0.0317	1.2326	0.8822	0.8854	00266	1.7587	0.9971	0.9973	0.0305	1.6044	0.9879	0.9883	0.0322	1.2453	0.8894	0.8924	00269	1.7628	0.9987	0.9987	0.0308	1.6130	0.9915	0.9918	0.0338	1.2789	0.9080	0.9106	00281	1.7615	0.9982	0.9982	0.0314	1.6192	0.9941	0.9943	0.0338	1.2836	0.9106	0.9131	00283	1.7628	0.9987	0.9987	0.0323	1.6228	0.9956	0.9957	0.0353	1.3094	0.9246	0.9268	00286	1.7628	0.9987	0.9987	0.0335	1.6337	1.0001	1.0001	0.0365	1.3360	0.9389	0.9407	00287	-1.7670	-1.0002	-1.0002	0.0338	1.6293	0.9983	0.9984	0.0369	1.3414	0.9418	0.9435	00348	-1.7670	-1.0002	-1.0002	0.0340	1.6278	0.9977	0.9977	0.0385	1.3665	0.9550	0.9564	00449	1.7737	1.0026	1.0025	0.0354	1.6317	0.9993	0.9993	0.0401	1.3916	0.9681	0.9691	00585	1.7777	1.0041	1.0039	0.0360	1.6324	0.9996	0.9996	0.0404	1.3916	0.9681	0.9691	00464	0.0464	1.6325	0.9996	0.9997	0.0406	1.3993	0.9721	0.9730	00558	0.0558	1.6290	0.9982	0.9982	0.0406	1.3981	0.9715	0.9724	00660	0.0660	1.6313	0.9991	0.9992	0.0408	1.3982	0.9715	0.9724	00414	0.0414	1.4081	0.9766	0.9773	00418	0.0418	1.4190	0.9822	0.9827	00430	0.0430	1.4199	0.9827	0.9832	00435	0.0435	1.4308	0.9882	0.9886	00437	0.0437	1.4308	0.9882	0.9886	00450	0.0450	1.4409	0.9933	0.9935	00463	0.0463	1.4468	0.9953	0.9964	00465	0.0465	1.4496	0.9976	0.9977	00480	0.0480	1.4570	1.0014	1.0013	00502	0.0502	1.4553	1.0005	1.0005	00524	0.0524	1.4520	0.9989	0.9989	00626	0.0626	1.4499	0.9978	0.9979	00723	0.0723	1.4478	0.9967	0.9968	00820	0.0820	1.4499	0.9978	0.9979

Table 2b (Contd)

 $x = 0.7$  $x = 0.833$  $x = 0.983$ 

$y$	$M$	$\frac{u}{u_0}$	$\frac{u}{u_0}$	$y$	$M$	$\frac{u}{u_0}$	$\frac{u}{u_0}$	$y$	$M$	$\frac{u}{u_0}$	$\frac{u}{u_0}$		
0.0010	0.4669	0.4049	0.4096	0.0010	0.6508	0.5661	0.5712	0.0010	0.7148	0.6330	0.6378		
0.0012	0.4710	0.4083	0.4131	0.0012	0.6662	0.5785	0.5837	0.0012	0.7235	0.6401	0.6448		
0.0015	0.4773	0.4136	0.4183	0.0015	0.6811	0.5905	0.5956	0.0015	0.7361	0.6502	0.6550		
0.0018	0.4747	0.4114	0.4162	0.0017	0.6909	0.5983	0.6034	0.0017	0.7438	0.6555	0.6612		
0.0020	0.4870	0.4217	0.4265	0.0017	0.6861	0.5945	0.5996	0.0020	0.7559	0.6662	0.6709		
0.0025	0.4948	0.4281	0.4330	0.0020	0.6932	0.6002	0.6053	0.0025	0.7717	0.6798	0.6834		
0.0035	0.5028	0.4347	0.4396	0.0025	0.7090	0.6127	0.6178	0.0030	0.7944	0.6967	0.7013		
0.0045	0.5126	0.4428	0.4478	0.0030	0.7249	0.6253	0.6304	0.0030	0.7944	0.6967	0.7013		
0.0055	0.5248	0.4529	0.4579	0.0035	0.7316	0.6306	0.6357	0.0035	0.8055	0.7055	0.7100		
0.0080	0.5463	0.4705	0.4756	0.0045	0.7468	0.6425	0.6476	0.0045	0.8372	0.7302	0.7345		
0.0101	0.5700	0.4899	0.4950	0.0055	0.7595	0.6524	0.6574	0.0056	0.8572	0.7457	0.7499		
0.0104	0.5732	0.4925	0.4977	0.0065	0.7740	0.6637	0.6687	0.0066	0.8734	0.7581	0.7621		
0.0105	0.5665	0.4870	0.4922	0.0076	0.7899	0.6760	0.6809	0.0077	0.8907	0.7713	0.7752		
0.0106	0.5721	0.4915	0.4967	0.0086	0.7959	0.6806	0.6854	0.0087	0.8998	0.7782	0.7820		
0.0109	0.5697	0.4896	0.4948	0.0097	0.8036	0.6865	0.6914	0.0098	0.9119	0.7872	0.7910		
0.0111	0.5795	0.4976	0.5028	0.0108	0.8136	0.6942	0.6990	0.0098	0.9148	0.7894	0.7932		
0.0116	0.5795	0.4976	0.5028	0.0108	0.8150	0.6952	0.7000	0.0108	0.9255	0.7973	0.8010		
0.0125	0.5892	0.5054	0.5106	0.0109	0.8175	0.6971	0.7019	0.0108	0.9192	0.7927	0.7965		
0.0136	0.5972	0.5119	0.5171	0.0111	0.8229	0.7013	0.7060	0.0112	0.9253	0.7973	0.8010		
0.0146	0.6046	0.5178	0.5231	0.0114	0.8211	0.6999	0.7046	0.0115	0.9295	0.8005	0.8041		
0.0170	0.6311	0.5390	0.5443	0.0114	0.8211	0.6999	0.7046	0.0116	0.9293	0.8003	0.8039		
0.0195	0.6561	0.5589	0.5643	0.0114	0.8193	0.6985	0.7033	0.0120	0.9307	0.8013	0.8049		
0.0195	0.6532	0.5566	0.5620	0.0117	0.8229	0.7013	0.7060	0.0125	0.9336	0.8035	0.8071		
0.0200	0.6578	0.5603	0.5656	0.0127	0.8314	0.7077	0.7124	0.0130	0.9420	0.8098	0.8133		
0.0203	0.6605	0.5624	0.5677	0.0132	0.8352	0.7106	0.7152	0.0135	0.9420	0.8098	0.8133		
0.0205	0.6614	0.5631	0.5685	0.0143	0.8441	0.7173	0.7219	0.0145	0.9545	0.8190	0.8224		
0.0210	0.6667	0.5672	0.5726	0.0153	0.8529	0.7239	0.7285	0.0155	0.9572	0.8210	0.8243		
0.0220	0.6746	0.5735	0.5789	0.0163	0.8598	0.7291	0.7337	0.0166	0.9667	0.8280	0.8312		
0.0230	0.6875	0.5836	0.5889	0.0173	0.8649	0.7329	0.7374	0.0176	0.9733	0.8328	0.8360		
0.0240	0.7000	0.5934	0.5987	0.0184	0.8733	0.7392	0.7437	0.0187	0.9786	0.8367	0.8398		
0.0265	0.7243	0.6122	0.6175	0.0195	0.8800	0.7442	0.7486	0.0198	0.9838	0.8405	0.8436		
0.0290	0.7516	0.6332	0.6385	0.0205	0.8871	0.7494	0.7538	0.0198	0.9838	0.8405	0.8436		
0.0293	0.7602	0.6399	0.6451	0.0205	0.8882	0.7503	0.7546	0.0206	0.9866	0.8425	0.8456		
0.0295	0.7645	0.6431	0.6483	0.0207	0.8871	0.7494	0.7538	0.0208	0.9889	0.8442	0.8472		
0.0298	0.7661	0.6443	0.6495	0.0210	0.8888	0.7507	0.7551	0.0210	0.9878	0.8434	0.8465		
0.0301	0.7639	0.6427	0.6479	0.0212	0.8936	0.7543	0.7586	0.0212	0.9891	0.8443	0.8474		
0.0303	0.7712	0.6482	0.6534	0.0215	0.8920	0.7531	0.7574	0.0215	0.9927	0.8470	0.8500		
0.0308	0.7754	0.6514	0.6566	0.0220	0.8959	0.7567	0.7610	0.0217	0.9940	0.8479	0.8509		
0.0317	0.7859	0.6594	0.6645	0.0225	0.9027	0.7610	0.7652	0.0223	0.9952	0.8488	0.8518		
0.0328	0.7984	0.6687	0.6739	0.0230	0.9058	0.7633	0.7675	0.0227	1.0003	0.8525	0.8554		
0.0338	0.8084	0.6763	0.6814	0.0241	0.9121	0.7679	0.7721	0.0227	1.0003	0.8525	0.8554		
0.0353	0.8163	0.6822	0.6873	0.0252	0.9184	0.7725	0.7766	0.0232	1.0017	0.8534	0.8564		
0.0363	0.8374	0.6979	0.7028	0.0261	0.9275	0.7791	0.7832	0.0243	1.0091	0.8588	0.8617		
0.0385	0.8610	0.7153	0.7201	0.0272	0.9365	0.7857	0.7896	0.0253	1.0152	0.8632	0.8660		
0.0387	0.8667	0.7195	0.7243	0.0282	0.9439	0.7910	0.7949	0.0264	1.0176	0.8650	0.8677		
0.0389	0.8664	0.7192	0.7240	0.0293	0.9540	0.7983	0.8022	0.0274	1.0250	0.8702	0.8729		
0.0390	0.8676	0.7202	0.7250	0.0303	0.9611	0.8035	0.8072	0.0285	1.0333	0.8762	0.8787		
0.0394	0.8695	0.7216	0.7263	0.0306	0.9644	0.8058	0.8096	0.0296	1.0369	0.8787	0.8812		
0.0396	0.8700	0.7219	0.7267	0.0308	0.9701	0.8099	0.8136	0.0296	1.0369	0.8787	0.8812		
0.0401	0.8753	0.7258	0.7305	0.0310	0.9714	0.8108	0.8145	0.0306	1.0452	0.8847	0.8871		
0.0410	0.8909	0.7371	0.7417	0.0314	0.9729	0.8119	0.8156	0.0306	1.0416	0.8821	0.8845		
0.0420	0.9009	0.7443	0.7489	0.0316	0.9757	0.8139	0.8175	0.0308	1.0452	0.8847	0.8871		
0.0430	0.9127	0.7528	0.7573	0.0321	0.9784	0.8158	0.8194	0.0311	1.0452	0.8847	0.8871		
0.0441	0.9223	0.7597	0.7642	0.0326	0.9847	0.8203	0.8239	0.0314	1.0462	0.8853	0.8877		
0.0455	0.9380	0.7709	0.7753	0.0331	0.9902	0.8242	0.8277	0.0316	1.0462	0.8853	0.8877		
0.0479	0.9684	0.7923	0.7964	0.0342	0.9969	0.8289	0.8323	0.0321	1.0486	0.8870	0.8894		
0.0534	1.0242	0.8310	0.8346	0.0352	1.0035	0.8336	0.8369	0.0326	1.0552	0.8903	0.8926		
0.0598	1.0915	0.9763	0.8791	0.0362	1.0087	0.8373	0.8406	0.0326	1.0543	0.8911	0.8934		
0.0630	1.1365	0.9058	0.9080	0.0370	1.0139	0.8409	0.8442	0.0331	1.0555	0.8919	0.8942		
0.0685	1.1885	0.9391	0.9406	0.0374	1.0204	0.8454	0.8486	0.0342	1.0646	0.8983	0.9005		
0.0720	1.2277	0.9636	0.9645	0.0383	1.0304	0.8524	0.8555	0.0353	1.0668	0.8999	0.9020		
0.0775	1.2587	0.9826	0.9830	0.0394	1.0354	0.8559	0.8590	0.0363	1.0735	0.9045	0.9066		
0.0839	1.2780	0.9943	0.9944	0.0402	1.0421	0.8605	0.8635	0.0370	1.0760	0.9063	0.9083		
0.0870	1.2860	0.9991	0.9991	0.0403	1.0433	0.8614	0.8643	0.0370	1.0734	0.9045	0.9065		
0.0922	1.2866	0.9995	0.9995	0.0405	1.0457	0.8630	0.8659	0.0373	1.0792	0.9085	0.9105		
0.0960	-	1.2879	-	1.0003	-	1.0405	1.0441	0.8619	0.8648	0.0384	1.0868	0.9138	0.9157
0.1105	1.2875	1.0001	1.0001	0.0408	1.0506	0.8664	0.8693	0.0395	1.0901	0.9161	0.9180		
0.1193	1.2865	0.9995	0.9995	0.0410	1.0506	0.8664	0.8693	0.0395	1.0901	0.9161	0.9180		
0.0445	1.0555	0.8698	0.8726	0.0400	1.0902	0.9040	0.9092	0.0420	1.0902	0.9162	0.9180		
0.0420	1.0599	0.8728	0.8755	0.0403	1.0892	0.9043	0.9155	0.0426	1.0913	0.9173	0.9202		
0.0426	1.0622	0.8744	0.8771	0.0405	1.0934	0.9184	0.9202	0.0436	1.0923	0.9176	0.9194		
0.0436	1.0718	0.8809	0.8835	0.0408	1.0923	0.9176	0.9202	0.0436	1.0923	0.9176	0.9202		
0.0447	1.0799	0.8865	0.8890	0.0408	1.0935	0.9184	0.9202	0.0447	1.0935	0.9184	0.9202		
0.0457	1.0868	0.8912	0.8936	0.0410	1.0933	0.9184	0.9202	0.0447	1.0935	0.9184	0.9202		
0.0466	1.0949	0.8967	0.8990	0.0415	1.0966	0.9247	0.9229	0.0457	1.0977	0.9246	0.9229		
0.0478	1.1051	0.9035	0.9057	0.0420	1.0999	0.9249	0.9229	0.0466	1.0977	0.9246	0.9229		
0.0489	1.1118	0.9080	0.9101	0.0425	1.1010	0.9245	0.9229	0.0467	1.0977	0.9246	0.9229		
0.0499	1.1185	0.9125	0.9145	0.0436	1.1084	0.9287	0.9303	0.0465	1.0930	0.9287	0.9303		
0.0563	1.1668	0.9443	0.9456	0.0447	1.1137	0.9324	0.9339	0.0465	1.0936	0.9346	0.9351		
0.0630	1.2045	0.9687	0.9694	0.0457	1.1169	0.9346	0.9351	0.0467	1.0940	0.9346	0.9351		
0.0665	1.2234	0.9806	0.9811	0.0468	1.1232	0.9389	0.9402	0.0468	1.0942	0.9346	0.9351		
0.0724	1.2389	0.9904	0.9907	0.0470	1.1223	0.9383	0.9402	0.0470	1.0942	0.			

Table 2a  $M_{\infty} = 1.404$   $Re_{\delta} = 19.34 \times 10^6$  $x = 0.4$  $x = 0.475$  $x = 0.55$ 

$y$	$M$	$\frac{u}{u_0}$	$\frac{u}{u_0}$	$y$	$M$	$\frac{u}{u_0}$	$\frac{u}{u_0}$	$y$	$M$	$\frac{u}{u_0}$	$\frac{u}{u_0}$
r = 0.89	r = 1			r = 0.89	r = 1			r = 0.89	r = 1		
0.0010	0.9116	0.5985	0.6068	0.0010	0.7468	0.5268	0.5344	0.0010	0.6009	0.4663	0.4725
0.0013	0.9396	0.6144	0.6227	0.0013	0.7693	0.5413	0.5488	0.0013	0.5970	0.4635	0.4697
0.0016	0.9490	0.6198	0.6280	0.0015	0.7873	0.5526	0.5602	0.0015	0.6061	0.4701	0.4763
0.0017	0.9704	0.6317	0.6400	0.0018	0.8007	0.5611	0.5687	0.0018	0.6252	0.4840	0.4902
0.0022	1.0165	0.6572	0.6653	0.0033	0.8792	0.6097	0.6173	0.0023	0.6328	0.4895	0.4958
0.0028	1.0502	0.6754	0.6834	0.0049	0.9452	0.6494	0.6568	0.0023	0.6403	0.4949	0.5012
0.0042	1.1387	0.7220	0.7295	0.0065	1.0038	0.6837	0.6909	0.0039	0.6953	0.5341	0.5406
0.0058	1.2223	0.7642	0.7710	0.0081	1.0653	0.7188	0.7256	0.0054	0.7326	0.5604	0.5668
0.0073	1.2958	0.7998	0.8060	0.0096	1.1295	0.7542	0.7606	0.0070	0.7648	0.5827	0.5892
0.0088	1.3607	0.8301	0.8357	0.0104	1.1413	0.7606	0.7669	0.0085	0.7943	0.6030	0.6094
0.0098	1.4364	0.8641	0.8688	0.0107	1.1545	0.7677	0.7739	0.0105	0.8449	0.6371	0.6435
0.0100	1.4497	0.8700	0.8745	0.0109	1.1638	0.7728	0.7788	0.0108	0.8472	0.6587	0.6451
0.0103	1.4515	0.8708	0.8753	0.0112	1.1726	0.7774	0.7834	0.0109	0.8397	0.6337	0.6401
0.0103	1.3345	0.8180	0.8238	0.0112	1.1874	0.7853	0.7911	0.0110	0.8502	0.6407	0.6470
0.0105	1.4619	0.8752	0.8796	0.0127	1.2154	0.8000	0.8056	0.0113	0.8596	0.6470	0.6533
0.0110	1.4839	0.8847	0.8889	0.0143	1.2812	0.8337	0.8386	0.0118	0.8621	0.6486	0.6549
0.0115	1.4994	0.8914	0.8953	0.0143	1.2975	0.8419	0.8466	0.0118	0.8666	0.6516	0.6579
0.0123	1.4922	0.8883	0.8923	0.0158	1.3369	0.8613	0.8657	0.0130	0.9016	0.6747	0.6808
0.0130	1.5467	0.9112	0.9145	0.0169	1.3798	0.8821	0.8859	0.0154	0.9111	0.6808	0.6870
0.0144	1.5877	0.9279	0.9307	0.0174	1.3930	0.8883	0.8920	0.0149	0.9479	0.7047	0.7106
0.0159	1.6309	0.9451	0.9473	0.0190	1.4452	0.9127	0.9157	0.0165	0.9806	0.7254	0.7312
0.0173	1.6425	0.9497	0.9517	0.0195	1.4623	0.9205	0.9233	0.0181	1.0060	0.7414	0.7470
0.0174	1.6699	0.9603	0.9619	0.0203	1.4781	0.9277	0.9302	0.0204	1.0633	0.7767	0.7819
0.0190	1.7141	0.9771	0.9780	0.0205	1.4943	0.9350	0.9373	0.0207	1.0830	0.7886	0.7936
0.0193	1.7197	0.9791	0.9800	0.0206	1.4835	0.9301	0.9326	0.0210	1.0862	0.7906	0.7955
0.0195	1.7227	0.9802	0.9811	0.0208	1.4929	0.9344	0.9367	0.0212	1.0911	0.7935	0.7984
0.0198	1.7254	0.9813	0.9820	0.0211	1.5008	0.9379	0.9401	0.0215	1.1004	0.7991	0.8039
0.0202	1.7340	0.9845	0.9851	0.0221	1.5245	0.9484	0.9503	0.0220	1.1050	0.8018	0.8066
0.0207	1.7469	0.9892	0.9897	0.0226	1.5385	0.9546	0.9562	0.0220	1.1095	0.8045	0.8092
0.0209	1.7319	0.9837	0.9843	0.0236	1.5637	0.9655	0.9668	0.0227	1.1271	0.8149	0.8195
0.0222	1.7636	0.9953	0.9955	0.0242	1.5726	0.9693	0.9704	0.0229	1.1421	0.8237	0.8281
0.0222	1.7392	0.9864	0.9869	0.0248	1.5810	0.9729	0.9739	0.0236	1.1540	0.8307	0.8350
0.0236	1.7704	0.9977	0.9978	0.0257	1.5995	0.9807	0.9814	0.0251	1.1935	0.8534	0.8573
0.0237	1.7577	0.9932	0.9935	0.0262	1.6100	0.9851	0.9857	0.0267	1.2273	0.8725	0.8760
0.0251	1.7744	0.9992	0.9992	0.0273	1.6259	0.9918	0.9921	0.0282	1.2624	0.8921	0.8951
0.0259	1.7740	0.9991	0.9991	0.0288	1.6384	0.9969	0.9970	0.0304	1.3105	0.9182	0.9206
0.0266	1.7772	1.0002	1.0002	0.0288	1.6364	0.9961	0.9962	0.0306	1.3051	0.9153	0.9177
0.0369	1.7798	1.0012	1.0011	0.0300	1.6426	0.9987	0.9987	0.0307	1.3116	0.9188	0.9212
0.0462	1.7813	1.0017	1.0016	0.0303	1.6425	0.9986	0.9987	0.0309	1.3153	0.9207	0.9231
0.0530	1.7837	1.0026	1.0025	0.0304	1.6436	0.9991	0.9991	0.0312	1.3250	0.9259	0.9281
0.0592	1.7936	1.0061	1.0058	0.0305	1.6448	0.9996	0.9996	0.0317	1.3310	0.9292	0.9313
				0.0308	1.6446	0.9995	0.9995	0.0317	1.3347	0.9311	0.9331
				0.0314	1.6454	0.9998	0.9998	0.0326	1.3641	0.9466	0.9482
				0.0412	1.6454	0.9998	0.9998	0.0328	1.3639	0.9465	0.9481
				0.0500	1.6484	1.0010	1.0010	0.0330	1.3582	0.9435	0.9452
				0.0607	1.6430	0.9988	0.9988	0.0333	1.3725	0.9509	0.9524
								0.0348	1.4058	0.9680	0.9690
								0.0364	1.4259	0.9782	0.9789
								0.0380	1.4424	0.9865	0.9869
								0.0383	1.4370	0.9838	0.9843
								0.0401	1.4626	0.9965	0.9966
								0.0403	1.4586	0.9945	0.9947
								0.0404	1.4623	0.9963	0.9965
								0.0406	1.4623	0.9963	0.9965
								0.0409	1.4645	0.9974	0.9975
								0.0414	1.4655	0.9979	0.9980
								0.0414	1.4655	0.9979	0.9980
								0.0425	1.4674	0.9989	0.9989
								0.0427	1.4686	0.9995	0.9995
								0.0430	1.4698	1.0001	1.0001
								0.0526	1.4696	1.0000	1.0000
								0.0625	1.4674	0.9989	0.9989
								0.0726	1.4664	0.9984	0.9984

Table 2a (Contd)

x = 0.7				x = 0.833				x = 0.983			
y in	M	$\frac{u}{u_0}$	$\frac{u}{u_0}$	y in	M	$\frac{u}{u_0}$	$\frac{u}{u_0}$	y in	M	$\frac{u}{u_0}$	$\frac{u}{u_0}$
r = 0.89	r = 1	r = 0.89	r = 1	r = 0.89	r = 1	r = 0.89	r = 1	r = 0.89	r = 1	r = 0.89	r = 1
0.0010	0.4919	0.4252	0.4301	0.0010	0.7242	0.6184	0.6235	0.0010	0.7402	0.6551	0.6599
0.0012	0.5040	0.4353	0.4402	0.0013	0.7350	0.6275	0.6327	0.0013	0.7509	0.6638	0.6684
0.0015	0.5081	0.4367	0.4436	0.0015	0.7443	0.6348	0.6399	0.0015	0.7732	0.6816	0.6862
0.0015	0.5074	0.4381	0.4430	0.0018	0.7532	0.6417	0.6468	0.0018	0.7808	0.6877	0.6923
0.0017	0.5198	0.4483	0.4533	0.0020	0.7600	0.6469	0.6520	0.0020	0.7902	0.6951	0.6997
0.0020	0.5237	0.4515	0.4566	0.0026	0.7727	0.6567	0.6618	0.0023	0.7976	0.7010	0.7055
0.0025	0.5312	0.4577	0.4627	0.0031	0.7814	0.6634	0.6684	0.0026	0.8142	0.7140	0.7185
0.0030	0.5385	0.4636	0.4687	0.0036	0.8042	0.6808	0.6857	0.0031	0.8230	0.7209	0.7253
0.0035	0.5485	0.4718	0.4769	0.0036	0.8005	0.6780	0.6829	0.0041	0.8573	0.7476	0.7517
0.0044	0.5591	0.4805	0.4856	0.0041	0.8087	0.6842	0.6891	0.0046	0.8706	0.7578	0.7618
0.0055	0.5701	0.4894	0.4946	0.0052	0.8183	0.6914	0.6963	0.0046	0.8707	0.7579	0.7619
0.0064	0.5768	0.4948	0.5000	0.0062	0.8357	0.7045	0.7093	0.0051	0.8801	0.7651	0.7691
0.0074	0.5836	0.5004	0.5056	0.0073	0.8394	0.7073	0.7121	0.0057	0.8902	0.7728	0.7767
0.0089	0.5965	0.5107	0.5160	0.0082	0.8470	0.7130	0.7177	0.0067	0.8978	0.7786	0.7824
0.0101	0.6151	0.5257	0.5310	0.0092	0.8562	0.7199	0.7246	0.0077	0.9101	0.7879	0.7916
0.0103	0.6151	0.5257	0.5310	0.0105	0.8617	0.7239	0.7286	0.0087	0.9252	0.7992	0.8028
0.0104	0.6085	0.5204	0.5257	0.0108	0.8690	0.7293	0.7340	0.0098	0.9312	0.8037	0.8072
0.0106	0.6183	0.5282	0.5336	0.0111	0.8744	0.7333	0.7379	0.0108	0.9412	0.8112	0.8147
0.0106	0.6178	0.5278	0.5331	0.0113	0.8744	0.7333	0.7379	0.0108	0.9413	0.8113	0.8147
0.0108	0.6215	0.5308	0.5361	0.0116	0.8744	0.7333	0.7379	0.0111	0.9386	0.8092	0.8127
0.0111	0.6246	0.5333	0.5386	0.0118	0.8760	0.7345	0.7391	0.0113	0.9429	0.8125	0.8159
0.0116	0.6274	0.5355	0.5408	0.0124	0.8795	0.7371	0.7417	0.0116	0.9455	0.8144	0.8178
0.0121	0.6333	0.5402	0.5455	0.0129	0.8830	0.7397	0.7442	0.0118	0.9455	0.8144	0.8178
0.0126	0.6386	0.5444	0.5498	0.0134	0.8918	0.7461	0.7506	0.0121	0.9483	0.8164	0.8198
0.0136	0.6473	0.5514	0.5567	0.0134	0.8903	0.7450	0.7495	0.0124	0.9497	0.8175	0.8209
0.0146	0.6564	0.5585	0.5639	0.0139	0.8903	0.7450	0.7495	0.0129	0.9580	0.8236	0.8269
0.0156	0.6674	0.5672	0.5726	0.0150	0.8985	0.7510	0.7554	0.0134	0.9606	0.8256	0.8289
0.0166	0.6756	0.5737	0.5790	0.0160	0.9051	0.7559	0.7603	0.0134	0.9606	0.8256	0.8289
0.0181	0.6889	0.5841	0.5894	0.0170	0.9134	0.7619	0.7662	0.0139	0.9608	0.8257	0.8290
0.0195	0.7045	0.5962	0.6016	0.0178	0.9232	0.7690	0.7732	0.0145	0.9664	0.8298	0.8330
0.0195	0.7040	0.5959	0.6012	0.0189	0.9264	0.7713	0.7755	0.0145	0.9685	0.8314	0.8346
0.0197	0.7069	0.5981	0.6034	0.0202	0.9375	0.7793	0.7834	0.0150	0.9696	0.8321	0.8354
0.0200	0.7069	0.5981	0.6034	0.0205	0.9392	0.7805	0.7847	0.0155	0.9753	0.8354	0.8395
0.0200	0.7069	0.5981	0.6034	0.0208	0.9439	0.7839	0.7880	0.0166	0.9818	0.8411	0.8442
0.0202	0.7116	0.6018	0.6071	0.0210	0.9439	0.7839	0.7880	0.0177	0.9870	0.8449	0.8479
0.0205	0.7121	0.6021	0.6075	0.0213	0.9454	0.7850	0.7890	0.0187	0.9949	0.8507	0.8536
0.0210	0.7170	0.6060	0.6113	0.0215	0.9439	0.7839	0.7880	0.0197	0.9988	0.8535	0.8564
0.0215	0.7244	0.6117	0.6170	0.0221	0.9469	0.7860	0.7901	0.0206	1.0016	0.8556	0.8584
0.0220	0.7292	0.6154	0.6207	0.0226	0.9579	0.7939	0.7979	0.0208	1.0053	0.8582	0.8610
0.0230	0.7407	0.6243	0.6296	0.0231	0.9596	0.7951	0.7991	0.0209	1.0015	0.8556	0.8584
0.0241	0.7524	0.6332	0.6385	0.0231	0.9564	0.7928	0.7968	0.0211	1.0029	0.8564	0.8593
0.0249	0.7597	0.6388	0.6440	0.0236	0.9593	0.7949	0.7989	0.0214	1.0030	0.8565	0.8594
0.0260	0.7709	0.6473	0.6525	0.0247	0.9682	0.8012	0.8051	0.0216	1.0077	0.8600	0.8628
0.0275	0.7862	0.6589	0.6640	0.0257	0.9740	0.8053	0.8091	0.0219	1.0077	0.8600	0.8628
0.0290	0.7987	0.6683	0.6734	0.0268	0.9797	0.8094	0.8131	0.0222	1.0101	0.8617	0.8645
0.0293	0.8175	0.6824	0.6874	0.0277	0.9912	0.8175	0.8211	0.0227	1.0152	0.8653	0.8681
0.0295	0.8196	0.6839	0.6890	0.0288	0.9983	0.8224	0.8260	0.0232	1.0188	0.8680	0.8707
0.0298	0.8255	0.6883	0.6933	0.0300	1.0080	0.8292	0.8327	0.0237	1.0174	0.8670	0.8697
0.0298	0.8196	0.6839	0.6890	0.0306	1.0192	0.8370	0.8403	0.0243	1.0201	0.8689	0.8716
0.0300	0.8233	0.6866	0.6917	0.0309	1.0192	0.8370	0.8403	0.0243	1.0207	0.8693	0.8720
0.0303	0.8234	0.6868	0.6918	0.0311	1.0192	0.8370	0.8403	0.0248	1.0244	0.8720	0.8746
0.0308	0.8354	0.6956	0.7006	0.0314	1.0219	0.8388	0.8422	0.0253	1.0295	0.8756	0.8782
0.0313	0.8432	0.7015	0.7064	0.0316	1.0219	0.8388	0.8422	0.0263	1.0330	0.8781	0.8807
0.0318	0.8432	0.7015	0.7064	0.0322	1.0273	0.8426	0.8459	0.0274	1.0425	0.8849	0.8873
0.0328	0.8562	0.7110	0.7159	0.0327	1.0301	0.8445	0.8478	0.0284	1.0438	0.8858	0.8882
0.0338	0.8674	0.7192	0.7241	0.0332	1.0344	0.8474	0.8507	0.0295	1.0498	0.8901	0.8924
0.0348	0.8769	0.7261	0.7309	0.0332	1.0354	0.8481	0.8514	0.0306	1.0548	0.8936	0.8959
0.0353	0.8838	0.7166	0.7214	0.0337	1.0393	0.8509	0.8540	0.0306	1.0545	0.8934	0.8956
0.0358	0.8840	0.7313	0.7360	0.0348	1.0495	0.8578	0.8609	0.0309	1.0548	0.8936	0.8959
0.0373	0.8999	0.7428	0.7474	0.0358	1.0557	0.8621	0.8650	0.0311	1.0583	0.8961	0.8983
0.0385	0.9187	0.7563	0.7608	0.0369	1.0620	0.8664	0.8693	0.0314	1.0571	0.8953	0.8975
0.0387	0.9202	0.7574	0.7619	0.0370	1.0620	0.8664	0.8693	0.0316	1.0592	0.8968	0.8990
0.0390	0.9202	0.7574	0.7619	0.0378	1.0721	0.8732	0.8760	0.0319	1.0627	0.8992	0.9013
0.0390	0.9218	0.7586	0.7630	0.0388	1.0783	0.8774	0.8801	0.0322	1.0649	0.9007	0.9029
0.0392	0.9265	0.7619	0.7663	0.0401	1.0993	0.8848	0.8874	0.0327	1.0649	0.9007	0.9029
0.0395	0.9299	0.7643	0.7687	0.0402	1.0986	0.8849	0.8875	0.0332	1.0694	0.9039	0.9060
0.0400	0.9316	0.7655	0.7699	0.0405	1.0920	0.8866	0.8891	0.0343	1.0751	0.9079	0.9099
0.0405	0.9382	0.7702	0.7745	0.0407	1.0943	0.8882	0.8907	0.0343	1.0745	0.9075	0.9095
0.0409	0.9447	0.7748	0.7791	0.0410	1.0968	0.8898	0.8923	0.0348	1.0757	0.9084	0.9103
0.0420	0.9570	0.7835	0.7877	0.0412	1.0968	0.8898	0.8923	0.0353	1.0794	0.9109	0.9128
0.0430	0.9709	0.7933	0.7973	0.0418	1.1088	0.8978	0.9001	0.0364	1.0858	0.9154	0.9173
0.0440	0.9786	0.7986	0.8026	0.0423	1.1066	0.8963	0.8987	0.0370	1.0890	0.9176	0.9195
0.0442	0.9708	0.7932	0.7972	0.0428	1.1104	0.8988	0.9012	0.0373	1.0890	0.9176	0.9195
0.0449	0.9860	0.8038	0.8077	0.0428	1.1114	0.8995	0.9018	0.0383	1.0947	0.9216	0.9233
0.0465	1.0048	0.8168	0.8206	0.0435	1.1125	0.9003	0.9026	0.0394	1.1003	0.9255	0.9271
0.0479	1.0187	0.8263	0.8300	0.0444	1.1240	0.9079	0.9100	0.0400	1.0996	0.9250	0.9267
0.0534	1.0758	0.8649	0.8679	0.0454	1.1307	0.9122	0.9143	0.0403	1.1008	0.9258	0.9274
0.0598	1.1438	0.9095	0.9117	0.0464	1.1387	0.9175	0.9194	0.0405	1.1040	0.9280	0.9296
0.0633	1.1891	0.9384	0.9400	0.0466	1.1398	0.9193	0.9202	0.0405	1.1058	0.9293	0.9309
0.0684	1.2355	0.9673	0.9682	0.0473	1.1467	0.9227	0.9246	0.0408	1		

Table 2d  $N_\infty = 1.700$   $Re_\delta = 10.00 \times 10^6$  $x = 0.4$ 

$y$ in	M	$\frac{u}{u_\delta}$	$\frac{u}{u_\delta}$
		r = 0.89	r = 1

00010	0.9728	0.5746	0.5847
00013	0.9859	0.5812	0.5913
00015	0.9991	0.5878	0.5979
00017	1.0242	0.6003	0.6104
00020	1.0562	0.6160	0.6260
00022	1.0756	0.6253	0.6353
00025	1.1091	0.6414	0.6512
00028	1.1281	0.6504	0.6602
00030	1.1598	0.6651	0.6748
00037	1.1947	0.6811	0.6907
00048	1.2657	0.7128	0.7220
00057	1.3251	0.7385	0.7472
00073	1.4040	0.7712	0.7794
00088	1.4786	0.8010	0.8084
00098	1.5607	0.8322	0.8389
00100	1.5678	0.8349	0.8414
00103	1.5678	0.8349	0.8414
00105	1.5775	0.8385	0.8449
00108	1.5874	0.8421	0.8484
00108	1.5725	0.8366	0.8431
00110	1.5945	0.8447	0.8510
00112	1.6039	0.8481	0.8542
00115	1.6140	0.8518	0.8578
00117	1.6278	0.8567	0.8626
00125	1.6475	0.8637	0.8694
00128	1.6496	0.8645	0.8701
00135	1.6866	0.8774	0.8826
00145	1.7194	0.8886	0.8934
00148	1.7186	0.8883	0.8931
00150	1.7758	0.9074	0.9115
00168	1.7932	0.9130	0.9169
00174	1.8201	0.9217	0.9253
00188	1.8507	0.9313	0.9345
00190	1.8876	0.9427	0.9454
00193	1.8915	0.9439	0.9466
00194	1.8807	0.9406	0.9434
00195	1.8954	0.9451	0.9477
00198	1.8993	0.9463	0.9489
00200	1.9060	0.9483	0.9508
00202	1.9099	0.9495	0.9519
00205	1.9196	0.9524	0.9547
00207	1.9242	0.9538	0.9560
00210	1.9339	0.9567	0.9588
00212	1.9159	0.9513	0.9536
00215	1.9335	0.9566	0.9587
00217	1.9523	0.9621	0.9640
00225	1.9720	0.9679	0.9695
00235	1.9735	0.9683	0.9698
00236	1.9870	0.9722	0.9736
00237	1.9735	0.9683	0.9698
00250	2.0213	0.9820	0.9829
00254	2.0128	0.9796	0.9806
00256	2.0476	0.9893	0.9898
00273	2.0457	0.9888	0.9893
00281	2.0659	0.9943	0.9946
00283	2.0659	0.9943	0.9946
00285	2.0657	0.9943	0.9946
00286	2.0659	0.9943	0.9946
00288	2.0694	0.9953	0.9955
00290	2.0723	0.9961	0.9963
00293	2.0723	0.9961	0.9963
00295	2.0728	0.9962	0.9964
00298	2.0747	0.9967	0.9969
00300	2.0676	0.9948	0.9950
00305	2.0782	0.9972	0.9974
00307	2.0760	0.9971	0.9972
00310	2.0771	0.9974	0.9975
00316	2.0820	0.9987	0.9988
00322	2.0801	0.9982	0.9983
00325	2.0818	0.9986	0.9987
00325	2.0820	0.9987	0.9988
00341	2.0830	0.9990	0.9990
00344	2.0836	0.9991	0.9992
00355	2.0855	0.9996	0.9997
00363	2.0872	1.0001	1.0001
00466	2.0914	1.0012	1.0012
00568	2.0996	1.0034	1.0033
00651	2.1091	1.0060	1.0057
00731	2.1108	1.0064	1.0061

 $x = 0.55$ 

$y$ in	M	$\frac{u}{u_\delta}$	$\frac{u}{u_\delta}$
		r = 0.89	r = 1
00010	0.7222	0.4794	0.4877
00013	0.7285	0.4832	0.4915
00015	0.7330	0.4859	0.4943
00018	0.7436	0.4923	0.5007
00023	0.7632	0.5041	0.5126
00028	0.7834	0.5162	0.5246
00033	0.8051	0.5290	0.5375
00038	0.8251	0.5408	0.5493
00042	0.8405	0.5497	0.5583
00048	0.8593	0.5606	0.5692
00053	0.8720	0.5679	0.5765
00057	0.8884	0.5773	0.5859
00063	1.1678	0.7269	0.7346
00073	0.9319	0.6019	0.6104
00083	0.9571	0.6159	0.6244
00094	0.9867	0.6321	0.6406
00104	1.0147	0.6473	0.6557
00105	1.0304	0.6557	0.6641
00108	1.0314	0.6563	0.6646
00108	1.0319	0.6566	0.6649
00113	1.0384	0.6601	0.6683
00118	1.0471	0.6647	0.6729
00120	1.0494	0.6659	0.6741
00120	1.0494	0.6659	0.6741
00123	1.0567	0.6698	0.6780
00123	1.0569	0.6699	0.6781
00128	1.0697	0.6766	0.6848
00133	1.0846	0.6844	0.6925
00138	1.0920	0.6883	0.6963
00143	1.1065	0.6958	0.7037
00150	1.1195	0.7025	1.2056
00154	1.1345	0.7101	0.7180
00159	1.1499	0.7180	0.7257
00170	1.1797	0.7329	0.7404
00172	1.1797	0.7329	0.7404
00180	1.2057	0.7458	0.7531
00191	1.2330	0.7590	0.7662
00200	1.2614	0.7727	0.7795
00207	1.2964	0.7893	0.7959
00209	1.2970	0.7896	0.7961
00209	1.2981	0.7901	0.7967
00215	1.3051	0.7933	0.7998
00216	1.2970	0.7896	0.7961
00220	1.3115	0.7963	0.8028
00225	1.3243	0.8023	0.8086
00225	1.3243	0.8023	0.8086
00225	1.3104	0.7958	0.8023
00230	1.3395	0.8093	0.8154
00235	1.3526	0.8152	0.8213
00240	1.3617	0.8193	0.8253
00245	1.3745	0.8251	0.8309
00250	1.3878	0.8311	0.8368
00255	1.4027	0.8377	0.8432
00260	1.4145	0.8429	0.8483
00268	1.4290	0.8493	0.8545
00270	1.4480	0.8575	0.8625
00277	1.4376	0.8530	0.8581
00281	1.4734	0.8684	0.8731
00293	1.4984	0.8789	0.8833
00302	1.5325	0.8931	0.8970
00304	1.5432	0.8974	0.9013
00304	1.4963	0.8780	0.8825
00307	1.5447	0.8980	0.9019
00307	1.5451	0.8982	0.9020
00312	1.5528	0.9014	0.9051
00317	1.5582	0.9036	0.9072
00317	1.5612	0.9048	0.9084
00317	1.5581	0.9035	0.9071
00322	1.5691	0.9080	0.9115
00322	1.5702	0.9084	0.9119
00322	1.5533	0.9015	0.9053
00327	1.5842	0.9140	0.9173
00330	1.5549	0.9022	0.9059
00330	1.5581	0.9035	0.9071
00333	1.5965	0.9189	0.9220
00338	1.6042	0.9219	0.9250
00344	1.6154	0.9263	0.9292
00349	1.6320	0.9328	0.9355
00356	1.6229	0.9292	0.9320
00358	1.6514	0.9403	0.9427
00369	1.6909	0.9552	0.9571
00370	1.6749	0.9492	0.9513
00373	1.6677	0.9465	0.9486
00380	1.7010	0.9590	0.9607
00383	1.6754	0.9498	0.9518
00383	1.6764	0.9498	0.9518
00390	1.7225	0.9669	0.9683
00399	1.7266	0.9685	0.9698
00400	1.7506	0.9772	0.9782
00401	1.7541	0.9784	0.9794
00404	1.5462	0.8987	0.9025
00404	1.7551	0.9788	0.9797
00408	1.7649	0.9823	0.9831
00414	1.7625	0.9815	0.9823
00417	1.7645	0.9822	0.9829
00417	1.7617	0.9812	0.9820
00418	1.7692	0.9839	0.9846
00418	1.7701	0.9842	0.9849
00422	1.7687	0.9837	0.9844
00424	1.7771	0.9867	0.9872
00425	1.7576	0.9797	0.9806
00425	1.7604	0.9807	0.9815
00430	1.7852	0.9896	0.9900
00435	1.7894	0.9910	0.9914
00440	1.8032	0.9959	0.9961
00445	1.8032	0.9959	0.9961
00450	1.8059	0.9968	0.9970
00451	1.7934	0.9924	0.9928
00455	1.8123	0.9991	0.9991
00465	1.8164	1.0005	1.0005
00564	1.8150	1.0000	1.0000
00668	1.8137	0.9995	0.9996
00773	1.8110	0.9986	0.9987
00895	1.8106	0.9985	0.9985
00989	1.8065	0.9970	0.9972

Table 2d (Contd)

x = 0.7				x = 0.833				x = 0.983			
y in	M	$\frac{u}{u_\delta}$	$\frac{u}{u_\delta}$	y in	M	$\frac{u}{u_\delta}$	$\frac{u}{u_\delta}$	y in	M	$\frac{u}{u_\delta}$	$\frac{u}{u_\delta}$
		r = 0.89	r = 1			r = 0.89	r = 1			r = 0.89	r = 1
00010	05813	04263	04329	00010	07795	05763	05832	00010	08605	06397	06462
00012	05905	04327	04394	00015	08010	05906	05974	00012	08736	06483	06548
00015	05996	04389	04456	00017	08252	06066	06134	00015	08996	06652	06716
00018	06130	04481	04549	00022	08405	06165	06233	00017	09125	06735	06798
00020	06171	04509	04577	00027	08598	06291	06359	00020	09318	06858	06921
00028	06344	04627	04696	00035	08865	06463	06530	00025	09586	07028	07089
00035	06426	04683	04752	00048	09142	06638	06704	00030	09875	07209	07269
00043	06544	04763	04833	00060	09350	06769	06835	00035	09985	07278	07337
00057	06780	04922	04993	00081	09667	06966	07030	00045	10380	07520	07576
00072	07001	05070	05141	00108	09967	07151	07213	00056	10633	07673	07727
00087	07180	05188	05260	00108	09929	07127	07190	00066	10816	07782	07835
00101	07418	05346	05418	00111	09978	07157	07219	00077	11025	07906	07957
00104	07418	05346	05418	00114	10040	07195	07257	00092	11227	08025	08074
00105	07418	05346	05418	00120	10095	07229	07290	00108	11473	08167	08214
00106	07484	05389	05461	00125	10131	07251	07312	00108	11597	08124	08171
00109	07484	05389	05461	00132	10229	07310	07370	00112	11449	08153	08200
00111	07515	05409	05482	00145	10342	07377	07437	00115	11481	08172	08218
00119	07646	05495	05567	00159	10443	07438	07497	00116	11544	08208	08254
00126	07676	05514	05587	00179	10654	07563	07620	00120	11567	08221	08267
00134	07801	05595	05668	00205	11755	08196	08244	00125	11621	08252	08297
00148	08012	05731	05804	00205	10965	07745	07800	00130	11702	08299	08343
00153	08188	05844	05917	00210	10930	07725	07780	00135	11706	08301	08345
00178	08385	05969	06041	00212	10998	07764	07819	00145	11807	08358	08401
00195	08599	06104	06176	00218	11015	07775	07829	00155	11913	08418	08460
00195	08651	06136	06209	00222	11066	07804	07858	00166	11991	08462	08503
00197	08651	06136	06209	00230	11147	07851	07904	00176	12070	08507	08547
00200	08678	06153	06226	00243	11309	07944	07996	00192	12224	08592	08631
00203	08730	06186	06258	00255	11432	08014	08065	00206	12424	08033	08082
00205	08730	06186	06258	00276	11644	08134	08183	00209	12351	08662	08699
00212	08881	06280	06352	00303	11978	08320	08365	00210	12266	08615	08653
00220	08931	06310	06382	00306	11982	08322	08367	00212	12297	08633	08671
00228	09079	06402	06473	00310	12036	08352	08397	00215	12379	08678	08714
00243	09267	06517	06588	00314	12087	08380	08425	00215	12358	08666	08703
00258	09473	06642	06712	00318	12118	08398	08441	00217	12381	08679	08716
00272	09693	05774	06843	00324	12192	08438	08481	00223	12434	08708	08744
00290	09924	06912	06980	00331	12279	08486	08528	00227	12480	08733	08769
00293	10065	06995	07062	00345	12424	08564	08605	00232	12505	08747	08782
00295	10106	07020	07087	00357	12549	08632	08670	00243	12600	08799	08833
00298	10146	07043	07110	00370	12649	08686	08723	00253	12648	08825	08859
00301	10185	07066	07132	00376	12798	08765	08801	00264	12795	08904	08936
00303	10204	07077	07143	00402	13044	08894	08927	00274	12819	08918	08949
00310	10339	07156	07222	00405	13086	08916	08948	00290	12915	08969	08999
00317	10417	07201	07266	00405	13095	08921	08953	00306	13040	09036	09064
00326	10529	07266	07330	00408	13126	08937	08969	00306	13010	09020	09048
00340	10766	07401	07464	00413	13181	08965	08996	00308	13018	09024	09053
00353	10856	07452	07515	00418	13224	08988	09018	00311	13050	09041	09069
00355	10979	07522	07584	00426	13319	09037	09066	00314	13122	09079	09106
00370	11202	07647	07707	00439	13464	09112	09139	00314	13088	09061	09089
00385	11436	07777	07835	00452	13589	09175	09201	00316	13109	09073	09100
00387	11468	07795	07852	00466	13755	09259	09282	00321	13159	09099	09126
00398	11468	07795	07852	00473	13796	09280	09303	00326	13178	09109	09135
00399	11516	07821	07878	00499	14098	09430	09449	00331	13225	09134	09160
00394	11550	07840	07897	00563	14612	09681	09692	00342	13290	09168	09193
00396	11598	07866	07922	00630	14983	09857	09862	00353	13358	09204	09228
00403	11695	07919	07975	00665	15132	09927	09929	00363	13428	09240	09263
00410	11806	07979	08034	00724	15238	09976	09977	00370	13451	09252	09275
00418	11931	08047	08100	00760	15270	09991	09991	00373	13495	09275	09297
00433	12160	08170	08221	00820	15291	10001	10001	00390	13608	09334	09354
00441	12282	08234	08284	00921	15291	10001	10001	00400	13672	09366	09386
00448	12371	08281	08330	01016	15291	10001	10001	00403	13655	09356	09376
00462	12605	08404	08450	01176	15280	09996	09996	00405	13686	09373	09393
00479	12891	08551	08594	01270	15270	09991	09991	00408	13729	09395	09414
00534	13668	08941	08974					00408	13707	09384	09404
00598	14557	09366	09388					00408	13698	09379	09399
00630	15086	09610	09623					00410	13727	09394	09413
00685	15596	09837	09843					00415	13772	09418	09436
00720	15832	09941	09943					00420	13791	09427	09445
00775	15954	09994	09994					00425	13813	09438	09456
00841	15954	09994	09994					00436	13874	09470	09486
00960	15932	09984	09985					00447	13940	09503	09519
01075	15865	09955	09957					00457	14006	09536	09551
01156	15854	09950	09952					00468	14092	09580	09593
01243	15809	09931	09933					00470	14070	09569	09583
01335	15809	09931	09933					00484	14135	09601	09614
01420	15764	09911	09914					00500	14220	09644	09655
								00567	14516	09790	09797
								00632	14717	09888	09892
								00667	14784	09921	09923
								00728	14880	09967	09968
								00763	14926	09989	09989
								00827	14940	09996	09996
								00892	14966	10008	10008
								00988	14946	09999	09999
								01087	14943	09997	09997
								01187	14943	09997	09997
								01283	14943	09997	09997

Table 2e  $M_\infty = 2.000$   $Re_\delta = 9.88 \times 10^6$  $x = 0.4$  $x = 0.475$  $x = 0.55$ 

y in	$\frac{u}{u_\delta}$ $r = 0.89$	$\frac{u}{u_\delta}$ $r = 1$	y in	M	$\frac{u}{u_\delta}$ $r = 0.89$	$\frac{u}{u_\delta}$ $r = 1$	y in	M	$\frac{u}{u_\delta}$ $r = 0.89$	$\frac{u}{u_\delta}$ $r = 1$	
0.010	1.0038	0.5465	0.5582	0.0010	0.9265	0.5190	0.5302	0.0010	0.8104	0.4812	0.4913
0.015	1.0419	0.5639	0.5756	0.0015	0.9508	0.5307	0.5420	0.0015	0.8239	0.4883	0.4984
0.017	1.1177	0.5977	0.6094	0.0018	1.0166	0.5619	0.5732	0.0018	0.8558	0.5051	0.5153
0.020	1.1557	0.6142	0.6258	0.0020	1.0501	0.5774	0.5888	0.0020	0.8779	0.5166	0.5269
0.022	1.2071	0.6360	0.6475	0.0022	1.0660	0.5847	0.5960	0.0023	0.9051	0.5306	0.5410
0.025	1.2365	0.6482	0.6596	0.0027	1.1018	0.6009	0.6122	0.0028	0.9259	0.5411	0.5516
0.030	1.2787	0.6653	0.6766	0.0033	1.1311	0.6159	0.6252	0.0033	0.9597	0.5582	0.5686
0.035	1.3256	0.6840	0.6951	0.0043	1.1964	0.6423	0.6534	0.0038	0.9822	0.5694	0.5798
0.045	1.4119	0.7172	0.7277	0.0053	1.2482	0.6642	0.6751	0.0042	1.0034	0.5798	0.5903
0.055	1.4704	0.7587	0.7489	0.0065	1.2979	0.6846	0.6953	0.0053	1.0342	0.5948	0.6052
0.065	1.5373	0.7626	0.7722	0.0081	1.3706	0.7136	0.7238	0.0063	1.0704	0.6121	0.6225
0.075	1.5945	0.7822	0.7913	0.0096	1.4295	0.7362	0.7461	0.0079	1.1117	0.6316	0.6419
0.085	1.6600	0.8059	0.8124	0.0104	1.4847	0.7567	0.7662	0.0094	1.1597	0.6536	0.6638
0.095	1.7049	0.8183	0.8264	0.0107	1.4904	0.7588	0.7682	0.0105	1.2122	0.6772	0.6871
0.098	1.7246	0.8245	0.8324	0.0109	1.4971	0.7613	0.7706	0.0108	1.2261	0.6833	0.6932
0.100	1.7315	0.8266	0.8345	0.0112	1.5143	0.7675	0.7767	0.0109	1.2054	0.6742	0.6841
0.103	1.7414	0.8297	0.8375	0.0112	1.5028	0.7633	0.7726	0.0110	1.2338	0.6867	0.6965
0.105	1.7478	0.8317	0.8394	0.0114	1.5209	0.7698	0.7790	0.0113	1.2371	0.6882	0.6980
0.105	1.7482	0.8318	0.8395	0.0117	1.5309	0.7734	0.7825	0.0115	1.2371	0.6882	0.6980
0.108	1.7610	0.8357	0.8433	0.0122	1.5477	0.7794	0.7883	0.0118	1.2434	0.6909	0.7007
0.110	1.7804	0.8416	0.8490	0.0126	1.5663	0.7859	0.7947	0.0123	1.2562	0.6965	0.7062
0.112	1.7996	0.8474	0.8546	0.0127	1.5673	0.7862	0.7950	0.0125	1.2519	0.6946	0.7043
0.115	1.7937	0.8456	0.8529	0.0138	1.6152	0.8027	0.8110	0.0128	1.2688	0.7019	0.7115
0.117	1.8127	0.8513	0.8583	0.0148	1.6555	0.8163	0.8242	0.0133	1.2832	0.7081	0.7176
0.122	1.8350	0.8590	0.8658	0.0158	1.6980	0.8302	0.8377	0.0138	1.2974	0.7141	0.7235
0.125	1.8473	0.8614	0.8681	0.0174	1.7614	0.8503	0.8571	0.0150	1.3252	0.7258	0.7351
0.132	1.8822	0.8715	0.8777	0.0190	1.8180	0.8676	0.8738	0.0159	1.3601	0.7402	0.7492
0.135	1.8813	0.8712	0.8775	0.0203	1.8858	0.8875	0.8930	0.0175	1.4046	0.7582	0.7669
0.141	1.9171	0.8812	0.8871	0.0205	1.8808	0.8861	0.8916	0.0191	1.4517	0.7768	0.7851
0.152	1.9624	0.8937	0.8991	0.0206	1.8875	0.8880	0.8934	0.0206	1.4950	0.7925	0.8013
0.162	2.0153	0.9077	0.9125	0.0208	1.8957	0.8904	0.8957	0.0207	1.5230	0.8040	0.8116
0.171	2.0452	0.9155	0.9199	0.0211	1.9143	0.8957	0.9008	0.0209	1.5419	0.8110	0.8185
0.182	2.0758	0.9233	0.9273	0.0212	1.9195	0.8971	0.9022	0.0211	1.5453	0.8123	0.8197
0.190	2.1076	0.9312	0.9349	0.0216	1.9273	0.8993	0.9043	0.0215	1.5427	0.8113	0.8187
0.192	2.1113	0.9321	0.9357	0.0220	1.9338	0.9011	0.9060	0.0216	1.5501	0.8140	0.8214
0.193	2.1102	0.9318	0.9355	0.0221	1.9405	0.9030	0.9078	0.0220	1.5550	0.8158	0.8231
0.195	2.1182	0.9338	0.9374	0.0226	1.9560	0.9073	0.9119	0.0222	1.5440	0.8118	0.8192
0.198	2.1291	0.9364	0.9399	0.0236	1.9936	0.9176	0.9218	0.0225	1.5675	0.8204	0.8276
0.200	2.1346	0.9378	0.9411	0.0247	2.0313	0.9276	0.9313	0.0230	1.5821	0.8257	0.8327
0.202	2.1426	0.9397	0.9430	0.0257	2.0608	0.9353	0.9387	0.0235	1.5906	0.8287	0.8357
0.202	2.1382	0.9367	0.9420	0.0273	2.1106	0.9480	0.9507	0.0240	1.6062	0.8343	0.8411
0.205	2.1557	0.9429	0.9460	0.0288	2.1508	0.9579	0.9602	0.0250	1.6304	0.8429	0.8494
0.210	2.1669	0.9455	0.9485	0.0300	2.1857	0.9663	0.9682	0.0260	1.6675	0.8558	0.8619
0.212	2.1729	0.9470	0.9499	0.0303	2.1895	0.9673	0.9690	0.0276	1.7149	0.8718	0.8774
0.215	2.1861	0.9501	0.9528	0.0304	2.1926	0.9680	0.9697	0.0293	1.7594	0.8865	0.8915
0.221	2.2017	0.9537	0.9563	0.0305	2.1940	0.9683	0.9701	0.0304	1.8105	0.9028	0.9073
0.225	2.2121	0.9561	0.9586	0.0308	2.2032	0.9705	0.9721	0.0307	1.8265	0.9078	0.9121
0.234	2.2370	0.9618	0.9640	0.0310	2.2100	0.9721	0.9736	0.0307	1.7992	0.8992	0.9038
0.243	2.2557	0.9683	0.9701	0.0312	2.2147	0.9732	0.9747	0.0310	1.8328	0.9098	0.9139
0.253	2.2941	0.9746	0.9761	0.0317	2.2238	0.9753	0.9767	0.0312	1.8349	0.9104	0.9146
0.263	2.3133	0.9788	0.9800	0.0319	2.2266	0.9760	0.9773	0.0315	1.8349	0.9104	0.9146
0.274	2.3280	0.9819	0.9830	0.0323	2.2350	0.9779	0.9792	0.0317	1.8411	0.9124	0.9164
0.281	2.3459	0.9858	0.9866	0.0333	2.2587	0.9834	0.9843	0.0322	1.8535	0.9162	0.9201
0.282	2.3499	0.9866	0.9874	0.0342	2.2766	0.9875	0.9862	0.0322	1.8501	0.9151	0.9191
0.283	2.3509	0.9868	0.9876	0.0354	2.2943	0.9914	0.9919	0.0327	1.8685	0.9207	0.9245
0.286	2.3531	0.9873	0.9880	0.0369	2.3129	0.9956	0.9958	0.0333	1.8758	0.9230	0.9266
0.288	2.3604	0.9888	0.9895	0.0385	2.3239	0.9980	0.9981	0.0338	1.8887	0.9269	0.9303
0.290	2.3629	0.9894	0.9900	0.0388	2.3152	0.9961	0.9963	0.0349	1.9119	0.9338	0.9369
0.292	2.3621	0.9892	0.9898	0.0400	2.3348	1.0003	1.0003	0.0358	1.9396	0.9419	0.9447
0.293	2.3654	0.9899	0.9905	0.0400	2.3304	0.9954	0.9954	0.0375	1.9840	0.9546	0.9569
0.295	2.3750	0.9919	0.9924	0.0403	2.3299	0.9993	0.9993	0.0388	1.9939	0.9574	0.9595
0.300	2.3758	0.9921	0.9925	0.0405	2.3341	1.0002	1.0002	0.0390	2.0226	0.9654	0.9671
0.302	2.3765	0.9922	0.9927	0.0408	2.3319	0.9997	0.9997	0.0401	2.0746	0.9795	0.9806
0.304	2.3815	0.9932	0.9936	0.0410	2.3319	0.9997	0.9997	0.0404	2.0759	0.9799	0.9809
0.312	2.3886	0.9947	0.9950	0.0413	2.3319	0.9997	0.9997	0.0406	2.0778	0.9804	0.9814
0.315	2.3933	0.9957	0.9959	0.0414	2.3304	0.9994	0.9994	0.0406	2.0573	0.9749	0.9762
0.324	2.3997	0.9970	0.9972	0.0418	2.3299	0.9993	0.9993	0.0408	2.0797	0.9809	0.9819
0.333	2.4053	0.9981	0.9983	0.0423	2.3319	0.9997	0.9997	0.0411	2.0887	0.9833	0.9842
0.343	2.4077	0.9986	0.9987	0.0434	2.3355	1.0005	1.0005	0.0414	2.0887	0.9833	0.9842
0.352	2.4099	0.9991	0.9991	0.0443	2.3310	0.9995	0.9996	0.0418	2.0923	0.9842	0.9851
0.363	2.4099	0.9991	0.9991	0.0454	2.3332	1.0000	1.0000	0.0421	2.0317	0.9841	0.9849
0.372	2.4148	1.0001	1.0001	0.0469	2.3326	0.9999	0.9999	0.0424	2.1018	0.9868	0.9874
0.475	2.4219	1.0015	1.0014	0.0500	2.3326	0.9999	0.9999	0.0430	2.1118	0.9894	0.9899
0.550	2.4345	1.0041	1.0038	0.0644	2.3239	0.9980	0.9981	0.0435	2.1140	0.9900	0.9905
0.698	2.4453	1.0062	1.0059	0.0734	2.3194	0.9970	0.9972	0.0445	2.1259	0.9930	0.9934
0.781	2.4547	1.0081	1.0076	0.0826	2.3152	0.9961	0.9963	0.0445	2.1418	0.9971	0.9973
0.867	2.4618	1.0095	1.0089	0.0920	2.3152	0.9961	0.9963	0.0470	2.1508	0.9994	0.9995
			0.0109	2.3129	0.9956	0.9958	0.0483	2.1521	1.0000	1.0000	0.9996
					0.0584	2.1513	0.9956	0.9956			
					0.0682	2.1521	1.0000	1.0000			
					0.0779	2.1426	0.9973	0.9975			
					0.0915	2.1343	0.9952	0.9955			
					0.1041	2.1356	0.9955	0.9958			
					0.1200	2.1246	0.9927	0.9931			

Table 2e (Contd)

Table 2f  $M_\infty = 2.401$   $Re_\delta = 9.92 \times 10^6$  $x = 0.4$ 

$y$ in	M	$\frac{u}{u_\delta}$	$\frac{u}{u_\delta}$
		$r = 0.89$	$r = 1$

0.0010	0.9932	0.5004	0.5138
0.0013	1.1145	0.5510	0.5646
0.0015	1.1263	0.5558	0.5694
0.0017	1.1587	0.5687	0.5824
0.0022	1.2178	0.5918	0.6054
0.0028	1.2974	0.6217	0.6352
0.0032	1.4140	0.6634	0.6765
0.0043	1.5902	0.7214	0.7336
0.0052	1.8174	0.7879	0.7984
0.0065	2.0977	0.8582	0.8660
0.0078	2.3424	0.9102	0.9156
0.0090	2.5096	0.9414	0.9451
0.0098	2.6048	0.9577	0.9604
0.0100	2.6486	0.9649	0.9672
0.0100	2.6044	0.9576	0.9604
0.0103	2.6537	0.9657	0.9680
0.0105	2.6744	0.9690	0.9711
0.0110	2.6858	0.9709	0.9728
0.0113	2.6767	0.9694	0.9714
0.0115	2.7216	0.9765	0.9780
0.0120	2.7430	0.9798	0.9811
0.0125	2.7310	0.9779	0.9794
0.0130	2.7564	0.9818	0.9830
0.0140	2.7745	0.9845	0.9856
0.0152	2.7895	0.9868	0.9876
0.0165	2.7969	0.9879	0.9887
0.0176	2.8026	0.9887	0.9895
0.0187	2.8096	0.9897	0.9904
0.0190	2.8235	0.9917	0.9923
0.0193	2.8248	0.9919	0.9925
0.0195	2.8231	0.9917	0.9922
0.0198	2.8291	0.9926	0.9931
0.0200	2.8179	0.9909	0.9915
0.0202	2.8274	0.9923	0.9928
0.0207	2.8352	0.9934	0.9939
0.0212	2.8429	0.9945	0.9949
0.0212	2.8308	0.9928	0.9933
0.0222	2.8494	0.9955	0.9958
0.0232	2.8537	0.9961	0.9963
0.0243	2.8554	0.9963	0.9966
0.0256	2.8626	0.9974	0.9975
0.0269	2.8678	0.9981	0.9982
0.0278	2.8682	0.9981	0.9983
0.0281	2.8754	0.9992	0.9992
0.0283	2.8767	0.9993	0.9994
0.0286	2.8746	0.9990	0.9991
0.0288	2.8720	0.9987	0.9988
0.0290	2.8763	0.9993	0.9993
0.0293	2.8793	0.9997	0.9997
0.0298	2.8805	0.9999	0.9999
0.0302	2.8818	1.0001	1.0001
0.0405	2.9008	1.0027	1.0025
0.0541	2.9273	1.0063	1.0059
0.0628	2.9398	1.0080	1.0075
0.0719	2.9589	1.0106	1.0099
0.0842	2.9819	1.0137	1.0127
0.0920	2.9946	1.0153	1.0142
0.0999	3.0190	1.0185	1.0172
0.1081	3.0312	1.0200	1.0186
0.1167	3.0436	1.0216	1.0201

 $x = 0.55$ 

$y$ in	M	$\frac{u}{u_\delta}$	$\frac{u}{u_\delta}$
		$r = 0.89$	$r = 1$
0.0010	1.1387	0.5844	0.5971
0.0013	1.1933	0.6069	0.6194
0.0015	1.2365	0.6242	0.6367
0.0018	1.2571	0.6323	0.6448
0.0020	1.2905	0.6453	0.6577
0.0023	1.2983	0.6484	0.6606
0.0025	1.3475	0.6670	0.6791
0.0028	1.3636	0.6730	0.6850
0.0030	1.3910	0.6831	0.6950
0.0042	1.4642	0.7093	0.7207
0.0056	1.5383	0.7347	0.7457
0.0068	1.5948	0.7534	0.7640
0.0094	1.7110	0.7899	0.7995
0.0105	1.7802	0.8105	0.8195
0.0107	1.7668	0.8066	0.8157
0.0108	1.7926	0.8141	0.8230
0.0110	1.7995	0.8161	0.8249
0.0113	1.8068	0.8182	0.8263
0.0115	1.8154	0.8206	0.8293
0.0118	1.8208	0.8222	0.8308
0.0120	1.8419	0.8281	0.8365
0.0123	1.8538	0.8315	0.8397
0.0125	1.8671	0.8351	0.8433
0.0138	1.9143	0.8480	0.8556
0.0153	1.9645	0.8612	0.8684
0.0165	2.0207	0.8756	0.8822
0.0191	2.1183	0.8993	0.9048
0.0203	2.1750	0.9125	0.9174
0.0207	2.2029	0.9188	0.9234
0.0209	2.2129	0.9210	0.9255
0.0211	2.2239	0.9235	0.9278
0.0215	2.2239	0.9235	0.9278
0.0216	2.2309	0.9250	0.9293
0.0220	2.2356	0.9260	0.9303
0.0222	2.2582	0.9309	0.9349
0.0225	2.2574	0.9308	0.9348
0.0227	2.2682	0.9331	0.9370
0.0240	2.3068	0.9413	0.9447
0.0252	2.3429	0.9488	0.9518
0.0266	2.3798	0.9562	0.9589
0.0293	2.4424	0.9685	0.9704
0.0304	2.4818	0.9760	0.9775
0.0305	2.4772	0.9751	0.9767
0.0307	2.4811	0.9759	0.9773
0.0310	2.4860	0.9768	0.9782
0.0312	2.4860	0.9768	0.9782
0.0315	2.4919	0.9779	0.9793
0.0317	2.4968	0.9788	0.9801
0.0320	2.5024	0.9798	0.9811
0.0322	2.5111	0.9815	0.9826
0.0325	2.5111	0.9815	0.9826
0.0338	2.5312	0.9851	0.9860
0.0351	2.5456	0.9877	0.9885
0.0370	2.5603	0.9904	0.9910
0.0377	2.5749	0.9930	0.9934
0.0390	2.5843	0.9946	0.9950
0.0401	2.5985	0.9971	0.9973
0.0403	2.5925	0.9961	0.9963
0.0404	2.5975	0.9971	0.9971
0.0406	2.5975	0.9969	0.9971
0.0408	2.5975	0.9969	0.9971
0.0411	2.5985	0.9971	0.9973
0.0414	2.5985	0.9971	0.9973
0.0416	2.6038	0.9980	0.9982
0.0418	2.6029	0.9979	0.9980
0.0422	2.6076	0.9987	0.9988
0.0433	2.6026	0.9978	0.9980
0.0435	2.6079	0.9987	0.9988
0.0447	2.6126	0.9995	0.9996
0.0465	2.6129	0.9996	0.9996
0.0473	2.6129	0.9996	0.9996
0.0487	2.6129	0.9996	0.9996
0.0500	2.6160	1.0001	1.0001
0.0564	2.6026	0.9978	0.9980
0.0727	2.5975	0.9969	0.9971
0.0827	2.5928	0.9961	0.9964
0.0923	2.5881	0.9953	0.9956
0.1023	2.5834	0.9945	0.9948

Table 2f (Contd)

x = 0.7				x = 0.833				x = 0.983			
y in	M	$\frac{u}{u_0}$	$\frac{u}{u_0}$	y in	M	$\frac{u}{u_0}$	$\frac{u}{u_0}$	y in	M	$\frac{u}{u_0}$	$\frac{u}{u_0}$
		r = 0.89	r = 1			r = 0.89	r = 1			r = 0.89	r = 1
0.0110	1.0178	0.5599	0.5713	0.0010	1.0931	0.6241	0.6344	0.0010	1.1448	0.6566	0.6664
0.0012	1.0370	0.5688	0.5803	0.0012	1.1106	0.6323	0.6426	0.0012	1.1603	0.6638	0.6735
0.0015	1.0632	0.5807	0.5922	0.0015	1.1336	0.6430	0.6532	0.0015	1.1992	0.6816	0.6912
0.0025	1.1388	0.6145	0.6259	0.0017	1.1722	0.6607	0.6707	0.0017	1.2516	0.7049	0.7142
0.0035	1.2003	0.6411	0.6523	0.0022	1.2656	0.7020	0.7115	0.0020	1.2723	0.7140	0.7232
0.0047	1.2580	0.6652	0.6762	0.0027	1.3179	0.7242	0.7335	0.0022	1.3080	0.7294	0.7384
0.0060	1.2983	0.6817	0.6925	0.0027	1.3129	0.7221	0.7314	0.0025	1.3319	0.7396	0.7483
0.0101	1.4320	0.7338	0.7438	0.0031	1.3568	0.7404	0.7494	0.0028	1.3616	0.7520	0.7606
0.0104	1.4386	0.7363	0.7462	0.0043	1.4177	0.7650	0.7735	0.0033	1.3968	0.7665	0.7747
0.0106	1.4440	0.7383	0.7482	0.0054	1.4714	0.7860	0.7941	0.0038	1.4310	0.7803	0.7882
0.0116	1.4623	0.7451	0.7549	0.0063	1.5109	0.8011	0.8080	0.0043	1.4612	0.7923	0.8000
0.0125	1.4912	0.7557	0.7652	0.0074	1.5448	0.8137	0.8211	0.0043	1.4655	0.7939	0.8016
0.0139	1.5203	0.7661	0.7754	0.0085	1.5682	0.8223	0.8294	0.0050	1.5176	0.8140	0.8212
0.0150	1.5530	0.7777	0.7867	0.0097	1.5873	0.8293	0.8362	0.0064	1.5686	0.8332	0.8398
0.0195	1.6549	0.8123	0.8204	0.0108	1.6219	0.8416	0.8481	0.0075	1.6077	0.8475	0.8537
0.0197	1.6542	0.8121	0.8202	0.0109	1.6219	0.8416	0.8481	0.0090	1.6578	0.8653	0.8709
0.0200	1.6608	0.8143	0.8224	0.0110	1.6101	0.8374	0.8441	0.0105	1.6955	0.8787	0.8839
0.0210	1.6815	0.8211	0.8289	0.0111	1.6219	0.8416	0.8481	0.0108	1.7147	0.8849	0.8899
0.0220	1.7055	0.8288	0.8364	0.0114	1.6255	0.8429	0.8494	0.0112	1.7196	0.8865	0.8915
0.0234	1.7313	0.8370	0.8443	0.0120	1.6335	0.8457	0.8521	0.0115	1.7202	0.8868	0.8917
0.0245	1.7589	0.8456	0.8527	0.0121	1.6233	0.8421	0.8486	0.0116	1.7283	0.8895	0.8943
0.0293	1.8678	0.8783	0.8841	0.0125	1.6408	0.8482	0.8542	0.0120	1.7300	0.8900	0.8948
0.0295	1.8713	0.8793	0.8851	0.0125	1.6396	0.8478	0.8542	0.0122	1.7380	0.8927	0.8974
0.0298	1.8771	0.8810	0.8867	0.0130	1.6487	0.8510	0.8573	0.0125	1.7397	0.8933	0.8980
0.0308	1.8951	0.8861	0.8917	0.0132	1.6417	0.8486	0.8549	0.0127	1.7460	0.8954	0.9000
0.0309	1.8818	0.8823	0.8880	0.0140	1.6587	0.8545	0.8606	0.0132	1.7539	0.8980	0.9025
0.0317	1.9120	0.8909	0.8963	0.0151	1.6723	0.8591	0.8651	0.0138	1.7635	0.9012	0.9055
0.0330	1.9473	0.9008	0.9057	0.0161	1.6836	0.8630	0.8689	0.0143	1.7688	0.9029	0.9072
0.0343	1.9676	0.9064	0.9111	0.0171	1.6962	0.8673	0.8730	0.0143	1.7730	0.9043	0.9085
0.0345	2.0618	0.9313	0.9349	0.0182	1.7050	0.8703	0.8759	0.0150	1.7851	0.9086	0.9127
0.0348	2.0612	0.9312	0.9348	0.0195	1.7174	0.8744	0.8799	0.0164	1.8048	0.9146	0.9185
0.0390	2.0699	0.9334	0.9369	0.0205	1.7220	0.8760	0.8814	0.0173	1.8171	0.9185	0.9222
0.0398	2.0856	0.9374	0.9407	0.0207	1.7289	0.8782	0.8835	0.0190	1.8360	0.9245	0.9280
0.0401	2.0862	0.9375	0.9408	0.0208	1.7296	0.8785	0.8838	0.0205	1.8497	0.9288	0.9321
0.0410	2.1012	0.9413	0.9444	0.0210	1.7289	0.8782	0.8836	0.0206	1.8540	0.9301	0.9334
0.0423	2.1295	0.9484	0.9511	0.0212	1.7289	0.8782	0.8836	0.0210	1.8525	0.9297	0.9329
0.0435	2.1557	0.9548	0.9572	0.0218	1.7330	0.8796	0.8849	0.0212	1.8570	0.9311	0.9343
0.0449	2.2493	0.9768	0.9781	0.0219	1.7420	0.8819	0.8871	0.0215	1.8619	0.9326	0.9357
0.0554	2.3028	0.9888	0.9894	0.0222	1.7400	0.8819	0.8871	0.0217	1.8619	0.9326	0.9357
0.0597	2.3391	0.9967	0.9969	0.0222	1.7396	0.8818	0.8870	0.0220	1.8650	0.9335	0.9366
0.0640	2.3488	0.9988	0.9989	0.0227	1.7515	0.8857	0.8808	0.0223	1.8679	0.9344	0.9375
0.0676	2.3529	0.9927	0.9927	0.0230	1.7522	0.8859	0.8910	0.0225	1.8695	0.9349	0.9380
0.0745	- 2.3384	- 0.9966	- 0.9958	0.0239	1.7567	0.8874	0.8924	0.0230	1.8724	0.9358	0.9388
0.0880	2.3349	0.9958	0.9961	0.0249	1.7703	0.8918	0.8967	0.0236	1.8759	0.9372	0.9402
0.0969	2.3171	0.9920	0.9924	0.0260	1.7805	0.8951	0.8998	0.0241	1.8784	0.9377	0.9406
0.1064	2.3101	0.9904	0.9910	0.0270	1.7946	0.8996	0.9042	0.0241	1.8844	0.9395	0.9424
0.1151	2.2992	0.9880	0.9887	0.0280	1.8047	0.9028	0.9072	0.0248	1.8923	0.9419	0.9447
				0.0293	1.8147	0.9060	0.9103	0.0262	1.9027	0.9451	0.9477
				0.0306	1.8296	0.9105	0.9148	0.0273	1.9115	0.9477	0.9502
				0.0306	1.8296	0.9105	0.9148	0.0288	1.9246	0.9516	0.9540
				0.0308	1.8296	0.9106	0.9148	0.0304	1.9323	0.9539	0.9561
				0.0310	1.8296	0.9106	0.9148	0.0306	1.9363	0.9551	0.9573
				0.0314	1.8328	0.9116	0.9157	0.0308	1.9378	0.9555	0.9577
				0.0316	1.8377	0.9132	0.9172	0.0311	1.9421	0.9568	0.9589
				0.0318	1.8398	0.9138	0.9178	0.0316	1.9425	0.9569	0.9590
				0.0324	1.8462	0.9158	0.9197	0.0319	1.9425	0.9569	0.9590
				0.0324	1.8454	0.9155	0.9195	0.0319	1.9468	0.9582	0.9602
				0.0327	1.8524	0.9177	0.9215	0.0321	1.9453	0.9578	0.9598
				0.0329	1.8518	0.9175	0.9214	0.0325	1.9483	0.9586	0.9606
				0.0340	1.8615	0.9205	0.9242	0.0329	1.9511	0.9595	0.9614
				0.0350	1.8775	0.9254	0.9289	0.0335	1.9553	0.9607	0.9626
				0.0360	1.8919	0.9297	0.9330	0.0340	1.9526	0.9599	0.9618
				0.0367	1.8887	0.9288	0.9321	0.0340	1.9600	0.9621	0.9639
				0.0380	1.9115	0.9355	0.9386	0.0347	1.9676	0.9643	0.9660
				0.0394	1.9287	0.9406	0.9435	0.0360	1.9774	0.9671	0.9687
				0.0402	1.9278	0.9404	0.9435	0.0370	1.9816	0.9683	0.9699
				0.0403	1.9309	0.9413	0.9441	0.0370	1.9812	0.9682	0.9698
				0.0405	1.9309	0.9413	0.9441	0.0386	1.9915	0.9712	0.9726
				0.0407	1.9396	0.9438	0.9465	0.0400	1.9944	0.9720	0.9734
				0.0408	1.9370	0.9431	0.9458	0.0402	1.9991	0.9733	0.9747
				0.0413	1.9406	0.9441	0.9468	0.0403	1.9986	0.9732	0.9745
				0.0417	1.9519	0.9474	0.9500	0.0405	2.0015	0.9740	0.9752
				0.0418	1.9457	0.9459	0.9485	0.0408	2.0002	0.9736	0.9750
				0.0418	1.9513	0.9472	0.9498	0.0410	2.0002	0.9736	0.9750
				0.0423	1.9589	0.9494	0.9519	0.0413	2.0017	0.9741	0.9753
				0.0428	1.9641	0.9509	0.9533	0.0415	2.0044	0.9748	0.9761
				0.0434	1.9635	0.9507	0.9532	0.0418	2.0058	0.9752	0.9765
				0.0445	1.9789	0.9551	0.9573	0.0423	2.0086	0.9760	0.9772
				0.0455	1.9909	0.9585	0.9606	0.0429	2.0115	0.9768	0.9780
				0.0463	1.9999	0.9611	0.9630	0.0433	2.0115	0.9768	0.9780
				0.0465	2.0005	0.9612	0.9632	0.0433	2.0160	0.9781	0.9792
				0.0475	2.0125	0.9646	0.9655	0.0441	2.0207	0.9794	0.9805
				0.0489	2.0228	0.9674	0.9691	0.0455	2.0260	0.9809	0.9819
				0.0511	2.0347	0.9707	0.9722	0.0465	2.0289	0.9817	0.9826
				0.0513	2.0420	0.9727	0.9741	0.0470	2.0339	0.9831	0.9840
				0.0523	2.0524	0.9756	0.9768	0.0481	2.0384	0.9844	0.9852
				0.0561	2.0808	0.9832	0.9841	0.0498	2.0418	0.9853	0.9861
				0.0630	2.1094	0.9908	0.9913	0.0567	2.0662	0.9920	0.9924
				0.0662	2.1207	0.9937	0.9941	0.0630	2.0795	0.995	

Table 2g  $M_\infty = 2.799$   $Re_\delta = 10 \times 10^6$

$x = 0.4$

$x = 0.55$

$y$	$M$	$\frac{u}{u_\delta}$	$\frac{u}{u_\delta}$
		$r = 0.89$	$r = 1$

00010	1.1790	0.5468	0.5620
00013	1.2365	0.5679	0.5831
00015	1.2790	0.5831	0.5982
00017	1.3425	0.6051	0.6202
00022	1.4584	0.6435	0.6582
00028	1.5135	0.6608	0.6754
00037	1.6506	0.7017	0.7156
00048	1.7931	0.7408	0.7538
00057	1.9536	0.7809	0.7928
00073	2.2044	0.8362	0.8459
00088	2.4281	0.8786	0.8863
00098	2.6057	0.9083	0.9144
00100	2.6428	0.9141	0.9198
00103	2.6620	0.9170	0.9226
00105	2.7045	0.9234	0.9286
00105	2.6811	0.9199	0.9253
00110	2.7833	0.9348	0.9393
00115	2.8128	0.9389	0.9432
00123	2.8573	0.9450	0.9489
00125	2.8986	0.9505	0.9540
00135	2.9501	0.9572	0.9602
00138	2.9722	0.9600	0.9629
00145	3.0200	0.9659	0.9684
00153	3.0424	0.9686	0.9709
00160	3.0702	0.9719	0.9740
00174	3.1188	0.9776	0.9792
00190	3.1351	0.9794	0.9810
00192	3.1606	0.9823	0.9836
00193	3.1467	0.9808	0.9822
00195	3.1537	0.9815	0.9829
00198	3.1698	0.9833	0.9846
00202	3.1812	0.9846	0.9858
00207	3.1881	0.9854	0.9865
00210	3.1987	0.9865	0.9875
00217	3.2071	0.9874	0.9884
00224	3.2176	0.9886	0.9894
00226	3.2169	0.9885	0.9894
00236	3.2432	0.9913	0.9920
00240	3.2454	0.9916	0.9922
00250	3.2618	0.9933	0.9938
00266	3.2804	0.9952	0.9956
00281	3.3061	0.9979	0.9981
00282	3.3017	0.9975	0.9976
00283	3.3039	0.9977	0.9979
00286	3.3135	0.9987	0.9988
00288	3.3120	0.9985	0.9986
00293	3.3193	0.9993	0.9993
00298	3.3193	0.9993	0.9993
00300	3.3201	0.9993	0.9994
00307	3.3193	0.9993	0.9993
00315	3.3201	0.9993	0.9994
00316	3.3171	0.9990	0.9991
00326	3.3266	1.0000	1.0000
00329	3.3288	1.0002	1.0002
00341	3.3354	1.0009	1.0008
00433	3.3629	1.0036	1.0033
00510	3.3830	1.0056	1.0052
00631	3.4222	1.0094	1.0087
00710	3.4484	1.0119	1.0110
00862	3.5007	1.0167	1.0154
00940	3.5180	1.0183	1.0169
01019	3.5359	1.0199	1.0184
01186	3.5869	1.0244	1.0225

$y$	$M$	$\frac{u}{u_\delta}$	$\frac{u}{u_\delta}$
		$r = 0.89$	$r = 1$
00010	1.2604	0.5944	0.6086
00013	1.2831	0.6027	0.6169
00015	1.3584	0.6295	0.6435
00018	1.3889	0.6400	0.6540
00020	1.4186	0.6501	0.6640
00023	1.4761	0.6692	0.6828
00028	1.5203	0.6835	0.6969
00038	1.6079	0.7107	0.7256
00048	1.6711	0.7295	0.7420
00063	1.7685	0.7570	0.7689
00079	1.8455	0.7777	0.7890
00094	1.9463	0.8034	0.8158
00105	1.9713	0.8095	0.8197
00107	2.0284	0.8231	0.8328
00108	2.0300	0.8235	0.8332
00110	2.0476	0.8276	0.8371
00113	2.0580	0.8300	0.8394
00115	2.0777	0.8345	0.8437
00118	2.0972	0.8389	0.8479
00123	2.1372	0.8478	0.8564
00133	2.1810	0.8572	0.8655
00143	2.2180	0.8650	0.8729
00159	2.3184	0.8852	0.8922
00175	2.3773	0.8965	0.9029
00191	2.4220	0.9048	0.9107
00203	2.4967	0.9181	0.9233
00207	2.4314	0.9065	0.9123
00209	2.4980	0.9183	0.9235
00211	2.5130	0.9209	0.9260
00215	2.5207	0.9223	0.9272
00216	2.5368	0.9250	0.9298
00220	2.5451	0.9264	0.9312
00225	2.5853	0.9333	0.9376
00235	2.6069	0.9367	0.9408
00245	2.6459	0.9429	0.9467
00260	2.6843	0.9489	0.9523
00276	2.7429	0.9579	0.9607
00293	2.7817	0.9636	0.9661
00304	2.7841	0.9639	0.9664
00305	2.8108	0.9678	0.9700
00307	2.8183	0.9689	0.9710
00310	2.8258	0.9699	0.9720
00312	2.8327	0.9709	0.9729
00315	2.8401	0.9719	0.9739
00317	2.8555	0.9741	0.9759
00322	2.8612	0.9749	0.9766
00335	2.8815	0.9777	0.9792
00344	2.9023	0.9805	0.9819
00358	2.9379	0.9853	0.9862
00370	2.9406	0.9856	0.9866
00375	2.9643	0.9887	0.9895
00390	2.9867	0.9916	0.9922
00401	3.0078	0.9943	0.9947
00403	3.0067	0.9942	0.9946
00404	3.0137	0.9951	0.9954
00406	3.0137	0.9951	0.9954
00408	3.0137	0.9951	0.9954
00411	3.0207	0.9959	0.9962
00414	3.0218	0.9961	0.9964
00418	3.0271	0.9968	0.9970
00430	3.0325	0.9974	0.9976
00440	3.0395	0.9983	0.9984
00445	3.0464	0.9991	0.9992
00455	3.0427	0.9987	0.9988
00470	3.0522	0.9999	0.9999
00487	3.0538	1.0001	1.0001
00500	3.0602	1.0008	1.0008
00633	3.0427	0.9987	0.9988
00727	3.0357	0.9978	0.9980
00827	3.0293	0.9970	0.9972
00923	3.0293	0.9970	0.9972
01023	3.0223	0.9961	0.9964

Table 2g (Contd)

$x = 0.7$				$x = 0.833$				$x = 0.983$			
$y$ in	M	$\frac{u}{u_\delta}$	$\frac{u}{u_\delta}$	$y$ in	M	$\frac{u}{u_\delta}$	$\frac{u}{u_\delta}$	$y$ in	M	$\frac{u}{u_\delta}$	$\frac{u}{u_\delta}$
		$r = 0.89$				$r = 1$				$r = 0.89$	
0.0010	1.3326	0.6461	0.6589	0.0010	1.3350	0.6794	0.6907	0.0010	1.3477	0.6908	0.7018
0.0012	1.3621	0.6569	0.6696	0.0012	1.4048	0.7058	0.7168	0.0012	1.3769	0.7021	0.7129
0.0015	1.4009	0.6708	0.6834	0.0015	1.4248	0.7132	0.7241	0.0015	1.4343	0.7236	0.7341
0.0020	1.4751	0.6956	0.7088	0.0017	1.5000	0.7403	0.7507	0.0017	1.4616	0.7336	0.7439
0.0035	1.6044	0.7390	0.7504	0.0020	1.5245	0.7489	0.7590	0.0022	1.5359	0.7600	0.7698
0.0050	1.6845	0.7637	0.7745	0.0025	1.6001	0.7746	0.7841	0.0025	1.5717	0.7724	0.7819
0.0065	1.7536	0.7841	0.7943	0.0030	1.6372	0.7868	0.7960	0.0030	1.6115	0.7858	0.7949
0.0080	1.8113	0.8005	0.8102	0.0035	1.6729	0.7983	0.8072	0.0030	1.6115	0.7858	0.7949
0.0092	1.8610	0.8141	0.8294	0.0045	1.7343	0.8175	0.8258	0.0035	1.6456	0.7971	0.8059
0.0101	1.9039	0.8256	0.8344	0.0055	1.7863	0.8332	0.8410	0.0045	1.7157	0.8195	0.8277
0.0104	1.9110	0.8275	0.8363	0.0071	1.8562	0.8536	0.8607	0.0060	1.7921	0.8429	0.8503
0.0105	1.9028	0.8253	0.8342	0.0086	1.9012	0.8662	0.8728	0.0077	1.8685	0.8653	0.8718
0.0106	1.9176	0.8292	0.8379	0.0108	1.9573	0.8815	0.8875	0.0092	1.9234	0.8807	0.8866
0.0111	1.9311	0.8327	0.8413	0.0108	1.9451	0.8782	0.8844	0.0108	1.9872	0.8979	0.9032
0.0125	1.9846	0.8463	0.8544	0.0109	1.9614	0.8826	0.8885	0.0108	1.9755	0.8948	0.9002
0.0140	2.0366	0.8592	0.8667	0.0111	1.9583	0.8817	0.8878	0.0112	1.9913	0.8990	0.9042
0.0155	2.0937	0.8728	0.8798	0.0114	1.9703	0.8850	0.8908	0.0115	1.9991	0.9011	0.9062
0.0170	2.1479	0.8852	0.8917	0.0117	1.9714	0.8852	0.8911	0.0116	2.0028	0.9021	0.9071
0.0183	2.1783	0.8921	0.8982	0.0122	1.9751	0.8862	0.8920	0.0122	2.0147	0.9052	0.9101
0.0195	2.2092	0.8989	0.9046	0.0127	1.9877	0.8896	0.8952	0.0125	2.0224	0.9072	0.9120
0.0195	2.2373	0.9049	0.9104	0.0132	1.9962	0.8918	0.8974	0.0130	2.0302	0.9092	0.9139
0.0197	2.2148	0.9001	0.9058	0.0143	2.0140	0.8964	0.9018	0.0130	2.0302	0.9092	0.9139
0.0200	2.2327	0.9039	0.9095	0.0153	2.0301	0.9005	0.9057	0.0135	2.0378	0.9112	0.9158
0.0205	2.2327	0.9039	0.9095	0.0169	2.0591	0.9079	0.9128	0.0145	2.0571	0.9161	0.9205
0.0220	2.2844	0.9148	0.9198	0.0184	2.0754	0.9120	0.9167	0.0160	2.0798	0.9218	0.9260
0.0235	2.3183	0.9218	0.9265	0.0205	2.1028	0.9187	0.9231	0.0176	2.1090	0.9291	0.9329
0.0250	2.3677	0.9317	0.9358	0.0205	2.0996	0.9180	0.9224	0.0192	2.1317	0.9346	0.9382
0.0265	2.3957	0.9372	0.9410	0.0207	2.1028	0.9187	0.9231	0.0206	2.1489	0.9388	0.9421
0.0278	2.4221	0.9422	0.9458	0.0210	2.0990	0.9178	0.9222	0.0208	2.1536	0.9399	0.9432
0.0290	2.4486	0.9472	0.9505	0.0212	2.1070	0.9198	0.9241	0.0210	2.1498	0.9390	0.9423
0.0293	2.4601	0.9494	0.9525	0.0215	2.1159	0.9219	0.9261	0.0212	2.1571	0.9407	0.9440
0.0295	2.4601	0.9494	0.9525	0.0220	2.1239	0.9239	0.9280	0.0215	2.1536	0.9399	0.9432
0.0298	2.4656	0.9504	0.9535	0.0225	2.1233	0.9237	0.9278	0.0220	2.1608	0.9416	0.9448
0.0303	2.4706	0.9513	0.9543	0.0230	2.1312	0.9256	0.9296	0.0223	2.1680	0.9433	0.9464
0.0317	2.4971	0.9562	0.9589	0.0241	2.1400	0.9277	0.9317	0.0227	2.1715	0.9441	0.9472
0.0333	2.5178	0.9599	0.9624	0.0252	2.1588	0.9322	0.9359	0.0232	2.1790	0.9459	0.9489
0.0349	2.5478	0.9652	0.9674	0.0266	2.1784	0.9368	0.9403	0.0243	2.1895	0.9484	0.9512
0.0353	2.5552	0.9685	0.9686	0.0282	2.1938	0.9404	0.9437	0.0259	2.2038	0.9517	0.9544
0.0363	2.5843	0.9716	0.9734	0.0303	2.2243	0.9473	0.9503	0.0274	2.2215	0.9558	0.9583
0.0375	2.5884	0.9723	0.9740	0.0306	2.2276	0.9481	0.9510	0.0290	2.2392	0.9598	0.9621
0.0385	2.5992	0.9741	0.9758	0.0308	2.2276	0.9481	0.9510	0.0305	2.2450	0.9611	0.9633
0.0387	2.6036	0.9749	0.9765	0.0310	2.2276	0.9481	0.9510	0.0306	2.2522	0.9628	0.9649
0.0388	2.5944	0.9733	0.9750	0.0314	2.2276	0.9481	0.9510	0.0308	2.2459	0.9613	0.9638
0.0390	2.6044	0.9750	0.9766	0.0316	2.2361	0.9500	0.9528	0.0311	2.2528	0.9629	0.9650
0.0396	2.5892	0.9741	0.9758	0.0321	2.2400	0.9509	0.9536	0.0314	2.2564	0.9637	0.9657
0.0410	2.6291	0.9792	0.9805	0.0326	2.2466	0.9523	0.9550	0.0319	2.2633	0.9652	0.9672
0.0425	2.6441	0.9816	0.9828	0.0331	2.2541	0.9540	0.9566	0.0321	2.2666	0.9660	0.9679
0.0440	2.6531	0.9831	0.9842	0.0342	2.2624	0.9559	0.9584	0.0326	2.2672	0.9661	0.9680
0.0441	2.6602	0.9843	0.9853	0.0352	2.2728	0.9581	0.9605	0.0326	2.2638	0.9654	0.9673
0.0455	2.6734	0.9865	0.9873	0.0368	2.2949	0.9630	0.9651	0.0326	2.2702	0.9668	0.9686
0.0468	2.6773	0.9871	0.9879	0.0370	2.2914	0.9622	0.9644	0.0331	2.2702	0.9668	0.9686
0.0479	2.6870	0.9887	0.9894	0.0383	2.3060	0.9654	0.9674	0.0342	2.2805	0.9690	0.9708
0.0534	2.7209	0.9941	0.9944	0.0402	2.3241	0.9692	0.9710	0.0357	2.2907	0.9713	0.9729
0.0598	2.7369	0.9966	0.9968	0.0403	2.3165	0.9676	0.9695	0.0370	2.3002	0.9734	0.9749
0.0630	-2.7529	-1.0000	-1.0000	0.0405	2.3203	0.9684	0.9702	0.0373	2.3010	0.9735	0.9751
0.0720	2.7494	0.9985	0.9986	0.0405	2.3244	0.9693	0.9711	0.0390	2.3111	0.9757	0.9771
0.0839	2.7282	0.9952	0.9955	0.0408	2.3275	0.9700	0.9717	0.0400	2.3070	0.9748	0.9763
0.0922	2.7186	0.9937	0.9941	0.0410	2.3247	0.9693	0.9711	0.0403	2.3111	0.9757	0.9771
0.1010	2.7090	0.9922	0.9927	0.0415	2.3319	0.9709	0.9726	0.0405	2.3143	0.9764	0.9778
0.1193	2.6948	0.9899	0.9906	0.0420	2.3278	0.9700	0.9718	0.0408	2.3178	0.9772	0.9785
				0.0426	2.3313	0.9708	0.9725	0.0408	2.3205	0.9778	0.9790
				0.0436	2.3500	0.9747	0.9762	0.0413	2.3245	0.9786	0.9799
				0.0447	2.3531	0.9753	0.9768	0.0415	2.3245	0.9786	0.9799
				0.0462	2.3708	0.9790	0.9802	0.0420	2.3285	0.9795	0.9807
				0.0466	2.3708	0.9790	0.9802	0.0420	2.3280	0.9794	0.9806
				0.0478	2.3779	0.9805	0.9816	0.0425	2.3280	0.9794	0.9806
				0.0499	2.3920	0.9834	0.9843	0.0436	2.3379	0.9815	0.9826
				0.0563	2.4236	0.9897	0.9903	0.0451	2.3414	0.9822	0.9833
				0.0630	2.4512	0.9952	0.9955	0.0468	2.3512	0.9843	0.9852
				0.0666	2.4580	0.9965	0.9967	0.0470	2.3507	0.9842	0.9851
				0.0724	2.4681	0.9985	0.9986	0.0484	2.3546	0.9850	0.9859
				0.0740	2.4681	0.9985	0.9986	0.0500	2.3673	0.9877	0.9884
				0.0820	2.4749	0.9998	0.9998	0.0567	2.3870	0.9918	0.9923
				0.0921	2.4749	0.9998	0.9998	0.0632	2.4037	0.9952	0.9955
				0.1016	2.4749	0.9998	0.9998	0.0667	2.4096	0.9964	0.9966
				0.1270	2.4681	0.9985	0.9986	0.0728	2.4169	0.9979	0.9980
								0.0763	2.4195	0.9984	0.9985
								0.0827	2.4254	0.9998	0.9998
								0.0931	2.4264	0.9998	0.9998
								0.1024	2.4264	0.9998	0.9998
								0.1187	2.4200	0.9985	0.9986
								0.1283	2.4135	0.9972	0.9974

TABLE 3

Integral Properties of the Boundary Layers.

(a)  $r = 0.89$ 

$x$	$\delta_1$ in	$\delta_2$ in	$\delta_3$ in	$\delta_1^i$ in	$\delta_2^i$ in	$\delta_3^i$ in	$H_{12}$	$H_{32}$	$H_{12}^i$	$H_{32}^i$	$\frac{u_\delta}{v_\delta} \times 10^5$ /in	$M_\delta$
$M_\infty = 0.597 \quad Re_\ell = 9.98 \times 10^6$												
0.4	0.0635	0.0363	0.0624	0.0590	0.0375	0.0645	1.751	1.720	1.571	1.718	1.752	0.642
0.475	0.1095	0.0630	0.1064	0.1030	0.0649	0.1096	1.739	1.690	1.587	1.689	1.644	0.586
0.55	0.1572	0.0939	0.1597	0.1480	0.0965	0.1641	1.675	1.701	1.533	1.700	1.612	0.570
0.7	0.3059	0.1858	0.3157	0.2897	0.1906	0.3235	1.646	1.699	1.520	1.697	1.472	0.538
0.833	0.1683	0.1142	0.2037	0.1566	0.1166	0.2080	1.473	1.784	1.343	1.783	1.543	0.566
0.983	0.0859	0.0609	0.1130	0.0781	0.0620	0.1149	1.411	1.856	1.261	1.855	1.662	0.622
$M_\infty = 1.398 \quad Re_\ell = 10.08 \times 10^6$												
0.4	0.0654	0.0234	0.0417	0.0422	0.0282	0.0500	2.799	1.784	1.499	1.775	1.516	1.766
0.475	0.0970	0.0362	0.0628	0.0671	0.0437	0.0755	2.681	1.737	1.535	1.727	1.592	1.633
0.55	0.1581	0.0618	0.1043	0.1189	0.0736	0.1234	2.559	1.687	1.616	1.678	1.647	1.454
0.7	0.3244	0.1359	0.2263	0.2576	0.1573	0.2607	2.388	1.665	1.638	1.658	1.702	1.288
0.833	0.1837	0.0916	0.1629	0.1381	0.1014	0.1799	2.006	1.779	1.362	1.775	1.706	1.254
0.983	0.1233	0.0665	0.1224	0.0912	0.0714	0.1313	1.855	1.842	1.276	1.839	1.695	1.215
$M_\infty = 1.404 \quad Re_\ell = 19.34 \times 10^6$												
0.4	0.0584	0.0207	0.0370	0.0376	0.0249	0.0443	2.824	1.789	1.509	1.779	2.922	1.777
0.475	0.0840	0.0312	0.0544	0.0578	0.0377	0.0654	2.692	1.744	1.533	1.735	3.051	1.646
0.55	0.1356	0.0534	0.0906	0.1008	0.0635	0.1073	2.542	1.698	1.587	1.689	3.219	1.470
0.7	0.2866	0.1234	0.2077	0.2252	0.1421	0.2382	2.322	1.683	1.584	1.676	3.219	1.289
0.833	0.1594	0.0806	0.1450	0.1179	0.0887	0.1593	1.979	1.799	1.329	1.796	3.218	1.269
0.983	0.1112	0.0605	0.1120	0.0820	0.0647	0.1197	1.839	1.851	1.267	1.849	3.303	1.211

TABLE 3(a)—continued

x	$\delta_1$ in	$\delta_2$ in	$\delta_3$ in	$\delta_1^i$ in	$\delta_2^i$ in	$\delta_3^i$ in	$H_{12}$	$H_{32}$	$H_{12}^i$	$H_{32}^i$	$\frac{u_\delta}{v_\delta} \times 10^5$ /in	$M_\delta$
$M_\infty = 1.700 \quad Re_\ell = 10.00 \times 10^6$												
0.4	0.0800	0.0244	0.0438	0.0461	0.0312	0.0556	3.273	1.792	1.474	1.779	1.419	2.087
0.55	0.1594	0.0538	0.0925	0.1051	0.0684	0.1168	2.963	1.720	1.537	1.708	1.592	1.815
0.7	0.2901	0.1070	0.1807	0.2081	0.1315	0.2206	2.712	1.689	1.583	1.678	1.712	1.597
0.833	0.1763	0.0764	0.1365	0.1195	0.0881	0.1570	2.309	1.788	1.356	1.782	1.712	1.529
0.983	0.1172	0.0545	0.1009	0.0770	0.0603	0.1114	2.149	1.851	1.276	1.847	1.768	1.495
$M_\infty = 2.000 \quad Re_\ell = 9.88 \times 10^6$												
0.4	0.0916	0.0238	0.0429	0.0471	0.0322	0.0575	3.851	1.802	1.462	1.785	1.311	2.414
0.475	0.1232	0.0329	0.0583	0.0668	0.0453	0.0795	3.746	1.770	1.473	1.754	1.363	2.333
0.55	0.1678	0.0482	0.0839	0.0986	0.0656	0.1131	3.481	1.739	1.504	1.724	1.487	2.153
0.7	0.2736	0.0878	0.1505	0.1751	0.1149	0.1954	3.117	1.714	1.524	1.701	1.693	1.918
0.833	0.1689	0.0636	0.1148	0.1023	0.0764	0.1372	2.654	1.804	1.340	1.796	1.778	1.804
0.983	0.1180	0.0478	0.0888	0.0695	0.0544	0.1008	2.469	1.858	1.277	1.853	1.816	1.751
$M_\infty = 2.401 \quad Re_\ell = 9.92 \times 10^6$												
0.4	0.0582	0.0110	0.0194	0.0296	0.0172	0.0297	5.312	1.768	1.723	1.731	1.266	2.881
0.55	0.1170	0.0281	0.0510	0.0549	0.0392	0.0705	4.165	1.815	1.403	1.800	1.453	2.615
0.7	0.1903	0.0527	0.0950	0.0965	0.0707	0.1264	3.608	1.802	1.365	1.788	1.631	2.354
0.833	0.1447	0.0475	0.0885	0.0722	0.0569	0.1058	3.048	1.865	1.267	1.858	1.813	2.145
0.983	0.0959	0.0322	0.0606	0.0485	0.0375	0.0704	2.977	1.883	1.292	1.874	1.849	2.096
$M_\infty = 2.799 \quad Re_\ell = 10.10 \times 10^6$												
0.4	0.0796	0.0129	0.0233	0.0337	0.0214	0.0379	6.167	1.804	1.576	1.770	1.216	3.37
0.55	0.1323	0.0259	0.0474	0.0537	0.0387	0.0701	5.112	1.830	1.387	1.810	1.411	3.053
0.7	0.1410	0.0329	0.0611	0.0581	0.0442	0.0816	4.285	1.858	1.313	1.844	1.608	2.759
0.833	0.1199	0.0333	0.0631	0.0510	0.0404	0.0763	3.599	1.895	1.262	1.885	1.866	2.476
0.983	0.0998	0.0283	0.0536	0.0436	0.0339	0.0639	3.531	1.896	1.286	1.886	1.922	2.427

TABLE 3—*continued*(b)  $r = 1$ 

$x$	$\delta_1$ in	$\delta_2$ in	$\delta_3$ in	$\delta_1^i$ in	$\delta_2^i$ in	$\delta_3^i$ in	$H_{12}$	$H_{32}$	$H_{12}^i$	$H_{32}^i$	$\frac{u_\delta}{v_\delta}$ $\times 10^5$ /in	$M_\delta$
$M_\infty = 0.597 \quad Re_\ell = 9.98 \times 10^6$												
0.4	0.0638	0.0360	0.0620	0.0587	0.0374	0.0643	1.771	1.721	1.569	1.719	1.752	0.642
0.475	0.1099	0.0626	0.1059	0.1026	0.0647	0.1094	1.756	1.692	1.585	1.690	1.644	0.586
0.55	0.1578	0.0933	0.1588	0.1474	0.0963	0.1638	1.691	1.702	1.531	1.701	1.612	0.570
0.7	0.3069	0.1849	0.3143	0.2887	0.1902	0.3229	1.660	1.700	1.518	1.698	1.472	0.538
0.833	0.1689	0.1135	0.2026	0.1559	0.1162	0.2073	1.488	1.785	1.341	1.784	1.543	0.566
0.983	0.0863	0.0604	0.1122	0.0777	0.0616	0.1144	1.429	1.856	1.260	1.865	1.662	0.622
$M_\infty = 1.398 \quad Re_\ell = 10.08 \times 10^6$												
0.4	0.0663	0.0225	0.0403	0.0412	0.0276	0.0491	2.948	1.789	1.493	1.779	1.516	1.766
0.475	0.0982	0.0350	0.0609	0.0657	0.0430	0.0745	2.808	1.742	1.526	1.732	1.592	1.633
0.55	0.1599	0.0601	0.1017	0.1168	0.0728	0.1224	2.661	1.692	1.606	1.682	1.647	1.454
0.7	0.3275	0.1328	0.2217	0.2541	0.1560	0.2591	2.467	1.670	1.628	1.661	1.702	1.288
0.833	0.1858	0.0894	0.1594	0.1357	0.1000	0.1778	2.078	1.783	1.357	1.778	1.706	1.254
0.983	0.1263	0.0656	0.1208	0.0907	0.0710	0.1306	1.926	1.842	1.276	1.839	1.695	1.215
$M_\infty = 1.404 \quad Re_\ell = 19.34 \times 10^6$												
0.4	0.0591	0.0199	0.0356	0.0366	0.0243	0.0434	2.977	1.794	1.505	1.784	2.922	1.777
0.475	0.0851	0.0301	0.0527	0.0565	0.0370	0.0645	2.822	1.749	1.525	1.740	3.051	1.646
0.55	0.1371	0.0518	0.0882	0.0989	0.0627	0.1062	2.645	1.703	1.578	1.693	3.219	1.470
0.7	0.2895	0.1205	0.2034	0.2219	0.1409	0.2365	2.401	1.687	1.575	1.679	3.219	1.289
0.833	0.1611	0.0782	0.1409	0.1157	0.0870	0.1564	2.059	1.802	1.329	1.797	3.218	1.269
0.983	0.1126	0.0591	0.1095	0.0805	0.0637	0.1179	1.906	1.854	1.264	1.851	3.303	1.211

TABLE 3(b)—continued

$x$	$\delta_1$ in	$\delta_2$ in	$\delta_3$ in	$\delta_1^i$ in	$\delta_2^i$ in	$\delta_3^i$ in	$H_{12}$	$H_{32}$	$H_{12}^i$	$H_{32}^i$	$\frac{u_\delta}{v_\delta} \times 10^5$ /in	$M_\delta$
$M_\infty = 1.700 \quad Re_\ell = 10.00 \times 10^6$												
0.4	0.0811	0.0233	0.0419	0.0446	0.0304	0.0543	3.480	1.799	1.468	1.784	1.419	2.087
0.55	0.1535	0.0487	0.0833	0.0986	0.0643	0.1097	3.152	1.711	1.534	1.707	1.592	1.815
0.7	0.2935	0.1036	0.1755	0.2040	0.1299	0.2185	2.832	1.694	1.570	1.682	1.712	1.597
0.833	0.1779	0.0737	0.1322	0.1161	0.0861	0.1539	2.414	1.793	1.348	1.787	1.712	1.529
0.983	0.1197	0.0531	0.0984	0.0757	0.0594	0.1098	2.254	1.853	1.275	1.849	1.768	1.495
$M_\infty = 2.000 \quad Re_\ell = 9.88 \times 10^6$												
0.4	0.0929	0.0225	0.0407	0.0454	0.0312	0.0559	4.125	1.809	1.454	1.791	1.311	2.414
0.475	0.1249	0.0312	0.0555	0.0645	0.0441	0.0777	4.002	1.778	1.462	1.761	1.363	2.333
0.55	0.1701	0.0460	0.0803	0.0956	0.0641	0.1110	3.698	1.747	1.491	1.731	1.487	2.153
0.7	0.2772	0.0843	0.1451	0.1705	0.1129	0.1927	3.289	1.721	1.510	1.707	1.698	1.918
0.833	0.1714	0.0612	0.1106	0.0993	0.0746	0.1343	2.802	1.809	1.332	1.801	1.778	1.804
0.983	0.1197	0.0459	0.0855	0.0673	0.0528	0.0981	2.610	1.863	1.274	1.857	1.816	1.751
$M_\infty = 2.401 \quad Re_\ell = 9.92 \times 10^6$												
0.4	0.0589	0.0103	0.0183	0.0285	0.0166	0.0289	5.723	1.776	1.714	1.739	1.266	2.881
0.55	0.1257	0.0283	0.0520	0.0546	0.0397	0.0720	4.435	1.836	1.375	1.815	1.453	2.615
0.7	0.1930	0.0500	0.0904	0.0928	0.0685	0.1229	3.862	1.809	1.355	1.795	1.631	2.354
0.833	0.1476	0.0453	0.0846	0.0697	0.0551	0.1026	3.261	1.870	1.264	1.861	1.813	2.145
0.983	0.0974	0.0306	0.0578	0.0467	0.0361	0.0679	3.181	1.887	1.290	1.878	1.849	2.096
$M_\infty = 2.799 \quad Re_\ell = 10.10 \times 10^6$												
0.4	0.0805	0.0120	0.0218	0.0323	0.0206	0.0365	6.696	1.813	1.568	1.777	1.216	3.327
0.55	0.1340	0.0242	0.0445	0.0512	0.0371	0.0674	5.543	1.838	1.379	1.818	1.411	3.053
0.7	0.1430	0.0309	0.0575	0.0554	0.0423	0.0783	4.633	1.865	1.308	1.850	1.608	2.759
0.833	0.1219	0.0314	0.0597	0.0487	0.0386	0.0730	3.879	1.898	1.261	1.889	1.866	2.476
0.983	0.1014	0.0267	0.0507	0.0417	0.0324	0.0612	3.803	1.901	1.286	1.890	1.922	2.427

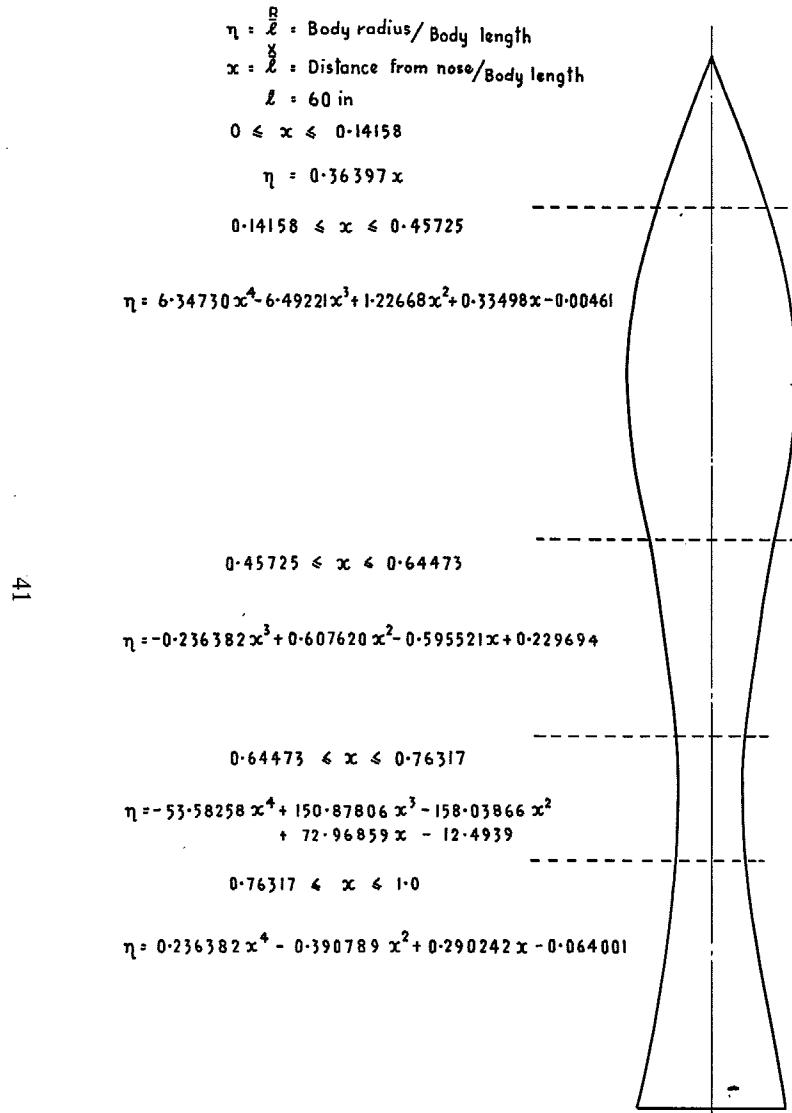


FIG. 1. Geometry of body.

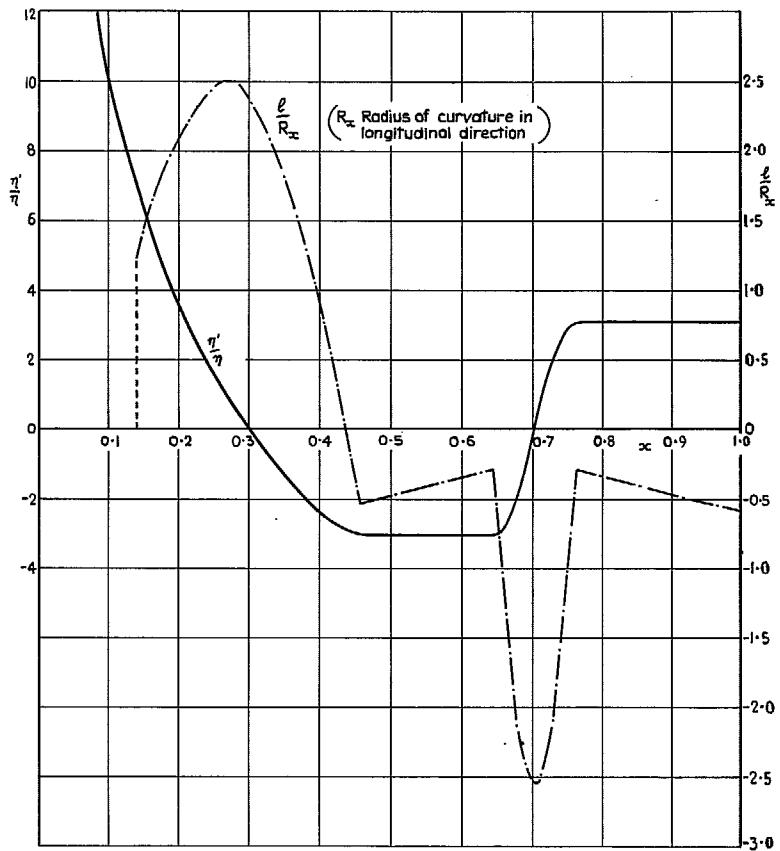


FIG. 2. Divergence parameter and longitudinal curvature.

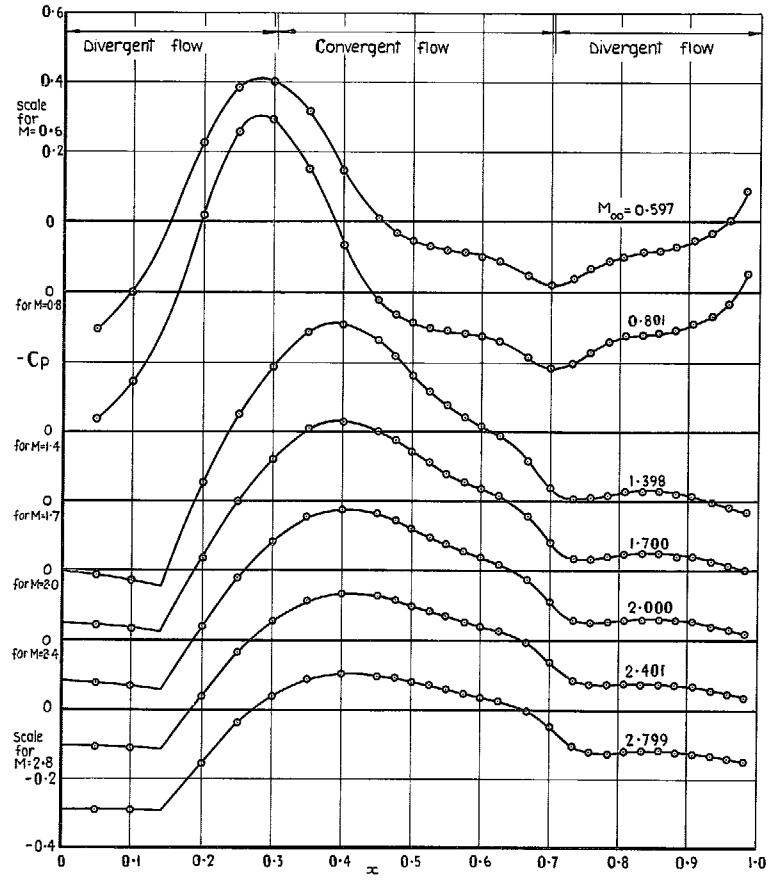


FIG. 3. Pressure distribution  $Re_l \approx 10^7$ .

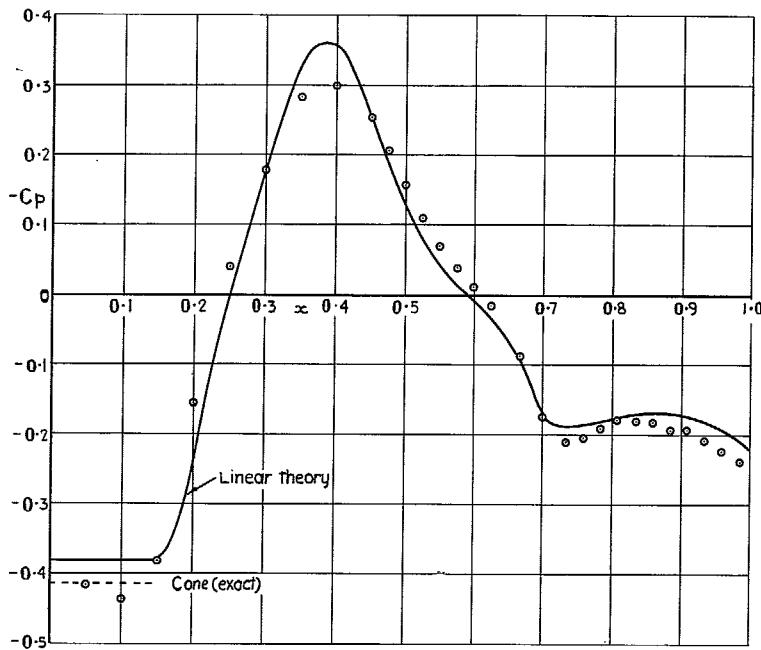


FIG. 4. Comparison of predicted (inviscid) and measured pressure distribution  $M = 1.404$   
 $Re_l = 19.97 \times 10^6$ .

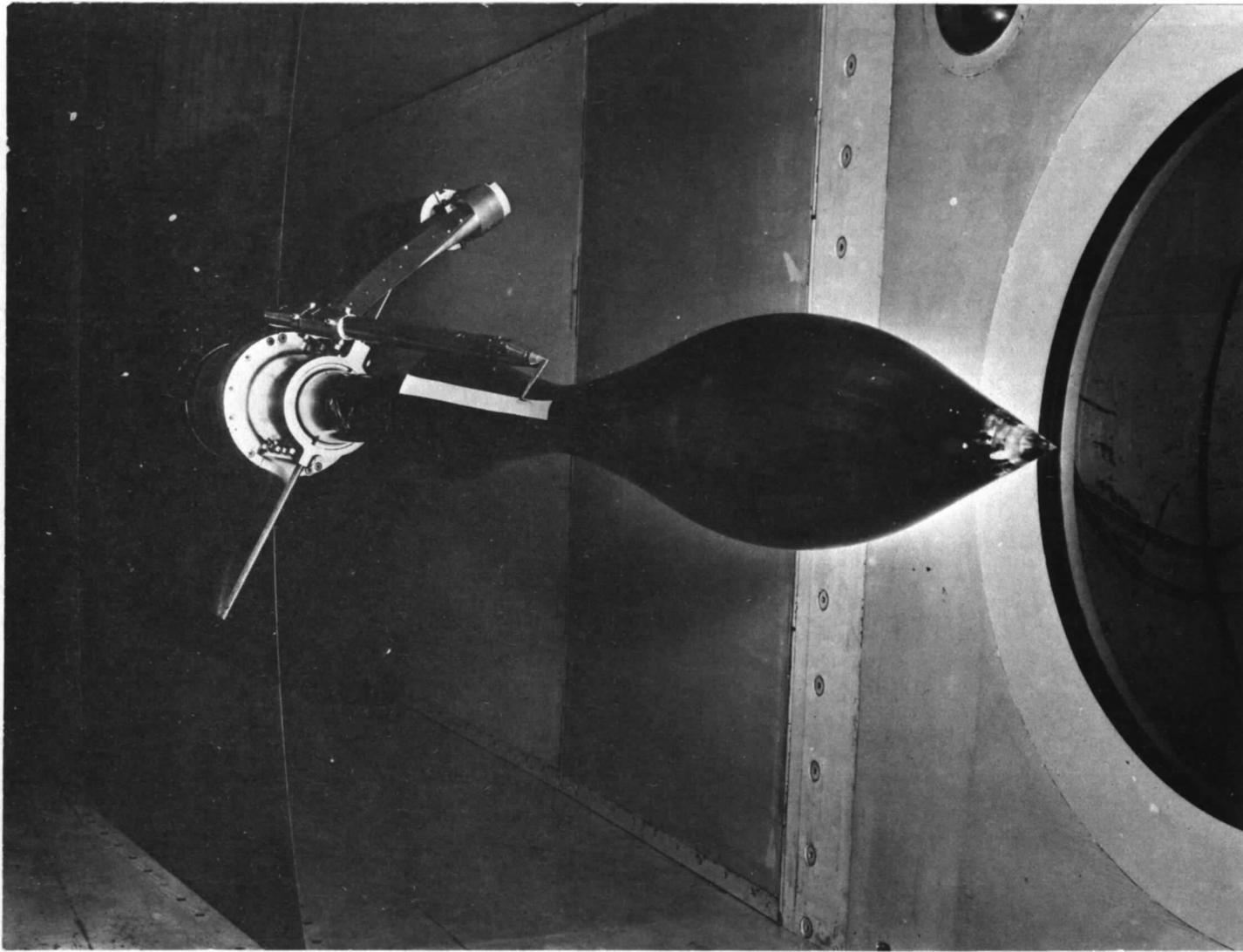


FIG. 5a. Model with boundary-layer survey equipment.

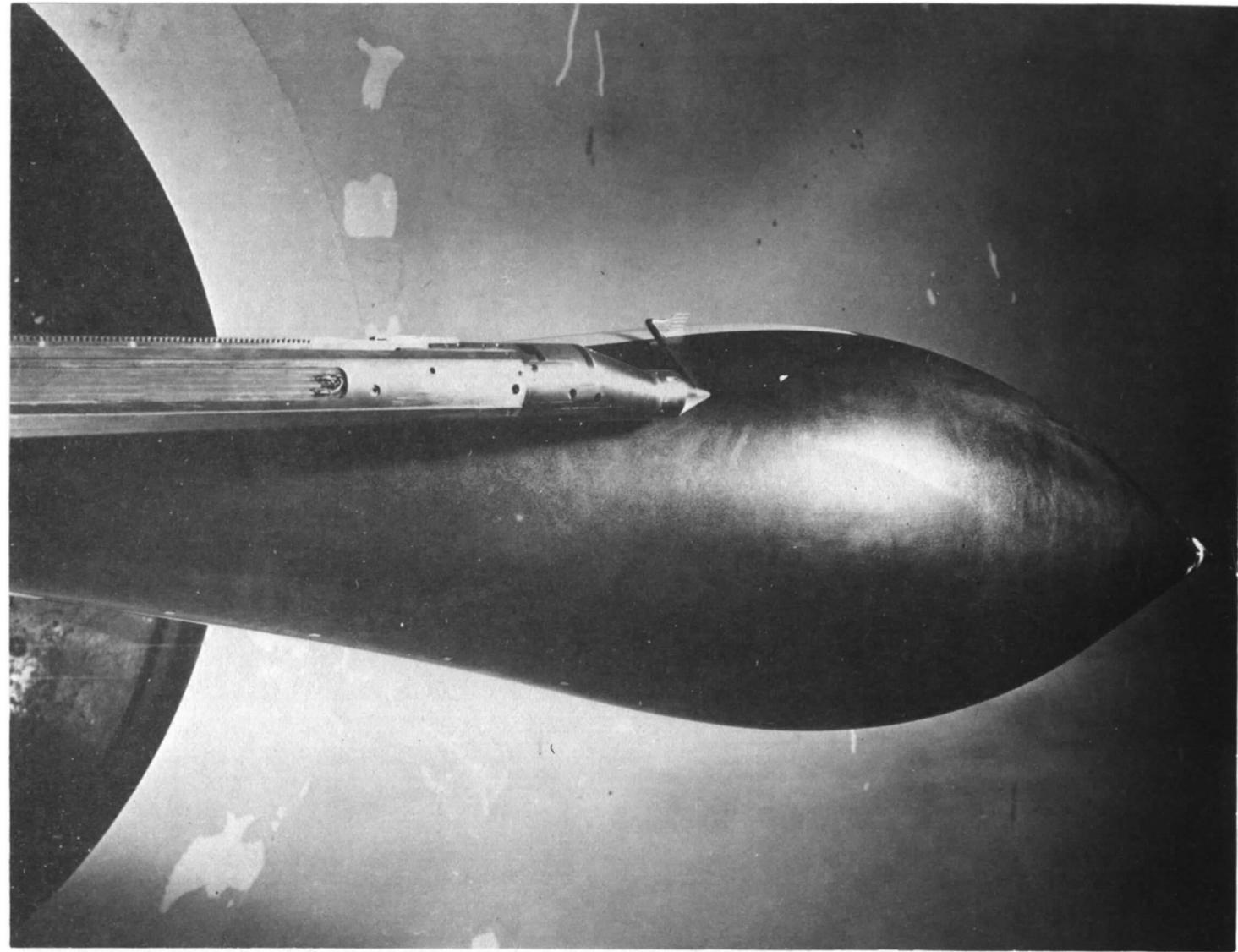


FIG. 5b. Detail of model with rake.

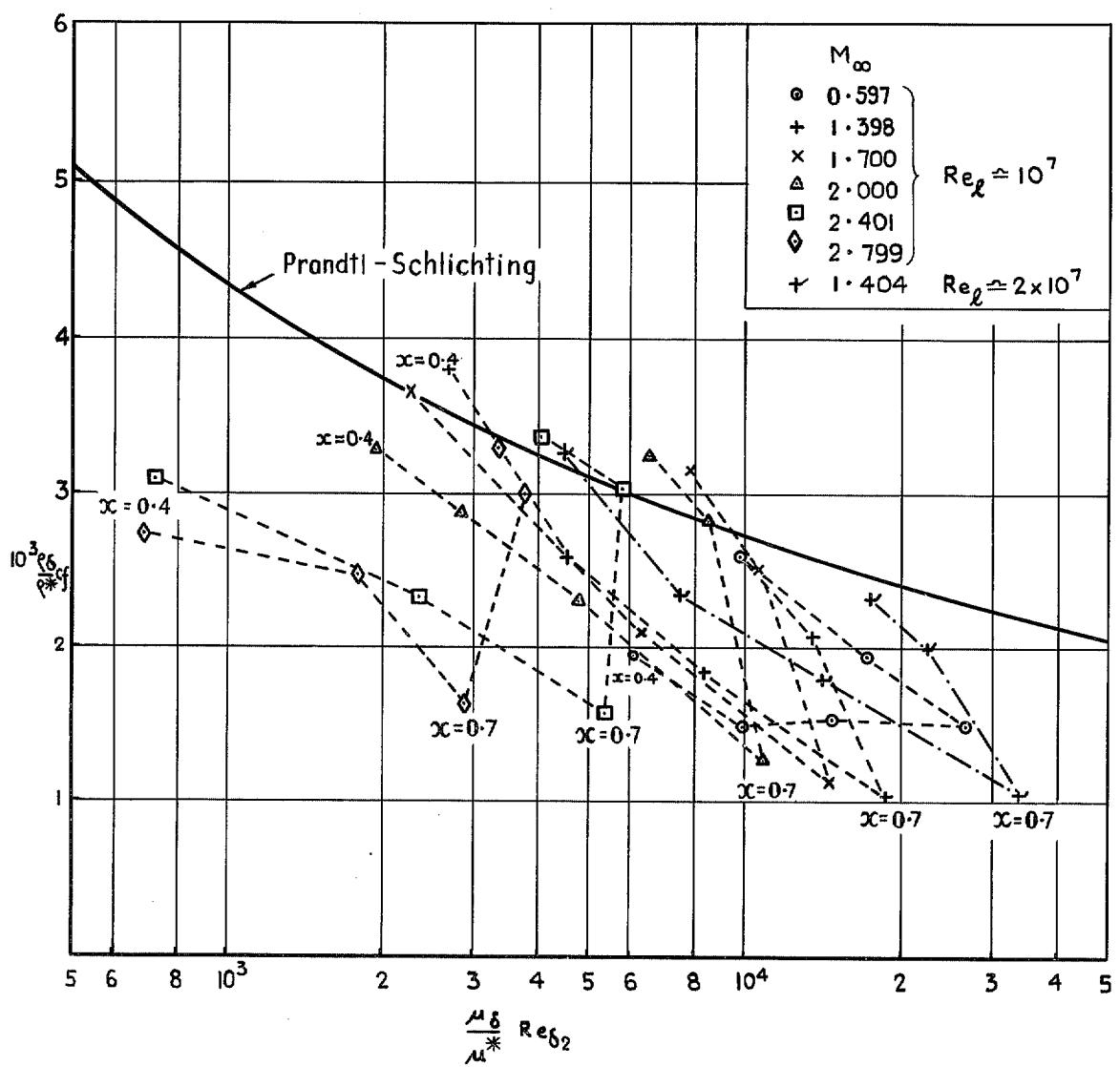


FIG. 6. Local skin friction as a function of momentum thickness Reynolds number in intermediate temperature form.

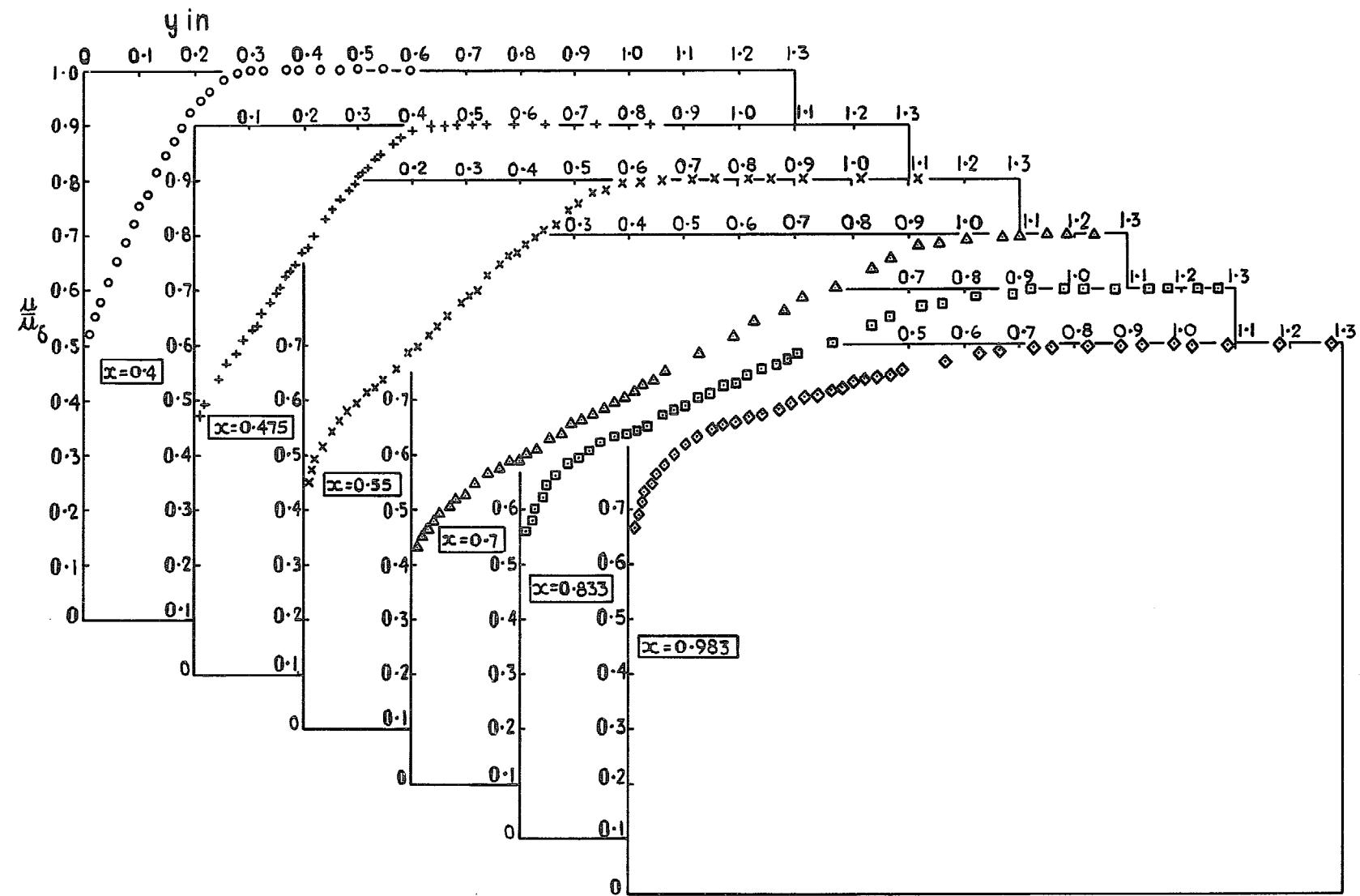


FIG. 7a. Velocity profiles  $M_\infty = 0.597$   $Re_t = 9.98 \times 10^6$ .

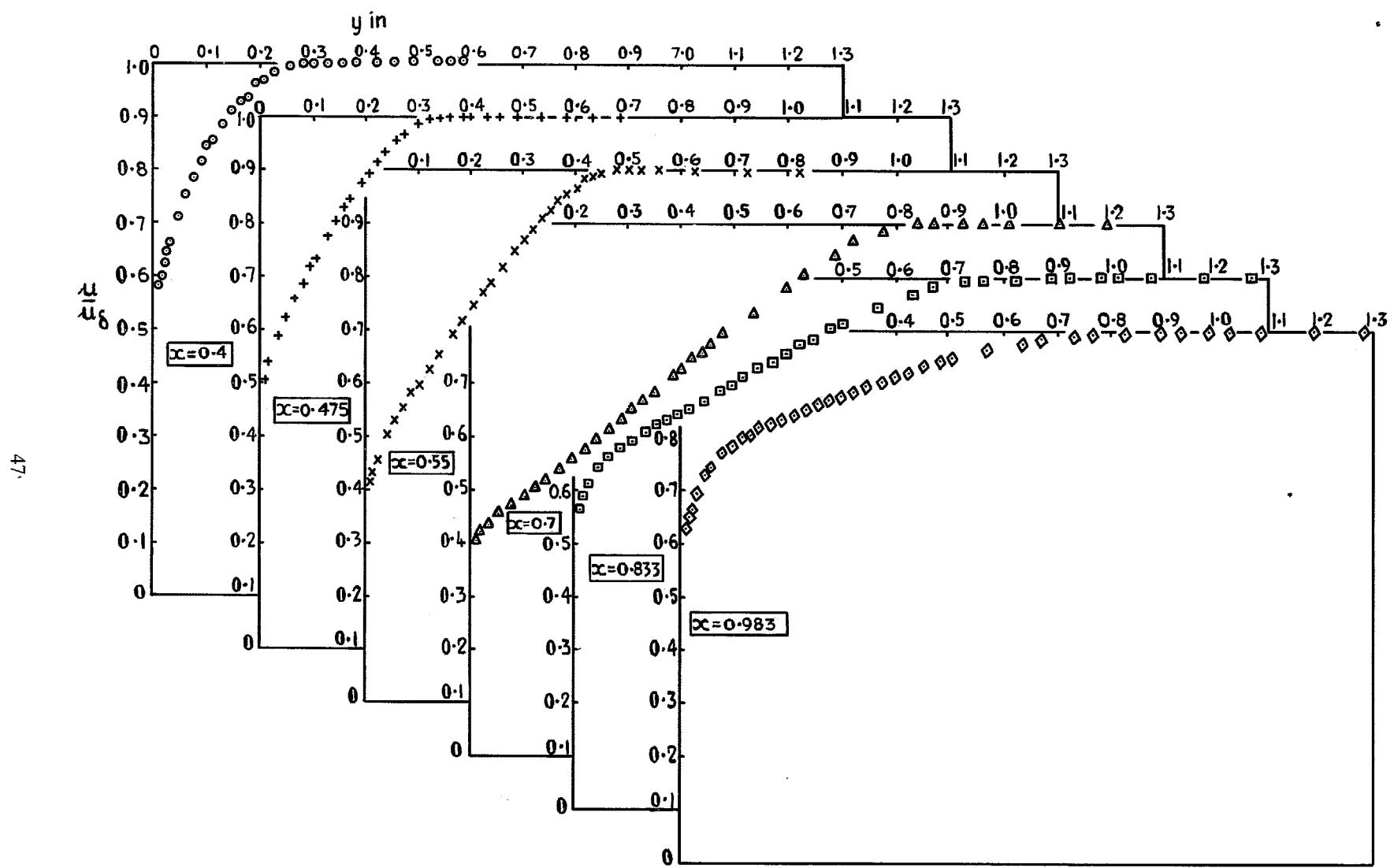


FIG. 7b. Velocity profiles  $M_\infty = 1.398$   $Re_l = 10.1 \times 10^6$ .

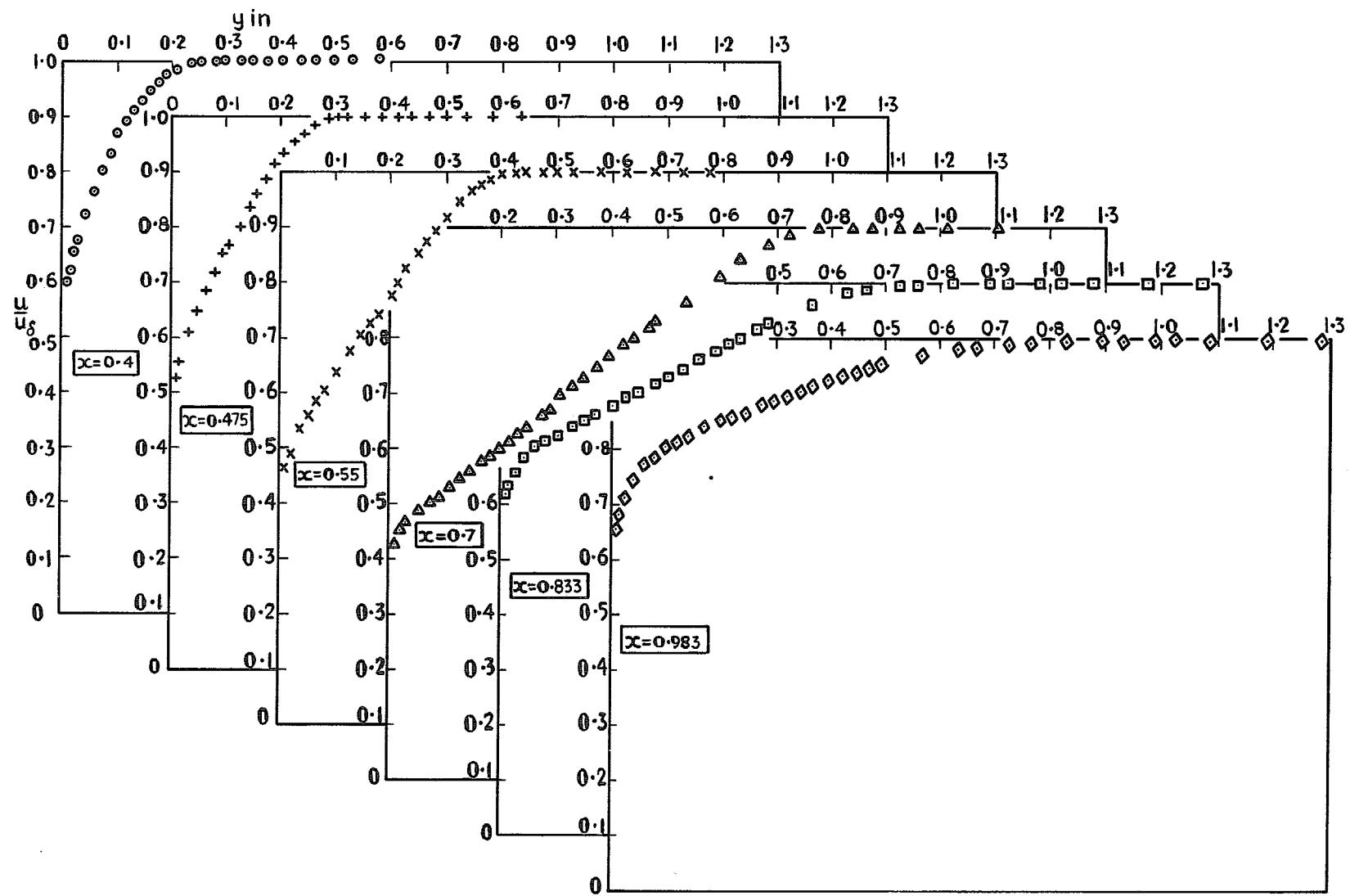


FIG. 7c. Velocity profiles  $M_\infty = 1.404$   $Re_l = 19.34 \times 10^6$ .

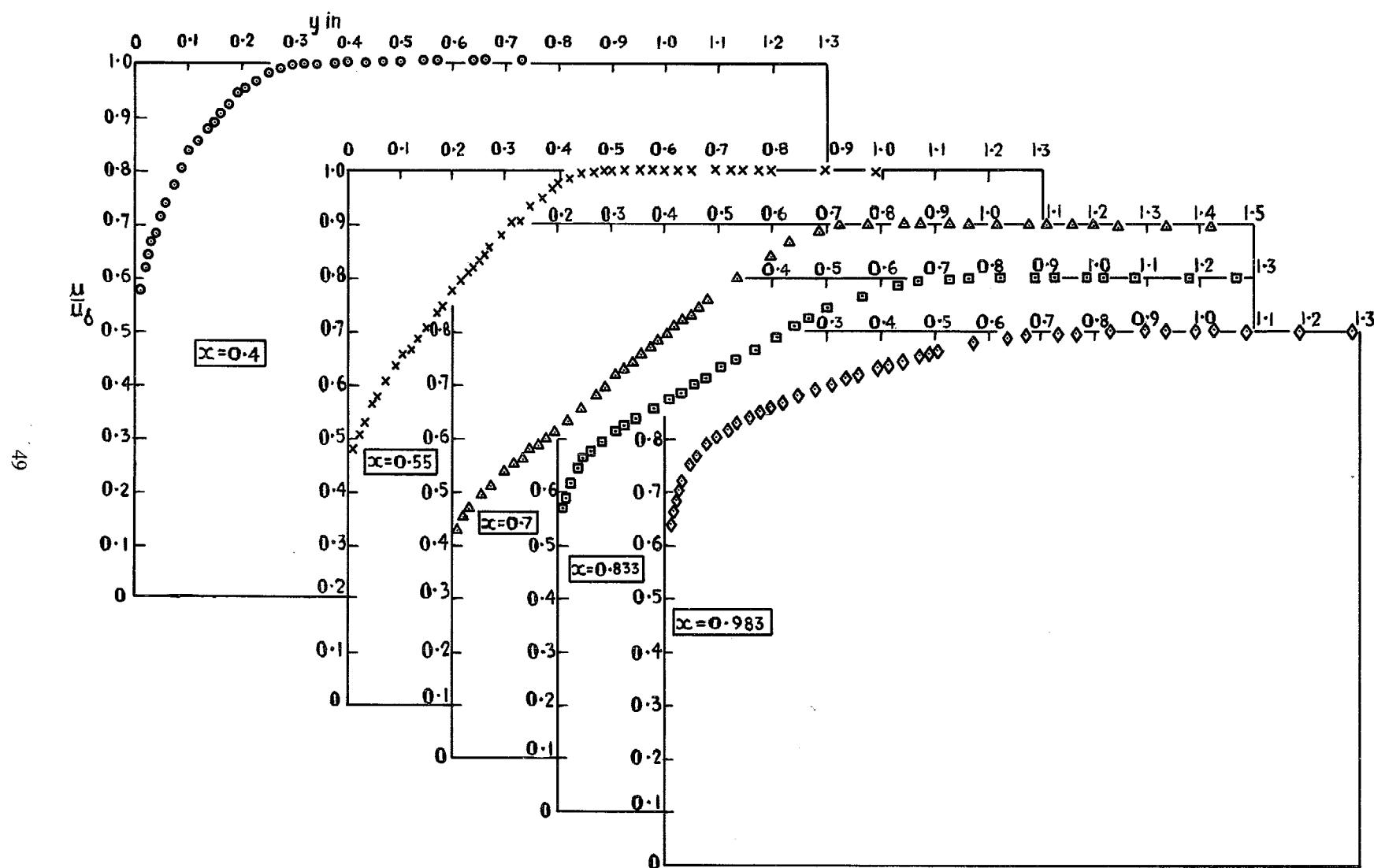


FIG. 7d. Velocity profiles  $M_\infty = 1.700$   $Re_l = 10.00 \times 10^6$ .

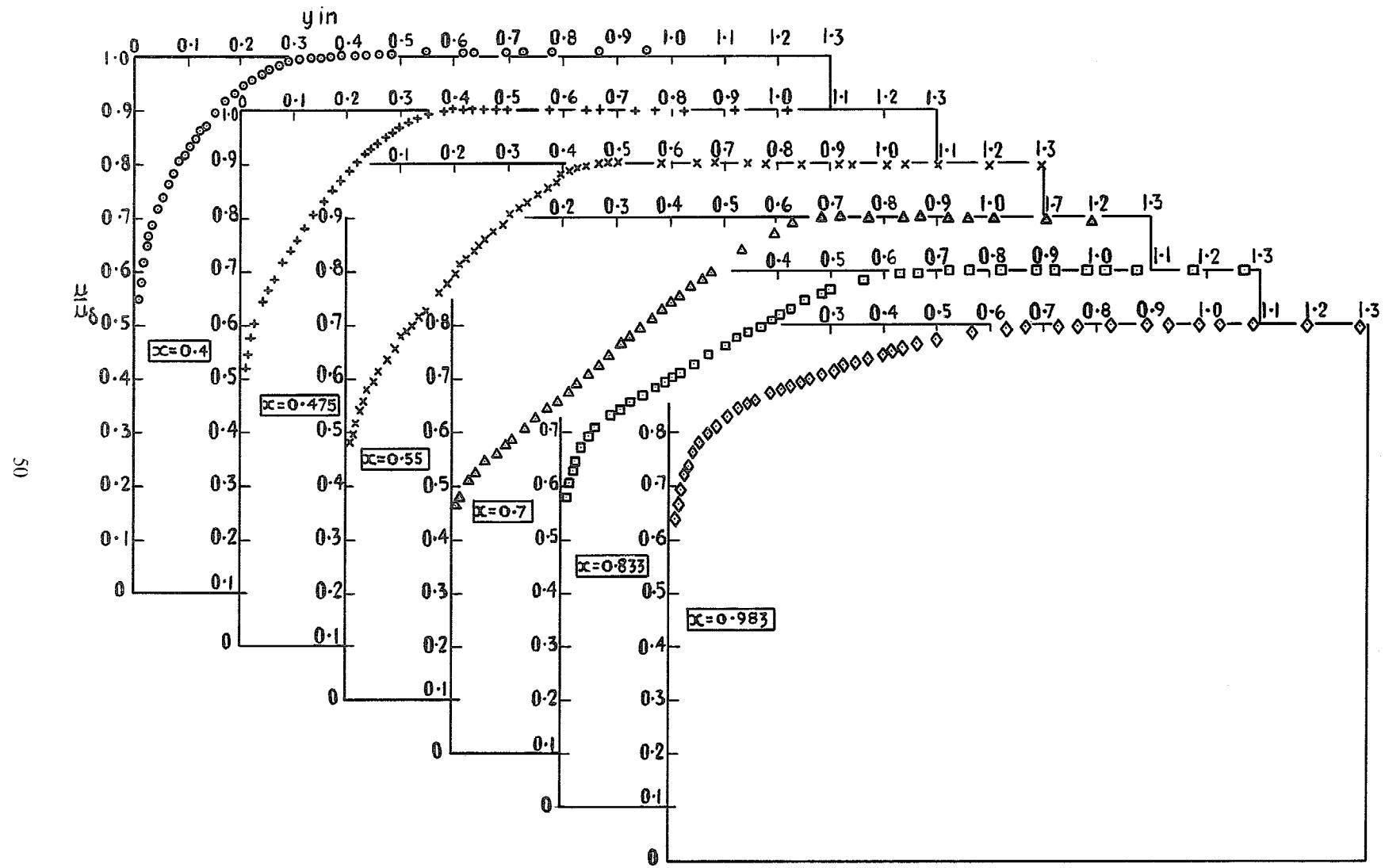


FIG. 7e. Velocity profiles  $M_\infty = 2.001$   $Re_l = 9.88 \times 10^6$ .

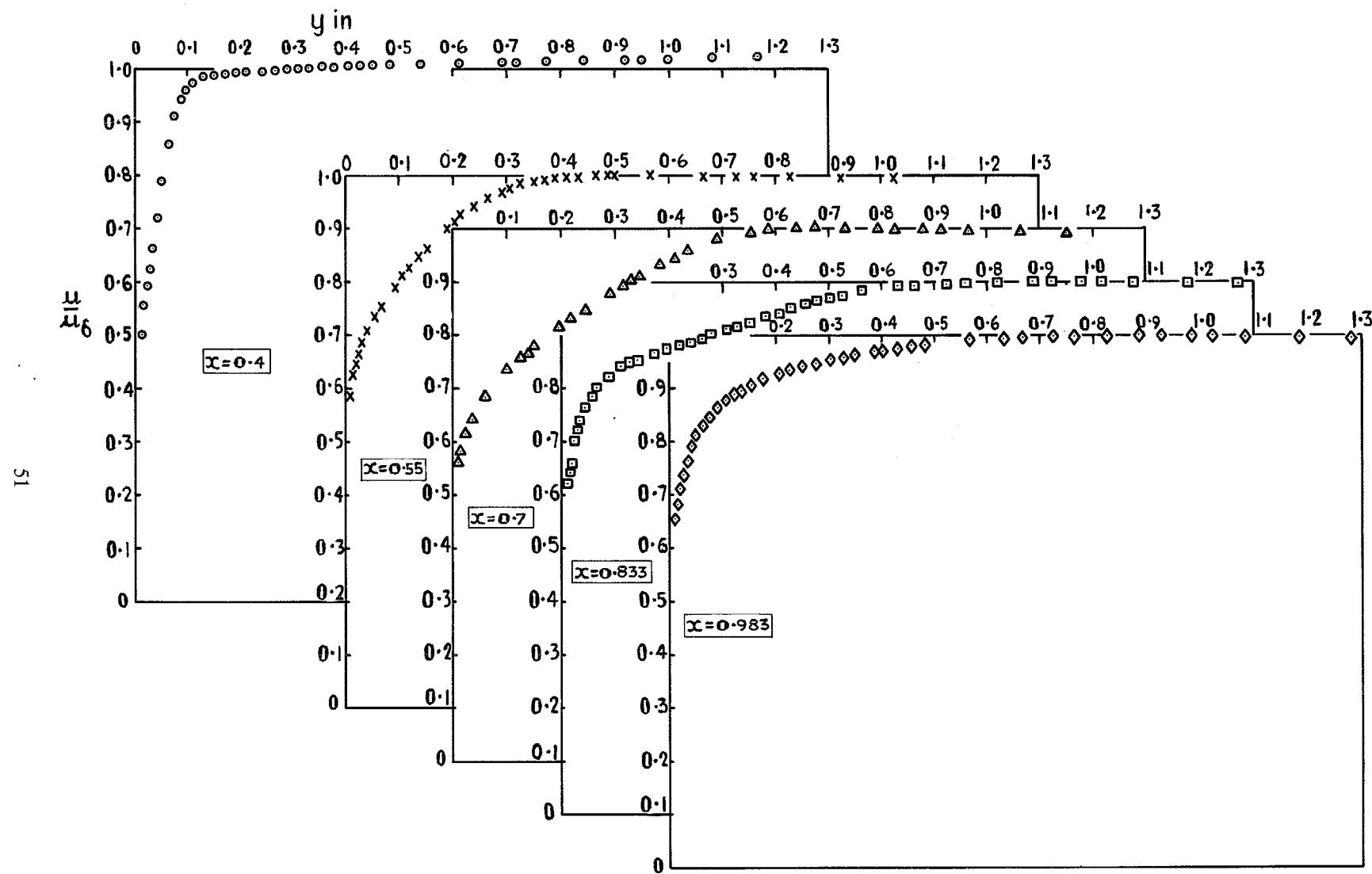


FIG. 7f. Velocity profiles  $M_\infty = 2.401$   $Re_t = 9.92 \times 10^6$ .

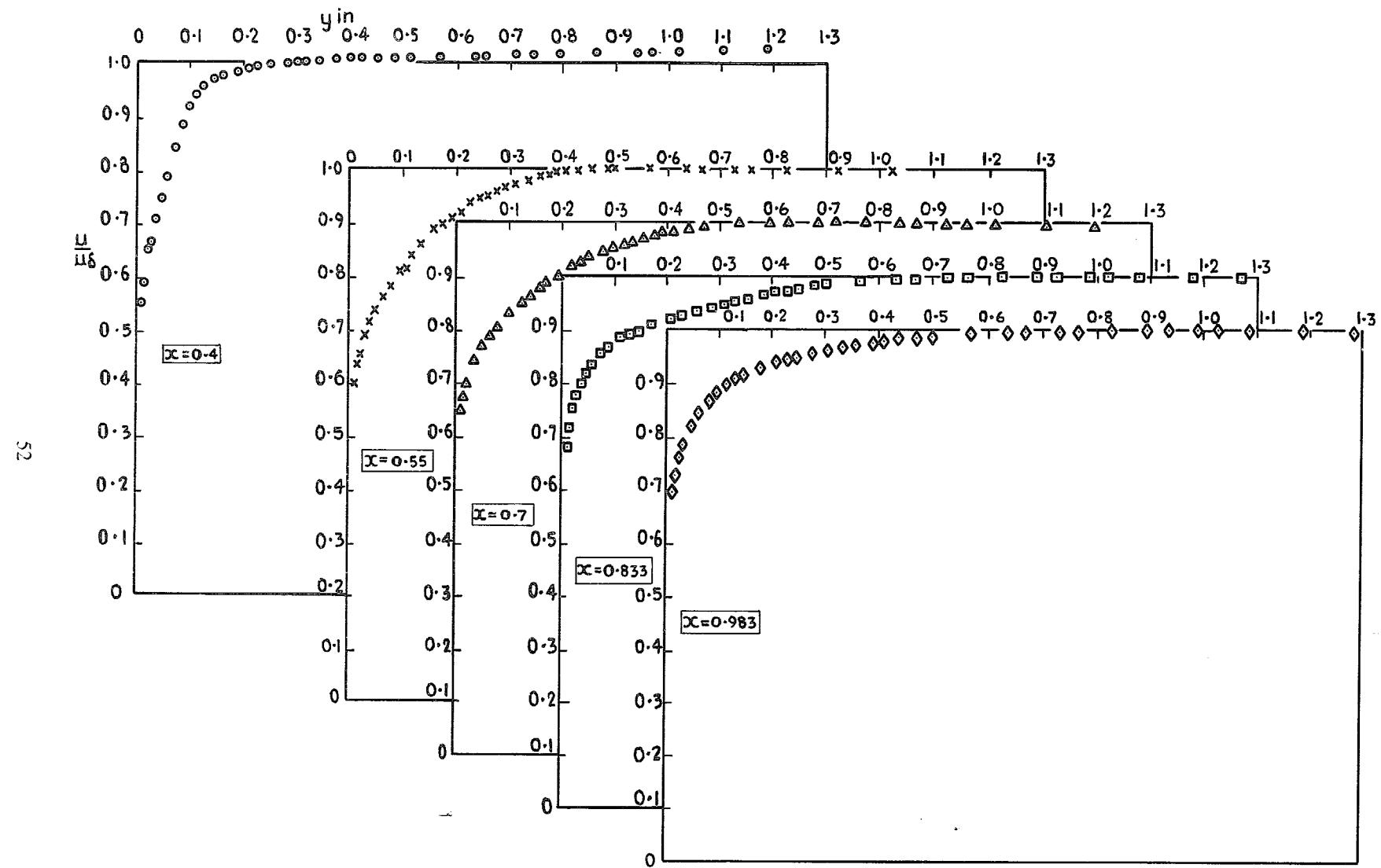
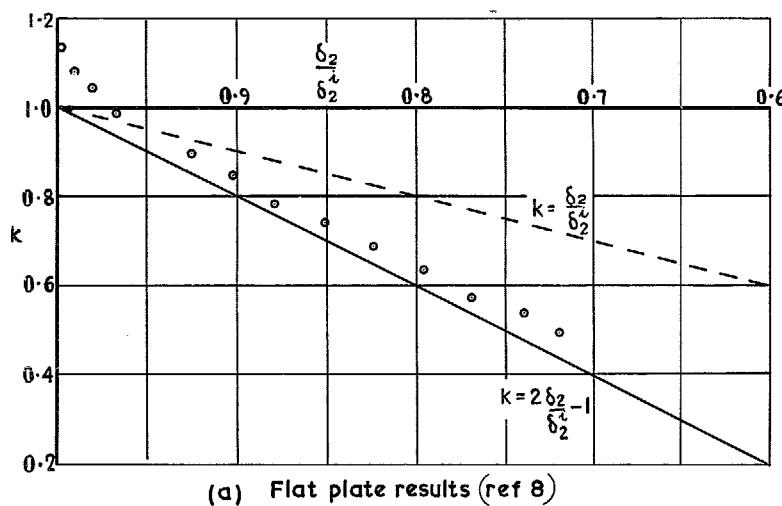
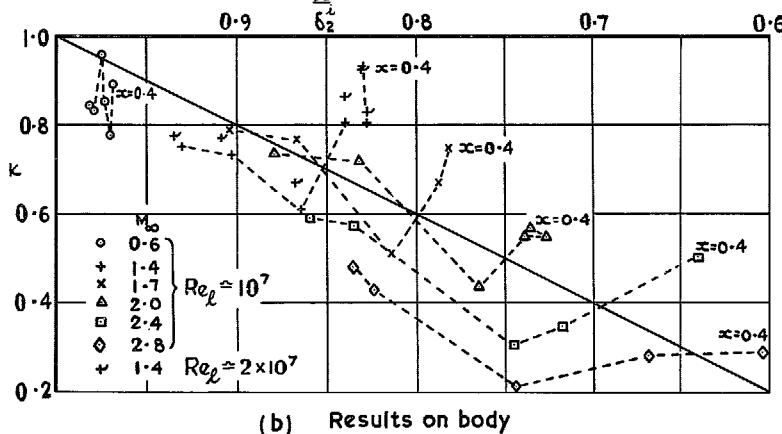


FIG. 7g. Velocity profiles  $M_x = 2.798$   $Re_l = 10.10 \times 10^6$ .



(a) Flat plate results (ref 8)

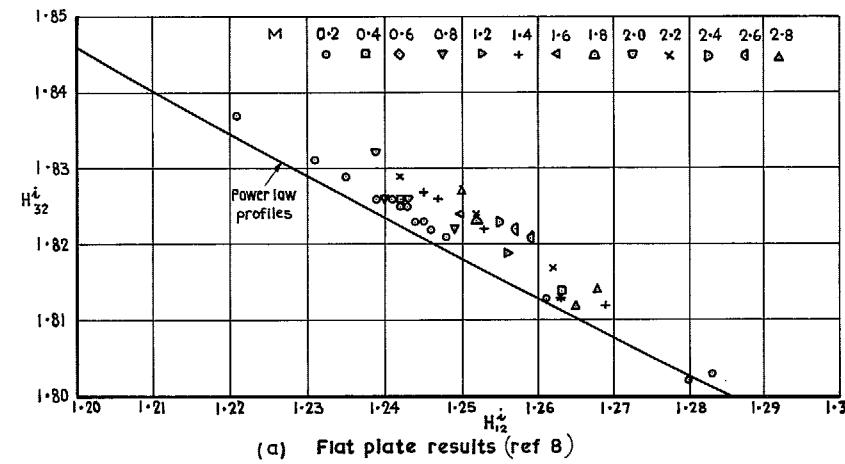
$$k = \frac{c_f}{0.246 \left( \frac{\rho_0 u_\infty \delta_2}{\mu_w} \right)^{0.268}} \quad 10^{-0.678 H_{12}^{1/2}}$$



(b) Results on body

FIG. 8 a & b. Compressibility correction to Ludwig-Tillman formula.

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(a) Flat plate results (ref 8)

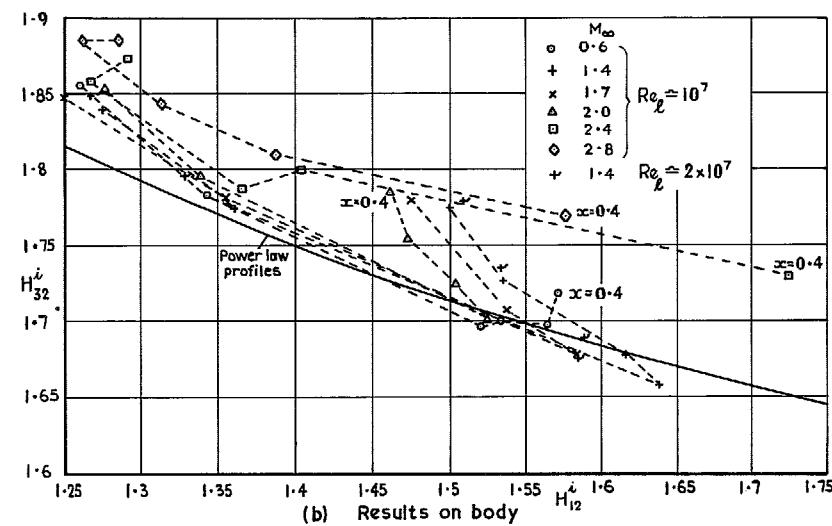
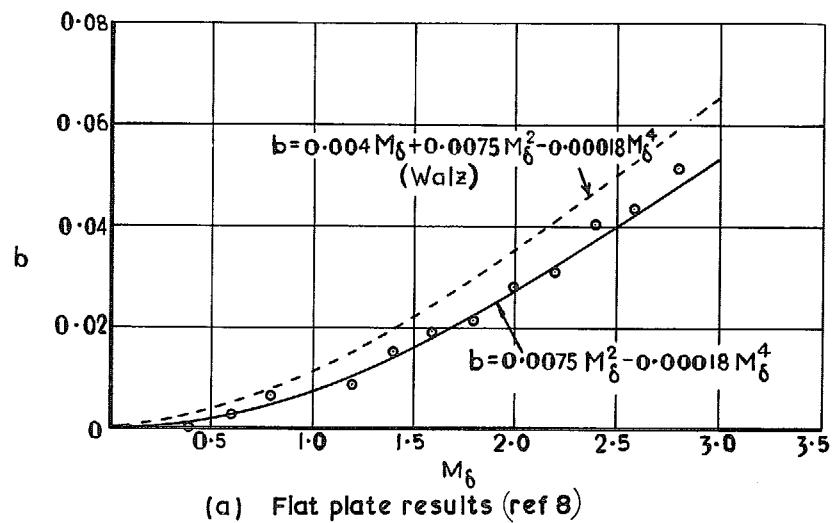


FIG. 9 a & b. Relationship between 'incompressible' shape parameters.



$$H_{32} = H_{32}^i \left[ 1 + (2 - H_{32}^i) b \right]$$

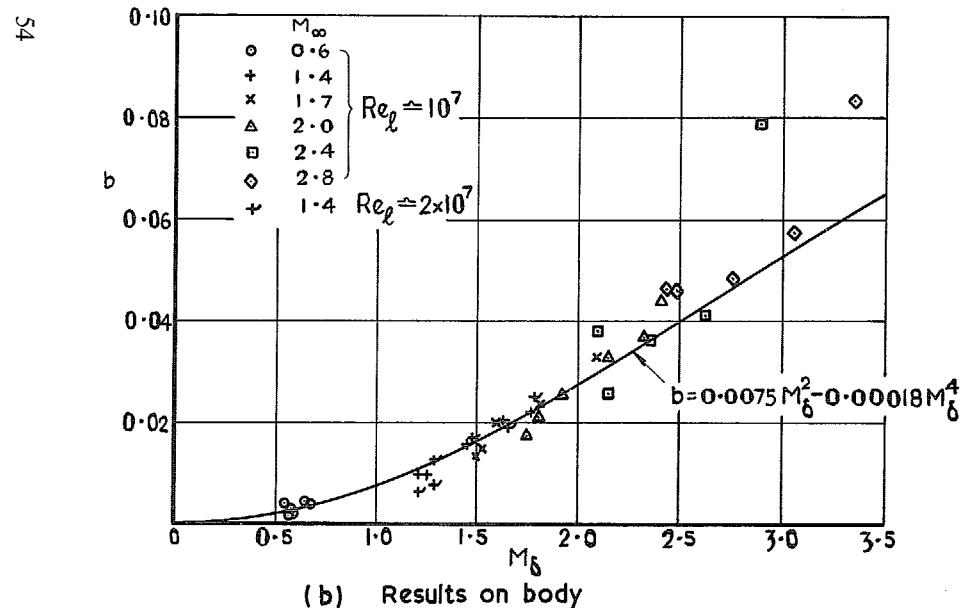
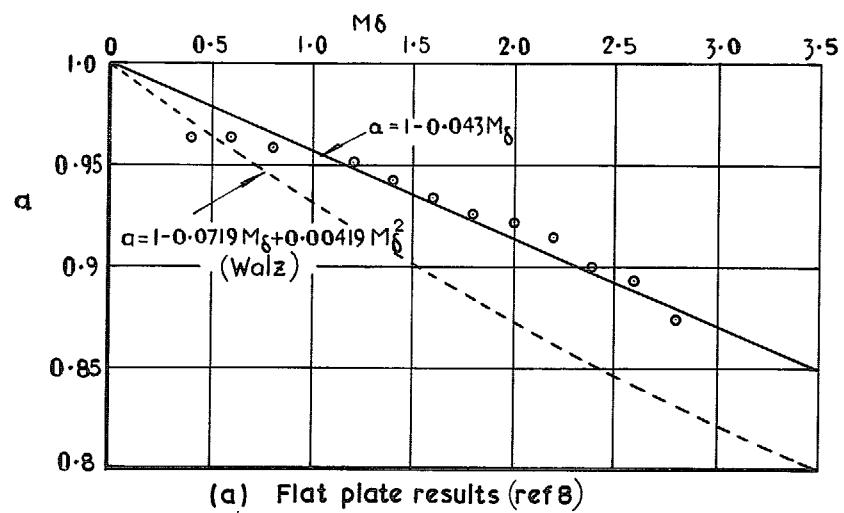


FIG. 10 a & b. Relationship between  $H_{32}$  and  $H_{32}^i$ .



$$\frac{\delta_2^i}{\delta_2} = 1 + \tau \frac{Y-1}{2} M_\infty^2 H_{32}^i (2 - H_{32}^i) a$$

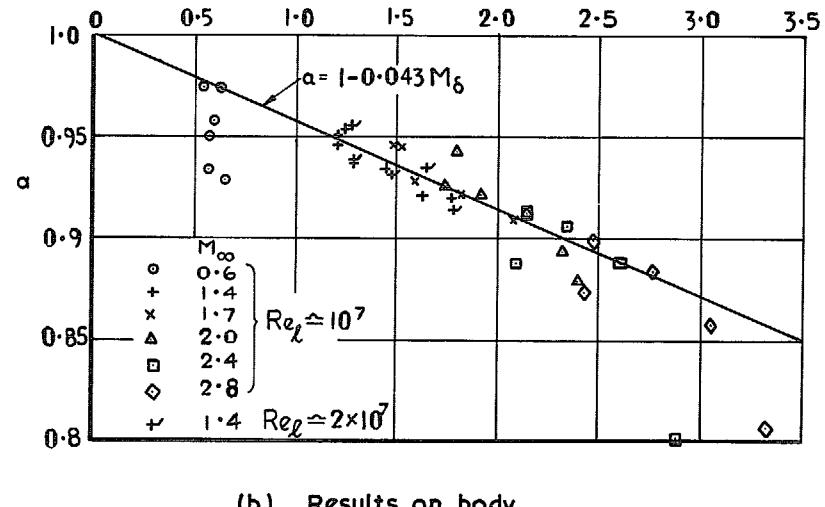
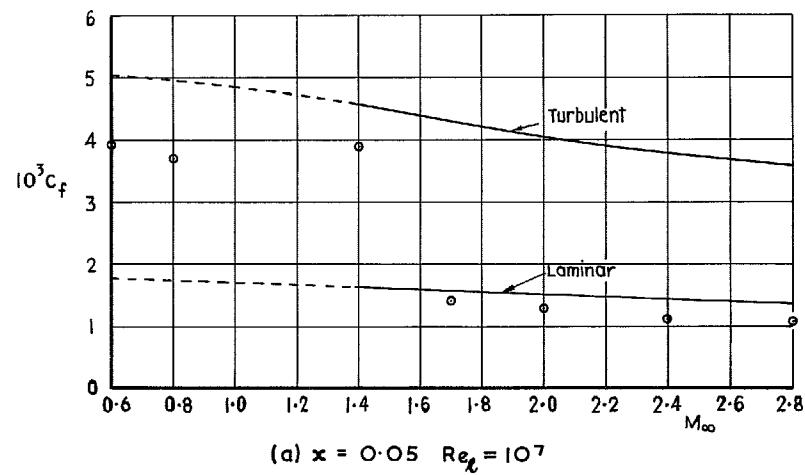


FIG. 11 a & b. Determination of  $\frac{\delta_2^i}{\delta_2}$ .



(a)  $x = 0.05 \quad Re_l = 10^7$

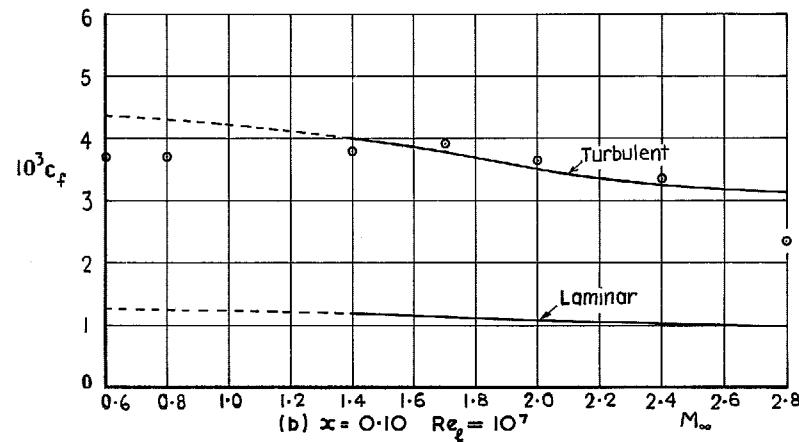


FIG. 12 a & b. Skin friction on conical nose.

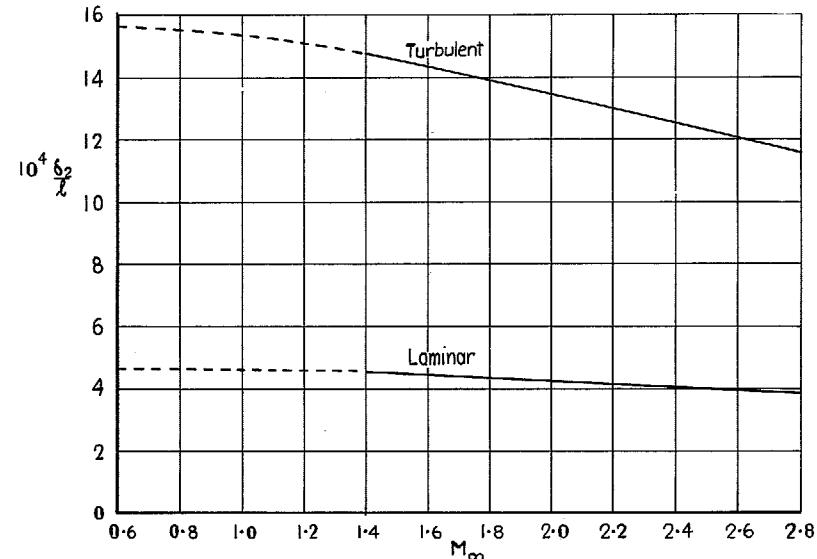


FIG. 13. Calculated momentum thickness  
 $x = 0.1416 \quad Re_l = 10^7$ .

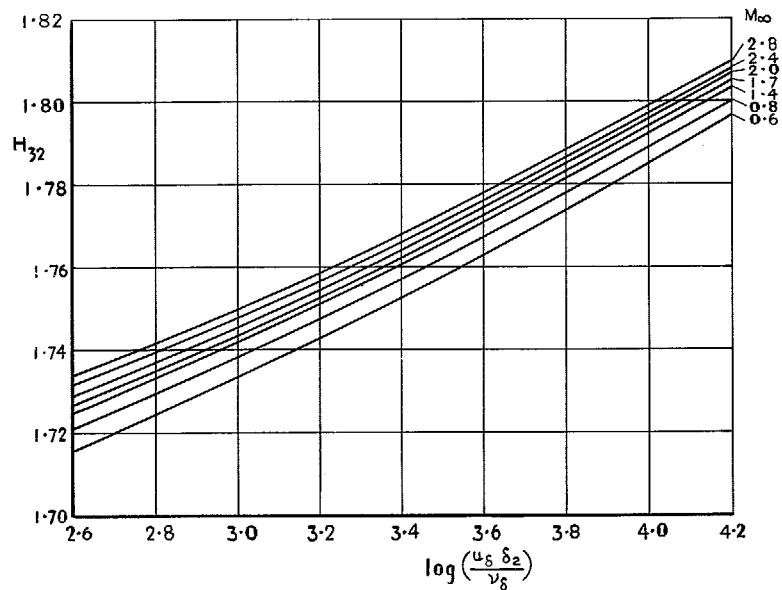


FIG. 14. Chart for determination of  $H_{32}$  at  
 $x = 0.1416$ .

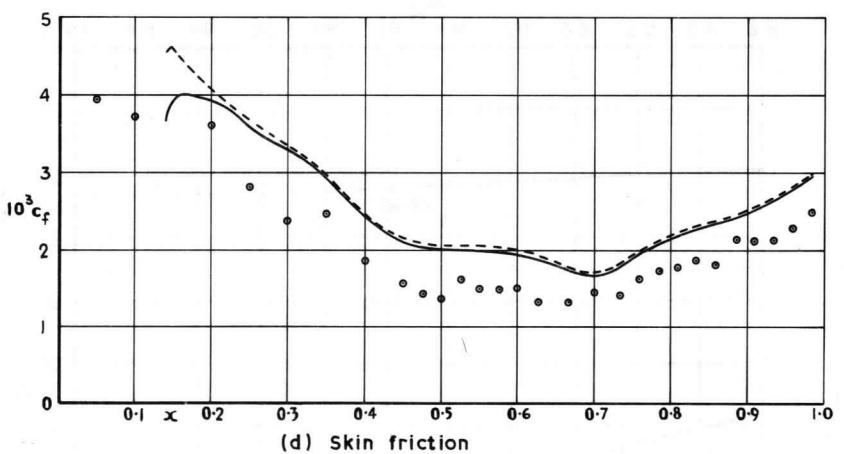
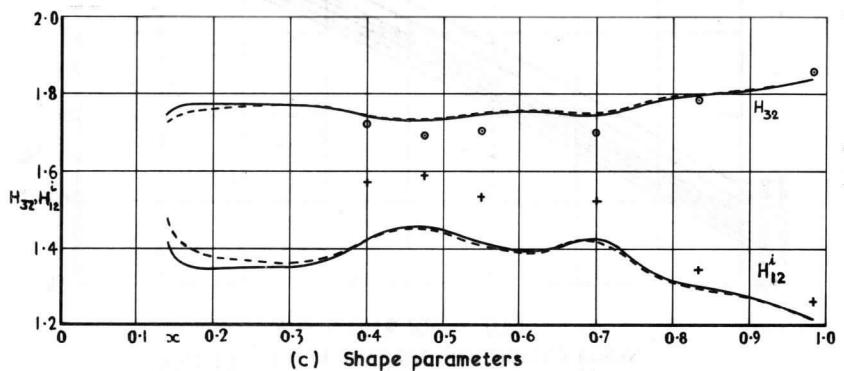
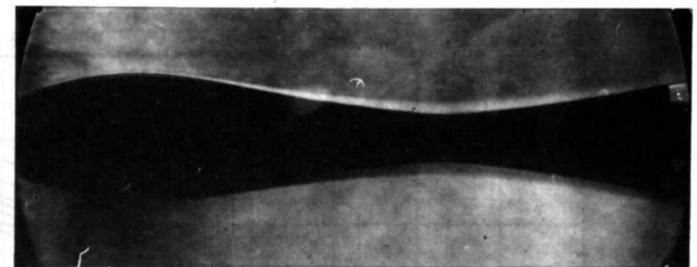
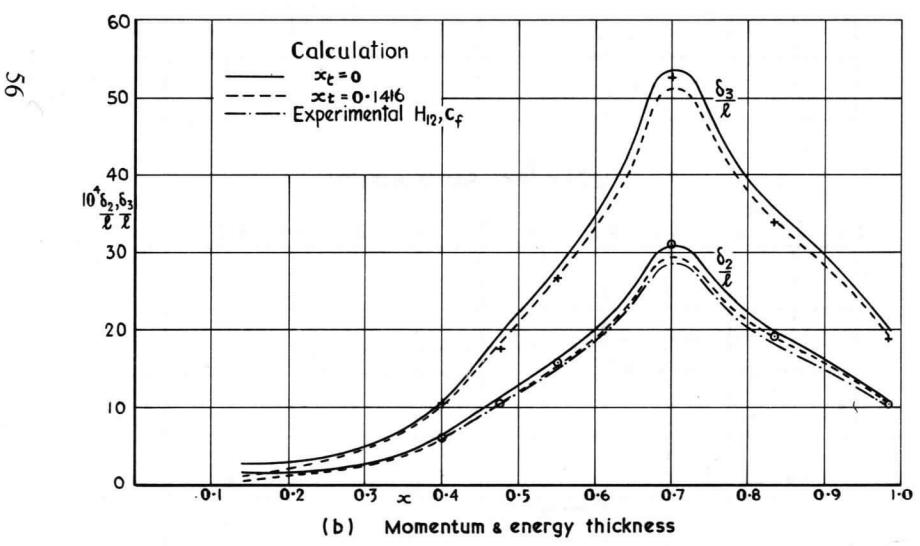
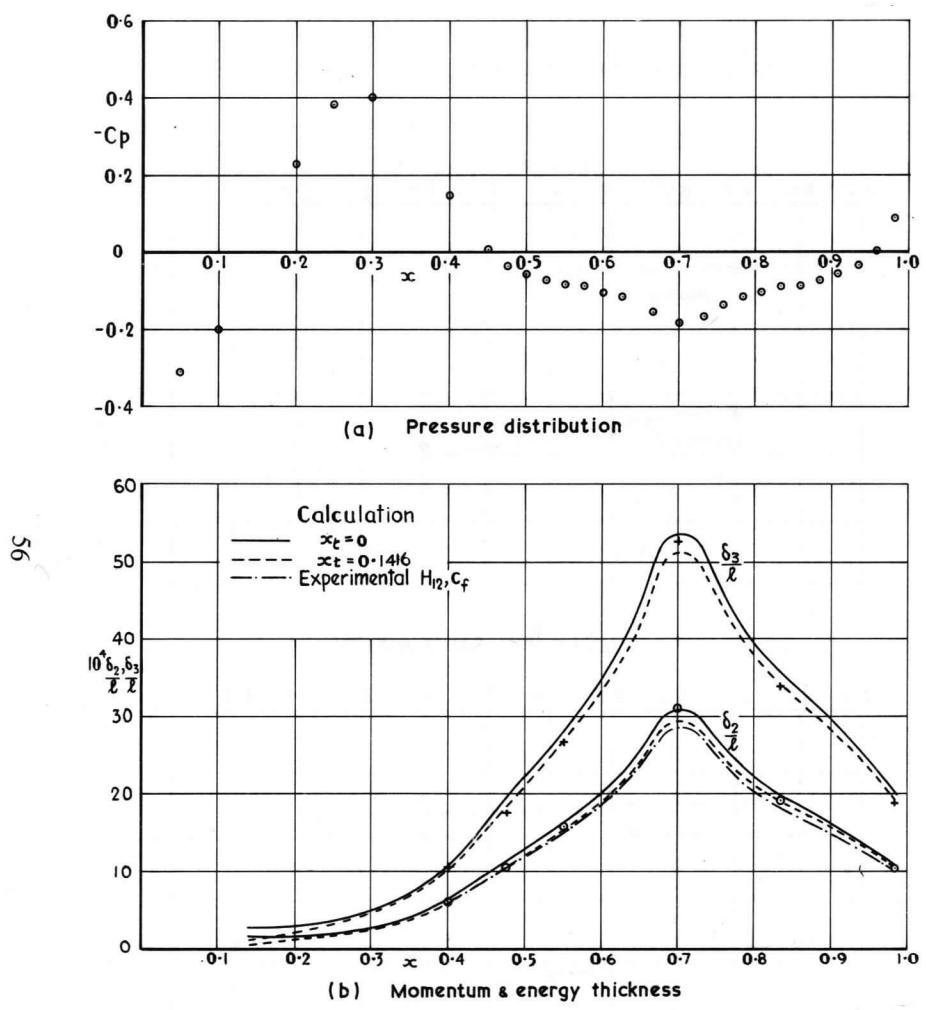


FIG. 15. Comparison of calculation and experiment  $M_\infty = 0.597$   $Re_l \approx 10^7$ .

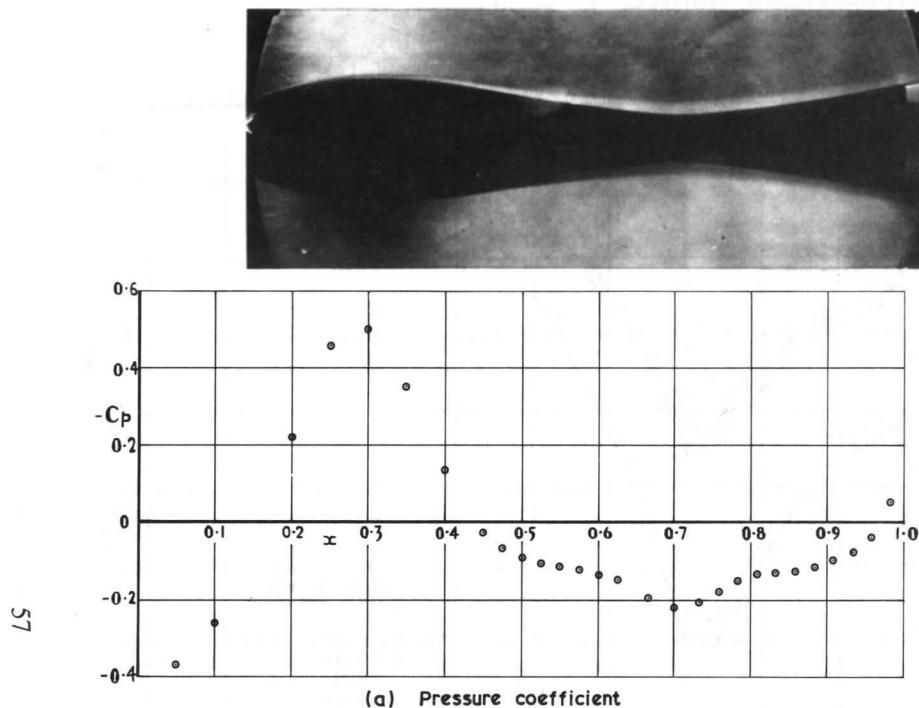


FIG. 16 a & b. Comparison of experiment and calculation  $M_\infty = 0.801$   $Re_l \approx 10^7$ .

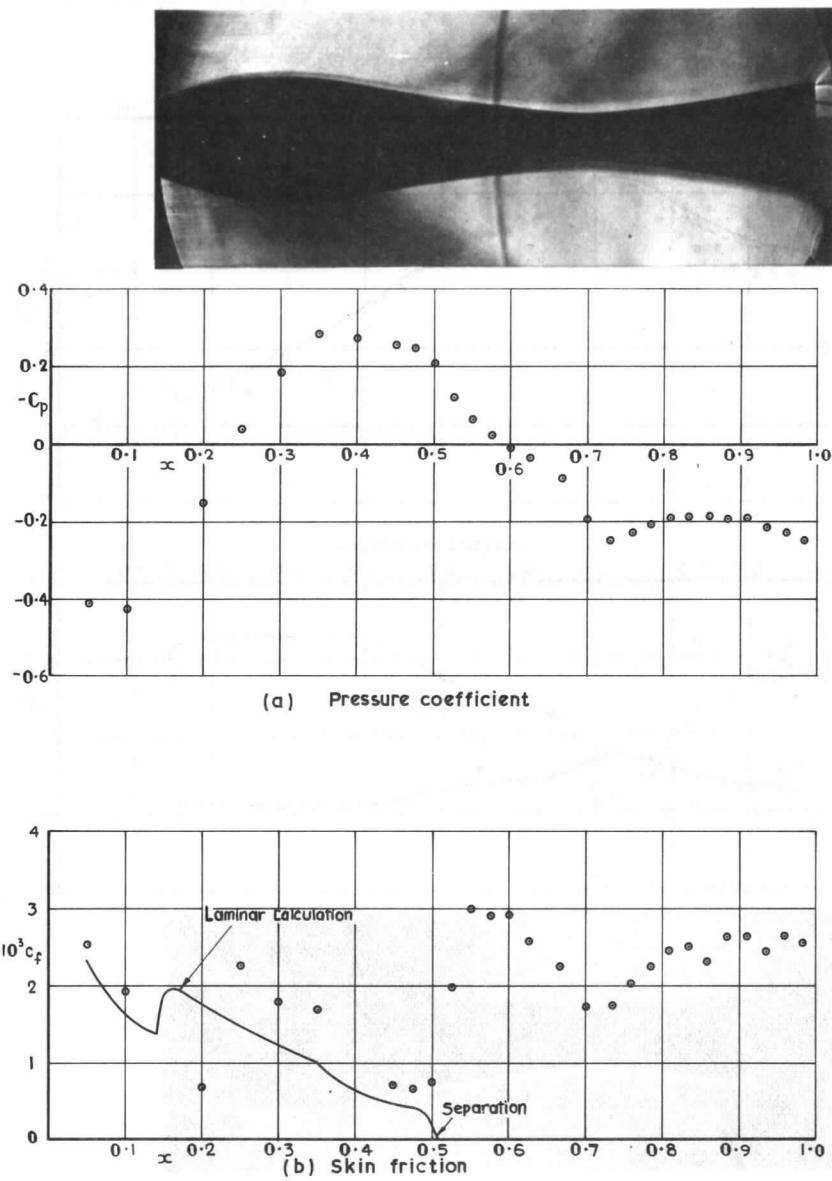


FIG. 17 a & b. Comparison of experiment and calculation  $M_\infty = 1.390$   $Re_l \approx 5 \times 10^6$ .

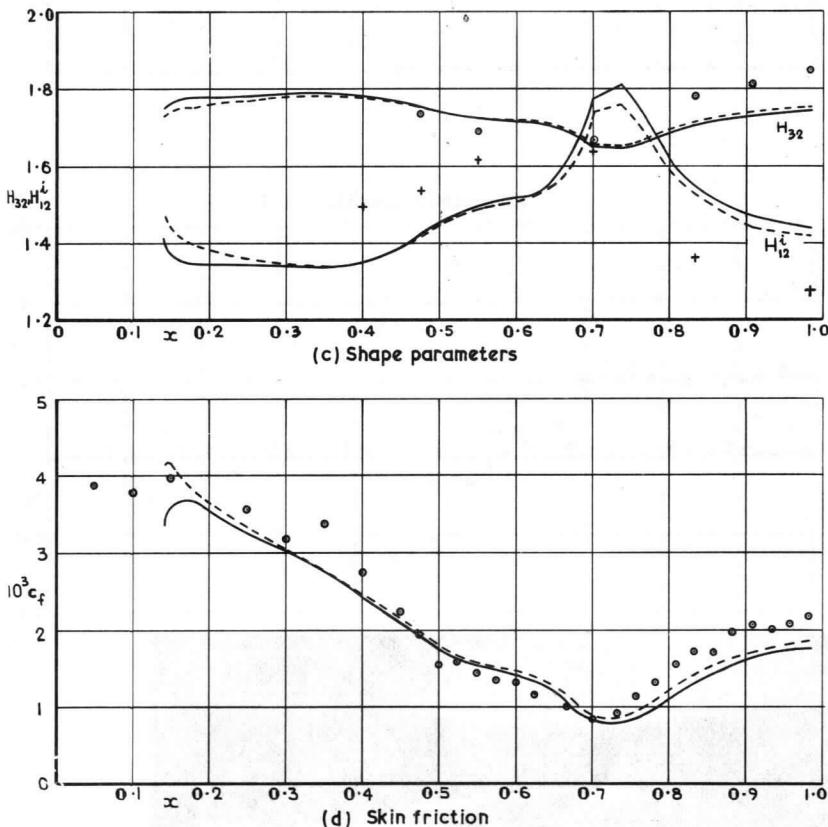
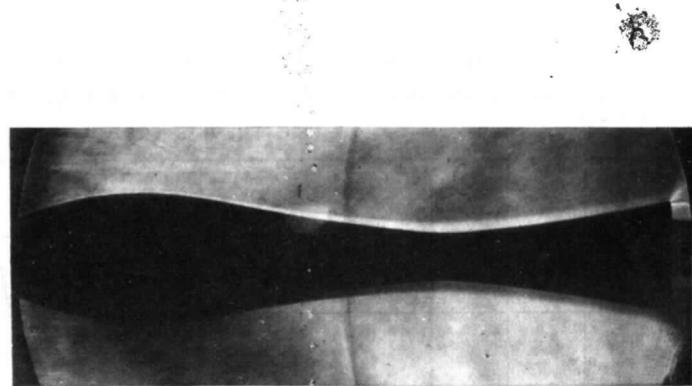
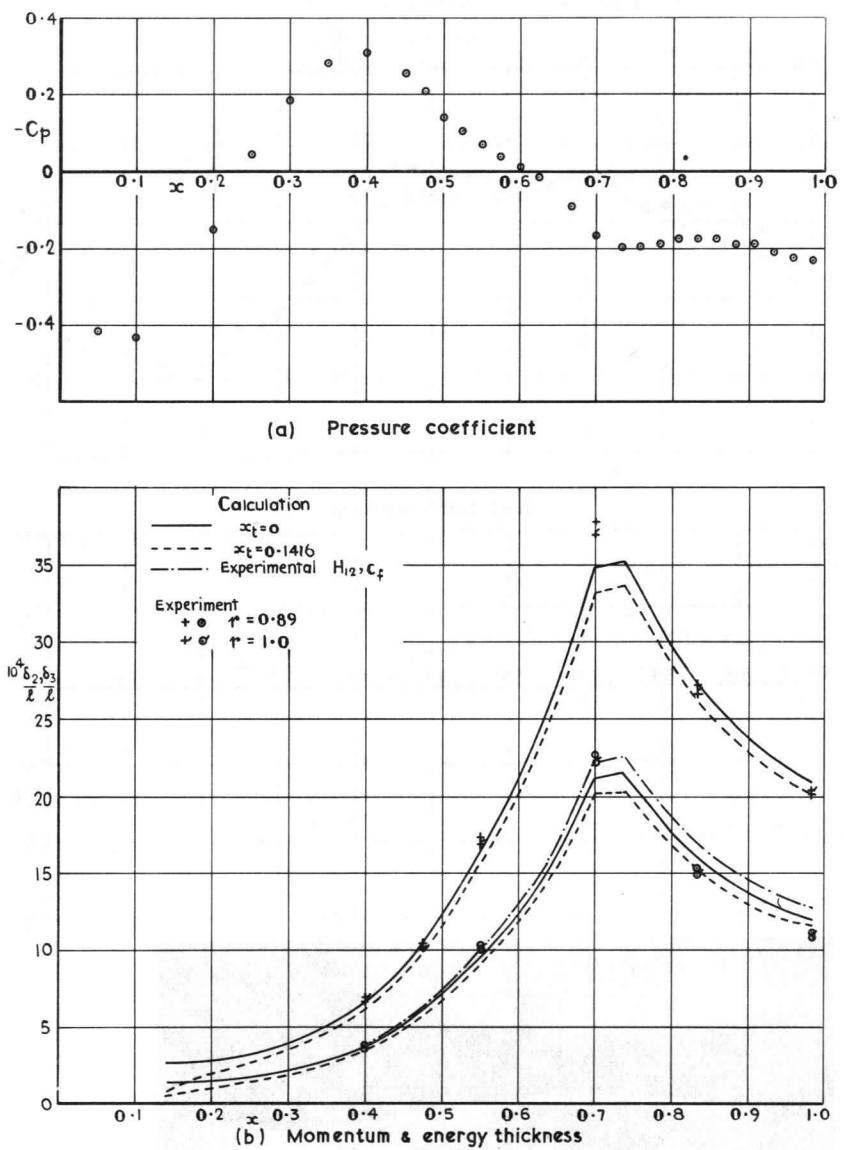
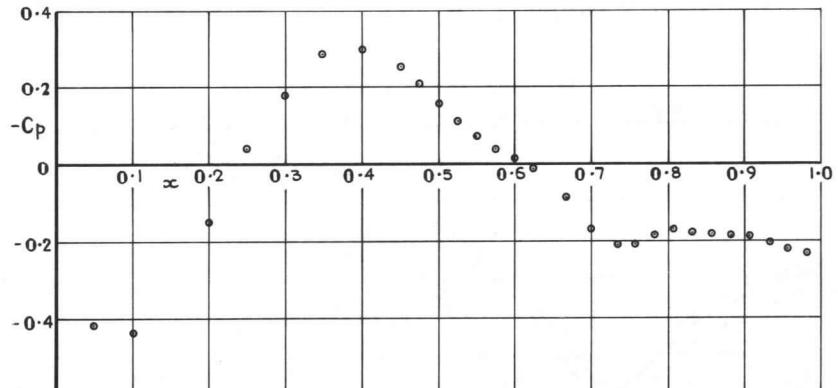


FIG. 18. Comparison of experiment and calculation  $M_\infty = 1.398$   $Re_l \approx 10^7$ .



(a) Pressure coefficient

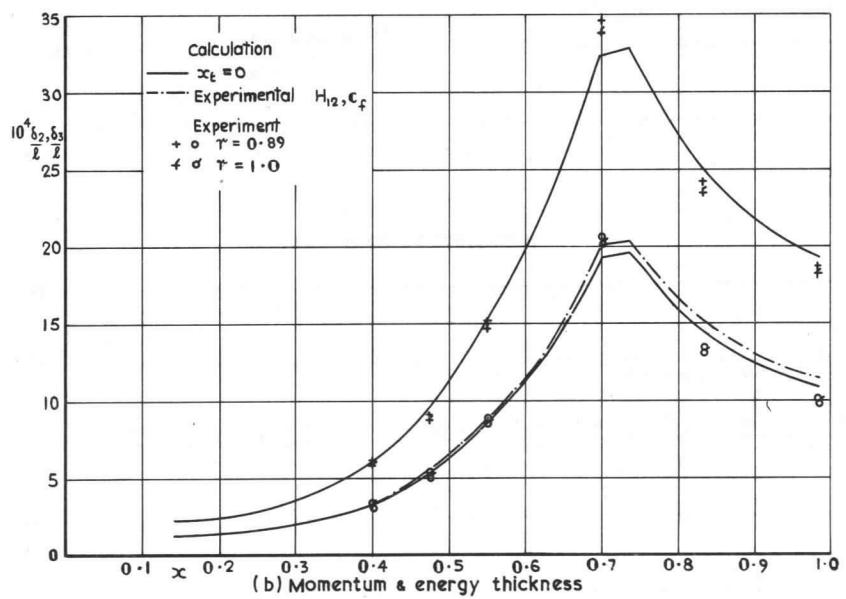
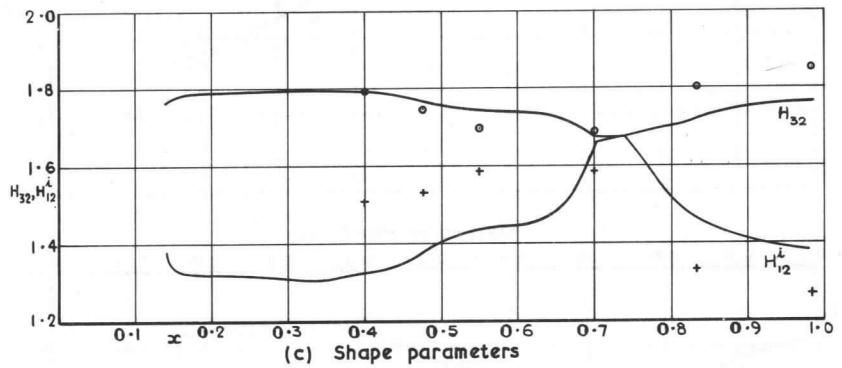
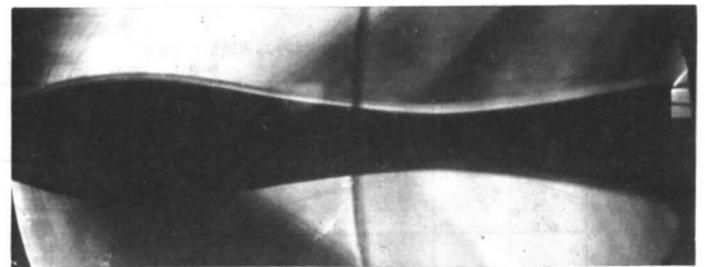
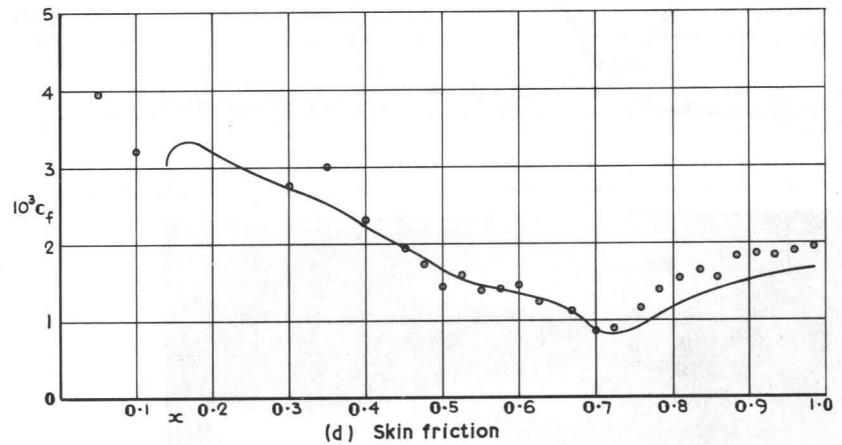


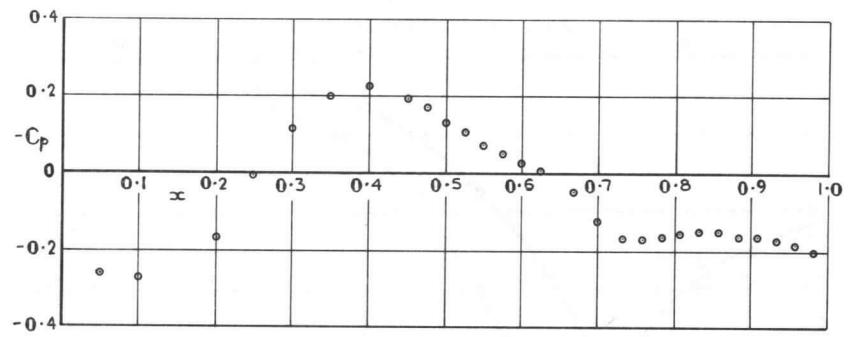
FIG. 19. Comparison of calculation and experiment  $M_\infty = 1.404$   $Re_l \approx 2 \times 10^7$ .



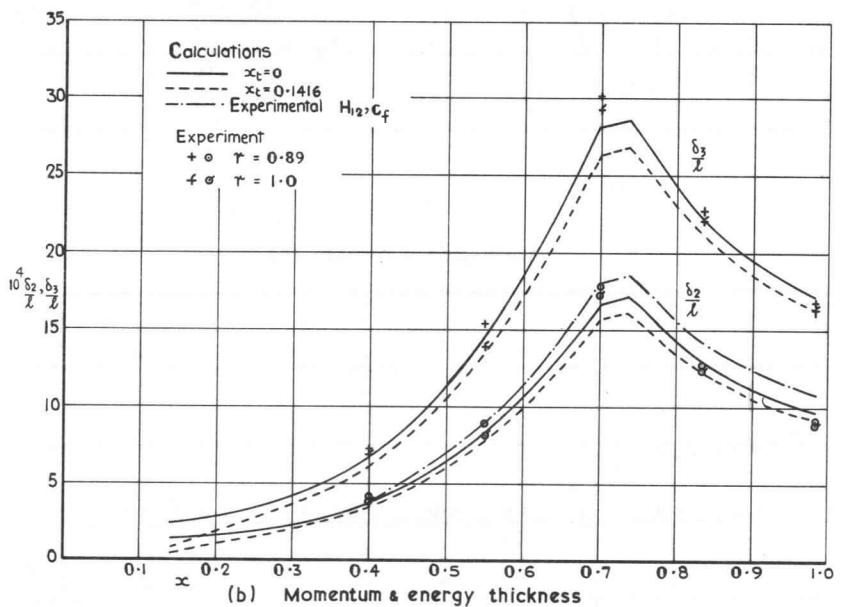
(c) Shape parameters



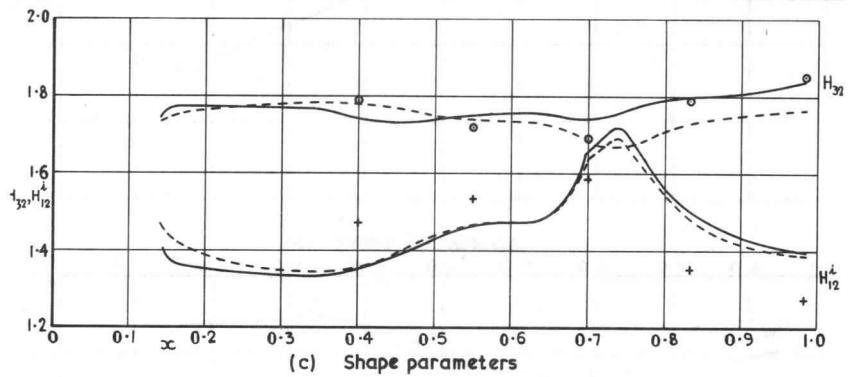
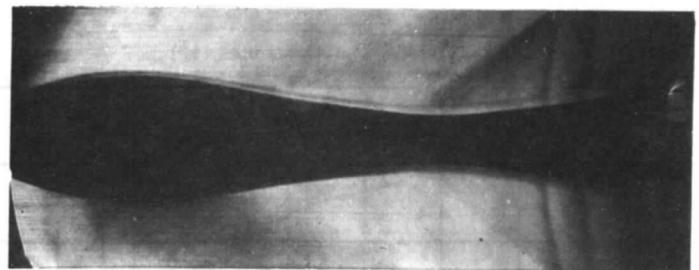
(d) Skin friction



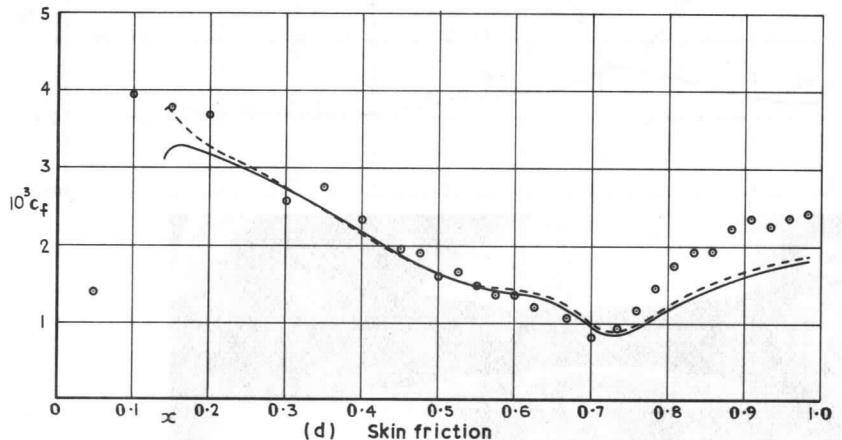
(a) Pressure coefficient



(b) Momentum & energy thickness

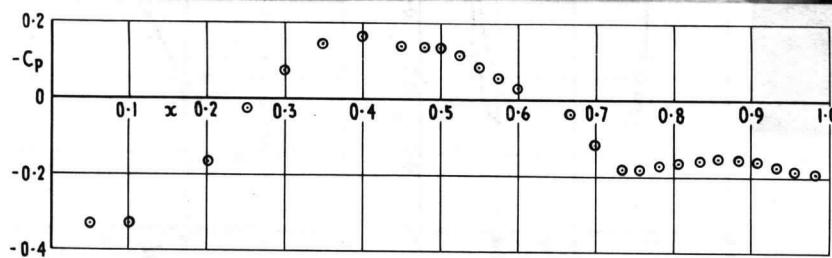
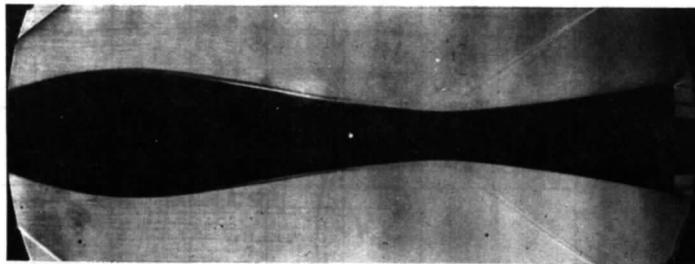


(c) Shape parameters

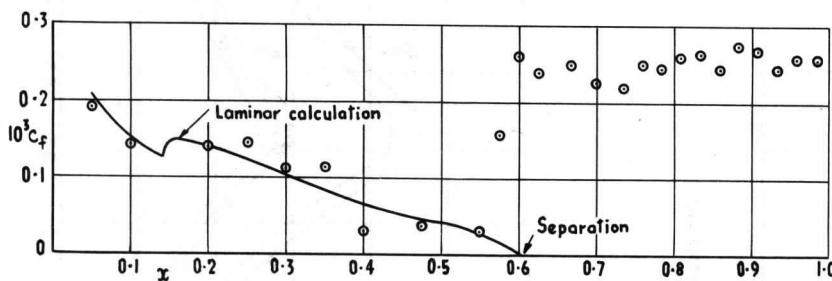


(d) Skin friction

FIG. 20. Comparison of calculation and experiment  $M_\infty = 1.700$   $Re_l \approx 10^7$ .

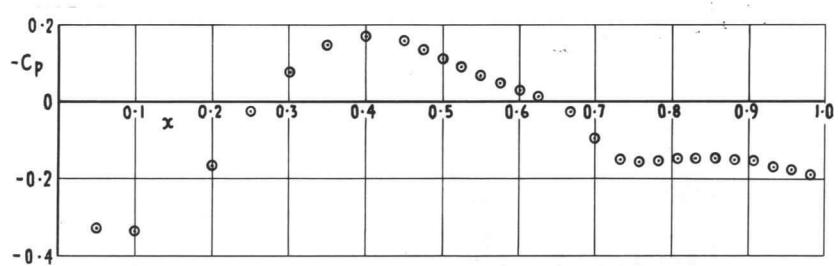


(a) Pressure coefficient

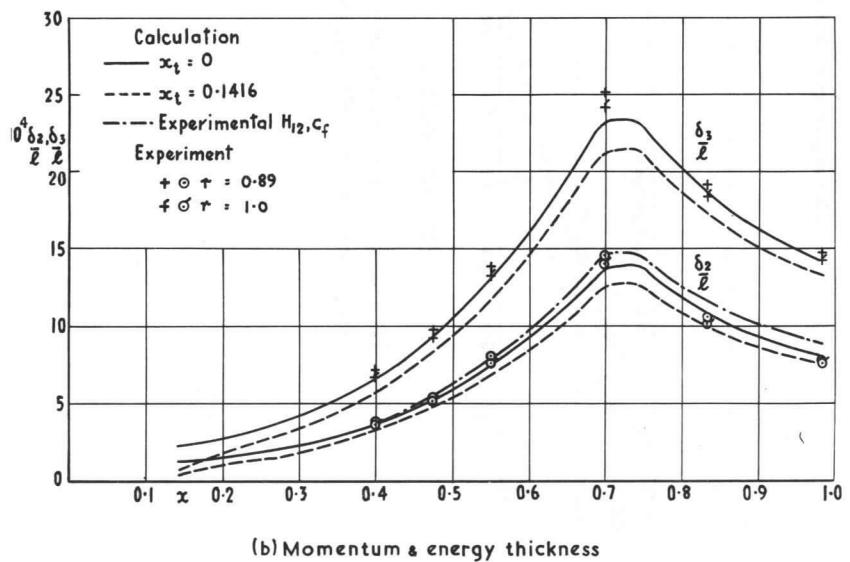


(b) Skin friction

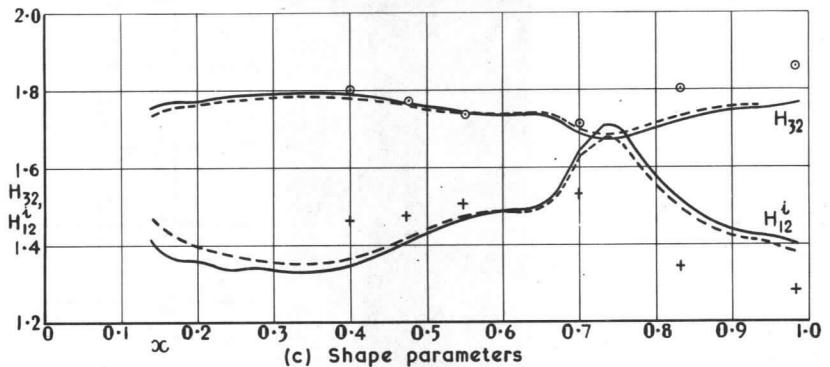
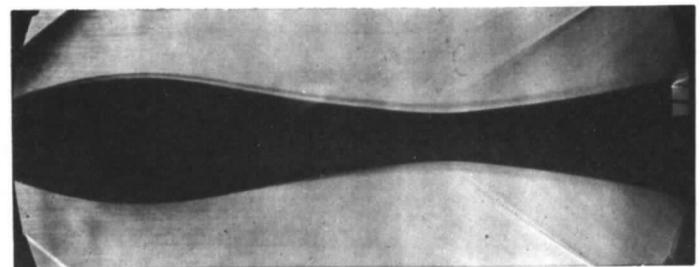
FIG. 21 a & b. Comparison of calculation and experiment  $M_\infty = 1.996$   $Re_l \approx 5 \times 10^6$ .



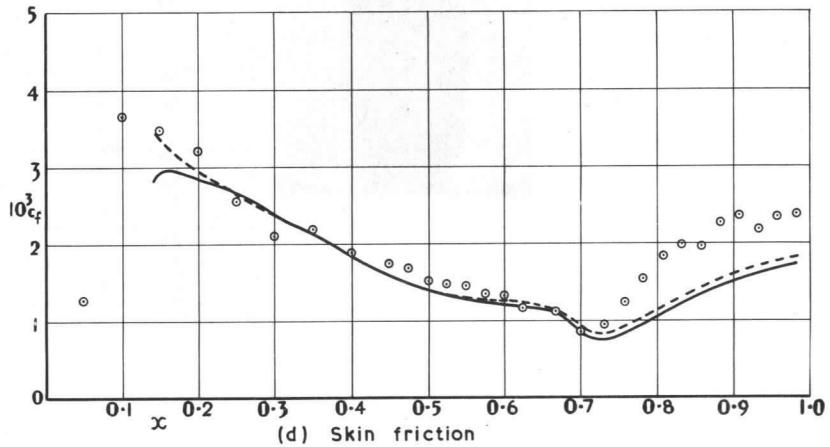
(a) Pressure coefficient



(b) Momentum &amp; energy thickness

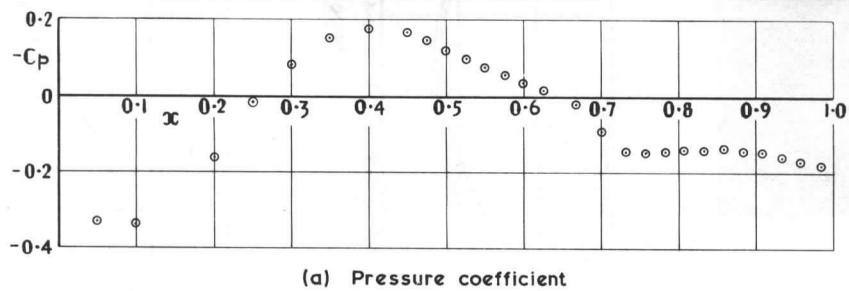
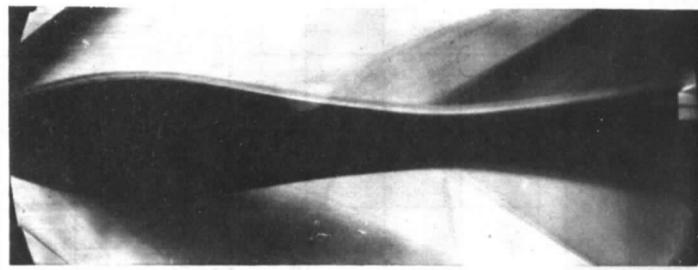


(c) Shape parameters



(d) Skin friction

FIG. 22. Comparison of calculation and experiment  $M_\infty = 2.000$   $Re_l \approx 10^7$ .



(a) Pressure coefficient

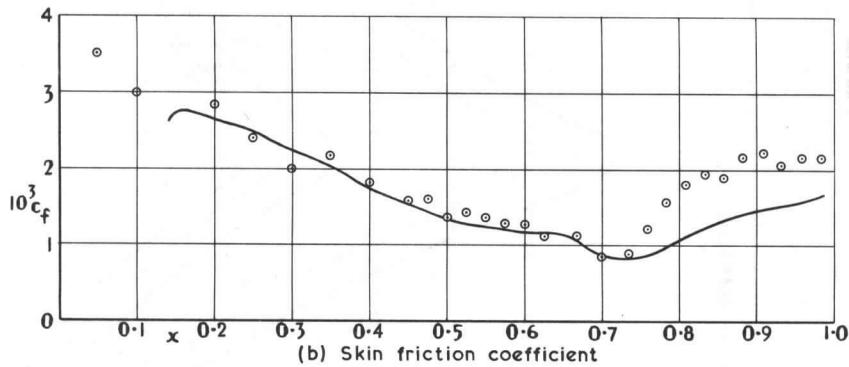
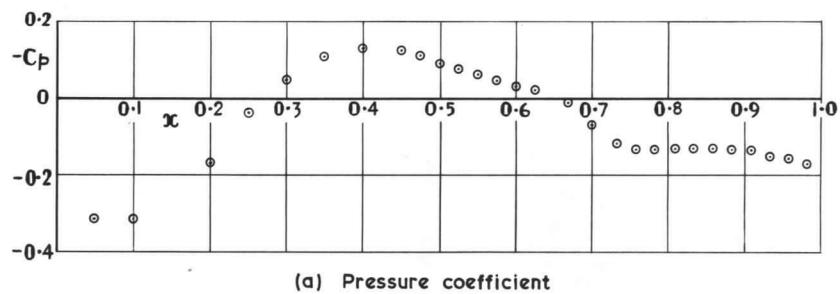
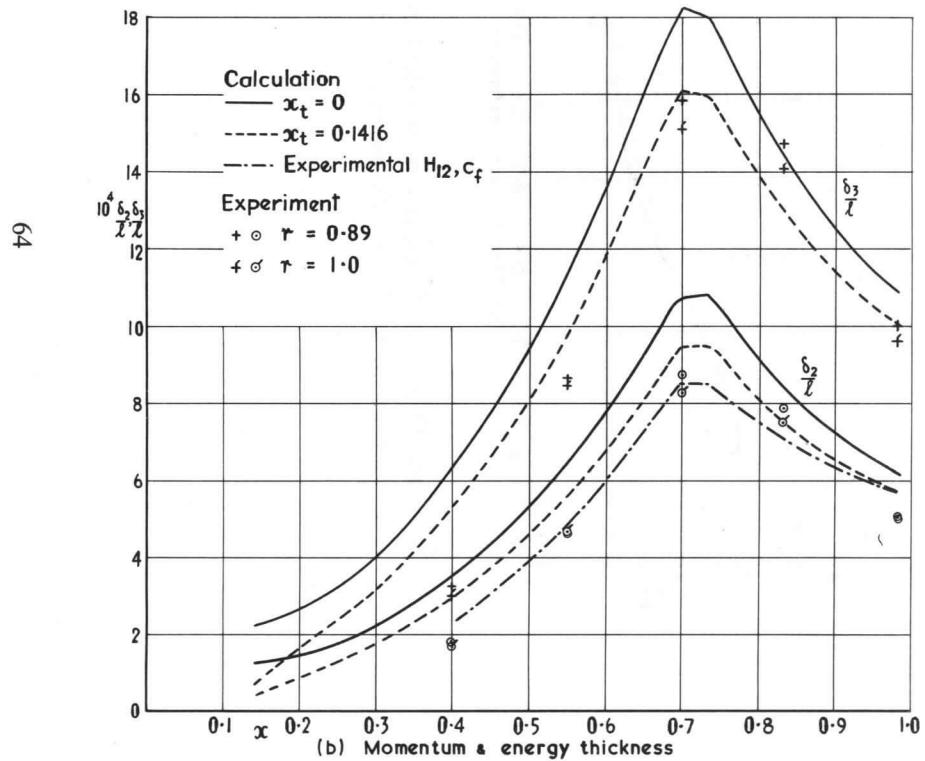
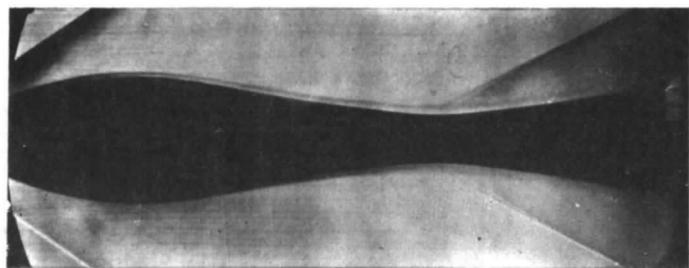


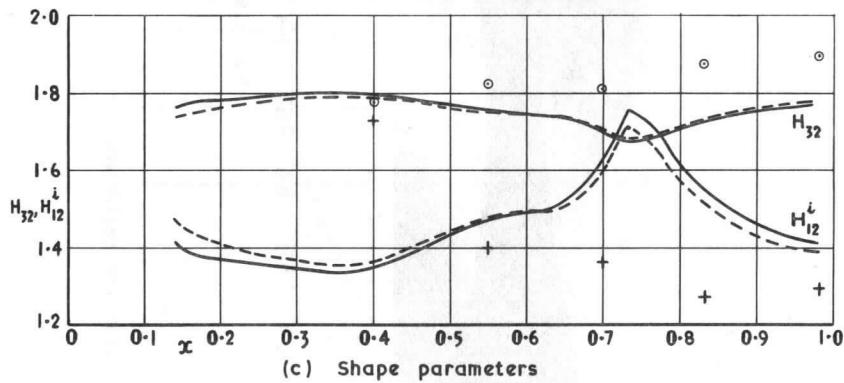
FIG. 23 a & b. Comparison of calculation and experiment  $M_\infty = 2.002$   $Re_l \approx 1.7 \times 10^7$ .



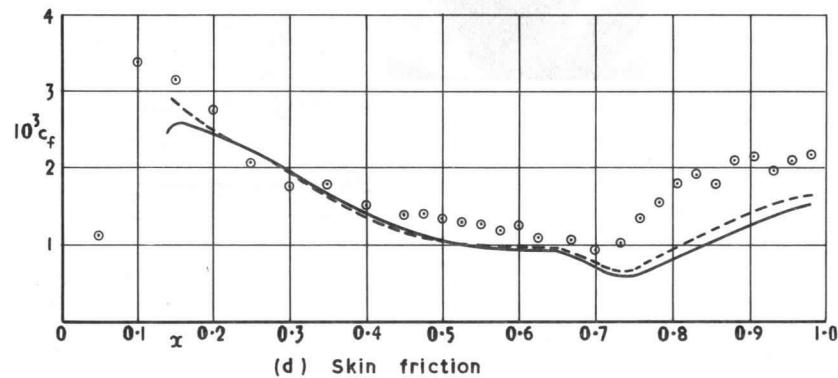
(a) Pressure coefficient



(b) Momentum & energy thickness

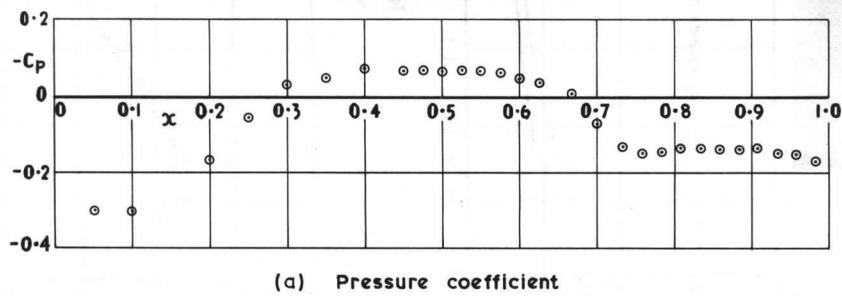
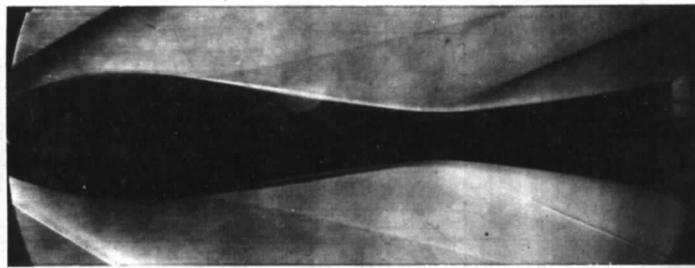


(c) Shape parameters



(d) Skin friction

FIG. 24. Comparison of calculation and experiment  $M_\infty = 2.401$   $Re_l \approx 10^7$ .



(a) Pressure coefficient

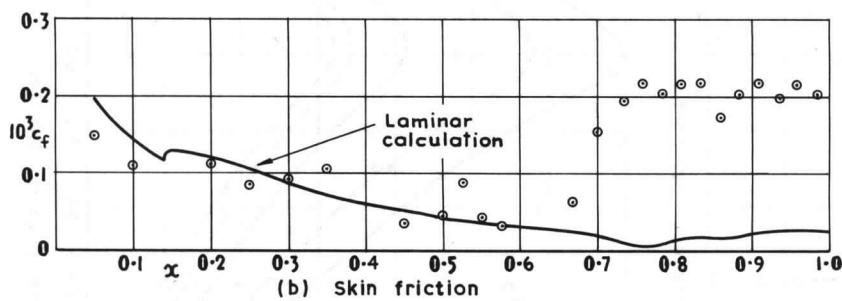
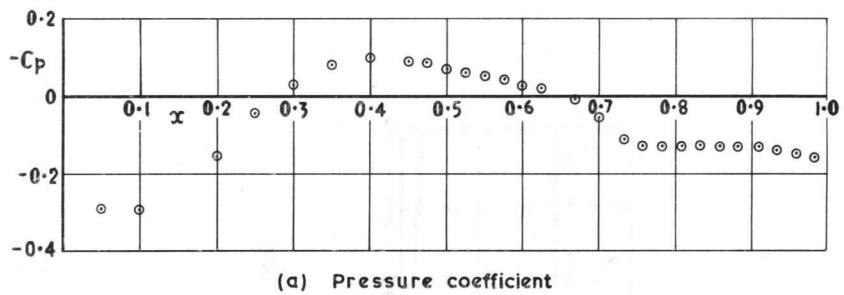
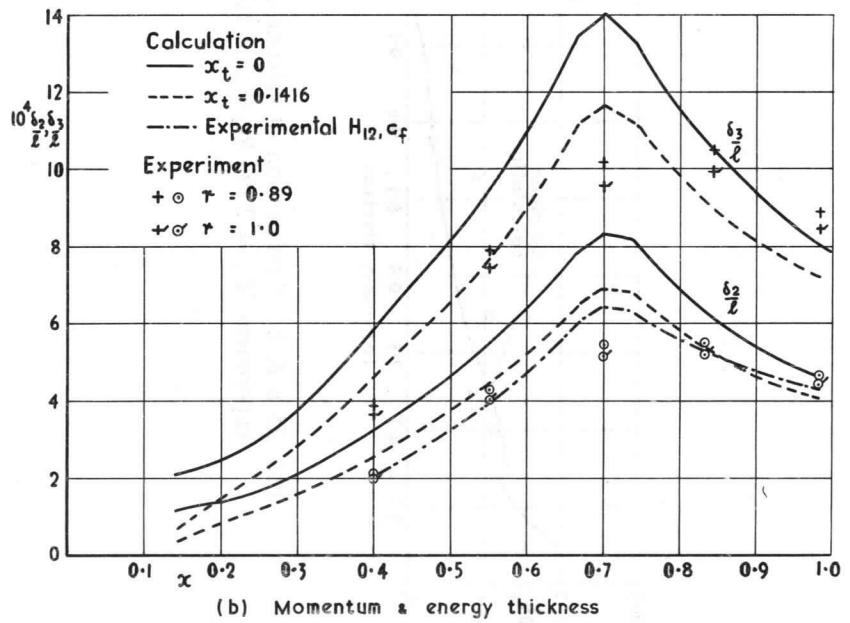


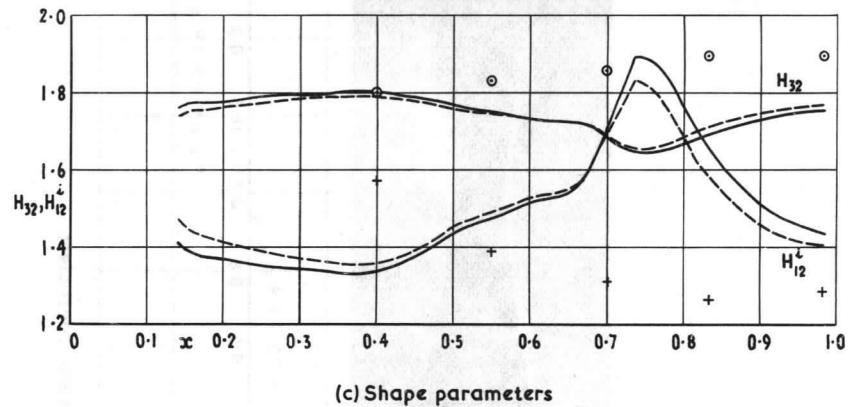
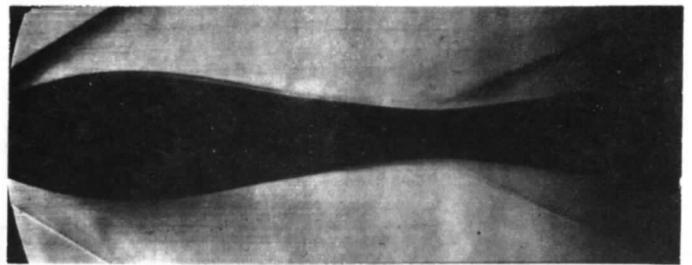
FIG. 25 a & b. Comparison of calculation and experiment  $M_\infty = 2.793$   $Re_l \approx 5 \times 10^6$ .



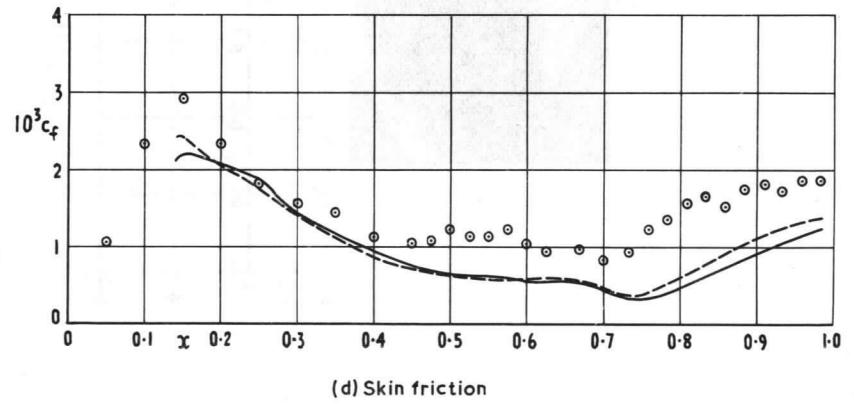
(a) Pressure coefficient



(b) Momentum &amp; energy thickness



(c) Shape parameters



(d) Skin friction

FIG. 26. Comparison of calculation and experiment  $M_\infty = 2.799$   $Re_l \simeq 10^7$ .

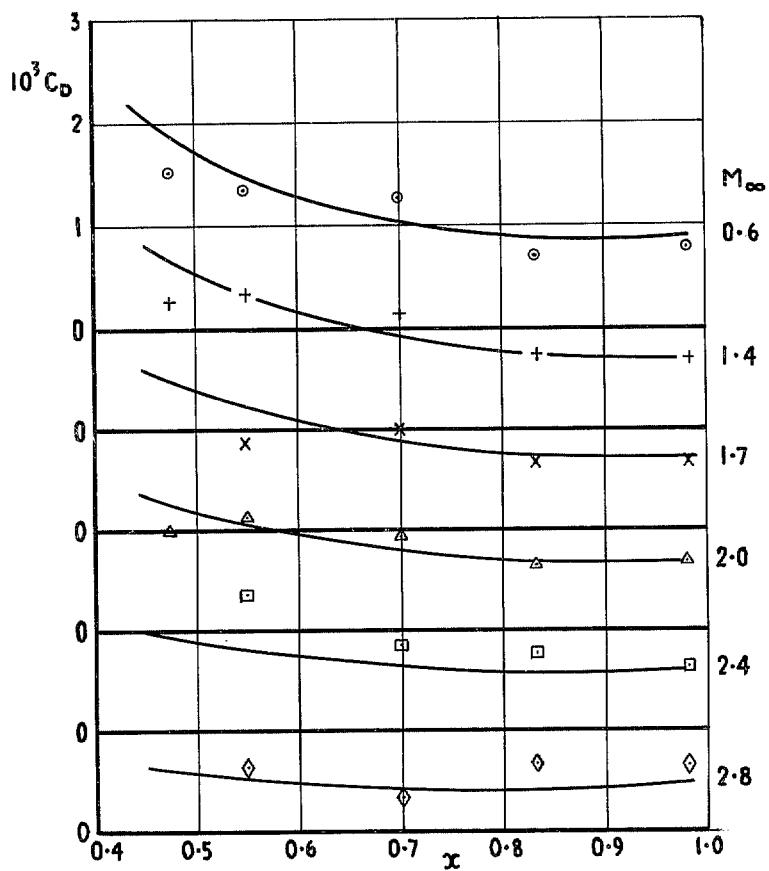


FIG. 27. 'Mean' dissipation coefficient  $Re_l \approx 10^7$ .

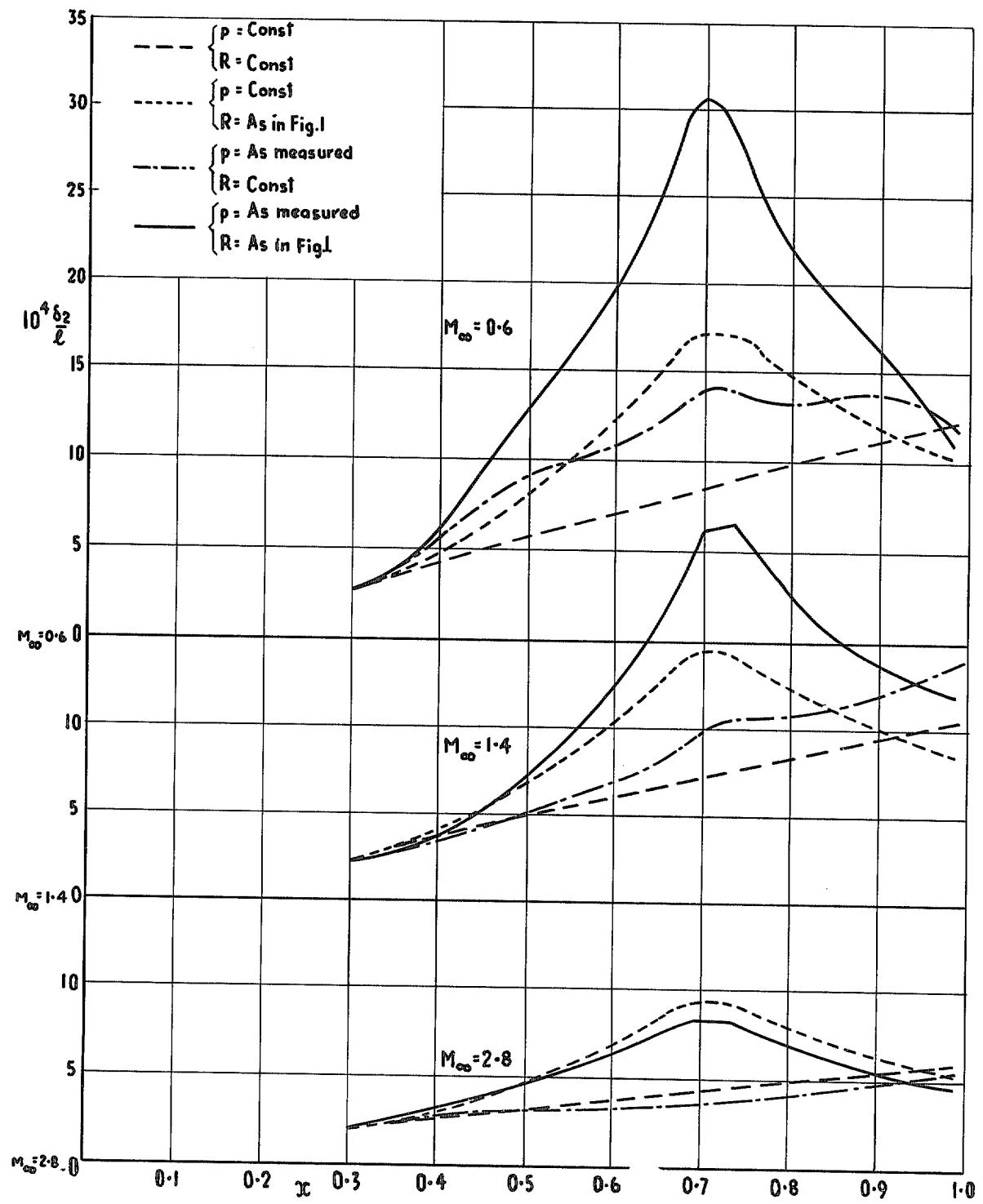


FIG 28. Influence of pressure gradient and streamline convergence on momentum thickness  $Re_l = 10^7$ .

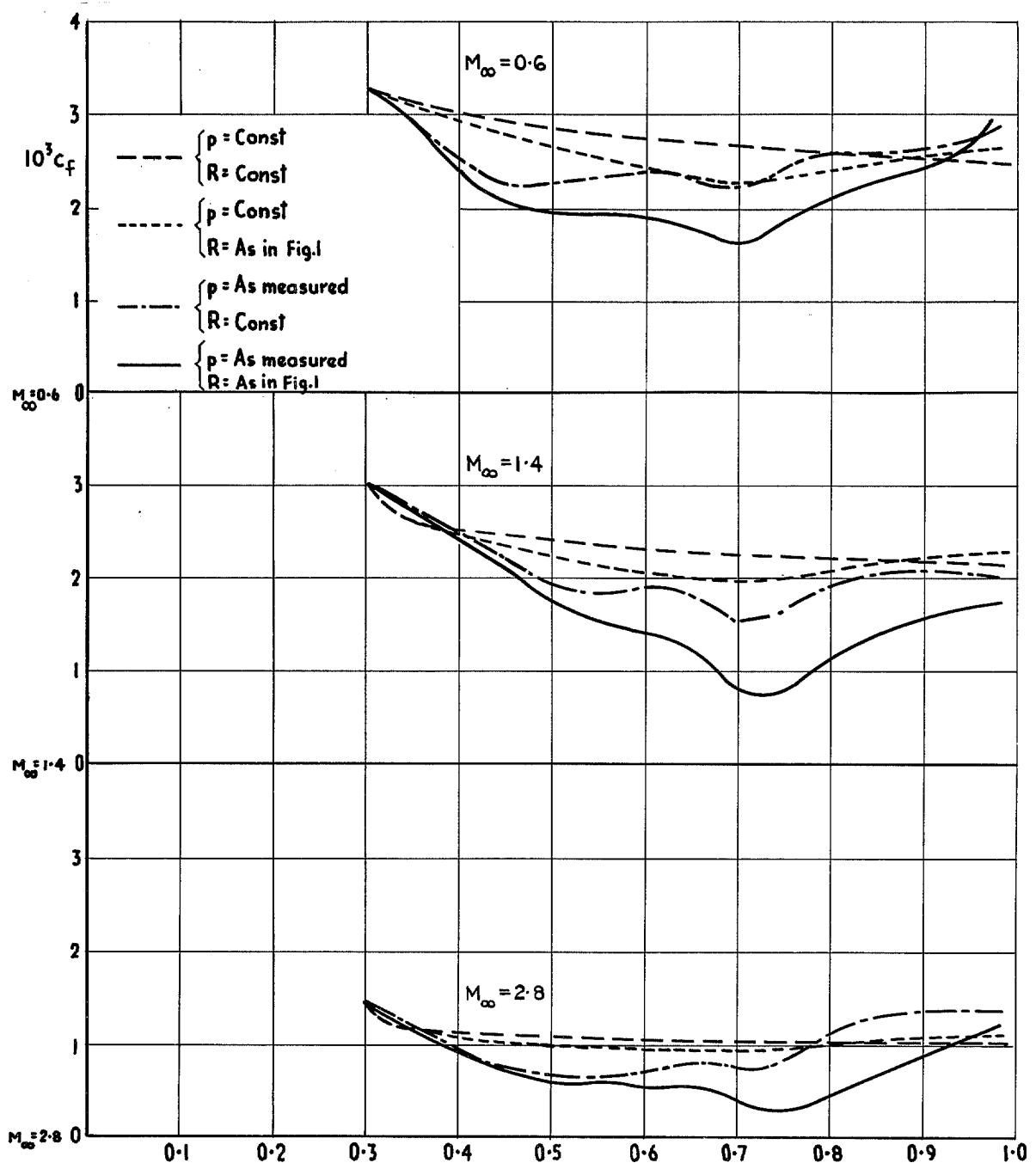


FIG. 29. Influence of pressure gradient and streamline convergence on skin friction  $Re_l = 10^7$ .

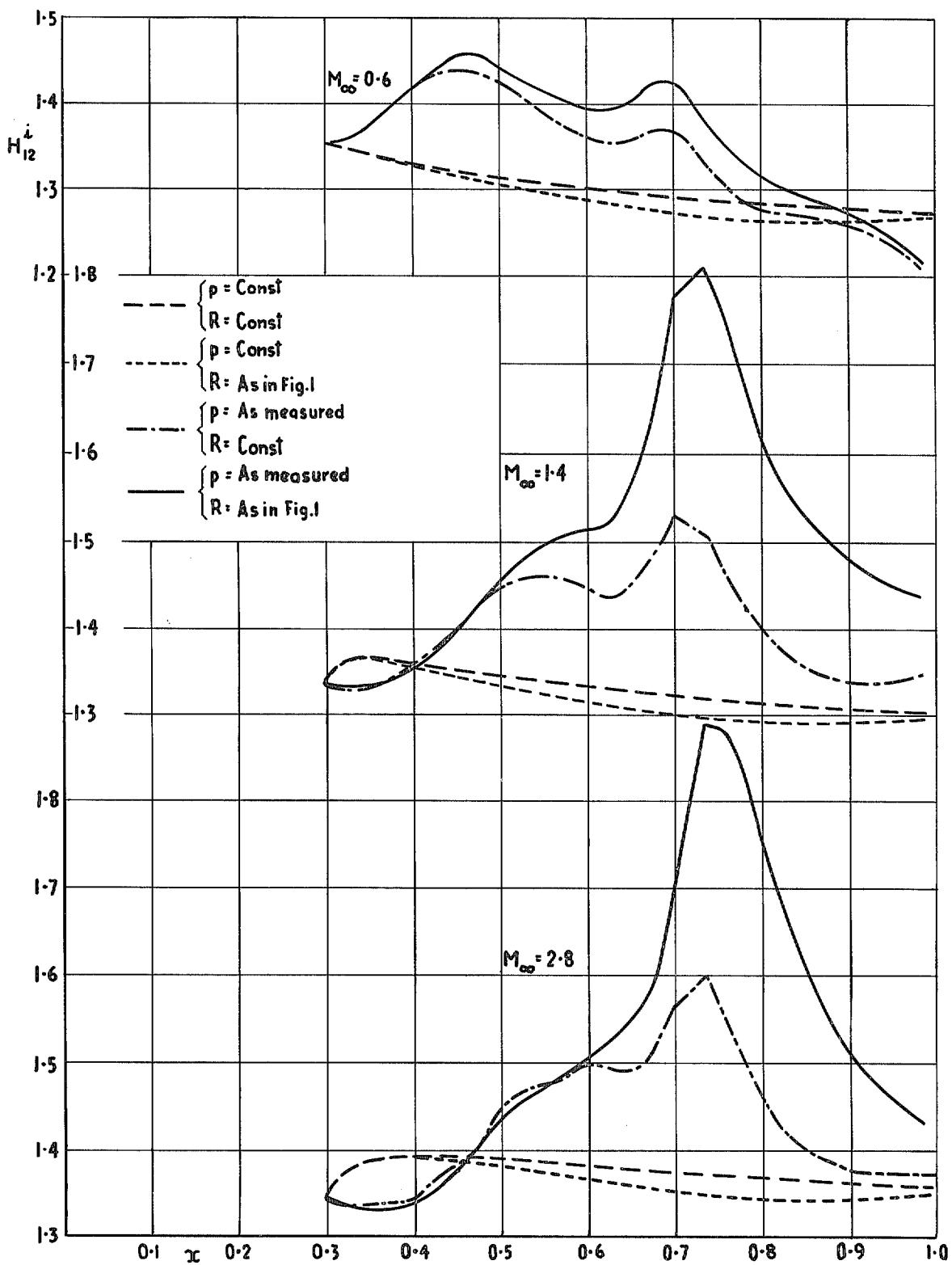


FIG. 30. Influence of pressure gradient and streamline convergence on shape parameter  $H_{12}^i$   $Re_l = 10^7$ .

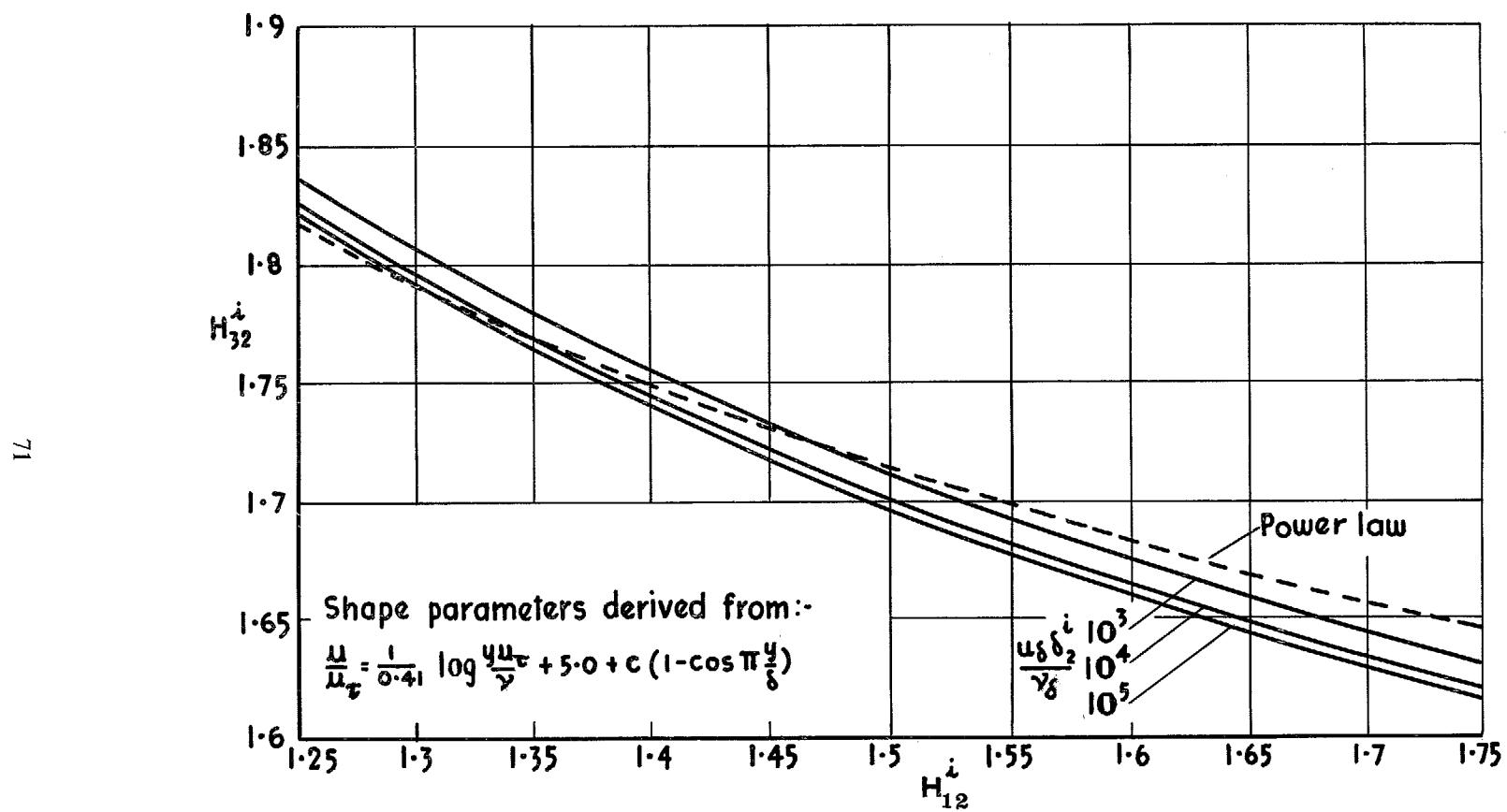


FIG. 31. Alternative shape parameter correlation.

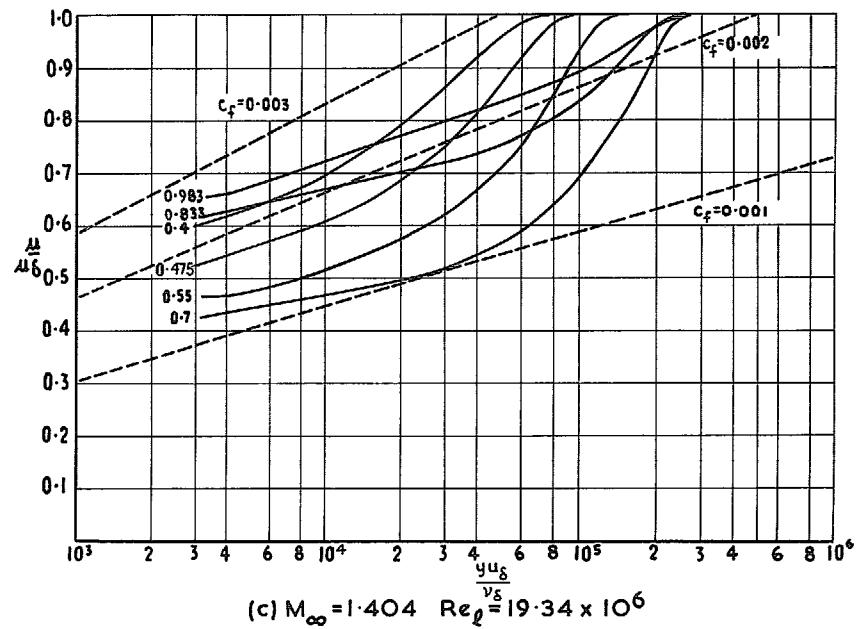
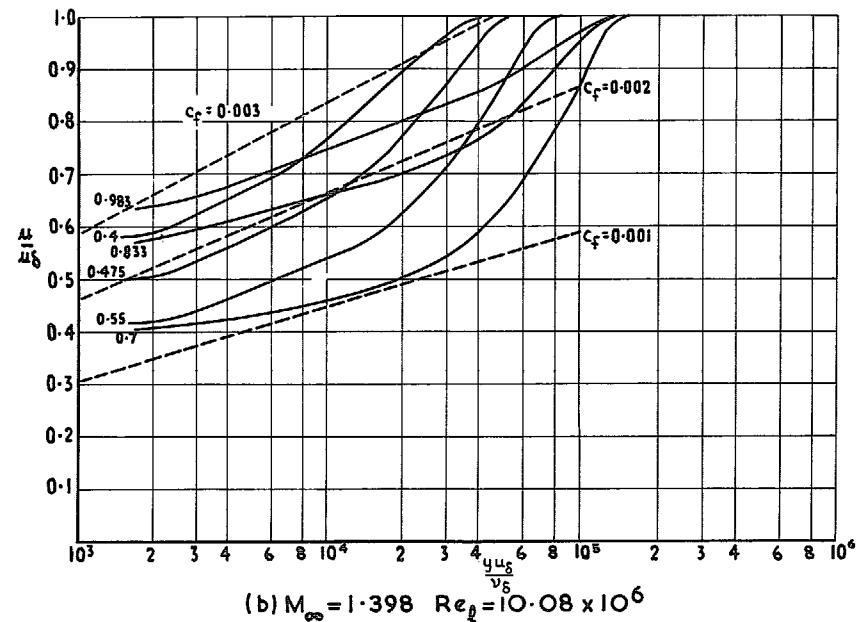
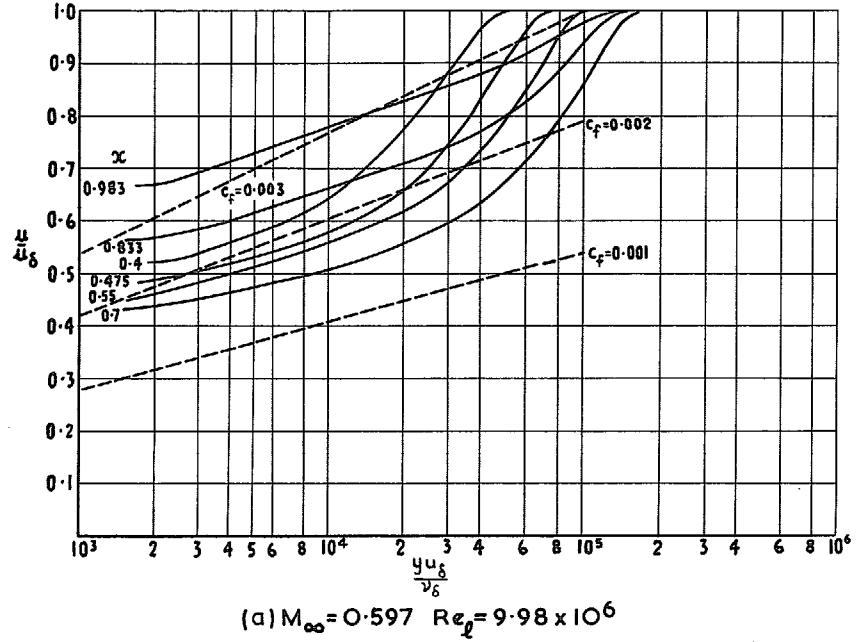


FIG. 32 a to c. Semi-logarithmic plot of velocity profiles.

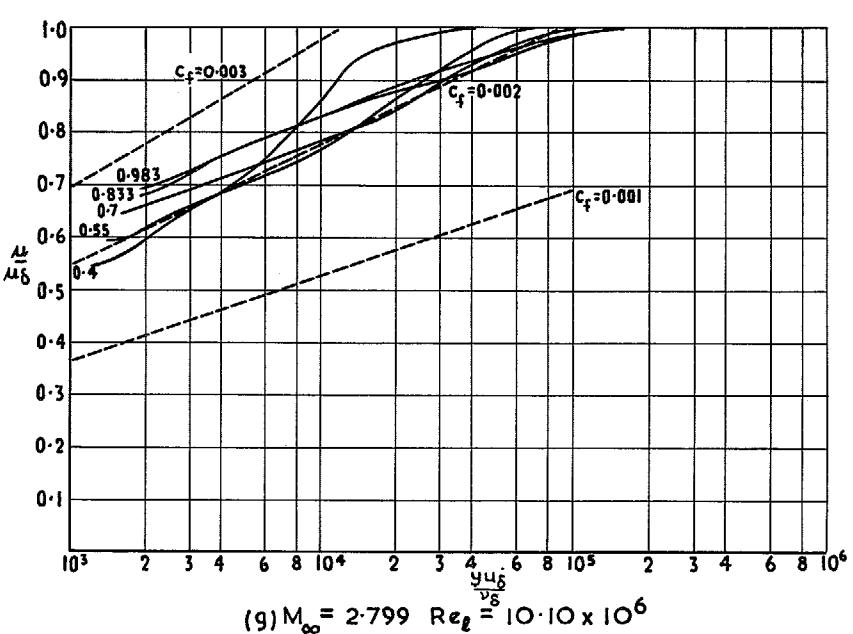
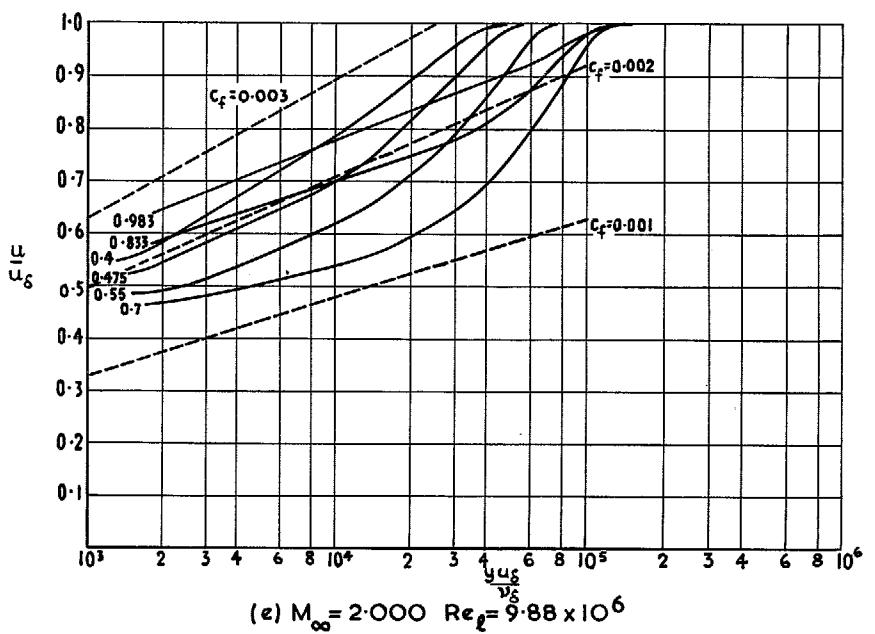
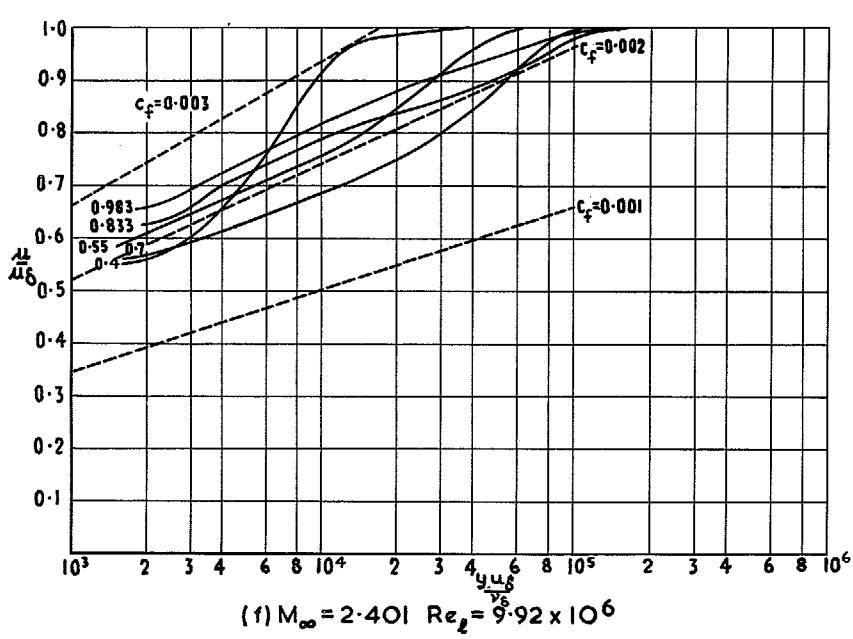
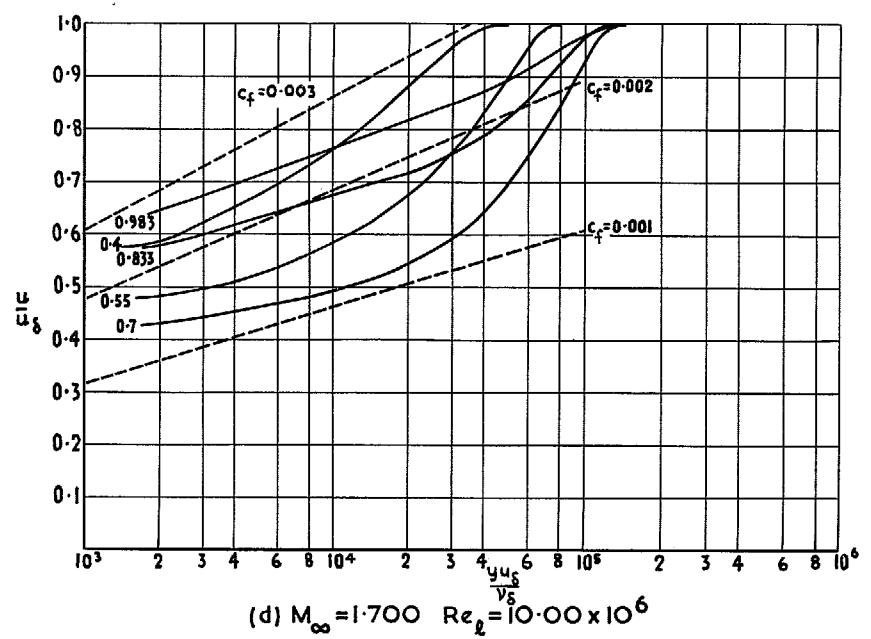


FIG. 32d to g. Semi-logarithmic plot of velocity profiles.

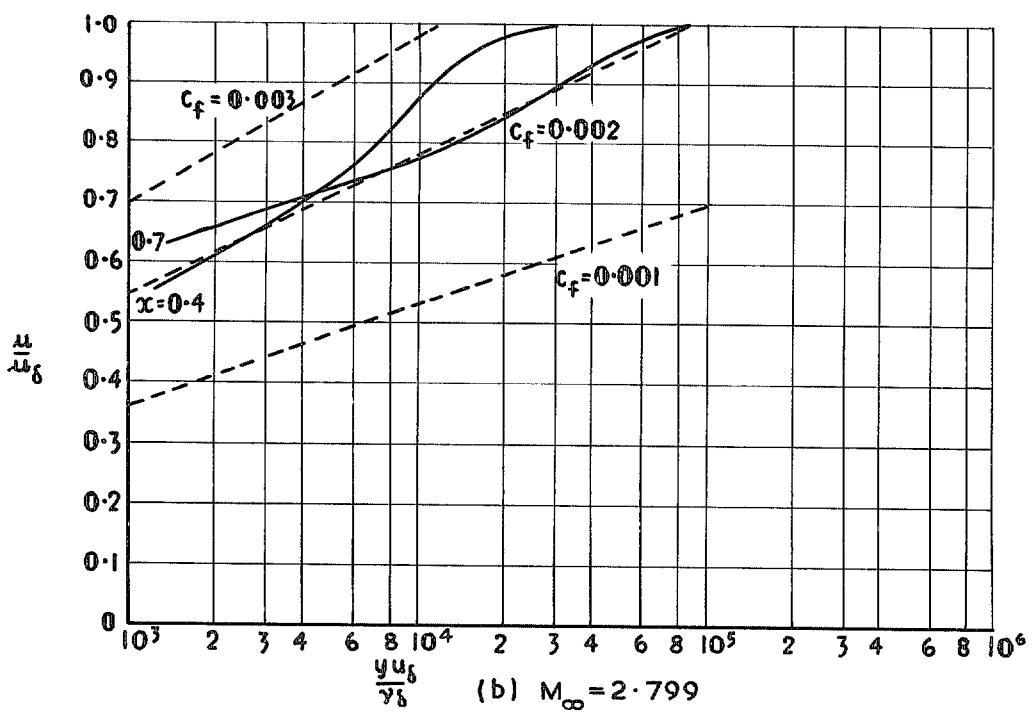
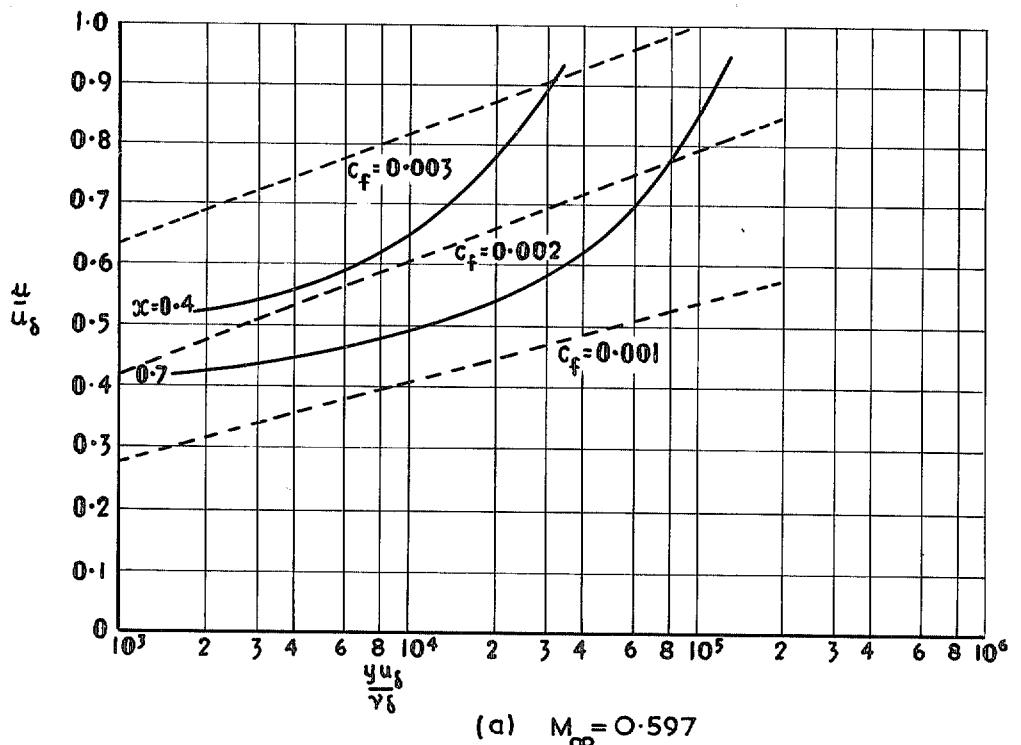
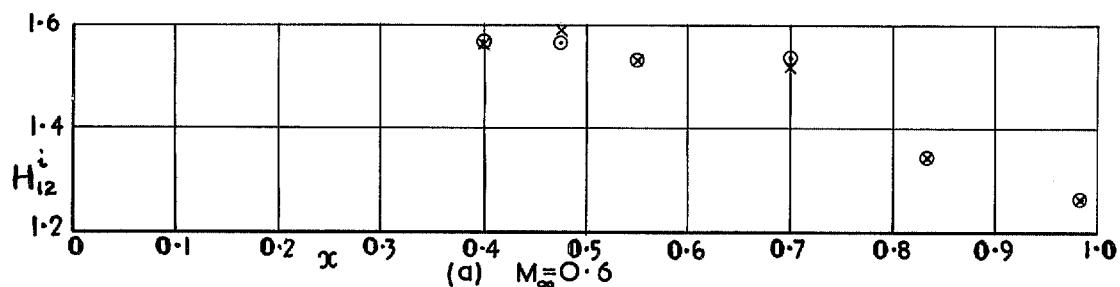


FIG. 33 a & b. Velocity profiles corrected for normal pressure gradient.



× Static pressure constant  
○ With calculated normal pressure variation

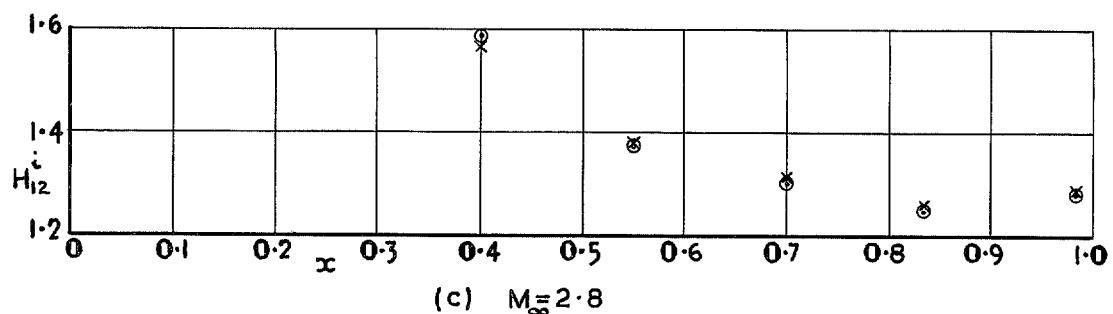
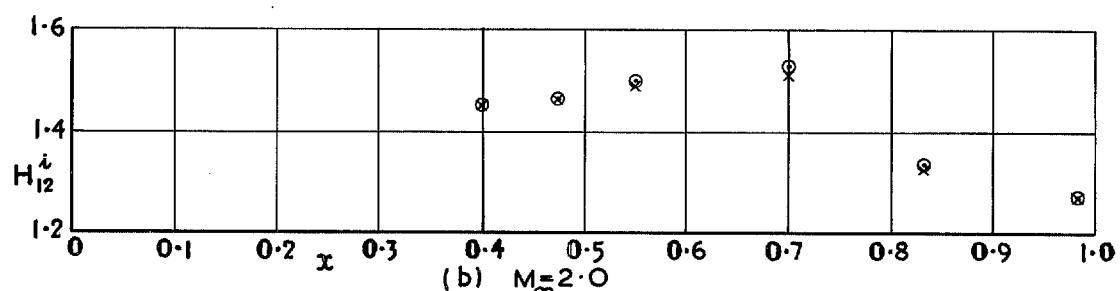


FIG. 34 a to c. Calculated effect of normal pressure gradients on shape parameter  $H_{12}^i$  ( $r = 1$ ).

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